

Article

# **Effect of an External Oriented Magnetic Field on Entropy Generation in Natural Convection**

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Abstract: The influence of an external oriented magnetic field on entropy generation in natural convection for air and liquid gallium is numerically studied in steady-unsteady states by solving the mass, the momentum and the energy conservation equations. Entropy generation depends on five parameters which are: the Prandtl number, the irreversibility coefficients, the inclination angle of the magnetic field, the thermal Grashof and the Hartmann numbers. Effects of these parameters on total and local irreversibilities as well as on heat transfer and fluid flow are studied. It was found that the magnetic field tends to decrease the convection currents, the heat transfer and entropy generation inside the enclosure. Influence of inclination angle of the magnetic field on local irreversibility is then studied.

**Keywords:** heat transfer; convection; magnetic field; cavity; entropy generation; numerical methods

Classification: PACS 05.70.Ln

# Nomenclature

а	thermal diffusivity $(m^2 \cdot s^{-1})$	а	dimensio	
В	magnetic field (T)	С	cold wal	
E	electric field ( $V m^{-1}$ )	h	hot wall	
$E_M$	electromagnetic force (N)	Mag	magnetic	
g	gravitational acceleration $(m \cdot s^{-2})$	Th	thermal	
h	heat transfer coefficient $(W \cdot m^{-2} \cdot K^{-1})$	t	total	
$Gr_T$	thermal Grashof number	Vis	viscous	
На	Hartmann number			
Ha <sub>c</sub>	critical Hartmann number			
J	current density $(A \cdot m^{-2})$			
k	thermal Conductivity $(J \cdot m^{-1} \cdot s^{-1} \cdot K^{-1})$			
L	length of the cavity (m)			
P	dimensionless pressure			
р	pressure $(N \cdot m^{-2})$			
Pr	Prandtl number			
$\dot{S}_{gen}$	rate of entropy generation per unit volume $(J \cdot s^{-1} \cdot K^{-1} \cdot m^{-3})$			
Т	temperature (K)			
$T_0$	mean Temperature $(T_0 = (T_h + T_c)/2)$ (K)			
t	time (s)			
u, v	velocity components in x and y directions respectively $(m \cdot s^{-1})$			
U, V	dimensionless velocity components in X and Y directions respectively			
υ	dimensionless velocity vector			
W	dimensional velocity vector $(\mathbf{m} \cdot \mathbf{s}^{-1})$			
<i>x, y</i>	Cartesian coordinates (m)			
XY	dimensionless Cartesian coordinates			

dimensionless Cartesian coordinates X, Y

# **Greek letters**

- inclination angle of the magnetic field (°) α
- thermal expansion coefficient  $(K^{-1})$ β

$$\Delta T$$
 temperature difference ( $\Delta T = T_h - T_c$ ) (K)

- irreversibility coefficient (i=1, 2)  $\chi_{i}$
- dynamic viscosity (kg·m<sup>-1</sup>·s<sup>-1</sup>) μ
- kinematic viscosity  $(m^2 \cdot s^{-1})$ ν
- mass density  $(kg \cdot m^{-3})$ ρ
- dimensionless entropy generation  $\sigma$
- electric conductivity  $(\Omega^{-1} \cdot m^{-1})$  $\sigma_{e}$
- dimensionless temperature θ
- dimensionless time τ
- volume of the system  $\Omega$

## 1. Introduction

Use of an external magnetic field is of considerable importance in many industrial applications, particularly as a control mechanism in material manufacturing. Homogeneity and quality of single crystals grown from doped semiconductor melts is of interest to manufacturers of electronic chips. One of the main purposes of electromagnetic control is to stabilize the flow and suppress oscillatory

# **Subscripts**

a	dimensionless
c c	cold wall
-	
h	hot wall
Mag	magnetic
Th	thermal
t	total
Vis	viscous

instabilities, which degrades the resulting crystal. Oreper and Szekely [1] showed that the magnetic field suppresses the natural convection currents and the magnetic field strength is one of the most important factors for crystal formation. As a consequence there has been increased interest in the flows of electrically conducting fluid in cavities subjected to external magnetic field. For an electrically conducting fluid exposed to a magnetic field, Lorentz force is also active and interacts with the buoyancy force in governing the flow and temperature fields. Rudraiah et al. [2] investigated the effect of surface tension on buoyancy driven flow of an electrically conducting fluid in a square cavity in presence of a vertical transverse magnetic field to see how this force damps hydrodynamic movements, since, this is required to enhance crystal purity, increase compositional uniformity and reduce defect density. Al-Najem et al. [3] used the power control volume approach to determine the flow and temperature fields under a transverse magnetic field in a titled square enclosure with isothermal vertical walls and adiabatic horizontal walls at Prandtl number of 0.71. They showed that the suppression effect of the magnetic field on convection currents and heat transfer is more significant for low inclination angles and high Grashof numbers. Ishak et al. [4] numerically studied a steady two-dimensional flow of an electrically conducting fluid due to a stretching cylindrical tube. They showed that Nusselt number increases as Prandtl number increases (from Pr = 0.7 to Pr = 7). Moreover, the effect of the magnetic field is found to be more pronounced for fluids with smaller Prandtl number (Pr = 0.7), since fluids with smaller Prandtl number have larger thermal diffusivity. Ece and Büyük [5] investigated the influence of a magnetic field in an inclined rectangular enclosure heated from the left vertical wall and cooled from the top wall, while the other walls are kept adiabatic for the case of a laminar natural convection flow of a fluid characterized by Pr = 1, which is an approximate value for most gases. They showed that the flow characteristics and therefore the convection heat transfer depend strongly upon the strength and direction of the magnetic field, the aspect ratio and the inclination of the enclosure. Circulation and convection become stronger with increasing Grashof number but they are significantly suppressed by the presence of a strong magnetic field. Magnetic field significantly reduces the local Nusselt number by suppressing the convection currents. Natural convection of low Prandtl number fluid in the presence of a magnetic field was numerically studied by Ozoe and Maruo [6], they obtained correlations for the Nusselt number in terms of Rayleigh, Prandtl and Hartmann numbers. Rudraiah et al. [7] numerically investigated the effect of a transverse magnetic field on natural convection flow inside a rectangular enclosure with isothermal vertical walls and adiabatic horizontal walls and found out that a circulating flow is formed with a relatively weak magnetic field and that the convection is suppressed and the rate of convective heat transfer is decreased when the magnetic field strength increases. Alchaar et al. [8] numerically investigated the natural convection in a shallow cavity heated from below in the presence of an inclined magnetic field and showed that the convection modes inside the cavity strongly depend on both the strength and orientation of the magnetic field and that horizontally applied magnetic field is the most effective in suppressing the convection currents.

