## Article

# Internal Flow in an Enhanced Tube Having Square-cut Twisted Tape Insert 

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#### Abstract

In this study, a numerical simulation has been conducted in order to evaluate the thermal hydraulic performance of a turbulent single-phase flow inside an enhanced tube equipped with a square-cut twisted tape (STT) insert. The classical twisted tape (CTT) insert was also investigated for comparison. The $k-\varepsilon$ renormalized group turbulence model has been utilized as the turbulent model. Various twist ratios $(y / W)$ of $2.7,4.5$, and 6.5 were investigated for the Reynolds number range of 8000-18,000, with water as the working fluid. The numerical results indicated that, in comparison with the plain tube (PT), the tube equipped with the STT with the twist ratios of $2.7,4.5$, and 6.5 led to an increase in the values of the Nusselt number and friction factor in the inner tube by $45.4-80.7 \%$ and 2.0-3.3 times, respectively; in addition, the highest thermal performance of 1.23 has been obtained. The results further indicated that the tube equipped with the CTT of the same twist ratios improved the Nusselt number and friction factor in the inner tube by $40.3-74.4 \%$ and $1.7-3.0$ times, respectively, in comparison with the PT; further, the maximum thermal performance of 1.18 was achieved.


Keywords: square-cut twisted tape insert; twisted ratio; thermal performance factor; turbulent flow; numerical investigation

## 1. Introduction

Numerous research studies have been performed on heat exchangers, to enhance the heat transfer, in order to achieve a higher heat exchange performance [1,2]. For this purpose, the following efforts have been reported in our previous works: a direct contact system for adsorption cycle [3-5], using nanofluid as the working fluid [6,7]; improvement of maldistribution inside the distributor of heat exchangers [8-10]; using inserts inside the tubes [11-15]. Based on the published reports, it is known that the investigations on passive heat transfer enhancement methods using various inserts do not consider the existing problems. The designs used in the above-said investigations utilize an enhanced tube equipped with various inserts to achieve a high heat transfer rate. However, those designs were not able to reduce the power required for pumping fluids. Therefore, several efforts have been made to lower the pump duty, to achieve the required performance under several design constraints. Passive heat transfer enhancement methods, which are currently adopted by many researchers, mainly employ swirl devices with twisted tapes [16-19]. Twisted tape inserts are one of the popular techniques
available, to enhance the heat transfer performance of heat exchangers, due to their high economic performance and easy installation. They create a continuously swirling stream to enhance the heat transfer rate. The swirling flow induces turbulence near the pipe walls, which results in a longer fluid flow path in the pipeline, improved fluid mixing, and reduced thermal boundary area, thereby increasing the rate of convection heat transfer. We investigated experimentally the perforated twisted tapes at a constant twist ratio $(y / W)$ of 3.97 with various axial pitch ratios at the Reynolds number range of 5400-17,500 [17]. The result indicated that the thermal performance increased with the decrease in axial pitch ratio. We continued to examine experimentally the V-cut twisted tapes for turbulent flow at the similar operating conditions and a constant twist ratio $(y / W)$ of 3.97 with various width ratios [18]. It demonstrated that as the width ratio decreased, the thermal performance increased.

Results indicate that a significant improvement in the heat transfer cannot be realized together with the improvement in the friction factor (pressure drop). Several modified and improved twisted tapes have been designed to minimize the pressure loss [20-25]; they have been observed under several conditions to determine the key factors affecting the heat transfer and pressure drop of the heat exchangers. An experimental study on the effect of peripherally-cut twisted tape inserts on the thermal performance characteristics in a tube was evaluated in [26]. It was found that the peripherally-cut insert can potentially improve the system performance. Moreover, the system performance can also be improved by increasing the depth ratio and decreasing the width ratio. A square-cut twisted tape insert in the heat exchanger has been adopted in [27]. It was demonstrated that the square-cut twisted tape inserts can provide higher performance than the plain twisted tape inserts. Furthermore, Murugesan et al. [28] studied a V-cut twisted tape insert and performed an experimental study on the heat and friction factor characteristics. They found that the thermal performance was affected by the twist and width ratios. Bhuiya et al. [29] studied the thermal performance in an enhanced tube using perforated twisted tape inserts. It was found that the perforated twisted tape inserts could provide a significantly higher performance compared to that of the plain tubes. In addition, small cut variations using rectangular-cut twisted tape inserts were observed in [30].

