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# Life Cycle Assessment of Classic and Innovative Batteries for Solar Home Systems in Europe

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**Abstract:** This paper presents an environmental sustainability assessment of residential user-scale energy systems, named solar home systems, encompassing their construction, operation, and end of life. The methodology adopted is composed of three steps, namely a design phase, a simulation of the solar home systems' performance and a life cycle assessment. The analysis aims to point out the main advantages, features, and challenges of lithium-ion batteries, considered as a benchmark, compared with other innovative devices. As the environmental sustainability of these systems is affected by the solar radiation intensity during the year, a sensitivity analysis is performed varying the latitude of the installation site in Europe. For each site, both isolated and grid-connected solar home systems have been compared considering also the national electricity mix. A general overview of the results shows that, regardless of the installation site, solid state nickel cobalt manganese and nickel cobalt aluminium lithium-ion batteries are the most suitable choices in terms of sustainability. Remarkably, other novel devices, like sodium-ion batteries, are already competitive with them and have great potential. With these batteries, the solar home systems' eco-profile is generally advantageous compared to the energy mix, especially in on-grid configurations, with some exceptions.

**Keywords:** energy storage; LCA; batteries; solar energy; photovoltaic; smart grids

## 1. Introduction

This work addresses the issue concerning the choice of the most suitable in terms of sustainability battery energy storage systems (BESSs) for specific applications, namely the so-called solar home systems (SHSs). These systems belong to a larger category of residential installations that allow energy users to produce and exchange energy with the grid, thus becoming prosumers [1], and share their management to create grid-connected or isolated communities and microgrids [2–4].

SHSs are composed of a PV system, a converter named charge controller (CC), an inverter (In) and a BESS. The choice of the battery is particularly complex because many factors are involved simultaneously and contribute to the environmental and energy performance: manufacturing processes, raw materials consumption, operative parameters, working conditions, and waste management are those that mainly affect the overall performance. Furthermore, the most sustainable solution is

intrinsically dependent on the geographical site, as one installation might not be the best one in a different context, or it could have a different effectiveness. For all these reasons, designing SHSs to be competitive with the national electricity mix can be challenging, especially if innovative technologies are considered. The aim of this work is to approach such an issue from a broader perspective that could support in the definition of the best BESSs for SHSs by evaluating their environmental performances and including a sensitivity analysis of the installation site.

Life cycle assessment (LCA) has a crucial role in the methodological approach presented in this paper because it allows to consider the whole life cycle of the SHS, from cradle to grave. LCA, standardized by the ISO family of rules [5,6], is one of the most recognized methods for environmental impact evaluation. The life cycle perspective of LCA allows to consider the raw material consumption and the emissions to the environment occurring during the whole life cycle of a product, process, or service. LCA has been widely used in the field of renewable energies whose greenhouse gases direct emissions might be null or, at least, be much more limited than for fossil fuels-based power systems. On the other hand, they may have remarkable environmental impacts due to their production and end of life disposal. For instance, the scientific literature provides examples of LCA applied to solar energy-based systems such as collectors [7] or traditional and novel PV systems [8–10].

Currently lithium-ion batteries (LIBs) represent the most mature storage devices on the market [11], but they still have some technical, environmental and economic drawbacks pushing scientific research to find alternative types of BESSs. Many LCA studies are available in the literature, most of them collected and harmonized in the work of Peters and Weil [11]. In this paper, the following batteries are considered: nickel cobalt aluminium (NCA) [12] nickel cobalt manganese (NCM) [13,14]; lithium manganese oxide (LMO) [15], lithium iron phosphate (LFP) [14,16] and lithium iron titanate (LTO) [12]. Recently, new types of LIBs have been designed like lithium manganese nickel oxide (LMNO), molybdenum-disulfide NCM (NCM-MoS<sub>2</sub>) and lithium cobalt phosphate (LCP). The eco-profile of such LIBs has been assessed by Cusenza et al. [17], Deng et al. [18] and Raugei and Winfield [19], respectively. Another interesting development in LIBs is the replacement of the liquid electrolyte with a solid one [20], thus moving towards solid state lithium-ion batteries (SSLIBs). Troy et al. [21] and Lastoskie and Dai [22] proposed an interesting environmental assessment of SSLIBs that showed them to be competitive with classic LIBs. Regardless of the electrode materials, LIBs are intrinsically affected by the availability of lithium that is quite limited [19]; moreover cobalt, used in the cathodes of most of LIBs to increase the energy density, is even more rare and expensive than lithium [23]. Indeed, lithium-cobalt oxide (LCO) batteries, whose LCA is performed by Grimsmo et al. [24], are the most widely used devices, but the impact of cobalt extraction in the Congo represents a major contribution to the overall environmental burden. For these reasons, research is focusing on the study of novel cobalt-free batteries working with the same principle of LIBs but replacing lithium-ions with sodium, magnesium or aluminium. The environmental assessment of sodium-ion batteries (SIBs) and aluminium-ion batteries (AIBs) has been performed by Peters et al. [25] and Delgado et al. [26], respectively. According to these studies SIBs already display good performance whereas AIBs are still at a laboratory level and far from industrial scale up. From the same perspective, other solutions to obtain lithium- and cobalt-free BESSs are sodium-nickel chloride batteries, named ZEBRA [27], and vanadium redox flow batteries (VRFBs). Some LCA studies [28,29] have demonstrated that these batteries have a very interesting potential to improve the environmental performance of stationary installations. Scientific and industrial research is focusing on high energy density batteries to make BESSs smaller and lighter: some of them have lithium metal as anodic material, like lithium-sulfur batteries (LiSBs) or lithium-air batteries. Environmental assessments of these devices have already been performed by Deng et al. [30] and Zackrisson et al. [31], who concluded that their potential is remarkable, but the fast degradation due to several ageing mechanisms at the moment hinders their diffusion in the market. The same kind of conclusions have been drawn by LCA studies of sodium sulphur [32], magnesium-sulphur [33] and zinc-air [34] batteries aiming to replace lithium.

The literature analysis shows that the environmental impact of batteries represents a very interesting research topic many authors have addressed. Nevertheless, all the abovementioned studies are performed at the components level and are focused on the production phase and, only in some cases, on the end of life stage of BESSs. The operation phase is usually neglected or modelled in a simplified way which does not really allow one to determine the effect of the BESS operative parameters on the results. Some detailed environmental analyses of BESSs applications do however exist and were reviewed by Tian et al. [35]. For instance, grid-connected SHSs economic and environmental feasibility, including LCA, have been assessed by Nagapurkar and Smith [36]. On the other hand, Wang et al. [37] analyzed a standalone battery system for an electric grid installed in Hong Kong. Solar systems assisted by batteries are also discussed by Longo et al. [38] who developed a new tool, based on LCA, to estimate the eco-profile of these systems. Kabakian et al. [39] compared a 1.8 kW PV system assisted by a BESS with the Lebanese electricity grid eco-profile underlining the substantive environmental merits of PV. All these studies at the system level are valuable but lack in analyzing how the different batteries can change the eco-profile of the system depending on the installation site.

Thus, it is possible to assert that there is a gap in the scientific literature concerning studies giving insights on how to choose the best battery to improve the environmental performance of SHSs. Ultimately, in the context highlighted by such a scientific study overview, comparative LCA studies about the effects of the components, in particular the batteries, on the overall system performances and eco-profiles are, to the best of our knowledge, not found in the literature. Indeed, this kind of analysis requires one to merge a detailed environmental assessment of batteries at the component level and a careful evaluation of the performances of SHSs depending on the batteries' operative parameters. In order to do this, we proposed a three-steps methodology in our previous papers [40,41] including the design, the operative parameter simulation and the LCA of SHSs equipped with LIBs in Italy. In this work, our approach is employed for its application to a larger number of case studies in several European countries. Moreover, a larger group of batteries is analyzed including LIBs and novel BESSs. Much effort has been done to extend the methodology, initially valid for LIBs, to be applicable to every BESS and thus investigate the differences among them. Remarkably, the improvement of the three-steps methodology [40,41] allowed us to perform the comparison of different batteries and installation sites for SHSs eco-profiles evaluation.

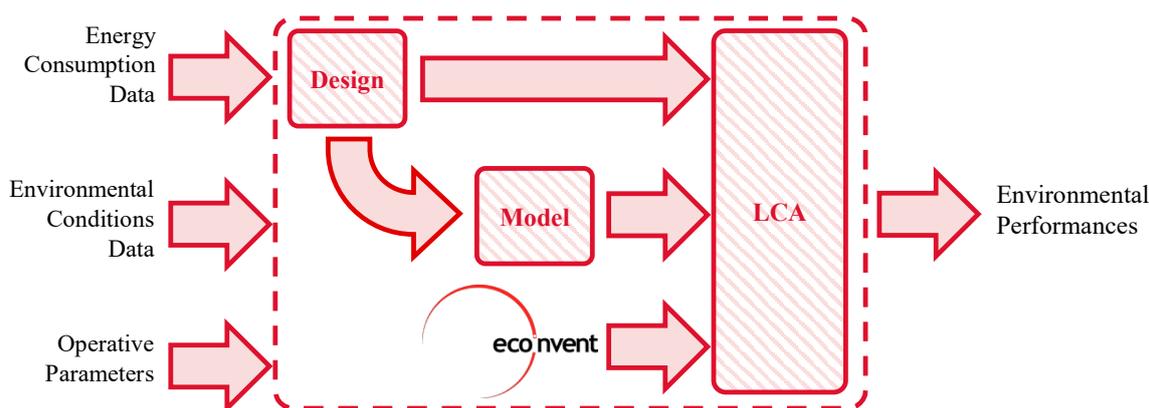
The remainder of this paper is organized as follows: in Section 2, we describe the methodology, in Section 3, we present the analyzed case studies. Finally, we discuss the results and our conclusions in Sections 4 and 5, respectively.

## 2. Methodology

As described in the Introduction, SHSs are composed of a PV plant, a BESS, an In and a CC. When SHSs are configured as isolated installations, a generator provides backup energy to the user whereas grid-connected SHSs can exchange energy with the electric utility [40]. The methodology used to evaluate the eco-profile of both types of SHSs is composed of three steps:

- The design phase, in which the calculation of the components' capacity is addressed.
- The modelling phase, which provides the dynamic simulation of the SHSs performances.
- The LCA for the SHSs environmental impact calculation.

A summary of BESSs is presented before the description of the abovementioned methodology steps and a flowchart illustrating such an approach is depicted in Figure 1.



**Figure 1.** Flowchart of the three-steps methodology implemented in this work.

### 2.1. Batteries Description

The operative parameters of the examined batteries are summarized in Table 1 which collects their construction materials, the energy density, the lifespan, the depth of discharge (DoD) and the efficiency.