Ikezoe *et al.* [9] have presented many interesting phenomena occurred in the magnetic field such as the levitation of a water droplet by strong magnetic field, driving of air flow due to magnetic field, *etc.* Wakayama [10] and Wakayama *et al.* [11,12] found very interesting phenomena such as jet stream of nitrogen gas into air (Wakayama jet) in a steeply decreasing magnetic field, enhancement of combustion flames and sustaining flame under microgravity. Filar *et al.* [13] numerically computed

three-dimensional convection of air in a vertical cylinder isothermally heated and cooled from a side wall in both magnetic and gravity fields. A single electric coil was placed around the cylinder to generate a magnetic field. It was found that the flow mode and heat transfer rate can be controlled by magnetic field. Further, axi-symmetric stable convection or even near the conduction state was obtained when the coil is located near the top plate of the cylinder, whereas strong and oscillatory convection was resulted when the magnetic coil is located near the bottom plate of the cylinder. Teamah [14] numerically studied steady heat and mass transfer by natural convection flow of a heat generating fluid in presence of a transverse magnetic field in a rectangular enclosure at fixed values of aspect ratio (A = 2), Lewis number (Le = 1) and Prandtl number (Pr = 0.7). It was found that magnetic field tends to reduce heat transfer and fluid circulation within the enclosure. For Hartmann number Ha > 20, average Nusselt and Sherwood numbers have constant values over a range of thermal Rayleigh number, this range increases with increasing Hartmann number. Tsai et al. [15] numerically studied the effects of variable viscosity and thermal conductivity on heat transfer for hydromagnetic flow over a continuous moving porous plate with ohmic heating. They showed that for Pr = 0.7, the fluid velocity decreases, whereas the temperature profile increases with increasing in magnetic field. The study showed that temperature increases with an increasing in thermal conductivity parameter and decreasing Prandtl number at fixed values of magnetic parameter and Eckert number (studied Prandtl numbers are 0.7 and 6.7 which corresponds to air and water, respectively). The effect of the variable viscosity on velocity and temperature profiles for air (Pr = 0.7) and water (Pr = 6.7) at constant values of magnetic parameter (M = 1), Eckert number (Ec = 0.5) and thermal conductivity parameter (S = 1), shows that velocity and temperature for air is more obviously than for liquid water. Bararnia *et al.* [16] employed a Homotopy analysis method (HAM) to investigate momentum, heat and mass transfer characteristics of MHD natural convection flow for the case of an electrically conducting and heat generation fluid over a porous surface immersed in a porous medium. They showed that at fixed imposed magnetic field, the increase in Prandtl number from liquid metal to liquid passing through gas (Pr = 0.1, 0.5, 0.7, 1 and 10) tends to reduce thermal boundary layer along the plate. This yields a reduction in the fluid temperature. Thus, the higher Prandtl number means more viscous fluid which increases boundary layer thickness and then causes reduction in shear stress. Alam et al. [17] numerically studied Dufour and Soret effects on two-dimensional steady combined free-forced convective and mass transfer flow of a viscous, incompressible and electrically conducting fluid over an isothermal semi-infinite vertical flat plate under the influence of transversely applied magnetic field. It was shown that (the fluid mixture is characterized by a Prandtl number Pr = 0.71 and a Schmidt number Sc = 0.22) the increase of magnetic field leads to the decrease of velocity field indicating that magnetic field retards the flow motion. Inversely, the increase of magnetic field induces the augmentation of both temperature and concentration distributions.

Study of convective flow in rotating system is of considerable importance in many industrial, geophysical and engineering applications. In this context, Singh *et al.* [18] studied a hydromagnetic convective flow of an incompressible viscous liquid over an accelerated porous plate. The whole system is in a state of solid body rotation. Numerical values of Prandtl number are chosen to be Pr = 0.71, Pr = 7.0 and Pr = 11.4, which corresponds to air, water at 20 °C and water at 4 °C, respectively. They found that an increase in magnetic field decreases the velocity field and that the increase in Prandtl number decreases the temperature field. Further, an increase in rotation parameter

increases the velocity and the temperature fields. A combined free and forced convection flow of an electrically conducting fluid in a channel in presence of a transverse magnetic field is of special technical significance because of its frequent occurrence in many industrial applications such as geothermal reservoirs, cooling of nuclear reactors, thermal insulation and petroleum reservoirs. These types of problem also arise in electronic packages, microelectronic devices during their operations. For more details reader can see [19–22] as examples.

Efficient utilization of energy is the primary objective in the design of any thermodynamic system. This can be achieved by minimizing entropy generation in processes. The theoretical method of entropy generation has been used in the specialized literature to treat external and internal irreversibilities. The irreversibility phenomena, which are expressed by entropy generation in a given system, are related to heat transfer, mass transfer, viscous dissipation, magnetic field, etc., Bejan [23-25], Bejan et al. [26], Arpaci and Selamet [27,28], Arpaci [29,30], Arpaci and Esmaeeli [31], Magherbi et al. [32,33] and Abbassi et al. [34] have studied the influence of operating parameters on entropy generation in different flow configurations. They showed that the flow parameters might be chosen in order to minimize entropy generation inside the system. Salas et al. [35] analytically showed a way of applying entropy generation analysis for modelling and optimization of magnetohydrodynamic induction devices. Salas et al. [35] restricted their analysis to only Hartmann model flow in a channel. Mahmud and Fraser [36] studied entropy generation in a fluid saturated porous cavity for laminar magnetohydrodynamic natural convection, where the magnetic force is assumed acting along the direction of the gravity force. It was found that increasing Hartmann number (*i.e.*, magnetic force), tends to retard the fluid motion, both average Nusselt and dimensionless entropy generation numbers decrease with increasing Hartmann number and approach a limiting value (asymptotic value). For other configurations and/or geometrical situation flows, a detailed analysis of the second law of thermodynamics for fundamental problems of heat transfer is given by Mahmud and Fraser [37]. Mahmud et al. [38] performed a thermodynamic analysis of steady mixed convection flow of an electrically conducting and heat-generating/absorbing fluid through a vertical channel in presence of a magnetic field applied normal to the flow direction. Thermophysical properties of the fluid are considered constant with a Prandtl number Pr = 0.7. It was found that the increase in Hartmann number (Ha) tends to slow down the fluid velocity in the channel for symmetric temperature at walls with a symmetric tendency of velocity profiles about the centreline of the channel. For asymmetric temperature at the walls, velocity profiles are not symmetric about the centreline of the channel and asymmetricity increases more as Hartmann number increases. In the case of symmetric temperature at the boundary, as Hartmann number increases, entropy generation decreases towards a minimum value at the centreline of the channel, then increases again. They numerically determined a correlation giving the value of the aspect ratio  $\alpha_0$  of the channel which corresponds to minimum entropy generation, and it is given by:

$$\begin{cases} \alpha_0 = 6.32581 (Ha)^{0.223384} \left(\frac{Gr}{Re}\right)^{-0.1179} \\ (0.1 \le \text{Ha} \le 10 \text{ and } 0.1 \le Gr/Re \le 10) \end{cases}$$
(1)

where Gr and Re are Grashof and Reynolds numbers, respectively.

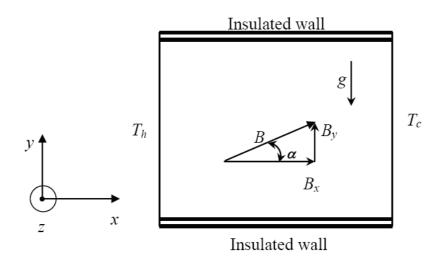
The main objective of this work is to examine the influence of an external oriented magnetic field on entropy generation as well as on heat transfer and fluid flow in natural convection of two different fluids which are air (with Pr = 0.71) and liquid gallium (with Pr = 0.02) enclosed in a square cavity. The numerical resolution is based on control volume finite element method for resolving the governing equations in 2D approximation. Local and total irreversibilities are studied by using five independent parameters, which are: the Prandtl number, the inclination angle of the magnetic field, the irreversibility coefficients and Grashof and Hartman numbers. The behaviour of entropy generation in transient state and then entropy generation analysis in stationary state are studied. This procedure may enhance the reversible work done by the fluid and minimize the degraded energy expressed by entropy generation.

#### 2. Governing Equations

Laminar, incompressible boundary heat transfer by convective flow of a fluid such that its thermophysical properties remain constant is considered. *x* axis and *y* axis are in the plane and *z* axis is normal to it with velocity components (*u*, *v*, 0). A uniform magnetic field of strength *B* ( $B_x$ ,  $B_y$ , 0) is applied and the magnetic Reynolds number ( $R_{em} = \mu_e \sigma_e V_0 L_0 \ll 1$ , where  $\sigma_e$ ,  $\mu_e$ ,  $V_0$  and  $L_0$  are the magnetic permeability, the viscosity, the characteristic velocity and length, respectively) is assumed to be small so that the induced magnetic field is negligible in comparison to the applied magnetic field. Since there is no applied or polarization voltage imposed on the flow field, the electric field E = 0.