Knowledge of the fluid flow mechanisms and heat transfer characteristics based on numerical approach is required, because it can be an important tool for further improvement of the heat exchanger performance. The influence of the insertion of twisted tape inserts in the tube and the enhancement of heat transfer have been clearly studied in [31] using simulation. It was found that, in the case of laminar flows, the tubes with twisted tape inserts achieved a two-times higher heat transfer rate than the tubes without twisted tape inserts. Furthermore, the heat transfer coefficients inside the corrugated tube having a twisted tape insert has been numerically evaluated in [32]. It was found that the numerical results showed a good agreement with the experimental results, which the difference between them was smaller than $\pm 20 \%$.

However, the above-mentioned studies did not encompass all the available enhancement methods. It is supposed that various other methods, especially numerical methods, need to be studied for heat transfer enhancement. Based on experiments, numerical methods are advantageous for predicting the system performance. Unfortunately, most of the experimental works related to the heat transfer augmentation which are adopting twisted tape inserts do not explain the fluid flow and heat transfer mechanisms. Therefore, after publishing Refs. [17,18], we were further motivated to extend the research to evaluate the thermal hydraulic performance of a turbulent single-phase flow inside an enhanced tube equipped with an innovative square-cut twisted tape (STT) insert. Thus, the current study retains its research originality compared with the previous works. In addition, in this study, we validate the obtained results through comparison with the previous results based on experiments [18]. Comparison with numerical results of the classical twisted tape (CTT) insert and the plain tube (PT) was provided for evaluation.

## 2. Numerical Method

Figure 1 shows the geometry of the concentric tube comprising an inner tube for hot fluid flow and an outer tube for cold fluid flow, based on Refs. [17,18]. A computational domain was developed, as shown in Figure 1, and the boundary condition to be applied in the domain was decided. The inner tube had an inside diameter $\left(d_{i}\right)$ of 14.3 mm and an outside diameter $\left(d_{0}\right)$ of 15.8 mm ; the outer tube had an inside diameter $\left(D_{i}\right)$ of 23.4 mm and an outside diameter $\left(D_{0}\right)$ of 25.4 mm ; the pipe length $(L)$ was 2110 mm . All the tapes had a width $(W)$ of 12.6 mm and a thickness $(\delta)$ of 0.7 mm . The twist ratio is defined as the ratio between the twist pitch $(y)$ and tape width $(W)$. The inlet temperature of the hot fluid was 333.15 K , with the Reynolds number ( $R e$ ) of $8000-18,000$ for the velocity inlet, whereas the inlet temperature for the cold fluid was 300.15 K , with a constant mass flow rate of $0.1027 \mathrm{~kg} / \mathrm{s}$. The exit of the tube was connected to the pressure outlet.

To evaluate the thermal performance of the fluid flow and heat transfer, and the characteristics of the thermal performance, in this study, water is utilized as the working fluid. The hot water and cold water are transported through the inner and outer tubes, respectively. The thermo-physical properties of water [15], which are considered as the inlet values during the calculation, are listed in Table 1.

Table 1. Thermo-physical properties of the hot and cold water at inner and outer tube inlets [15].

| Fluid | Temperature <br> $[\mathrm{K}]$ | Heat <br> Capacity $C_{\boldsymbol{p}}$ <br> $[\mathbf{k J} / \mathbf{k g} \cdot \mathrm{K}]$ | Dynamic <br> Viscosity $\boldsymbol{\mu}$ <br> $[\mathrm{kg} / \mathbf{m} \cdot \mathbf{s}]$ | Thermal <br> Conductivity $\boldsymbol{k}$ <br> $[\mathbf{W} / \mathbf{m} \cdot \mathrm{K}]$ | Density $\boldsymbol{\rho}$ <br> $\left[\mathbf{k g} / \mathbf{m}^{3}\right]$ | Prandtl <br> Number <br> $\boldsymbol{P r}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Hot water | 333.15 | 4.185 | $4.67\left(10^{-4}\right)$ | 0.654 | 983.3 | 2.99 |
| Cold water | 300.15 | 4.178 | $8.52\left(10^{-4}\right)$ | 0.613 | 997 | 5.81 |



STT

(a)

(c)

Figure 1. Schematic of the tube with inserts: (a) nomenclature of CTT and STT; (b) CTTs and STTs with twist ratio variation; (c) computational domain under the present study.