LIBs are electrochemical devices where lithium-ions move from the anode to the cathode during discharge, and back when charging. Traditional LIBs include an organic liquid electrolyte (like ethylene carbonate or ethylene glycol dimethyl ether [42]) where lithium salts are dissolved. SSLIBs represent a development of classic LIBs where the liquid electrolyte is replaced by a solid crystalline one, namely LiPON, allowing one to double the energy density [22]. Thus, the energy density of the SSLIBs has been estimated multiplying with a factor of two the values of the corresponding LIBs. Several types of LIBs are available nowadays, differing in the electrode materials and consequently their energy density, efficiency and lifespan values [40].

Even though LIBs are the most diffused BESSs, several other batteries with different levels of maturity are available on the market. Based on the data availability in the literature, some alternative BESSs (aBESSs) have been selected to perform their environmental assessment in this work.

Peters' devices (SIBs) [25] work similarly to LIBs because sodium-ions are exchanged by the electrodes with the same mechanism of lithium-ions in LIBs; indeed they belong to the same category named metal-ion batteries [43]. Sodium ions move from a sodium nickel manganese magnesium titanium oxide (NMMT) cathode to a hard carbon anode through a liquid electrolyte where sodium hexafluorophosphate ( $\text{NaPF}_6$ ) is dissolved [25]. These batteries are studied in the perspective of replacing lithium with sodium, much more abundant on the Earth. Nevertheless, according to a recent scientific report published by Yusoff et al. [43], the effects of the different size of sodium-ions are a lower cyclability, a lower capacity (and consequently energy density) and a lower power rate. Indeed Table 1 shows that SIBs energy density and cyclic lifespan are respectively 102 Wh/kg and 2000 cycles whereas in LIBs they can be significantly higher. In the literature there is lack of information about SIBs' natural lifespan but, as Yusoff et al. [43] do not stress any difference for this parameter, the same value assumed by LIBs has been assumed.

Deng batteries (LiSBs) have metal lithium as anodic material whereas sulphur is present in the cathode mixed with a graphene structure [30]. They can reach a high energy density although the electrolyte is liquid and composed of a solution of lithium bistrifluoromethanesulfonimide (LiTFSI), dimethyl glycol (DME), dioxolane (DOL) and lithium nitrate ( $\text{LiNO}_3$ ). The main drawback of this battery chemistry is the very fast cyclic degradation due to several chemical and physical ageing mechanisms [30,44]. Few data are available about their natural lifespan because research is mainly focused on studying the cyclic degradation that is the dominant effect. Deng et al. [30] estimate that, similarly to LIBs, LiSBs lifespan can reach 10 years that is set as reference value for the natural lifespan.

**Table 1.** Batteries operative parameters <sup>(a)</sup>.

	LIBs/SSLIBs							aBESS			
	M-B (LFP) <sup>(1)</sup>	Zack (LFP) <sup>(2)</sup>	Bauer (LTO) <sup>(3)</sup>	Notter (LMO) <sup>(4)</sup>	Bauer (NCA) <sup>(5)</sup>	Eli (NCM) <sup>(6)</sup>	M-B (NCM) <sup>(7)</sup>	Peters (SIBs) <sup>(8)</sup>	Deng (LiSBs) <sup>(9)</sup>	Eco. (ZEBRA) <sup>(10)</sup>	Weber (VRFBs) <sup>(11)</sup>
Cathode	LiFePO <sub>4</sub> <sup>(b)</sup>	LiFePO <sub>4</sub>	LiFePO <sub>4</sub>	LiMn <sub>2</sub> O <sub>4</sub> <sup>(c)</sup>	LiNiCoAlO <sub>2</sub> <sup>(d)</sup>	LiNiMnCoO <sub>2</sub> <sup>(e)</sup>	LiNiMnCoO <sub>2</sub> <sup>(e)</sup>	NMMT	Graphene-sulfur composite	Nickel chloride	PAN
Anode	Graphite	Graphite	Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub> <sup>(f)</sup>	Graphite	Graphite	Graphite	Graphite	Hard carbon	Lithium metal	Sodium chloride	PAN
Electrolyte	LiPF <sub>6</sub> <sup>(g)</sup> LiPON <sup>(j)</sup> (SS)	LiCl <sup>(h)</sup> LiPON <sup>(j)</sup> (SS)	NaBF <sub>4</sub> <sup>(i)</sup> LiPON <sup>(j)</sup> (SS)	LiPF <sub>6</sub> <sup>(g)</sup> LiPON (SS)	NaBF <sub>4</sub> <sup>(i)</sup> LiPON (SS)	LiPF <sub>6</sub> <sup>(g)</sup> LiPON (SS)	LiPF <sub>6</sub> <sup>(g)</sup> LiPON (SS)	NaPF <sub>6</sub>	LiTFSI, DOL, DME, LiNO <sub>3</sub>	Sodium aluminium chloride	Vanadium, sulfuric acid, phosphoric acid, water
Energy Density [Wh/kg]	109.3 218.6 (SS)	82.9 165.8 (SS)	52.4 104.8 (SS)	116.1 232.2 (SS)	133.1 266.2 (SS)	130.3 260.6 (SS)	139.1 278.2 (SS)	102	220	116	28
Lifespan [Cycles]	6000	3000	10,000	1000	5000	2000	3000	2000	400	4500	-
Lifespan [years]	10	10	10	10	10	10	10	10	-	15	20
DoD	80%	80%	80%	80%	80%	80%	80%	80%	85%	80%	95%
Efficiency	90%	90%	90%	85%	90%	95%	90%	90%	85%	90%	75%

(a) Parameters taken from [11,25,26,29,30,45]; (b) lithium-iron phosphate; (c) lithium manganese oxide; (d) lithium nickel cobalt aluminum oxide; (e) lithium nickel cobalt manganese oxide; (f) lithium titanate oxide; (g) lithium hexafluorophosphate; (h) lithium chloride; (i) sodium tetrafluoroborate; (j) lithium phosphorous oxy-nitride; (1) LFP battery proposed by Majeau-Bettez et al. [14], (2) LFP battery proposed by Zackrisson et al. [16]; (3) LTO battery proposed by Bauer et al. [12]; (4) LMO battery proposed by Notter et al. [15]; (5) NCA battery proposed by Bauer et al. [12]; (6) NCM battery proposed by Ellingsen et al. [13]; (7) NCM battery proposed by Majeau-Bettez et al. [14]; (8) SIB proposed by Peters et al. [25]; (9) LiSB proposed by Deng et al. [30]; (10) ZEBRA battery proposed by Ecoinvent 3.4 [46]; (11) VRFB proposed by Weber et al. [29].

Eco (ZEBRA) [46] batteries contain sodium composites in the electrolyte and in the anode, whereas nickel represents the main cathodic material [38]. Differently from the others, these devices operate at high temperatures, over 270 °C [28], and therefore they require a heating system to be constantly in operation [45]. The cyclic lifespan and the energy density is comparable to some types of LIBs but the natural lifespan is longer [45]. Among the alternative batteries analyzed in this study, ZEBRA batteries present the highest maturity level.

Weber systems (VRFBs) [29] are significantly different from the other devices: they are flow batteries where two vanadium-based liquid electrolytes are stored in two storage tanks which determine the capacity of the battery. The liquids are pumped through a piping system to a stack where they are separated by a proton exchange membrane that, together with polyacrylonitrile (PAN) carbon felt electrodes, allows the development of the reaction; the surface of the membrane determines the power of the battery [29]. Therefore, the strength of VRFBs is the possibility to design separately the storage tanks (devoted to store energy) and the stack (devote to exchange power) according with the needs of the user. Moreover, it is possible to recycle the electrolyte completely and to achieve a very long lifespan. Indeed, the natural lifespan of the electrolyte is 20 years, that of the stack is 10 years whereas the cyclic ageing is negligible [29]. The main drawback of VRFBs is the very low energy density which might be solved finding new types of electrolytes in the future.

## 2.2. SHS Design

The design equations [40] applied to evaluate the PV power ( $P_{PV}$ ) and the BESSs nominal capacity ( $E_{BESS}$ ) for a daily energy storage are defined as follows (1) and (2):

$$P_{PV} = \frac{E_{Load, day}}{\eta_{el} \cdot h_{eq}} \quad (1)$$

$$E_{BESS} = \frac{E_{Load, day}}{DoD} \quad (2)$$

where  $E_{Load, day}$  is the daily energy consumption,  $\eta_{el}$  is the electric efficiency of the SHS set to 72% [40],  $h_{eq}$  is the minimum equivalent daily full power operation time (expressed as hours) of the PV system (estimated using the online tool PV-GIS [47]) and DoD is the depth of discharge (80%) [40]. The nominal voltage of the BESS ( $V$ ) is set to 48 V [40].

The role of the CC is to connect the PV system and the BESS guaranteeing a match among their electrical characteristics; the In has to provide to the user the maximum power required by the load ( $P_{load}^{max}$ ), evaluated analyzing the users demand profile in time [48]. To this scope, the size of the CC ( $P_{CC}$ ) and of the In ( $P_{In}$ ) can be defined (3) and (4). Considering the design of the VRFB, its power is not physically correlated to its capacity, thus the BESS is designed to work with a power rate of 0.5 h<sup>-1</sup>, typical of stationary applications [49] (5):

$$P_{CC} = P_{PV} \quad (3)$$

$$P_{In} = P_{load}^{max} \quad (4)$$

$$P_{VRFB} = 0.5 E_{BESS} \quad (5)$$

## 2.3. SHS Modelling

After the SHS is designed, its performances are estimated by a dynamic simulation model. A discretization of the time variable ( $t$ ) is necessary to perform the simulation, and a time step  $\Delta t = 1$  h is defined. The outputs of the simulation are the amounts of missing ( $E_{miss}$ ) and exceeding ( $E_{exc}$ ) energy during the BESS lifespan ( $L_{BESS}$ ). The SHS model is composed of three parts:

- The PV productivity profiles ( $P_{PV, t}$ ), calculated with PV-GIS [47].
- The power demand profiles ( $P_{load, t}$ ), provided by Quoilin et al. [48].

- The BESS model that uses  $P_{PV,t}$  and  $P_{load,t}$  as inputs to evaluate the missing ( $P_{miss}$ ) and exceeding ( $P_{exc}$ ) power of the SHSs.  $E_{miss}$  and  $E_{exc}$  are calculated integrating  $P_{miss}$  and  $P_{exc}$  in time and an ageing model allows to estimate  $L_{BESS}$ .

In our previous work [40] the BESS operation has been modelled using a Matlab/Simulink block only valid for LIBs [50]. Therefore, this model is not adequate to describe all the batteries considered in this study and, thus, a flexible BESS model has been implemented here using the parameters collected in Table 1.