The right and the left walls are maintained at uniform temperatures  $T_c$  and  $T_h$ , respectively, and are such that  $T_c < T_h$ , horizontal walls are adiabatic as illustrated in Figure 1. The cavity is permeated by the uniform oriented magnetic field  $B = B_x e_x + B_y e_y$  (where  $B_x$  and  $B_y$  are space independent) of constant magnitude  $B_0 = \sqrt{B_x^2 + B_y^2}$  and  $e_x$  and  $e_y$  are unit vectors in Cartesian coordinate system. The orientation of the magnetic field forms an angle  $\alpha$  with horizontal axis, such that tan  $\alpha = B_y/B_x$ .

Figure 1. Cavity configuration in presence of an oriented magnetic field.



The electric current density and the electromagnetic force are defined as follows, respectively:

$$J = \sigma_{\rm e} \left( E + w \times B \right) \tag{2}$$

$$E_{M} = J \times B = \sigma_{e} \left( E + w \times B \right) \times B \tag{3}$$

As mentioned above, the electric field is negligible, so that Equation (2) and Equation (3) are given by:

$$J = \sigma_e \left( w \times B \right) \tag{4}$$

$$E_{M} = J \times B = \sigma_{e} (w \times B) \times B$$
(5)

For an oriented magnetic field (which makes an inclination angle  $\alpha$  with respect to x axis), and by taking into consideration the electromagnetic force components projected with respect to x and y directions, the continuity, change of linear momentum and energy equations in scalar form are written as follows:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{6}$$

$$\rho \left[ \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} \right] = -\frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) + \sigma_e B_0^2 \left( v \sin \alpha \cos \alpha - u \sin^2 \alpha \right)$$
(7)

$$\rho \left[ \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} \right] = -\frac{\partial p}{\partial y} + \mu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) + \sigma_e B_0^2 \left( u \sin \alpha \cos \alpha - v \cos^2 \alpha \right) + g \beta (T - T_0) \rho$$
(8)

$$\rho C_{p} \left[ \frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right] = k \left( \frac{\partial^{2} T}{\partial x^{2}} + \frac{\partial^{2} T}{\partial y^{2}} \right)$$
(9)

 $C_P$  is the isobaric specific heat of the fluid. Thus, the governing conservative equations of the mass, the momentum and the energy in their dimensionless variables take the following form:

• continuity equation:

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} = 0 \tag{10}$$

• momentum equation in *X* direction:

$$\frac{\partial U}{\partial \tau} + div (Uv - grad U) = -\frac{\partial P}{\partial X} + Ha^2 (V \sin \alpha \cos \alpha - U \sin^2 \alpha)$$
(11)

• momentum equation in *Y* direction:

$$\frac{\partial V}{\partial \tau} + div \left( Vv - grad \ V \right) = -\frac{\partial P}{\partial Y} + Gr_T \theta + Ha^2 \left( U \sin \alpha \cos \alpha - V \cos^2 \alpha \right)$$
(12)

• energy equation:

$$\frac{\partial \theta}{\partial \tau} + div \left( \theta v - \frac{1}{\Pr} \operatorname{grad} \theta \right) = \boldsymbol{\theta}$$
(13)

The governing equations are established on the basis of the following dimensionless variables:

$$X = \frac{x}{L}, Y = \frac{y}{L}, U = \frac{uL}{v}, V = \frac{vL}{v}, \theta = \frac{T - T_0}{T_h - T_c}, P = \frac{pL^2}{\rho_0 v^2}, Gr_T = \frac{g\beta \, \Delta TL^3}{v^2}$$

$$Pr = \frac{v}{a}, \tau = \frac{vt}{L^2}, Ha = B_0 L \sqrt{\frac{\sigma_e}{\mu}}$$
(14)

Governing equations show that the flow is governed by the inclination angle of the electromagnetic force, the Prandtl number which characterizes the relative importance of viscous to thermal effects, the thermal Grashof number which approximates the ratio of the buoyancy force to the viscous force acting on the fluid, the magnetic field and the Hartmann number. Hartmann number indicates the relative importance of the electromagnetic force to the viscous force.

Boundary conditions of the problem are given by:

$$U = V = 0$$
 for all walls;  $\theta = 0.5$  at  $X = 0$  and  $\theta = -0.5$  at  $X = 1$   
 $\frac{\partial \theta}{\partial Y} = 0$  at  $Y = 0$  and  $Y = 1$ 

Initial conditions (*i.e.*, at  $\tau = 0$ ) are:

$$U = V = 0$$
,  $P = 0$  and  $\theta = 0.5 - X$  for the overall cavity.

It is reasonable to notice that there is no temperature gradient at initial state.

Once the numerical value of the temperature  $\theta$  is calculated, the rate of heat flux in dimensionless form is given by Nusselt number that compares convection to conduction modes.

Equating the heat transfer by convection to the heat transfer by conduction at hot wall gives:

$$h\Delta T = -k \left(\frac{\partial T}{\partial x}\right)_{x=0} \tag{15}$$

Introducing the dimensionless variables defined in Equation (14), into Equation (15), gives the local Nusselt number:

$$Nu_{\ell} = -\left(\frac{\partial\theta}{\partial X}\right)_{X=0}$$
(16)

Consequently, the average Nusselt number is obtained by integrating the above local Nusselt number over the vertical hot wall:

$$Nu = \int_0^1 -\left(\frac{\partial\theta}{\partial X}\right)_{X=0} dY$$
(17)

#### 3. Second Law Formulation

Irreversible nature of heat transfer and viscous effects cause continuous generation of entropy in the fluid. Entropy generation is then due to non-equilibrium flow imposed by boundary conditions through the cavity. Since entropy generation results from the heat transfer and fluid friction, known scalar fields of temperature and velocity components provide the calculation of degraded energy expressed by entropy generation. Adding another external force (the magnetic force), the rate of entropy generation (which is derived from energy and entropy balances) is presented by its general form for a two-dimensional flow as follows (Woods [39]):

$$\dot{S}_{gen} = \frac{k}{T^2} \left[ \left( \frac{\partial T}{\partial x} \right)^2 + \left( \frac{\partial T}{\partial y} \right)^2 \right] + \frac{\mu}{T} \left[ 2 \left( \frac{\partial u}{\partial x} \right)^2 + 2 \left( \frac{\partial v}{\partial y} \right)^2 + \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)^2 \right] + \frac{(J - Qw)(E + w \times B)}{T}$$
(18)

It is assumed that in the effective current density term (J - Qw) of equation (18), J >> Qw, where Q is the electric charge density. In a similar way, the electric force per unit charge (E) is assumed negligible compared to the magnetic force per unit charge ( $w \times B$ ). Many authors, namely Mahmud and Fraser [40] and Tasnim and Mahmud [41] gave a dimensionless form of the local entropy generation which is a ratio between local entropy generation rate and a characteristic entropy transfer rate  $\sigma_0$ . According to Bejan [24], the characteristic entropy transfer rate is given by:

$$\sigma_0 = k \left(\frac{\Delta T}{LT_0}\right)^2 \tag{19}$$

where k, L,  $T_0$  and  $\Delta T$  are the thermal conductivity, the characteristic length of the enclosure, a reference temperature and a reference temperature difference, respectively.