Based on the thermo-physical properties of the working fluid (density, velocity, and viscosity) and the inner diameter of the inner tube, $R e$ can be estimated as:

$$
\begin{equation*}
R e=\frac{\rho u D_{i}}{\mu} \tag{1}
\end{equation*}
$$

where $\rho, u$, and $\mu$ are density, velocity, and dynamic viscosity of the water, respectively. In addition, to facilitate velocity variations, $R e$ is set to be between 8000 and 18,000.

Moreover, the heat transfer characteristic, which is defined as the Nusselt number ( $N u$ ), is calculated as:

$$
\begin{equation*}
N u=\frac{h D_{h}}{k} \tag{2}
\end{equation*}
$$

where $h$ and $k$ are convective heat transfer coefficient and thermal conductivity of the working fluid, respectively. $D_{h}$ devotes the hydraulic diameter of inner tube.

The fluid flow characteristics are evaluated by employing the friction factor ( $f$ ), which can be estimated as:

$$
\begin{equation*}
f=\frac{\Delta P}{\left(\rho u^{2} / 2\right)\left(L / d_{i}\right)} \tag{3}
\end{equation*}
$$

As shown in Equation (3), $f$ is influenced strongly by the pressure difference $(\Delta P)$ between the tube inlet and outlet.

Several assumptions are adopted in the current work to solve the numerical simulation [15]: (1) The flow caused in the pipe by the inserts is turbulent and incompressible, (2) the flow is in a steady state, (3) natural convection and thermal radiation are negligible, and (4) the properties of the fluid used depend on the temperature. The three governing equations, covering continuity, momentum, and energy are adopted in order to perform the calculation. These can be defined as follows:

Continuity equation:

$$
\begin{equation*}
\frac{\partial}{\partial x_{i}}\left(\rho u_{i}\right)=0 \tag{4}
\end{equation*}
$$

Momentum equation:

$$
\begin{equation*}
\frac{\partial}{\partial x_{i}}\left(\rho u_{i} u_{k}\right)=\frac{\partial}{\partial x_{i}}\left(\mu \frac{\partial u_{k}}{\partial x_{i}}\right)-\frac{\partial p}{\partial x_{k}} \tag{5}
\end{equation*}
$$

Energy equation:

$$
\begin{equation*}
\frac{\partial}{\partial x_{i}}\left(\rho u_{i} T\right)=\frac{\partial}{\partial x_{i}}\left(\frac{k}{c_{p}} \frac{\partial T}{\partial x_{i}}\right) \tag{6}
\end{equation*}
$$

where $\rho, u, p, \mu, c_{p}$, and $T$ are fluid density, mean velocity, pressure, fluid dynamic viscosity, specific heat, fluid thermal conductivity, and temperature, respectively. In addition, the subscripts $i$ and $k$ represent the direction in both $i$ and $k$, respectively.

The modeling and calculation is assumed to be three-dimensional, turbulent, and steady. In addition, the tube wall is assumed to be adiabatic, and a no-slip condition is considered at the tube walls. Similar to the tube walls, the boundary condition between the fluid and the inserts is also assumed to be adiabatic. In this study, the commercial software Fluent 15 is used for modelling and calculation [33]. This software basically runs based on the finite volume method. This method is also applied to solve Equations (4)-(6), together with the $k-\varepsilon$ renormalized group turbulence model. In addition, the standard-pressure and second-order upwind discretization methods are adopted in order to calculate both momentum and energy. The SIMPLE algorithm is employed to calculate the pressure-velocity coupling. Moreover, the tetrahedron-cell mesh configuration is adopted to validate the plain tube and all twisted tape inserts. The face sizing method is employed in the model in several areas.