The power flowing through the BESS during the charge ( $P_{BESS,t}^c$ ) and discharge ( $P_{BESS,t}^d$ ) phases is assessed by the following balances (6) and (7):

$$P_{BESS,t}^c = (\eta_{el} P_{PV,t} - P_{load,t}) \cdot \eta_{BESS,c} \quad (6)$$

$$P_{BESS,t}^d = \frac{(\eta_{el} P_{PV,t} - P_{load,t})}{\eta_{BESS,d}} \quad (7)$$

where  $\eta_{BESS,c}$  and  $\eta_{BESS,d}$  are the BESS charge and discharge efficiency values, both equal to the squared root of the overall Coulombic efficiency (Table 1). The actual power flowing through the BESS ( $P_{BESS,t}$ ) is equal to  $P_{BESS,t}^c$  during the charge phase ( $P_{BESS,t}^c > 0$ ) and to  $P_{BESS,t}^d$  during the discharge phase ( $P_{BESS,t}^d < 0$ ). Additionally, some constraints are necessary:

- if the battery capacity is totally full ( $SOC_{t-1} = 1$ ), the BESS cannot be furtherly charged and the exceeding power is exported to the grid or, in off-grid SHSs, it is dumped.
- if the battery capacity has reached the minimum level ( $SOC_{t-1} = 1 - DoD$ ), the BESS cannot be furtherly discharged and, in that case, the backup source intervenes.

The power rate ( $r_t$ ), representing the charge and discharge velocity [51], is defined as (8):

$$r_t = \frac{P_{BESS,t}}{E_{BESS}} \quad (8)$$

Every type of BESS has a maximum power rate allowed, but it will be demonstrated that it doesn't represent a limiting factor as usual in stationary applications [21,40,49]. At this point, the current BESS state of charge ( $SOC_t$ ) can be calculated using (9):

$$SOC_t = SOC_{t-1} + \frac{P_{BESS,t} \cdot \Delta t}{E_{BESS} \cdot SOH_t} \quad (9)$$

where the BESS state of health ( $SOH_t$ ) is assessed using an ageing model. Cardoso et al. [49] proposed a capacity fade model for the assessment of a generic battery using (10), evaluating the BESS capacity loss ( $Q_t$ ) as the sum of the cyclic ageing and the natural degradation.

$$Q_t = \frac{E_{BESS}^{ref}}{E_{BESS}} (\alpha T^2 + \beta T + \gamma) e^{(\delta T + \epsilon) r_t} \sum_t \frac{P_{BESS,t}^d}{V_{BESS}^{ref}} + \theta e^{-\frac{E_a}{RT}} \sqrt{t} \quad (10)$$

where:

- $r_t$  is the solution of (8).
- $E_{BESS}^{ref}$  is the capacity of a reference battery (712.9 Wh).
- $V_{BESS}^{ref}$  is the voltage of the reference battery (5 V).
- $E_a$  is the activation energy of the reaction of the reference battery (24,500 J · mol<sup>-1</sup>).
- $T$  is the cell temperature that, in SHSs application, can be set to a constant value (298 K for all the batteries [49] except for ZEBRA whose temperature is 543 K [46]).

- $R$  is the constant of gases.
- $\alpha, \beta, \gamma, \delta, \varepsilon, \theta$  are the ageing coefficients, calibrated to match with the values in Table 1 in nominal conditions ( $T = 298$  K and  $r_t = 1$  h<sup>-1</sup>).

The ageing parameters, calibrated grounding on the data provided by Cardoso et al. [49], are collected in Table 2.

**Table 2.** Ageing parameters of BESSs.

BESS	$\alpha$	$\beta$	$\gamma$	$\delta$	$\varepsilon$	$\theta$
	[Ah <sup>-1</sup> · K <sup>-2</sup> ]	[Ah <sup>-1</sup> · K <sup>-1</sup> ]	[Ah <sup>-1</sup> ]	[h K <sup>-1</sup> ]	[h]	[s <sup>-0.5</sup> ]
Bauer (LTO, SSLTO)	$2.95 \times 10^{-7}$	$-1.76 \times 10^{-4}$	$2.61 \times 10^{-2}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
Bauer (NCA, SSNCA)	$5.91 \times 10^{-7}$	$-3.51 \times 10^{-4}$	$5.23 \times 10^{-2}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
Eli (NCM, SSNCM)	$1.48 \times 10^{-6}$	$-8.78 \times 10^{-4}$	$1.31 \times 10^{-1}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
M-B (LFP, SSLFP)	$4.92 \times 10^{-7}$	$-2.93 \times 10^{-4}$	$4.35 \times 10^{-2}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
M-B (NCM, SSNCM)	$9.84 \times 10^{-7}$	$-5.85 \times 10^{-4}$	$8.71 \times 10^{-2}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
Notter (LMO, SSLMO)	$2.95 \times 10^{-6}$	$-1.76 \times 10^{-3}$	$2.61 \times 10^{-1}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
Zack (LFP, SSLFP)	$9.84 \times 10^{-7}$	$-5.85 \times 10^{-4}$	$8.71 \times 10^{-2}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
Peters (SIB)	$7.38 \times 10^{-6}$	$-4.39 \times 10^{-3}$	$6.53 \times 10^{-1}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
Deng (LiSB)	$3.04 \times 10^{-7}$	$-1.81 \times 10^{-4}$	$5.81 \times 10^{-2}$	$-3.11 \times 10^{-3}$	$2.35 \times 10^0$	$1.57 \times 10^1$
Eco. (ZEBRA)	$1.48 \times 10^{-6}$	$-8.78 \times 10^{-4}$	$1.31 \times 10^{-1}$	$-6.70 \times 10^{-3}$	$2.35 \times 10^0$	$1.93 \times 10^1$
Weber (VRFB)	$0.00 \times 10^0$	$0.00 \times 10^0$	$0.00 \times 10^0$	$0.00 \times 10^0$	$0.00 \times 10^0$	$1.36 \times 10^1$

Concluding,  $SOH_t$  is calculated using Equation (11):

$$SOH_t = 1 - \frac{Q_t}{100} \quad (11)$$

All these equations are implemented in Matlab/Simulink [52] and when the  $SOH_t$  is equal to 0.8, the simulation is stopped and  $L_{BESS}$  is calculated.

A further consideration must be done for VRFBs. Like every flow battery, the VRFBs electrolyte is pumped inside the cell consuming energy that is provided by the backup source. The power absorbed by the pump ( $P_{p,t}$ ), is calculated by (12) to overcome the pressure losses in the system ( $\Delta p_{tot,t}$ ) [53]:

$$P_{p,t} = \frac{q_t \cdot \Delta p_{tot,t}}{\eta_p} \quad (12)$$

where  $\eta_p$  is the efficiency of the pump (90%),  $\Delta p_{tot,t}$  can be calculated using well known fluid-dynamics equations and the electrolyte flow rate ( $q_t$ ) is calculated using Equation (13) [53].

$$q_t = f \frac{P_{BESS,t}}{V n F c} \quad (13)$$

where the oversizing factor  $f$  is set to 7.5,  $n$  is the number of electrons involved in the reaction (1 electron),  $F$  is the Faraday constant and  $c$  is the vanadium concentration (1.6 mg/L) [53].

#### 2.4. LCA

The last phase of the three-steps methodology is the implementation of the LCA. According to the ISO standards [5,6] four steps are necessary to perform correctly this analysis:

- Goal and scope definition: the objectives of the study are defined, thus the reference flow (RF) and the functional unit (FU) of the product system are set accordingly. Moreover, the system boundaries are drawn to choose which processes are included in the analysis and which ones are left outside.
- Life cycle inventory (LCI): all the input and output flows of matter and energy involved in the system boundaries are collected and quantified.

- Life cycle impact assessment (LCIA): in this step all the flows collected in the LCI are classified and multiplied for characterization factors to calculate the environmental impact indicators value.
- Interpretation: the results obtained should be carefully evaluated to point out possible improvements of the product system in accordance with the scope and goal of the assessment and, eventually, to modify and implement the LCA system model.

#### 2.4.1. Goal and Scope Definition

The goal of the study is estimating and comparing the environmental performances of several SHSs equipped with different types of BESSs to identify the most sustainable one. In this perspective, the effects of the installation site variation on the results are assessed through a sensitivity analysis. The comparison with the national electricity mixes allows us to estimate the SHSs environmental effectiveness in every country. The function of SHSs is producing useful electricity, therefore in off-grid systems the RF is equal to the user energy demand whereas in on-grid configurations it is the sum of the load and the electricity dispatched to the grid. In both cases the FU is 1 MWh. A cradle to grave approach encompassing the construction (CO), operation (OP) and end of life (EoL) of SHSs is implemented. The impact of the components' transportations to the installation sites have not been included to focus the attention only on the SHS site-specific performances.

#### 2.4.2. Life Cycle Inventory (LCI)

The LCI has been built using the Ecoinvent database v3.4 [46]. First of all, all the inventories have been modelled at a component level. Reproducible data for the CO of all the batteries are available in the scientific literature [11,25,29,30,44] except for SSLIBs. Therefore, it is necessary to convert LIBs to SSLIBs replacing the same amount of liquid electrolyte with LiPON, whose LCI is reported in Table 3.

**Table 3.** LCI for the LiPON electrolyte production.

Figure	Process	Amount	Unit
Inputs			
Heat	market for heat, district or industrial, natural gas—Europe without Switzerland	0.23	kWh
Hydrogen peroxide	market for hydrogen peroxide, without water, in 50% solution—GLO	2.28	kg
Lithium hydroxide	market for lithium hydroxide—GLO	1.60	kg
Outputs			
Lithium oxide	Lithium oxide production	1.00	kg
Inputs			
Ammonia	market for ammonia, liquid—RoW	0.52	kg
Phosphorus pentachloride	market for phosphorus pentachloride—GLO	3.84	kg
Outputs			
Triphosphorous pentanitride	triphosphorous pentanitride production	1.00	kg
Inputs			
Lithium oxide	Lithium oxide production	0.67	kg
Phosphorous pentoxide	market for phosphoric acid, industrial grade, without water, in 85% solution APOS, S—GLO	0.13	kg
Triphosphorous pentanitride	triphosphorous pentanitride production	0.20	kg
Heat	market for heat, district or industrial, natural gas—Europe without CH	2.96	kWh
Outputs			
LiPON	LiPON production	1	kg

According to Senevirathne et al. [20], LiPON precursors are lithium oxide, phosphorous pentoxide and triphosphorous pentanitride with a mass ratio 1 : 0.2 : 0.3.

- Lithium oxide is prepared by thermal decomposition of lithium peroxide that, on its turn, is produced with the reaction of hydrogen peroxide and lithium hydroxide [54] consuming 25.8 kJ/mol [54].
- Phosphorous pentoxide inventory has been approximated to phosphoric acid having a similar structure.
- Triphosphorous pentanitride is prepared from ammonia and phosphorus pentachloride [54].

Furthermore, LiPON powder is heated for 10 h with a temperature rate of 5 °C/min [20]; the energy consumption for the production of 1 kg of LiPON is estimated considering lithium powder specific heat as a proxy (0.85 cal/g/K) [55].

The inventories of SIBs, VRFBs and LiSBs have been faithfully reproduced using detailed LCIs available in the literature [25,29,30] whereas a complete LCI for ZEBRA batteries is available in Ecoinvent v 3.4 (market for battery, NaCl—GLO) [46].