Following this procedure, and in order to obtain a dimensionless expression of local entropy generation in natural convection in presence of a magnetic field, Equation (18) becomes (in this study E = 0):

$$\dot{S}_{gen} = \frac{k}{T_0^2} \left[ \left( \frac{\partial T}{\partial x} \right)^2 + \left( \frac{\partial T}{\partial y} \right)^2 \right] + \frac{\mu}{T_0} \left[ 2 \left( \frac{\partial u}{\partial x} \right)^2 + 2 \left( \frac{\partial v}{\partial y} \right)^2 + \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)^2 \right] + \frac{\sigma_e \left( w \ge B \right)^2}{T_0}$$
(20)

As can be seen from the right hand side of Equation (20), the first term represents irreversibility due to thermal gradients, the second is due to fluid friction and the third is due to magnetic force. By using dimensionless variables given in Equation (14), the dimensionless local entropy generation in presence of an oriented magnetic force is then given by:

$$\sigma_{l,a} = \left(\frac{\partial\theta}{\partial X}\right)^2 + \left(\frac{\partial\theta}{\partial Y}\right)^2 + \chi_1 \left[2\left(\frac{\partial U}{\partial X}\right)^2 + 2\left(\frac{\partial V}{\partial Y}\right)^2 + \left(\frac{\partial U}{\partial Y} + \frac{\partial V}{\partial X}\right)^2\right] + \chi_2 \left(U\sin\alpha - V\cos\alpha\right)^2 \quad (21)$$

From this dimensionless expression of local entropy generation, local irreversibilities due thermal gradients, viscous effects and the oriented magnetic field are given respectively by:

$$\sigma_{l,a,Th} = \left(\frac{\partial\theta}{\partial X}\right)^2 + \left(\frac{\partial\theta}{\partial Y}\right)^2 \tag{22}$$

$$\sigma_{l,a,Visc} = \chi_1 \left[ 2 \left( \frac{\partial U}{\partial X} \right)^2 + 2 \left( \frac{\partial V}{\partial Y} \right)^2 + \left( \frac{\partial U}{\partial Y} + \frac{\partial V}{\partial X} \right)^2 \right]$$
(23)

$$\sigma_{I,a,Mag} = \chi_2 \left( U \sin \alpha - V \cos \alpha \right)^2 \tag{24}$$

Dimensionless irreversibility coefficients related to viscous and magnetic field effects are defined respectively by:

$$\chi_1 = \frac{\mu T_0}{k} \left( \frac{\nu}{L(\Delta T)} \right)^2 \tag{25}$$

$$\chi_2 = \chi_1 H a^2 \tag{26}$$

Total dimensionless entropy generation is calculated by integrating Equation (21) through the entire cavity. It is given by:

$$\sigma_{t} = \int_{\Omega} \sigma_{l,a} \, d\Omega \tag{27}$$

#### 4. Numerical Scheme

A modified version based on control volume finite element method (CVFEM) of Saabas and Baliga [42] is used. This method is adapted to staggered grids in which pressure and velocity components are calculated and stored at different points. SIMPLER algorithm was applied to resolve the pressure-velocity coupling in conjunction with an alternating direction implicit scheme (ADI) for performing the time evolution.

From the calculated scalar fields of temperature and velocity components by using Equations (11)–(13), local entropy generation is determined by Equation (21), then total entropy generation is evaluated by numerical integration of Equation (27). Nusselt number is also calculated by Equation (17). For further details concerning CVFEM method, reader can see works of Saabas and Baliga [42], Prakash [43], Hookey [44] and Elkaim *et al.* [45]. The used numerical code written in FORTRAN language was described and validated in details in Abbassi *et al.* [46, 47]. In this study, the use of meshes with  $31 \times 31$ ,  $41 \times 41$  and  $51 \times 51$  points for  $Gr_T = 10^3$ ,  $10^4$  and  $10^5$  respectively, is found sufficiently enough to achieve the imposed global and local convergence criteria given respectively by:

$$\left(\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y}\right) \le 10^{-4}, \ \max\left|\frac{\Gamma^{\tau + \Delta \tau} - \Gamma^{\tau}}{\Gamma^{\tau + \Delta \tau}}\right| \le 10^{-5}$$
(28)

where  $\Gamma$  is the dependent variable,  $\Gamma = (U, V, \theta)$ . The used time step is set to be  $\Delta \tau = 10^{-3}$  and  $10^{-5}$  for Pr = 0.71 and 0.02, respectively.

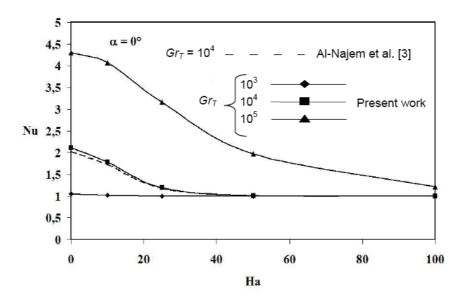
#### 5. Results and Discussions

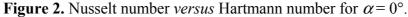
Problems of natural convection flow are numerically, analytically and experimentally investigated by many authors. The main originality of the present paper is to study numerically the influence of an external oriented magnetic field on entropy generation in natural convection flow. As indicated above, the independent operating parameters of the considered problem are: the thermal Grashof number  $Gr_T$ , ranging between 10<sup>3</sup> and 10<sup>5</sup>, the irreversibility coefficient related to fluid friction  $\chi_1$ , ranging between 10<sup>-4</sup> and 10<sup>-2</sup>, the Hartmann number *Ha*, ranging between 0 and 100 and the inclination angle of the magnetic field  $\alpha$ , ranging between 0° and 90°. Obviously, the irreversibility coefficient related to the magnetic field  $\chi_2$ , depends directly on  $\chi_1$  and *Ha*. To be realistic, the numerical values of Prandtl number are chosen to be Pr = 0.71 and Pr = 0.02, which, correspond to air and liquid gallium, respectively. Liquid gallium is widely used in integrated circuits with optoelectronic devices, to dope semiconductors and produce solid-state devices like transistors, as a component in low-melting alloys and in some high temperature thermometers.

Figure 2 shows the variation of Nusselt number *versus* Hartmann number for  $\alpha = 0^{\circ}$  and Pr = 0.71. Good agreement of our results and those found by Al-Najem *et al.* [3] is observed for  $Gr_T = 10^4$ , heat transfer decreases as Hartmann number increases. It is important to notice that heat transfer is reduced to pure conduction mode as Hartmann number tends towards the value 100. Consequently, the magnetic field tends to suppress the convection and retards the fluid motion via the Lorentz force (magnetic force).

Transient entropy generation is then studied for fixed values of the Prandtl number, the inclination angle of the magnetic field ( $\alpha = 0^{\circ}$ ) and the irreversibility coefficient related to fluid friction  $(\chi_1 = 10^{-3})$  at different values of thermal Grashof and Hartmann numbers as illustrated in Figures 3 and 4. At Pr = 0.71 and for  $Gr_T \le 10^3$ , Figure 3a shows that entropy generation magnitude increases from the value equal to unity at initial time towards an asymptotic value as time proceeds. Asymptotic value (which describes a stationary state) is rapidly achieved and considerably decreased in magnitude as Hartmann number increases. As a consequence, increasing Hartmann number induces the decrease of entropy generation. On increasing thermal Grashof number ( $Gr_T = 10^4$ ), same results are obtained as the previous case for higher values of Hartmann number (*i.e.*,  $25 \le Ha \le 100$ ) and inversely, an oscillatory behaviour of entropy generation is observed for lower values of Hartmann number ( $0 \le Ha \le 10$ ) before achieving the stationary state (see Figure 3b). For relatively considerable thermal Grashof number values ( $Gr_T \ge 10^5$ ), Figure 3c shows an oscillatory behaviour of entropy generation at the very beginning of transient state for lower values of Hartmann number ( $0 \le Ha \le 35$ ). A critical Hartmann number  $Ha_c = 40$  is obtained from which the oscillatory behaviour vanishes and entropy generation amplitude quickly reaches a maximum value before decreasing asymptotically towards the stationary state. As a consequence, amplitude and oscillation numbers of entropy generation are important as thermal Grashof number increases and Hartmann number decreases. Figure 4 depicts transient entropy generation for  $Gr_T = 10^4$  and  $10^5$  at different Hartmann number values for Pr = 0.02. Figures 4a and 4b show that at fixed Hartmann number, entropy generation increases with time towards a constant value. As Hartmann number increases, asymptotic behaviour of entropy generation is quickly achieved with decreased amplitude of irreversibility. As a consequence, increasing Hartmann number induces the decrease of entropy generation. This is due to the fact that the magnetic field causes the fluid velocity deceleration and the decrease in heat transfer.