## 3. Results and Discussion

During the calculation, the grid is modelled and designed based on the tetrahedral grid type. To make more confident that the grid is sufficiently dense as well as fulfills the grid independence, face sizing is also performed. The modelled grid contains approximately $1,380,314$ cells, which are used to simulate the case of a smooth-tube. Furthermore, the thermal hydraulic characteristics of the plain tube calculated in this study are compared with the several correlations which have been established in order to measure the results accuracy of the calculation. $N u$ is compared and evaluated using the Petukhov and Gnielinski equations [34], whereas $f$ is evaluated using the Petukhov and Blasius equations [35].

The Petukhov equation is estimated as:

$$
\begin{equation*}
N u=\frac{(f / 8) \operatorname{Re} \operatorname{Pr}}{1.07+12.7(f / 8)^{1 / 2}\left(\operatorname{Pr}^{2 / 3}-1\right)} \tag{7}
\end{equation*}
$$

for $10^{4}<\operatorname{Re}<5 \times 10^{6}$.
In addition, the Gnielinski equation is given by:

$$
\begin{equation*}
N u=\frac{(f / 8)(R e-1000) P r}{1+12.7(f / 8)^{1 / 2}\left(P r^{2 / 3}-1\right)} \tag{8}
\end{equation*}
$$

for $1 \times 10^{3}<\operatorname{Re}<5 \times 10^{6}$.
The Petukhov correlation for friction factor is:

$$
\begin{equation*}
f=(0.790 \ln R e-1.64)^{-2} \tag{9}
\end{equation*}
$$

for $10^{4}<\operatorname{Re}<10^{6}$.
The Blasius correlation used to predict the friction factor is given by:

$$
\begin{equation*}
f=0.3164 R e^{-0.25} \tag{10}
\end{equation*}
$$

for $4 \times 10^{3}<\operatorname{Re}<10^{5}$.
Figures 2 and 3 respectively represent the comparison of the $N u$ and $f$ for the smooth tube with the well-known correlations. Under all the evaluated cases, the difference between the results of the current study with the established correlations is relatively small. Therefore, it can be concluded that the results of calculation in the current study show a good accuracy.


Figure 2. Validation of $N u$ for plain tube.


Figure 3. Validation of $f$ for plain tube.
The deviations of the numerical results for the heat transfer ( $N u$ ), in comparison with the established correlations, are within $\pm 5.98 \%$ for the Petukhov correlation and $\pm 2.00 \%$ for the Gnielinski correlation; in the case of $f$, the deviations are within $\pm 6.98 \%$ for the Blasius correlation and $\pm 5.67 \%$ for the Petukhov correlation. Moreover, the differences in $N u$ and friction factor, in comparison with the experiments [18], are less than $5 \%$ and $7 \%$, respectively.

The tetrahedral grid is adopted for meshing during the calculation. To improve the calculation accuracy, the grid is highly converged in the insertion area. Approximately 2,600,000 cells are generated and employed for the tube with the twisted tape inserts. The effect of the twisted tape inserts on the heat transfer characteristics is represented in Figure 4. In general, a higher $N u$ can be obtained by using the twisted tape inserts than the smooth tube. $N u$ is greatly influenced by the distribution of fluid temperature which is flowing inside the enhanced tube. It can be expected that, by fixing the inlet conditions (cold and hot fluids) for all the evaluated cases, the turbulent flow generation will be apparent.


Figure 4. $N u$ for various CTTs and STTs.