Deng et al. [30] and Weber et al. [29] describe the EoL inventory for LiSBs and VRFBs as well as the CO. Contrarily, LIBs waste treatment is not considered by Peters and Weil [11], but Huang et al. [56] clearly describes that each part of these BESSs can be recycled with an efficiency of about 90%. During the EoL, the battery pack is disassembled and then, after a thermal treatment for the evaporation of the liquid electrolyte, the main CO materials can be recovered: a pyrometallurgical process is necessary if cobalt is present in the battery, otherwise a hydrometallurgical process is preferred. On the other hand, plastic materials and LiPON are supposed to be incinerated. Therefore, after the evaluation of the mass contribution of each part of the battery pack, the inventory for LIBs and SSLIBs waste treatment has been modeled (Table 4) including the recovered materials. The same approach has been used also for Peters (SIB) EoL.

**Table 4.** LIBs, SSLIBs and Peters (SIB) inventory for EoL.

	Bauer (LTO)	Bauer (NCA)	Eli (NCM)	M-B (LFP)	M-B (NCM)	Notter (LMO)	Zack (LFP)	Peters (SIBs)		
Inputs										
Waste BESS									1	kg
Treatment of used Li-ion battery, hydrometallurgical GLO	0.49	0.00	0.00	0.5	0.00	0.61	0.53	0.47	kg	
Treatment of used Li-ion battery, pyrometallurgical GLO	0.00	0.52	0.6	0.00	0.5	0.00	0.00	0.00	kg	
Market for hazardous waste, for incineration Europe without CH	0.44	0.4	0.35	0.41	0.41	0.39	0.39	0.14	kg	
Market for waste electric and electronic equipment GLO	0.05	0.05	0.05	0.05	0.05	0.05	0.05	0.06	kg	
Market for scrap steel—Europe without CH	0.02	0.02	0.02	0.02	0.02	0.02	0.02	0.35	kg	
Market for inert waste, for final disposal RoW	0.23	0.14	0.14	0.26	0.15	0.16	0.30	0.14	kg	
Market for diesel, burned in building machine GLO									0.1	MJ
Market for electricity, medium voltage Europe without CH									0.01	kWh
Outputs (Avoided Products)										
Market for lithium hexafluorophosphate GLO	19 (l) 0 (s)	15 (l) 0 (s)	13 (s) 0 (s)	16 (l) 0 (s)	16 (l) 0 (s)	15 (l) 0 (s)	16 (l) 0 (s)	0	mg	
Sodium hexafluorophosphate production	0	0	0	0	0	0	0	12	mg	
Market for lithium GLO	10	8	9	12	8	6	15	20	mg	
Market for sodium GLO	0	0	0	0	0	0	0	3	mg	
Market for cobalt GLO	0	67	75	0	70	0	0	0	mg	
Market for copper GLO	9	125	179	116	116	185	49	0	mg	
Market for aluminium scrap, new RER	107	94	46	55	55	115	25	54	mg	
Market for nickel, 99.5% GLO	0	67	75	0	70	0	0	8	mg	
Market for manganese GLO	0	0	70	0	65	101	0	76	mg	
Market for steel, unalloyed GLO	0	0	0	0	0	0	0	308	mg	
Market for iron ore, beneficiated, 65% Fe GLO	79	0	0	95	0	0	119	0	mg	
Market for titanium, primary GLO	167	0	0	0	0	0	0	7	mg	
Market for graphite GLO	0	148	121	94	111	162	134	210	mg	

Moving to the system level, a complete LCI of the SHS valid for all the installation sites is collected in Table 5. The PV system and the wires are supposed to be recycled (with efficiency 90%), whereas the plastic materials are incinerated; the EoL of converters and electronics (like the In and CC) are modeled using a specific Ecoinvent [46] process.

Table 5. LCI of the SHS.

Process	Amount	Unit	Description
Inputs			
Market for photovoltaic slanted-roof installation, 3 kWp, single-Si, panel, mounted, on roof—GLO (inverter considered separately)	$\frac{P_{PV}}{3} \frac{L_{SHS}}{L_{PV}}$	items	CO of the PV system, mounting system; the In has been excluded.
Market for cable, unspecified cable, unspecified—GLO	$0.1 \frac{P_{PV}}{0.17} \frac{L_{SHS}}{L_w}$	kg	CO of cables for a 0.17 kW/m <sup>2</sup> PV system [57].
Market for tube insulation, elastomere—GLO	$0.06 \frac{P_{PV}}{0.17} \frac{L_{SHS}}{L_w}$	kg	CO of plastic wires coating for a 0.17 kW/m <sup>2</sup> PV system [57].
Market for inverter, 2.5kW—GLO	$\frac{P_{In}}{2.5} \frac{L_{SHS}}{L_{In}}$	items	-
Market for charger, electric passenger car—GLO	$1.53 P_{CC} \frac{L_{SHS}}{L_{CC}}$	kg	CO of a DC/DC converter weighting 1.53 kg/kW [58].
BESS	$E_{BESS} \frac{L_{SHS}}{L_{BESS}}$	kWh	CO of the BESS [25,29,30,42,44].
VRFB stack	$10.02 P_{VRFB} \frac{L_{PV}}{L_s}$	kg	In case of VRFB [29].
VRFB periphery	$5.13 P_{VRFB} \frac{L_{SHS}}{L_p}$	kg	In case of VRFB [29].
Market for electricity, low voltage	$E_{miss} \frac{L_{SHS}}{L_{BESS}}$	MWh	In case of grid-connected SHSs.
Market for diesel, burned in diesel-electric generating set, 18.5kW—GLO	$E_{miss} \frac{L_{SHS}}{L_{BESS}}$	MWh	In case of off-grid SHSs.
Market for waste electric wiring—GLO	$-0.1 \frac{P_{PV}}{0.17} \frac{L_{SHS}}{L_w} \cdot 10\%$	kg	EoL of cables for a 0.17 kW/m <sup>2</sup> PV system supposing 90% recycling efficiency [57].
Market for used cable—GLO	$-0.1 \frac{P_{PV}}{0.17} \frac{L_{SHS}}{L_w} \cdot 90\%$	kg	EoL of cables for a 0.17 kW/m <sup>2</sup> PV system supposing 90% recycling efficiency [57].
Market for waste wire plastic—GLO	$-0.06 \frac{P_{PV}}{0.17} \frac{L_{SHS}}{L_w}$	kg	EoL of plastic wires coating for a 0.17 kW/m <sup>2</sup> PV system [57].
Market for waste electric and electronic equipment—GLO	$-1.53 P_{CC} \frac{L_{SHS}}{L_{CC}}$	kg	EoL of a DC/DC converter weighting 1.53 kg/kW [40,58].
Market for waste electric and electronic equipment—GLO	$-4.37 P_{In} \frac{L_{SHS}}{L_{In}}$	kg	CO of a DC/AC converter weighting 4.37 kg/kW [40,59].
Market for auxiliary heating unit, electric, 5kW—GLO	$0.001 E_{ZE BRA} \frac{L_{SHS}}{L_h}$	items	Number of electric heaters considering an energy supply of 6.67W per kWh of capacity [46]
Outputs			
Electricity (RF)	$(E_{load} + E_{exc}) \frac{L_{SHS}}{L_{BESS}}$	MWh	In case of grid-connected SHS.
	$E_{load} \frac{L_{SHS}}{L_{BESS}}$	MWh	In case of off-grid SHS.
Exhausted BESS, waste treatment	$E_{BESS} \frac{L_{SHS}}{L_{BESS}}$	kWh	CO of a DC/AC converter weighting 4.37 kg/kW [40,59].
Exhausted PV, waste treatment	$4.29 P_{PV} \frac{L_{SHS}}{L_{PV}}$	kg	EoL of PV modules weighting 4.29 kg/kW [40,60,61].
Market for cable, unspecified—GLO	$0.1 \frac{P_{PV}}{0.17} \frac{L_{SHS}}{L_{SHS}} \cdot 90\%$	kg	Avoided product, from cables recycling.

A complete LCI is provided as Supplementary Materials. The lifespan of the SHS ( $L_{SHS}$ ) is set to 25 years and responds to that of the most long-living component (the PV plant) of the system. All the components lifespan values are collected in Table 6.

**Table 6.** Expected lifespan of the components.

Component		Lifespan	Unit	
PV	$L_{PV}$	25	yr	[62]
BESS	$L_{BESS}$	-	yr	[62]
In	$L_{In}$	10	yr	[62]
CC	$L_{CC}$	11	yr	[62]
Wiring	$L_w$	10	yr	[62]
VRFB stack	$L_s$	10	yr	[29]
VRFB periphery	$L_p$	10	yr	[29]
ZEBRA battery heater	$L_h$	10	yr	[45]

### 2.4.3. Life Cycle Impact Assessment (LCIA)

In this work the ReCiPe Endpoint (H) 2016 method, considering 17 impact categories with weighting set Europe H/A person/year specifically calibrated for the European context, is employed. LCIA results have been characterized both at the midpoint and endpoint level. The further aggregation of the endpoint results in single scores, measured as eco-points per MWh (Pts/MWh) allows an effective overview of the global environmental performances of the SHSs and a more concise discussion. For instance, fossil fuels based power systems may be concerned mostly about global warming potential and fossil resources depletion whereas PV or BESSs metals depletion may be more reasonable [62].

## 3. Case Studies

In this section, the above described three-steps methodology will be applied to some case studies. Different from our previous work [40], where a SHS was presumed to be installed in Siena (central Italy), this work is focused on the assessment of the SHSs eco-profile working at different installation sites [62]. This allows to evaluate how the SHS environmental performances respond to different operative conditions and to estimate its effectiveness with respect to the national electricity mixes. Eight different European countries, already considered by Quoilin et al. [48] for a statistic analysis of SHS energy consumption, have been selected for the analysis. To assess the environmental conditions of the installation sites, each country is represented by the respective capital city. The installation sites are the following: Denmark (DK)—Copenhagen, Spain (ES)—Madrid, France (FR)—Paris, Greece (GR)—Athens, Hungary (HU)—Budapest, Italy (IT)—Rome, Portugal (PT)—Lisbon and Romania (RO)—Bucharest.

According to the procedure described in Section 2, the design parameters need to be defined. DoD and  $\eta_{el}$  have already been specified in Section 2 and they don't depend on the installation site; contrarily,  $E_{Load, day}$  and  $h_{eq}$  are different and their values are collected in Table 7. Their estimate is based on the daily average energy consumption of a family composed of three people [63] and PV-GIS [47].

**Table 7.** Input data for the design of the SHSs in several countries.

Parameter	DK	ES	FR	GR	HU	IT	PT	RO
$E_{Load, day}$	5.4	4.5	7.2	5.6	3.3	3.2	3.8	1.8
$h_{eq}$	0.7	3.3	1.2	2.9	1.0	2.8	3.3	1.6

Concerning the modelling phase, the productivity profile of the PV plant, whose configuration is defined in the design phase, has been assessed using PV-GIS [47]. Furthermore, among the power demand profiles proposed by Quoilin et al. [48], the one whose integral is the closest to average energy

consumption value over one year [63] has been chosen and scaled proportionally to match exactly with that value. At the beginning of the simulation, the BESS is supposed to be totally charged and to be installed in a controlled environment having a temperature of 25 °C.