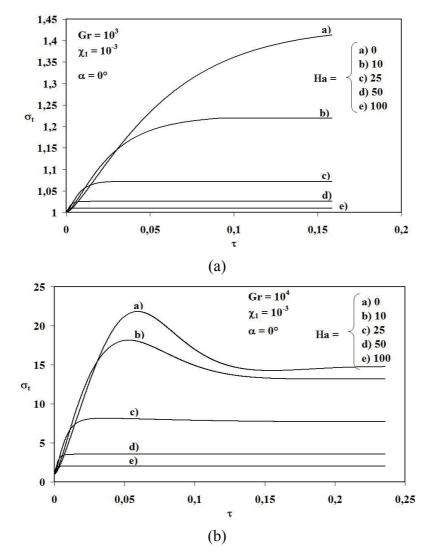
From Figure 3 and Figure 4, it is important to notice that at steady state, an increase in the value of Grashof number will increase the dominancy of the buoyancy force over the present magnetic field strength expressed by Hartmann number. As a consequence, for a fixed Hartmann number value, entropy generation magnitude increases as thermal Grashof number increases.





For Pr = 0.71, fluctuations of total entropy generation versus time for relatively higher thermal Grashof numbers show an oscillatory behaviour of fluid flow that depends on boundary conditions and the magnetic field amplitude. At the beginning of the transient state, heat transfer is mainly due to pure conduction, this is proved by the behaviour of isothermal lines which are parallel to active walls, as time proceeds, isothermal lines are gradually deformed due to convection mode which induces elongation of stream function lines. Consequently, a transition from a single cell towards double cells is obtained just before entropy generation reaches its maximum. This transition induces generation of internal waves in the velocity and temperature fields and than an oscillatory behaviour of entropy generation. Many previous works namely those of Ivey [48], Schladow [49] and Patterson and Armfield [50] showed the existence of transient oscillations in enclosures consisting of two isothermal vertical walls and two adiabatic horizontal walls in absence of the magnetic field. In fact, Ivey [48] showed that transition oscillations occurred because of an internal hydraulic jump with an increase of the horizontal intrusion layers. Transient oscillations consisting of two distinct boundary layer instabilities and whole cavity oscillations were observed by Schladow [49]. The whole cavity oscillations were attributed to the horizontal pressure gradient established by changes in the intrusion temperature field. Similar observations are given by Patterson and Armfield [50]. The two boundary layer oscillations were attributed to travelling wave instability on the boundary layer induced first by the leading edge effect of the vertical boundary layer and second by the impact of the horizontal intrusion from the opposing vertical wall with the boundary layer. The whole cavity oscillations are said to be caused by the splitting of the horizontal intrusion as it impacts the opposite wall. Liquid gallium (Pr = 0.02) is characterized by higher thermal conductivity as compared to air, consequently heat transfer is practically dominated by conduction mode and then no oscillatory behaviour of fluid flow is observed at any of the studied Hartmann and thermal Grashof numbers. This is proved by the plot of transient heat transfer of both fluids at  $Gr_T = 10^5$  and Ha = 0 as an illustrative example as shown in Figure 5.

**Figure 3.** Total dimensionless entropy generation ( $\sigma_t$ ) *versus* dimensionless time for Pr = 0.71,  $\alpha = 0^{\circ}$  and  $\chi_1 = 10^{-3}$  at different Hartmann number values: (a)  $Gr_T = 10^3$ , (b)  $Gr_T = 10^4$ , (c)  $Gr_T = 10^5$ .



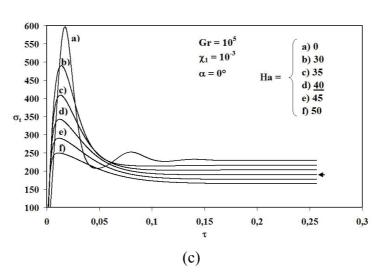
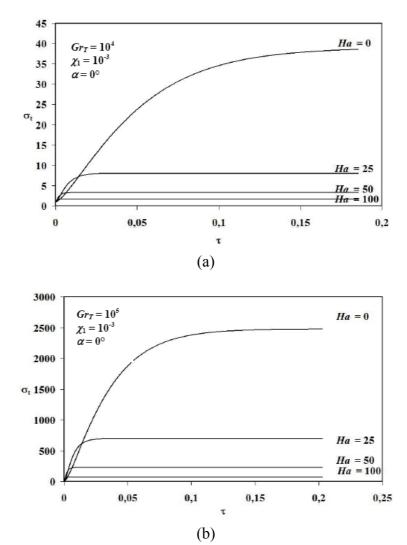
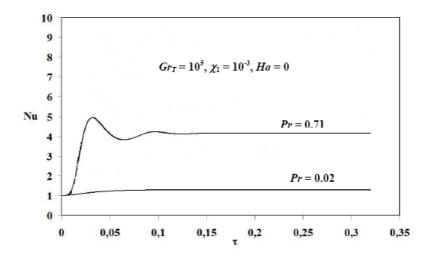


Figure 3. Cont.

**Figure 4.** Total dimensionless entropy generation ( $\sigma_t$ ) *versus* dimensionless time for Pr = 0.02,  $\alpha = 0^\circ$ , and  $\chi_1 = 10^{-3}$  at different Hartmann number values: (a)  $Gr_T = 10^4$ , (b)  $Gr_T = 10^5$ .