A comparison between the plain tube (PT, without insertion) and the corresponding classical twisted tape (CTT) inserts is also conducted to evaluate the heat transfer enhancement by the STTs, as shown in Figure 4. It can be observed that the heat transfer, in terms of $N u$, is improved with the increase in $R e$ (for most cases). The turbulent intensity of the flow increases following the increase in $R e$, leading to the enhancement of the convective heat transfer. These results are consistent with the those of the previous studies $[3-7,9,10]$. Figure 4 further shows that, for the STT, the pitch ratio $y / W$ of 2.7 yields the highest $N u$ followed by those of 4.5 and 6.5. This indicates that, for the same pitch ratio, employing the STTs provides better results than the CTTs. Using the STTs can improve the turbulent intensity of the fluid near the tube walls. Furthermore, the vorticity behind the square-cut increases, resulting in a higher convective heat transfer rate, compared with that of the CTTs. The $N u$ values for STTs and CTTs for the corresponding pitch ratios of $2.7,4.5$, and 6.5 range between $74-81 \%, 53-59 \%$, and $40-45 \%$ higher than the plain tube, respectively.

Figure 5 shows the comparisons of the temperature distribution of both smooth and enhanced tubes with STTs, CTTs, and plain tubes at a $R e$ of 14,100 at various cross sections $(x / D)$. In a tube having twisted tape inserts, in all geometries, the temperature is more equally distributed. Furthermore, as the twist pitch increases, the temperature distribution also shows a tendency towards homogeneous temperature distribution.


Figure 5. Contour plots of temperature at axial locations $x / D$ of 3.49, 48.95, 97.90, and 143.35 at $R e=14,100$ for (a)PT, (b) $y / W=2.7$ CTT, (c) $y / W=4.5$ CTT, (d) $y / W=6.5$ CTT, (e) $y / W=2.7$ STT, (f) $y / W=4.5$ STT, and (g) $y / W=6.5$ STT.

The temperature contours of both the CTTs and STTs display the same tendency for the corresponding twist ratios. Figure 6 shows the streamline in cross section under Re of 14,100. It is clear that, for the tubes with STTs and CTTs, an improved temperature distribution can be achieved, leading to more excellent temperature gradient compared to the smooth tube. The better temperature distribution leads to a higher temperature difference between the tube inlet and outlet, thereby improving the convective heat transfer coefficient. In addition, in the case of $y / W=2.7$ CTT, the highest temperature gradient and superior temperature distribution can be obtained over the other tube designs, thereby yielding the best performance for this geometry.


Figure 6. Streamline in cross sections at $R e=14,100$.
Figure 7 depicts the variation of friction factor $(f)$ with $R e$ for plain tube and three different twist pitch ratios of the CTTs and STTs. The $f$ value displays a decreasing trend with the increase in Re. Further, STTs provide a higher $f$ compared with the CTTs, for the corresponding pitch ratio. The $f$ values for the STTs and CTTs for the corresponding pitch ratios of $2.7,4.5$, and 6.5 range between 3.0-3.3, 2.3-2.5, and 1.7-2.0 times higher than the plain tube, respectively. Compared with the case of CTTs, the flow disturbance in the case of STTs increases the tangential velocity between the secondary flow and the tube wall surface. As expected, the twisted tape tubes with both the CTT and STT exhibit a sharper decline in $f$ compared with the plain tube, which is attributed to blockage and the subsequent decline in the flow's momentum by the twisted tape tube, as well as the pressure drop for the corresponding twisted tape tube.


Figure 7. Friction factor for various CTTs and STTs.
Figure 8 shows the comparison of velocity distributions of both smooth and enhanced tubes with the STTs, CTTs, and plain tube at a Re of 14,100 at various cross sections $(x / D)$. The plain tube domain reaches its maximum velocity at the center, thereby indicating a fully developed flow in these
locations. It is seen that the velocity is almost similar at all locations. It is clear that in the plain tube, the velocity near the walls is low, owing to the absence of the twisted tape. With the addition of the twisted tape inserts (both CTTs and STTs), a uniform distribution of the velocity is achieved due to the swirls generated by the twisted tape inserts. Compared with the plain tube, the tube fitted with the STT achieves higher velocity, owing to the increased velocity of the flow near the walls due to the swirls generated by the tape. The behavior of the STTs and CTTs is similar for the corresponding pitch ratios (Figures 4 and 5). It is expected that the insertion of the STT with square-cuts will create a new flow pattern. The working fluid flows through the square-cuts, and a new flow pattern is formed as an axial flow. The new flow pattern causes an increasingly random flow of the working fluid, thereby increasing the vorticity formation (due to the working fluid flowing through the square-cuts), which results in an increase in the heat transfer rate as shown in the Figure 4.