## 4. Results and Discussion

### 4.1. Design Phase Results

The outputs of the design phase are the SHSs components capacity values, namely  $P_{PV}$ ,  $P_{In}$ ,  $P_{CC}$  and  $E_{BESS}$ , that are collected in Table 8 for every installation site.

**Table 8.** Results of the design phase.

	$P_{PV}$ [kW]	$P_{In}$ [kW]	$P_{CC}$ [kW]	$E_{BESS}$ [kWh]		
				LIBs, SSLIBs, SIBs, ZEBRA	LiSBs	VRFBs
DK	32.03	4.53	32.03	18.53	17.44	17.61
ES	4.33	2.55	4.33	15.41	14.51	12.98
FR	16.86	17.44	16.86	24.54	23.10	20.67
GR	6.52	5.64	6.52	19.05	17.93	16.04
HU	8.22	2.21	8.22	11.45	10.77	9.64
IT	3.82	3.56	3.82	10.89	10.25	9.17
PT	4.27	4.43	4.27	13.00	12.24	10.95
RO	4.01	1.55	4.01	6.27	5.90	5.28

Analyzing the results in Table 8, it is possible to observe that large PV systems are required in DK and FR, as results of the combination of low solar radiation and high energy consumption (Table 7). Contrarily, smaller installations are required where the solar irradiance is elevated (IT, ES, PT) or the energy consumption is low (RO). As a consequence of the high peak power, in FR and DK the use of a large size In is required. Concerning the BESS, the size depends on the battery type and particularly on the DoD (Table 1): a big difference among the installation sites exists in relation to the different energy demand.

### 4.2. Modelling Phase Results

In this subsection the results of the modelling phase are described and discussed: the SHSs designed in the first step of the analysis are modelled and their performances are simulated in order to calculate  $L_{BESS}$ ,  $E_{miss}$  and  $E_{exc}$ . These results have been evaluated for each battery type and every installation site. Table 9 summarizes the results collecting the maximum and minimum values assumed by the model outputs. The lifespan of the VRFB is not present in Table 9 because, according to the assumptions used to model the ageing, it is equal to 20 years in any case. A full summary of the modelling phase results is provided as Supplementary Materials.

**Table 9.** Results of the modelling phase, minimum and maximum values, excluding the lifespan of VRFB.

	$L_{BESS}$ [yr]				$E_{miss}$ [MWh]				$E_{exc}$ [MWh]			
	Min	Deng (LiSB)		Max	Min	EII (NCM)		Max	Min	Weber (VRFB)		Max
DK	1.63	Deng (LiSB)	8.31	Eco. (ZEBRA)	11.31	EII (NCM)	13.93	Weber (VRFB)	337.73	Deng (LiSBs)	361.76	Peters (SIB)
ES	1.89	Deng (LiSB)	8.95	Eco. (ZEBRA)	7.30	EII (NCM)	13.02	Deng (LiSBs)	6.21	Weber (VRFB)	19.28	Deng (LiSBs)
FR	1.59	Deng (LiSB)	8.13	Eco. (ZEBRA)	8.30	EII (NCM)	11.67	Notter (LMO)	66.55	Notter (LMO)	103.48	M-B (NCM)
GR	1.86	Deng (LiSB)	8.86	Eco. (ZEBRA)	10.16	EII (NCM)	13.54	Weber (VRFB)	26.74	Weber (VRFB)	36.24	EII (NCM)
HU	1.72	Deng (LiSB)	8.52	Eco. (ZEBRA)	3.64	EII (NCM)	4.90	Weber (VRFB)	62.16	Weber (VRFB)	75.35	EII (NCM)
IT	1.97	Deng (LiSB)	9.06	Eco. (ZEBRA)	5.75	EII (NCM)	8.31	Weber (VRFB)	9.60	Weber (VRFB)	13.64	EII (NCM)
PT	1.71	Deng (LiSB)	8.52	Eco. (ZEBRA)	4.45	EII (NCM)	6.31	Weber (VRFB)	11.23	Weber (VRFB)	16.57	EII (NCM)
RO	1.86	Deng (LiSB)	8.88	Eco. (ZEBRA)	2.93	EII (NCM)	3.67	Weber (VRFB)	29.86	Weber (VRFB)	34.14	EII (NCM)

As expected, Deng batteries (LiSBs) have the shortest lifespan among the considered BESSs because of the low number of cycles that can be performed; contrarily, ZEBRA batteries result to

have the longest lifespan thanks to their long calendar life. For these reasons, the most and the less long-living batteries are the same regardless of the installation site. Nevertheless, their lifetime values can be slightly different; indeed, the different operative power rates, determined by the combination of the PV productivity and load profiles, can stress the BESS differently in each country.

Focusing on the energy flows evaluation, generally the use of Weber devices (VRFB) requires more backup energy than the others and have the lowest amount of surplus energy. This is due to the low efficiency of this BESS (Table 1) and to the power demand of the pumps. Contrarily EII batteries (NCM), thanks to their high efficiency, require less backup energy than the others, whereas the surplus energy is the most elevated. Nevertheless, there are some exceptions; indeed, certain combinations of power production, demand, and state of health of the battery can change the ranking (like in DK, ES and FR).

Comparing the installation sites, remarkable variations in terms of imported and exported energy exist as effect of the different sizes of the SHSs components and of the seasonal distribution of the solar radiation. Indeed, in southern installation sites, the solar radiation is more constant than in northern Europe, where variability is higher. Therefore, in FR and DK there is a remarkable difference between the summer and the winter in terms of PV productivity and, as the systems are designed for winter conditions, the missing and surplus energy are in respect to an optimum balance, higher than in the other sites.

Another piece of information provided by the simulation model is the operative BESS power rate that, as assumed preliminarily, is not a limiting factor as the maximum values are about  $0.35 \text{ h}^{-1}$ . Indeed, all the BESSs can reach maximum rates of at least  $0.7 \text{ h}^{-1}$  [64] whereas VRFBs are designed to reach  $0.5 \text{ h}^{-1}$ .

#### 4.3. LCA Results

In this section the results of the environmental assessment are illustrated: first the results will be depicted using midpoint indicators and then as single score impact values summarizing all the 17 impact categories proposed by ReCiPe for every SHSs and every installation site.

To provide a synthetic description of SHSs midpoint environmental performances, their eco-profiles will be focusing on a single installation site and three midpoint indicators. Similarly to our previous paper [40], Italy has been selected as reference location for SHSs whereas those indicators representing the highest contributions to the total environmental impact have been chosen: climate change, human toxicity and fossil fuel depletion.

The climate change indicator represents the amount of greenhouse gases emitted during SHSs' life cycles expressed as carbon dioxide equivalents ( $\text{kgCO}_2\text{eq/MWh}$ ) and is illustrated in Figure 2.

The results underline that installing EII (SSNCM) batteries allows one to minimize the climate changes burden: in on-grid systems, 61% of this burden is due to the energy embedded in the PV panels production, whereas the BESS accounts for 15% of the total. The impact of off-grid systems is clearly higher than grid-connected ones because of the contribution of the backup energy that increases from 15% to 30% whether the grid is replaced by a diesel generator. Contrarily Deng batteries (LiSBs) are by far the most impactful BESS because of their very short lifespan, indeed in both configurations it represents more than 70% of the total contribution.

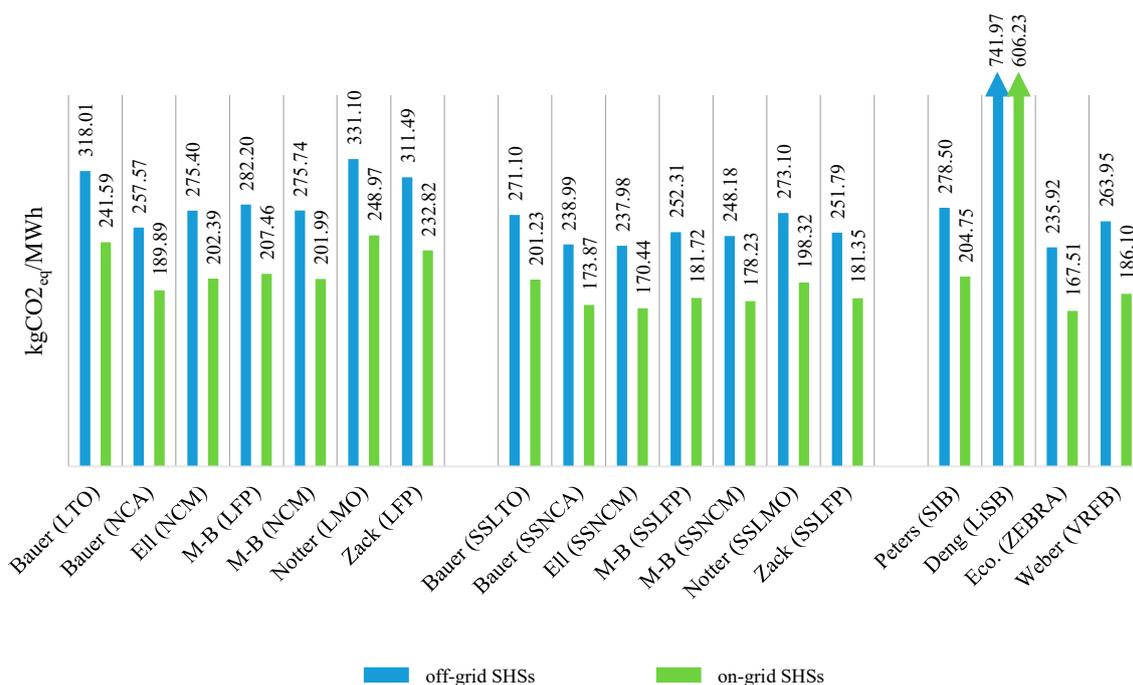


Figure 2. LCA impact values of SHSs in Italy for the climate change indicator.

Concerning the human toxicity, measured as equivalent 1,4-dichlorobenzene (kg 1,4-DB/MWh), similar considerations can be made: Figure 3 shows that M-B (SSNCM) are the most sustainable choice for this category. Like in the discussion of climate change indicator, the PV system is the main factor responsible for this burden accounting for about 50% of the total in both SHS configurations. Recycling copper and other metals is fundamental to lower the BESS from 30% to 10% of the total human toxicity impact. Also concerning this indicator, Deng batteries (LiSBs) have the worst eco-profile and their contribution to the SHS impact is higher than 60%.