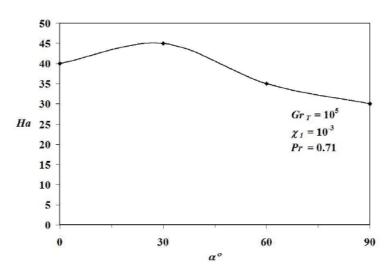




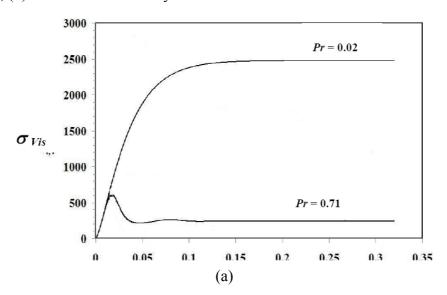
From thermodynamic viewpoint, the oscillatory behaviour of entropy generation at Pr = 0.71 is observed when  $Gr_T \ge 10^4$  for small Hartmann number values (Figures 3b-3c). This result is consistent with the findings of Magherbi *et al.* [51] when  $Gr_T \ge 10^4$  in absence of magnetic field. Magherbi *et al.* [51] showed that steady state is relatively far from equilibrium state, thus the system takes a spiral approach towards the stationary state corresponding to an oscillation of entropy generation over time. In this case the Prigogine's theorem [52] is not verified and the system evolves in the non-linear branch of thermodynamics for irreversible processes. The asymptotic behaviour of entropy generation observed for  $Gr_T \le 10^3$  (at any Hartmann number), for  $10^3 < Gr_T \le 10^4$  (when  $Ha \ge 10$ ) and for  $Gr_T = 10^5$  (when  $Ha \ge 40$ ), shows that the system evolves in the linear branch of thermodynamics for irreversible processes, where the famous Onsager reciprocity relations are applicable. In these cases, the stationary state is sufficiently close to the equilibrium state, as a consequence, entropy generation, quickly reaches a maximum value, then tends towards a constant value. In order to have clear idea, Figure 6 shows critical values of Hartmann number versus the inclination angle of the magnetic field for a fixed thermal Grashof number ( $Gr_T = 10^5$ ). For  $Ha > Ha_c$ , the system evolves in the linear branch of thermodynamics of irreversible processes. Further, for  $0^{\circ} \le \alpha \le 90^{\circ}$ , it was found that maximum  $Ha_c$  (= 45) is obtained at  $\alpha$  = 30° (see Figure 6), this indicates that the stationary regime is far from the equilibrium state as compared to other inclination angle values of the magnetic field. In this case,  $Ha_c = 30, 35$  and 40 for  $\alpha = 90^\circ, 60^\circ$  and  $0^\circ$ , respectively. As an important conclusion, increasing the inclination angle of the magnetic field  $(30^\circ \le \alpha \le 90^\circ)$  tends to decrease critical Hartmann number, and consequently to decrease transient oscillatory behaviour of entropy generation.

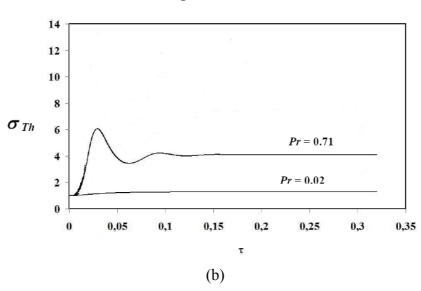
As mentioned above, no oscillatory behaviour is obtained for transient entropy generation at Pr = 0.02 as compared to the situation when Pr = 0.71 for the studied Grashof and Hartmann numbers. This is possible since low Prandtl number means higher thermal conductivity, consequently, fluid temperature increases as Prandtl number decreases (see Equation (13)). This is confirmed by Singh *et al.* [18], where they found that temperature decreases as Prandtl number increases. Further, source term of velocity depends on product of buoyancy and thermal effects as well as magnetic field (see Equation (12)), consequently, velocity gradients increase as thermal Grashof number and temperature increase. Hartmann number has the effect to suppress the fluid velocity and then to reduce the temperature profile. For these reasons, transient entropy generation increases via the increase of viscous irreversibility and is more pronounced for lower Prandtl number value as illustrated in Figure 7 as an example. Thus, larger inertial effects are obtained for liquid gallium because of its low Prandtl number. Observed asymptotic behaviour of entropy generation at Pr = 0.02 for both viscous and thermal irreversibilities (Figure 7a,7b) show that the system evolves in the linear branch of thermodynamics for irreversible processes, the stationary state is sufficiently close to the equilibrium state, as a consequence, entropy generation, quickly reaches a maximum value, then tends towards a constant value. It could be noticed that the magnetic field effect plays the major role in terms of minimizing energy degradation expressed by entropy generation, practically, one should simply choose the appropriate value of the magnetic field (expressed by Hartmann number) to get less degraded energy.

**Figure 6.** Hartmann number *versus* inclination angle of the magnetic field for Pr = 0.71,  $Gr_T = 10^5$  and  $\chi_1 = 10^{-3}$ .



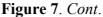
**Figure 7.** Transient entropy generation for  $Gr_T = 10^5$ ,  $\chi_1 = 10^{-3}$  and Ha = 0: (a) viscous irreversibility, (b) thermal irreversibility.



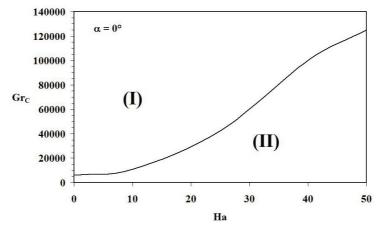


Since entropy generation exhibits fluctuations for Pr = 0.71 when  $Gr_T \ge 10^4$ , critical thermal Grashof number *versus* Hartmann number was studied for fixed values of the inclination angle of the magnetic field and irreversibility coefficient  $\chi_1$  (*i.e.*,  $\alpha = 0^\circ$  and  $\chi_1 = 10^{-3}$ ). Curve plotted in Figure 8 depicts critical values of thermal Grashof number obtained at each Hartmann number value ( $0 \le Ha \le 50$ ), thus for  $Gr_T > Gr_c$ , the stationary regime is far from the equilibrium state. Figure 8 is divided into two regions: (I) represents the region corresponding to higher values of thermal Grashof number for which the system evolves in the non linear branch of thermodynamics of irreversible processes. In this case, entropy generation exhibits oscillatory behaviour corresponding to a non equilibrium state. (II) represents the region corresponding to thermal Grashof number values for which the system evolves in the linear branch of thermodynamics of entropy generation vanishes and the system evolves in the linear branch of thermodynamics of irreversible processes. It's important to notice that as Hartmann number value increases, the system tends towards stationary state because critical thermal Grashof number for which the system evolves in the linear branch of thermodynamics of irreversible processes. It's is obtained at higher values. As an illustrative example,  $Gr_c \approx 10^4$  at Ha = 10 and  $Gr_c \approx 1.2 \times 10^5$  at Ha = 50.

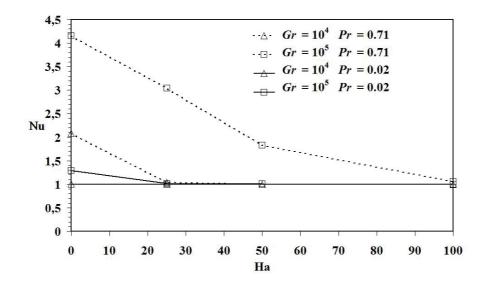
In steady state, magnitude of entropy generation is higher for lower Prandtl number value till Ha < 25 for  $Gr_T = 10^4$  and Ha > 50 for  $Gr_T = 10^5$  (see Figure 3 and Figure 4). As mentioned above, for Pr = 0.02, heat transfer by conduction mode is more pronounced than that for Pr = 0.71. This is proved by the plot of Nusselt number *versus* Hartmann number for  $Gr_T = 10^4$  and  $10^5$  as illustrated in Figure 9. As Hartmann number increases, Nusselt number tends towards unity and then isothermal lines become practically parallel to the active wall and the fluid velocity decreases.



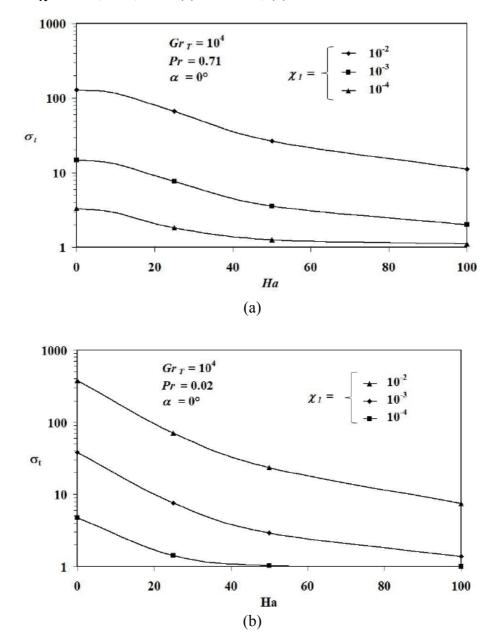
**Figure 8.** Critical thermal Grashof number *versus* Hartmann number for Pr = 0.71,  $\alpha = 0^{\circ}$  and  $\chi_1 = 10^{-3}$ .