Figure 8. Contour plots of velocity in inner tube at axial locations $x / D$ of 3.49, 48.95, 97.90, and 143.35 at $R e=14,100$ for (a) PT, (b) $y / W=2.7$ CTT, (c) $y / W=4.5 \mathrm{CTT}$, (d) $y / W=6.5 \mathrm{CTT}$, (e) $y / W=2.7$ STT, (f) $y / W=4.5$ STT, and (g) $y / W=6.5$ STT.

The thermal performance $(\eta)$ with $R e$ for a plain tube and three different twist pitch ratios of the CTTs and STTs is presented in Figure 9. The thermal performance of the enhanced tube heat exchanger can be determined as the ratio of both heat transfer and friction factor characteristics of the enhanced tube to those of the basic device, which only has the basic dimensions without design enhancements [36]. $\eta$ can be estimated as follows:

$$
\begin{equation*}
\eta=\left.\frac{h_{t}}{h_{o}}\right|_{p p}=\left.\frac{N u_{t}}{N u_{o}}\right|_{p p}=\left(\frac{N u_{t}}{N u_{o}}\right)\left(\frac{f_{t}}{f_{0}}\right)^{-\frac{1}{3}} \tag{11}
\end{equation*}
$$

As shown in Figure 9, all the results of the plain tube, CTTs, and STTs demonstrate a similar tendency. $\eta$ decreases with the increase in Re. Both the CTT and STT are more effective in disrupting the flow at lower Re. $\eta$ values for the STTs and CTTs for the corresponding pitch ratios of 2.7, 4.5, and 6.5 range between 1.18-1.23, 1.11-1.13, and 1.06-1.09 times higher than those of the plain tube, respectively. The results of the thermal performance indicate that, the efforts to improve the heat transfer performance have yielded significant results, but with an increase in $f$. Therefore, the geometrical modification of the inserts for an enhanced tube is advantageous in offering practical
solutions for improving the thermal performance of heat exchangers. It is evident that the velocity distribution significantly depends on the local momentum of the working fluid due to the geometry of the enhanced tube, thereby affecting the thermal hydraulic characteristics (Figures 5 and 8). These findings can contribute to the study of heat transfer enhancement, in order to minimize the energy consumption in a compact heat exchanger.


Figure 9. Thermal performance for various CTTs and STTs.
In addition, as shown in Figures 4, 7 and 9, the experimental results from our previous work in Ref. [18] are provided for the correlations of $N u$, friction factor, and the pressure drop, for the corresponding $R e$, respectively. The experimental results are shown by solid circles, which have a geometry installed with CTT. From Figure 4, it is clear that the experimental results are in good agreement with the present results. Further, Figures 7 and 9 display a similar tendency for friction factor and thermal performance, respectively. There are small discrepancies between the experimental and numerical results due the differences in the twist ratio $(y / W)$ of the CTT. The twist ratio of 3.97 was used in the experiment, in this study [18]. Therefore, the numerical method used in this study can be considered potential to be used to study the thermal hydraulic performance of a turbulent single-phase flow inside an enhanced tube equipped with an STT insert.

## 4. Concluding Remarks

A numerical study of an enhanced tube employing the CTTs and STTs with various pitch ratios was performed. The important conclusions of this study are as follows:

- $\quad N u, f$, and $\eta$ of both the CTTs and STTs with various pitch ratios of the enhanced tube are higher compared to those of the plain tube. the decrease of the pitch ratio leads to the increase of $N u, f$, and $\eta$.
- STT with $y / W=2.7$ yields higher heat transfer rate, friction factor, and thermal performance factor.
- The highest increases in $N u$ and $f$ of the enhanced tube can reach $81 \%$ and 3.3 times greater than ones of the smooth tube, respectively.
- The thermal performance factor has been visualized and it can reach a value of 1.23.
- Based on both the temperature and velocity distributions at the cross sections, the heat transfer mechanism has been definitely evaluated.

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