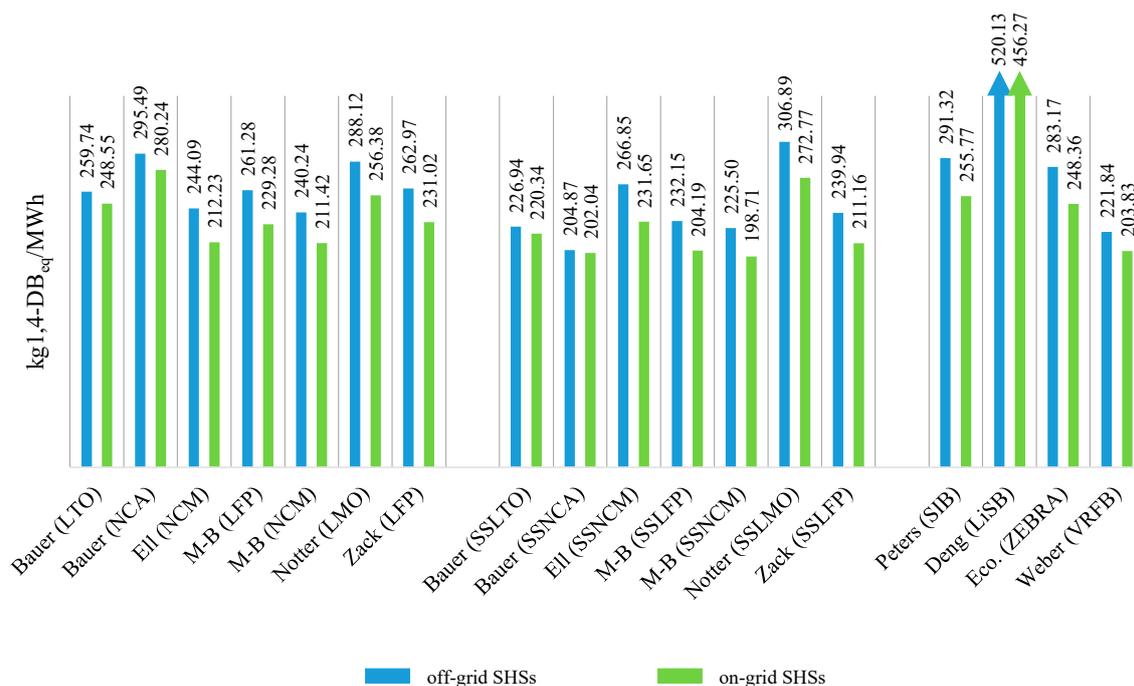


Figure 3. LCA impact values of SHSs in Italy for Human Toxicity indicator.

The last considered midpoint indicator is the fossil-fuel depletion: it is important to stress that SHSs' impact on fossil resources is more than on the metal because of the positive effects of BESS recycling. This impact category is evaluated as the equivalent amount of oil consumed over the product system life cycle (kgOil<sub>eq</sub>/MWh) and the results are illustrated in Figure 4.

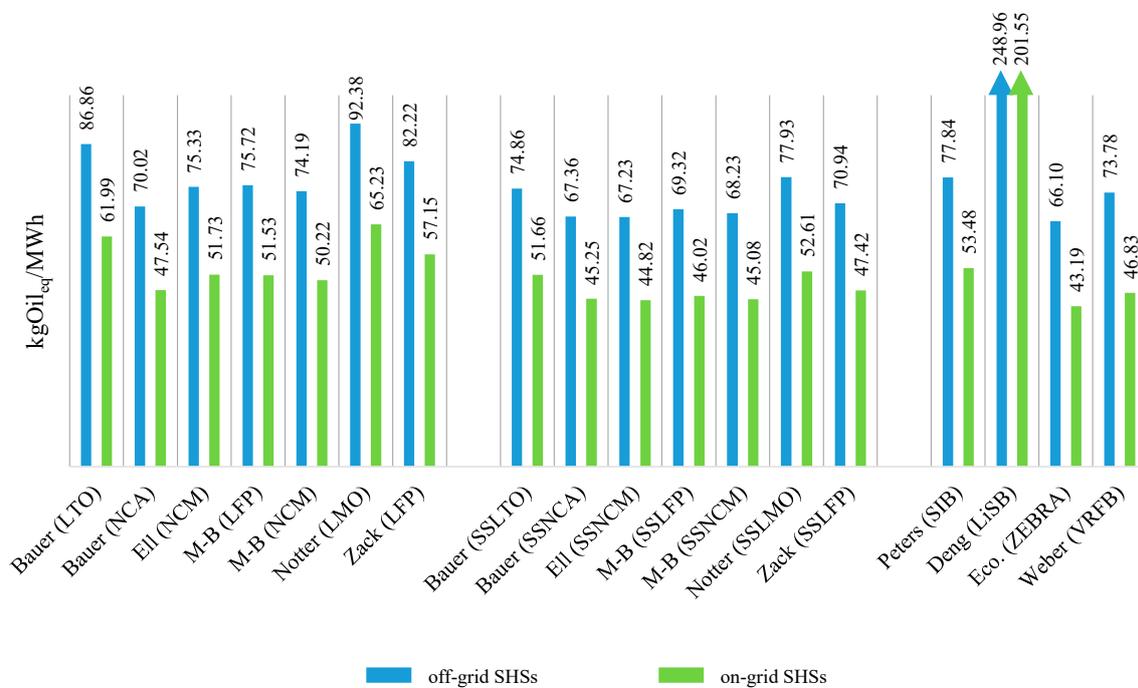


Figure 4. LCA impact values of SHSs in Italy for the fossil depletion indicator.

The most sustainable battery type is, in this case, Eco. (ZEBRA): its percentage contribution is 8% in off-grid systems and 10% in on-grid ones. In both configurations the PV system production represents the main feature responsible for this indicator as the percentage burden is 47% in off-grid and 60% in on-grid SHSs. The remarkable impact difference between these arrangements is due to the backup energy, representing 37% of the total impact whether provided by diesel and 18% in case on off-grid systems. The same considerations concerning Deng devices' (LiSBs) effects on climate changes and human toxicity are valid for fossil-fuel depletion as good and the BESS percentage burden is over 70% of the SHS one. The above midpoint indicators evaluated for all the other installation sites are provided as Supplementary Materials.

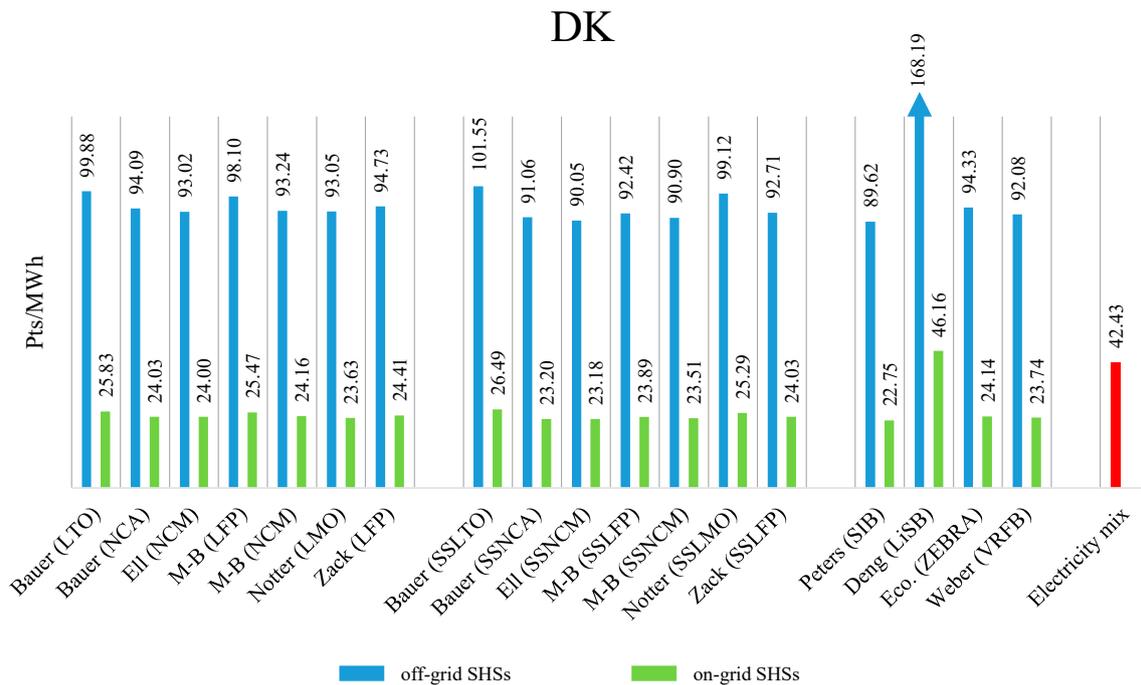
Differently from midpoint indicators, single score results allow a global comparison of all the SHSs. Table 10 collects the most sustainable SHSs for each battery group (LIBs, SSLIBs and aBESSs), Table 11 shows the contribution analysis of the components and Figures 5–12 provide further details about all the SHSs. Indeed, the environmental impact of all the batteries has been depicted together with the corresponding national electricity mix for an easy and immediate comparison. Both on-grid and off-grid configurations are reported. The red columns represent the environmental impacts of the national electricity mixes.

**Table 10.** LCIA results of the most sustainable batteries by categories and by installation sites.

	Best SHS, with LIBs [Pts/MWh]		Best SHS, with SSLIBs [Pts/MWh]			Best SHS, with aBESS [Pts/MWh]			Mix [Pts/MWh]	
	On-Grid	Off-Grid	On-Grid	On-Grid	Off-Grid	BESS	On-Grid	On-Grid		BESS
DK	24.00	93.02		23.18	90.05		22.75	89.62	Peters (SIB)	42.43
ES	19.24	26.39		16.76	23.63		18.78	27.90	Weber (VRFB)	37.45
FR	26.82	47.25		24.87	44.18		26.31	45.84	Weber (VRFB)	7.58
GR	24.59	31.10	Eil	22.40	28.34	Eil	25.99	31.13	Weber (VRFB)	112.96
HU	21.55	43.56	(NCM)	20.04	40.68	(SSNCM)	22.15	44.11	Peters (SIB)	55.36
IT	22.40	31.51		20.11	28.83		22.28	32.59	Weber (VRFB)	41.56
PT	20.95	28.12		18.50	25.23		20.02	27.36	Weber (VRFB)	39.53
RO	22.32	42.65		20.75	39.91		22.67	46.36	Weber (VRFB)	56.83

**Table 11.** Components contribution analysis of the most sustainable SHSs by categories and by installation sites.

	PV		BESS		In		CC		$E_{exc}$	
	On-Grid	Off-Grid	On-Grid	Off-Grid	On-Grid	Off-Grid	On-Grid	Off-Grid	On-Grid	Off-Grid
DK	83.24%	77.63%	9.76%	9.11%	2.46%	2.30%	0.29%	0.27%	4.25%	10.69%
ES	60.70%	47.86%	13.39%	10.57%	7.49%	5.90%	5.37%	4.24%	13.05%	31.43%
FR	70.50%	45.14%	7.11%	6.31%	15.25%	13.54%	6.24%	5.54%	0.90%	29.47%
GR	48.79%	48.61%	8.86%	8.83%	8.82%	8.79%	4.32%	4.30%	29.21%	29.47%
HU	75.85%	71.06%	6.85%	6.41%	4.26%	3.99%	6.71%	6.29%	6.33%	12.25%
IT	59.93%	48.99%	10.33%	8.44%	11.69%	9.55%	5.30%	4.34%	12.75%	28.68%
PT	60.84%	52.38%	12.04%	10.37%	13.21%	11.38%	5.39%	4.64%	8.52%	21.23%
RO	71.04%	64.43%	6.83%	6.20%	5.77%	5.24%	6.29%	5.73%	10.07%	18.40%