**Figure 9.** Nusselt number *versus* Hartmann at different thermal Grashof numbers for Pr = 0.71 and 0.02 at  $\alpha = 0^{\circ}$ .



In order to study the influence of the irreversibility coefficient on entropy generation at fixed inclination angle of the magnetic field in steady state, Figure 10 illustrates the dependence of entropy generation on Hartmann number for Pr = 0.71 and 0.02 at  $Gr_T = 10^4$ ,  $\alpha = 0^\circ$  and  $\chi_1 = 10^{-4}$ ,  $10^{-3}$  and  $10^{-2}$ , respectively. As can be seen from Figure 10, entropy generation decreases as Hartmann number increases, and inversely, it increases with the increase of irreversibility coefficient value. Thus, the presence of the magnetic field (described by Hartmann number), tends to reduce fluid flowing inside the cavity, as Hartmann number increases, the major part of the fluid becomes practically immobile and the flow is simply described by approximately conduction mode for higher values of Hartmann number.



**Figure 10.** Total dimensionless entropy generation *versus* Hartmann number at  $\alpha = 0^{\circ}$ ,  $Gr_T = 10^4$  at  $\chi_1 = 10^{-2}$ ,  $10^{-3}$ ,  $10^{-4}$ : (a) Pr = 0.71, (b) Pr = 0.02.

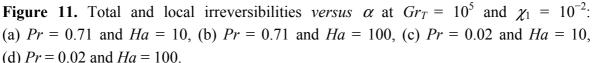
The influence of the inclination angle of the magnetic field on irreversibility due to thermal, viscous and magnetic effects as well as on total entropy generation in stationary state is illustrated in Figure 11. In this case, values of irreversibility coefficient  $\chi_1$  and thermal Grashof number  $Gr_T$  are fixed and set to be  $10^{-2}$  and  $10^5$ , respectively. As can be seen from Figure 11, the study of irreversibility *versus* inclination angle of the magnetic field was performed for lower (respectively higher) Hartmann number. For lower Hartmann number (Ha = 10), Figures 11a, 11c show that irreversibility due to fluid friction is the major contribution of total entropy generation.

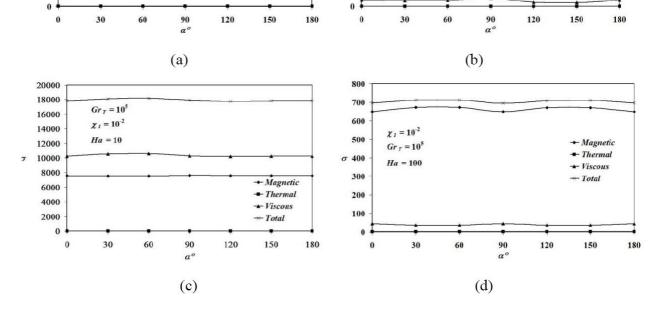
500

(a) Pr = 0.71 and Ha = 10, (b) Pr = 0.71 and Ha = 100, (c) Pr = 0.02 and Ha = 10, (d) Pr = 0.02 and Ha = 100. 3000 1200 1000 2500 800 2000  $\chi_1 = 10^{-2}$  $\chi_1 = 10^{-2}$ 600 σ 1500 + Magnetic  $\sigma$  $Gr_T = 10^5$  $Gr_{T} = 10^{5}$ - Thermal + Magnetic Ha = 101000 400 + Viscous Ha = 100- Thermal - Total + Viscous

200

- Total





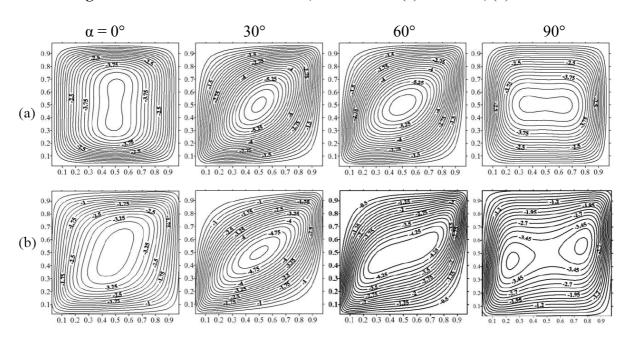
Entropy generation magnitude for Pr = 0.02 is higher than that for Pr = 0.71. It's important to notice that maximum values of irreversibility due to viscous effects as well as total entropy generation are obtained at  $\alpha \approx 90^{\circ}$  and  $60^{\circ}$  for Pr = 0.71 and 0.02, respectively. Inversely, irreversibility magnitude due to magnetic field is at its minimum value at the same angle for Pr = 0.71, while magnetic irreversibility magnitude slightly decreases as the inclination angle increases for Pr = 0.02. Viscous irreversibility magnitude increases when  $0^{\circ} \le \alpha \le 90^{\circ}$  and  $0^{\circ} \le \alpha \le 60^{\circ}$  for Pr = 0.71 and 0.02, respectively, this behaviour is reversed when  $90^{\circ} < \alpha \le 180^{\circ}$  and  $60^{\circ} < \alpha \le 180^{\circ}$  for Pr = 0.71and 0.02, respectively.

For Ha = 100 (considerable magnetic field), Figures 11b, 11d show considerable decrease in magnitude of all irreversibilities as compared to the previous case. Further, entropy generation magnitude for Pr = 0.02 is less than that for Pr = 0.71. The effect of the magnetic field is then more pronounced for liquid gallium than for air in terms of fluid velocity deceleration and temperature field decrease. In this case, total entropy generation increases via the increase of irreversibility due to magnetic field. For considerable Hartmann number (Ha = 100), irreversibility coefficient related to magnetic field is  $\chi_2 = \chi_1 H a^2 = 10^{-2} \times 100^2 = 100$ , further, local irreversibility due to magnetic field is given by  $\sigma_{La,Mag} = \chi_2 (U \sin a - V \cos a)^2$ , as a consequence total entropy generation is entirely dependent on magnetic irreversibility and convective currents are suppressed. For Pr = 0.71, Maximum value of irreversibilities due to magnetic field and viscous effects as well as total entropy generation is obtained at  $\alpha = 90^{\circ}$  (in this case  $\sigma_{l,a,Mag} = 100(U)^2$ ), minimum values of total, magnetic and viscous irreversibilities are obtained at  $\alpha \approx 135^{\circ}$ . For Pr = 0.02 (Figure 11d), maximum value of total entropy generation as well as that related to magnetic irreversibility is found at  $\alpha = 60^{\circ}$ . Minimum amplitude of magnetic as well as total irreversibilities is found at  $\alpha = 90^{\circ}$ , maximum viscous irreversibility is found also at  $\alpha = 90^{\circ}$ . From the previous figures, irreversibility due to thermal gradients is practically absent, this is due to the fact that the magnetic field induces a quasi equilibrium of isothermal lines through the cavity.

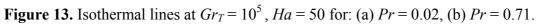
To understand these results, lets plot the streamlines and the isothermal lines for both studied fluids at  $Gr_T = 10^5$  in presence of a magnetic field (Ha = 50) as illustrated in Figures 12 and 13. It can be seen from Figure 12 that, as the direction of the external magnetic field changes from horizontal ( $\alpha = 0^\circ$ ) to vertical ( $\alpha = 90^\circ$ ), the flow increases up to angle  $\alpha = 60^\circ$  and  $30^\circ$  for Pr = 0.02and 0.71, respectively. A higher value of the buoyancy force ( $Gr_T = 10^5$ ) means that the effect of the magnetic field direction is so significant on the flow structure. Figure 13 depicts the corresponding isothermal lines. For liquid Gallium (Pr = 0.02), isothermal lines are practically parallel to the active walls, which means that heat transfer is conduced by conduction mode. For air, thermal boundary layer thickness decreases as the inclination angle increases inducing an increase in heat transfer from horizontal to vertical direction of the magnetic field.