**Figure 5.** LCA impact values of SHSs in Denmark as single scores.

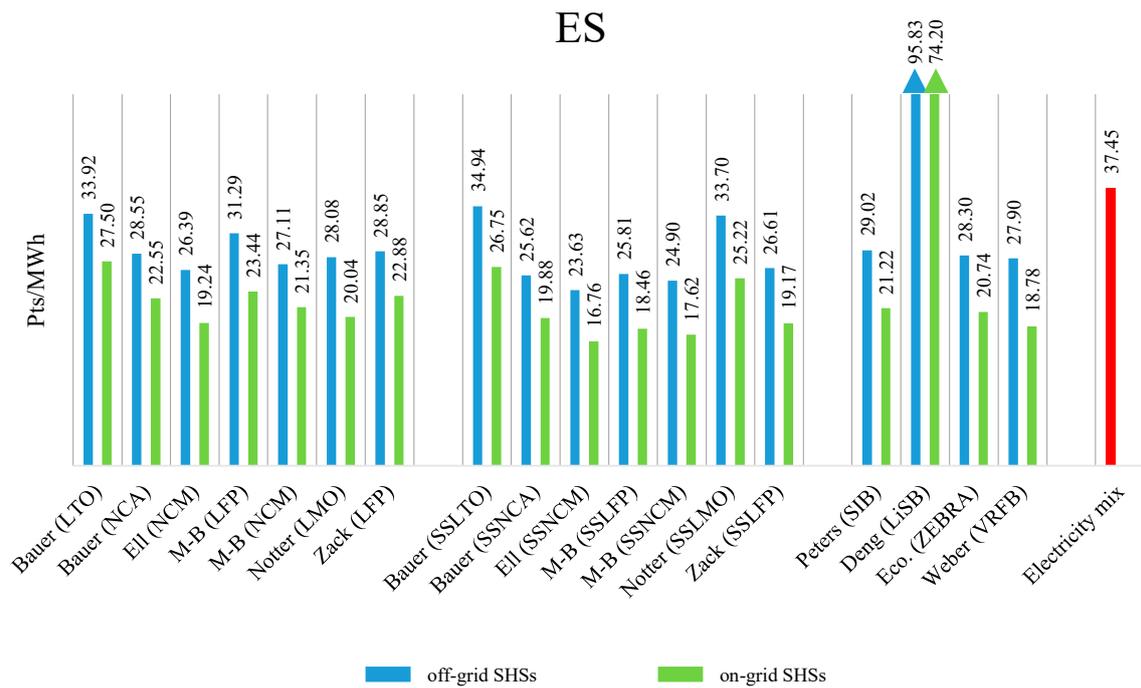


Figure 6. LCA impact values of SHSs in Spain as single scores.

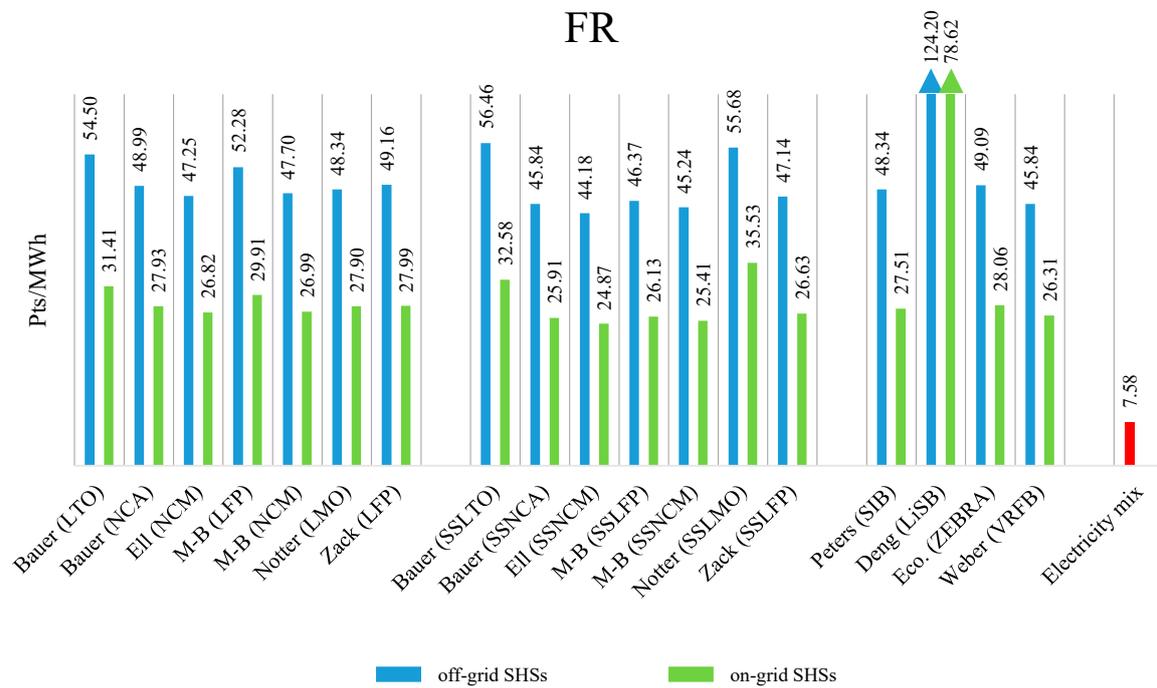


Figure 7. LCA impact values of SHSs in France as single scores.

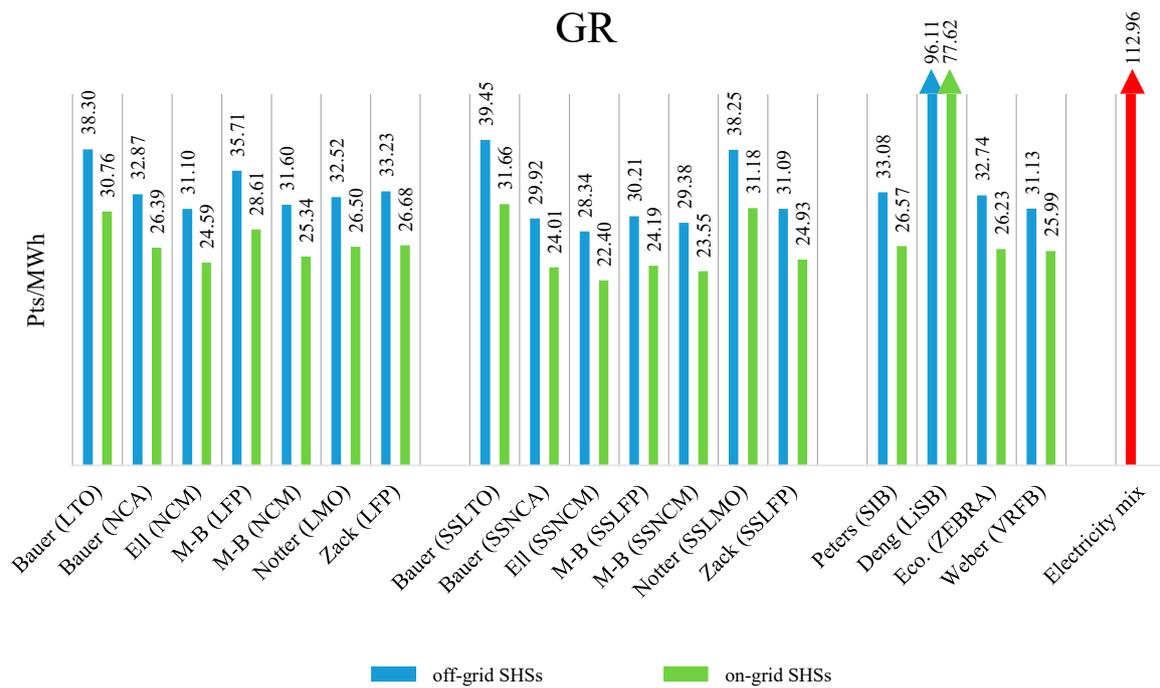


Figure 8. LCA impact values of SHSs in Greece as single scores.

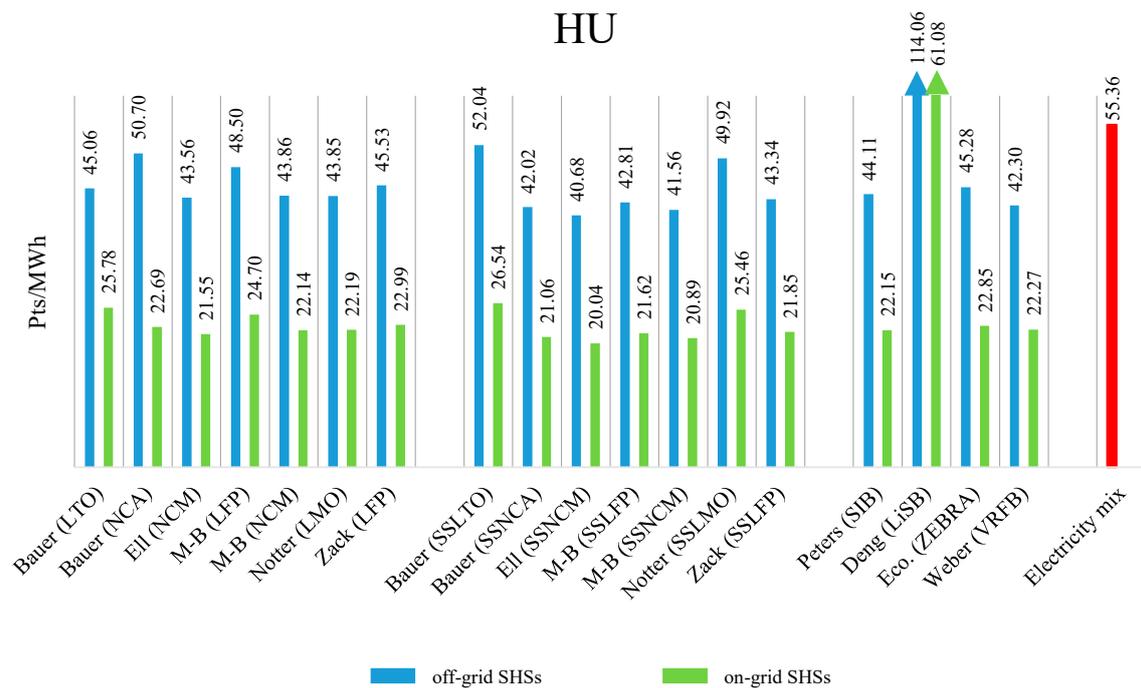


Figure 9. LCA impact values of SHSs in Hungary as single scores.