At local level, Figure 14 shows distribution of entropy generation lines inside the cavity in absence of the magnetic field (Ha = 0) for  $10^3 \le Gr_T \le 10^5$  at  $\chi_1 = 10^{-3}$ . For Pr = 0.71, entropy generation lines increase in magnitude with thermal Grashof number and are confined through the active walls (isothermal walls), namely on bottom of the warmed wall and on top of the cooled wall due to the presence of strong thermal and velocity gradients in these regions. For liquid gallium, Figure 14b shows distribution of irreversibility through the whole cavity except its center. Magnitude of entropy generation lines increases with buoyancy effect. For small Prandtl number value, as thermal Grashof number increases, velocity gradients considerably increase causing the augmentation of local entropy generation. In presence of the magnetic field (*i.e.*, for Ha = 50) and for  $Gr_T = 10^5$  and  $\chi_1 = 10^{-3}$ , Figure 15 shows the influence of the inclination angle of the magnetic field on entropy generates at a higher magnitude near the cavity walls. At  $\alpha = 0^\circ$ , both of the active walls act as strong concentrators of irreversibility due to higher value of magnetic irreversibility as shown above.

As compared to Figure 14, the presence of a magnetic field reduces the entropy generation amplitude. A significant portion of the cavity extended along the direction of the magnetic field inside the cavity and represents an idle region for entropy production, where entropy generation is practically zero. It can be seen that as the inclination angle increases, entropy generation lines increase in magnitude for both fluids ( $\alpha = 30^{\circ}$ ), then gradually decrease and are distributed on top of cooled and bottom of heated walls as well as on right side of upper and left side of lower adiabatic walls ( $\alpha = 60^{\circ}$ ). Finally at  $\alpha = 90^{\circ}$ , entropy generation lines are distributed through the entire cavity except its centre for Pr = 0.71, while irreversibility lines are mainly distributed through the insulated walls for Pr = 0.02.



**Figure 12.** Stream lines at  $Gr_T = 10^5$ , Ha = 50 for: (a) Pr = 0.02, (b) Pr = 0.71.



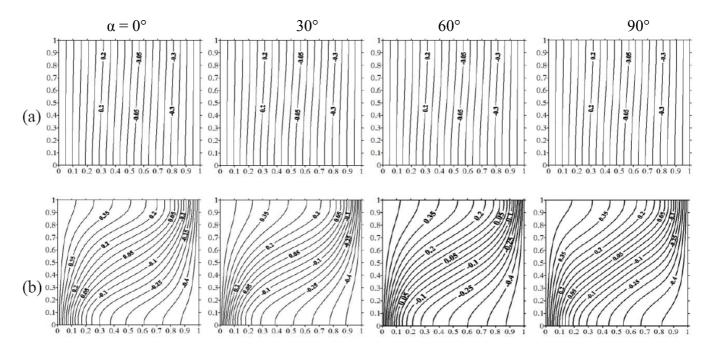


Figure 14. Entropy generation maps at Ha = 0 and  $\chi_1 = 10^{-3}$ : (a) Pr = 0.71, (b) Pr = 0.02, (1)  $Gr_T = 10^3$ , (2)  $Gr_T = 10^4$ , (3)  $Gr_T = 10^5$ .

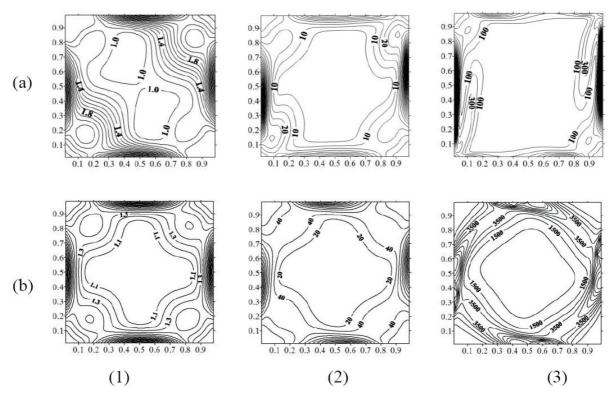
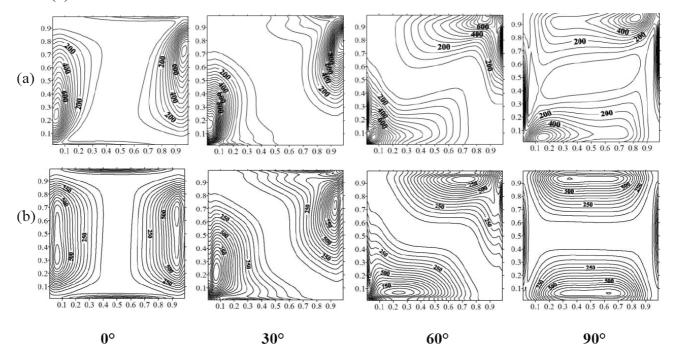


Figure 15. Entropy generation maps at  $Gr_T = 10^5$ ,  $\chi_1 = 10^{-3}$ , Ha = 50: (a) Pr = 0.71, (b) Pr = 0.02.



### 6. Conclusions

The effect of an oriented magnetic field on entropy generation in natural convection flow for air and liquid gallium is numerically studied. It's important to notice the following points:

- For fixed value of the inclination angle of the magnetic field, transient entropy generation exhibits oscillatory behaviour for air when  $Gr_T \ge 10^4$  at small values of Hartmann number (magnetic field). Asymptotic behaviour is obtained for considerable values of Hartmann number. Transient irreversibility always exhibits asymptotic behaviour for liquid gallium. Magnetic field induces the decrease of entropy generation magnitude.
- For air, increasing the inclination angle of the magnetic field  $(30^\circ \le \alpha \le 90^\circ)$ , tends to decrease critical Hartmann number, and consequently to decrease transient oscillatory behaviour of entropy generation.
- For air and at fixed inclination angle of the magnetic field, increasing Hartmann number tends to increase critical Grashof number from which the system evolves in the non-linear branch of thermodynamics for irreversible processes concerning air.
- In steady state, for lower Hartmann number value (Ha = 10) and for relatively higher thermal Grashof number ( $Gr_T = 10^5$ ), maximum value of entropy generation is found at an inclination angle of the magnetic field,  $\alpha = 90^\circ$  and  $60^\circ$  for air and liquid gallium, respectively. For both fluids, irreversibility due to viscous effects is the major contribution of entropy generation.
- In steady state, for higher Hartmann number (Ha = 100) and for relatively higher thermal Grashof number ( $Gr_T = 10^5$ ), for both studied fluids, entropy generation increases via the increase of magnetic irreversibility. Maximum value of irreversibility is also obtained at  $\alpha = 90^\circ$  and  $60^\circ$  for air and liquid gallium, respectively.
- Increasing Hartmann number (Ha ≥ 50), induces the decrease of entropy generation magnitude for lower Prandtl number values.
- Heat transfer rate is always described by pure conduction mode for liquid gallium, whereas it presents oscillatory behaviour for air when  $Gr_T \ge 10^4$ .
- At local level and for relatively higher thermal Grashof number ( $Gr_T = 10^5$ ), entropy generation distribution is strongly dependent on magnetic field direction, magnitude of irreversibility lines increases up to 30°, then gradually decreases. No entropy is generated in the cavity center.

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