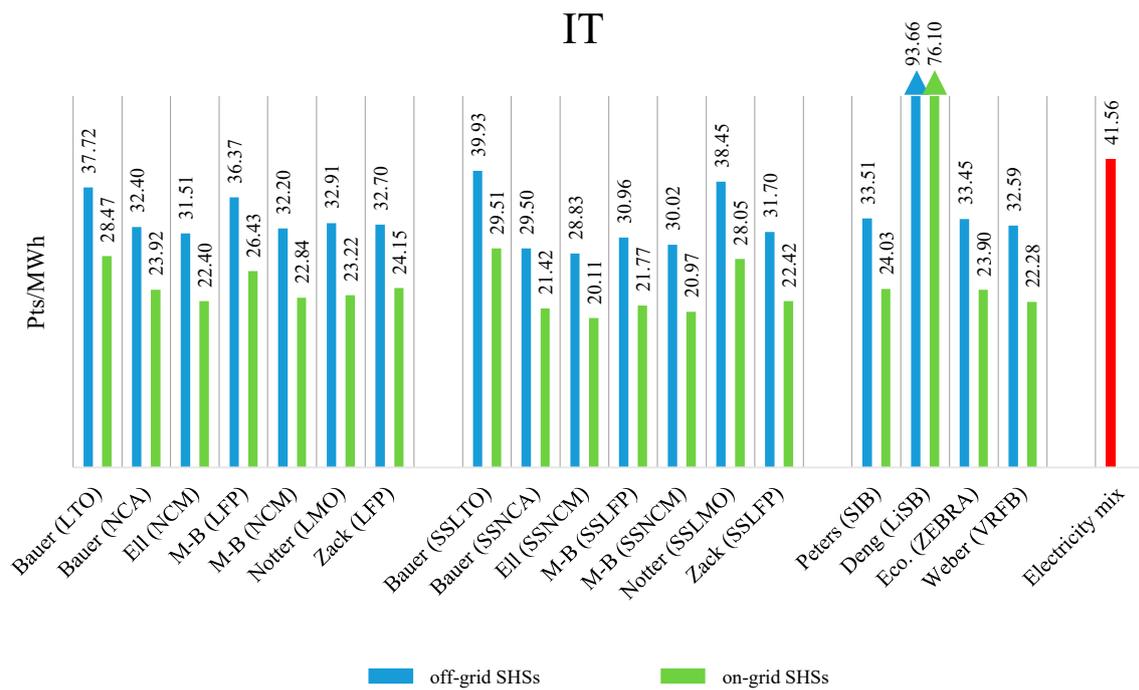


Figure 10. LCA impact values of SHSs in Italy as single scores.

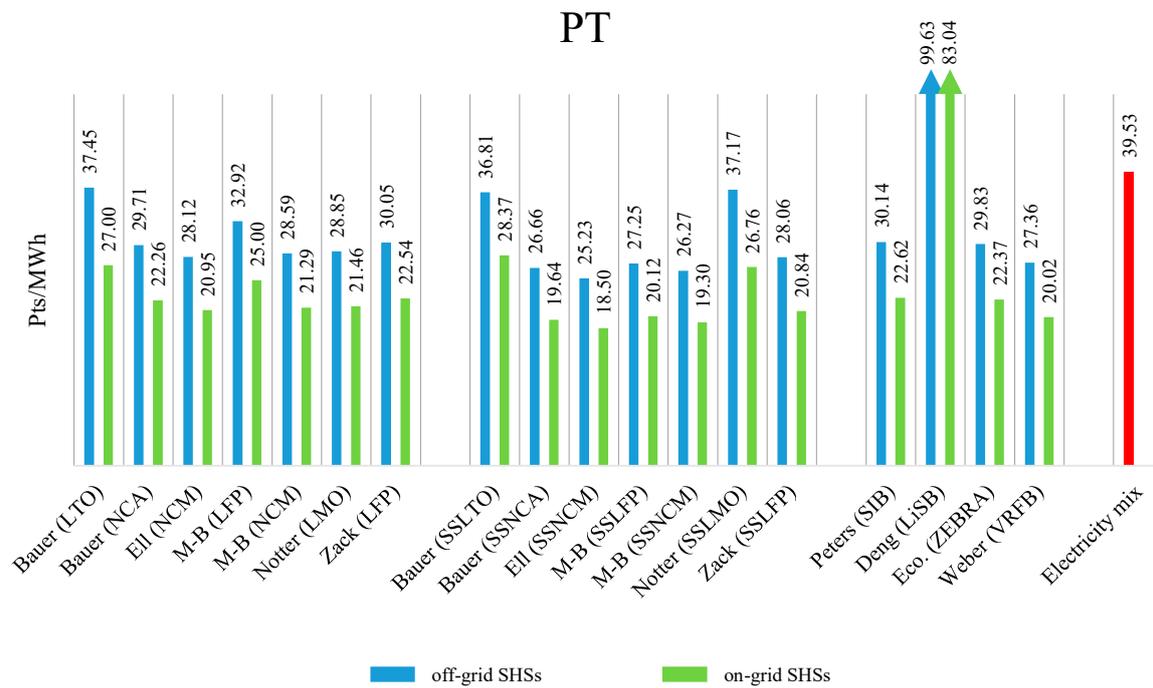


Figure 11. LCA impact values of SHSs in Portugal as single scores.

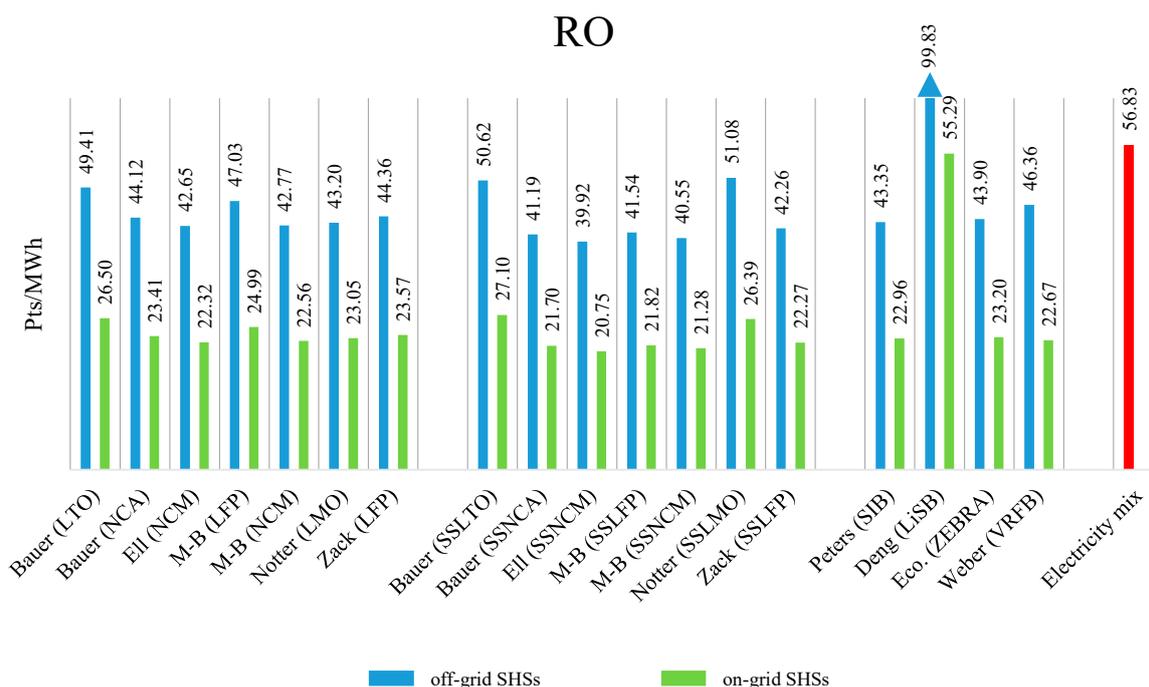


Figure 12. LCA impact values of SHSs in Romania as single scores.

From the results presented in Table 10, it is possible to observe that among LIBs, Eil (NCM) batteries allow us to minimize the SHS environmental impact values thanks to a good combination of efficiency, energy density, materials availability, and lifespan. For the same reasons, Eil (SSNCM) represents the most sustainable choice among SSLIBs. The best aBESS varies with the installation site as Peters (SIB) represents the best solution in DK and HU whereas Weber (VRFB) is assessed as the best in the other countries. A general comparison including all the BESSs categories shows that SHSs equipped with Eil (SSNCM) have the most sustainable environmental performance in every installation site, except for DK, where Peters (SIBs) results to be the best configuration. These results underline that solid electrolytes have an environmental benefit because their impact is comparable to the liquid ones, but a double energy density allows to halve the weight of the battery as well as their contribution to the total SHS impact. Particularly, moving from Eil (NCM) to Eil (SSNCM) the SHS environmental burden is reduced of a remarkable percentage.

Concerning the environmental impact values, different considerations can be done for on-grid and off-grid SHSs. The burdens of grid-connected systems are included in a quite narrow range (16.76 Pts/MWh–24.87 Pts/MWh in case of Eil (SSNCM) installation) depending on the installation site. In northern countries a low solar radiation value imposes the use of large power plant thus representing a major contribution to the overall impact (Table 11). Nevertheless, in these conditions, the amount of energy exceeding the batteries’ capacity is relevant and the possibility to inject it to the grid (Table 9) mitigates the environmental impact per MWh. On the contrary, in off-grid SHSs this possibility does not exist, and the surplus energy must be dissipated. For such reason, the environmental impact per MWh increases, especially in northern installation sites, and the range of values assumed by the SHSs impact is much larger (23.63 Pts/MWh–90.05 Pts/MWh in case of Eil (SSNCM) installation). Therefore off-grid SHSs are more impactful than on-grid configurations and the diesel generator contribution, higher than that of the electricity imported from the grid, strengthens this difference. The only exception is GR, where most of the electricity is produced by coal and its burden is comparable with that of SHSs.

Concerning the national electricity mixes eco-profiles, that of FR is particularly low because of the high nuclear energy contribution to the electricity mix. However, a detailed discussion about the FR electricity mix sustainability is beyond the scope of this paper. This value will be just used as a

reference for comparison. In this context, on-grid systems are more sustainable than the electricity mix in all the installation sites except for FR whereas off-grid systems are not competitive with the grid in DK and FR. The batteries recycling phase has an important role in the SHS environmental impact mitigation: indeed, the best BESSs have a percentage contribution in the order of 10%, but without an adequate recycling of the raw materials this percentage could be over 25%.

The previous considerations have been done analyzing the best BESSs for every battery group. Histograms reported in Figures 4–11 are used to provide a more general overview about all the others SHSs. These figures show that many SHSs, although not the best, are effective to produce more sustainable electricity than the energy mix thanks to their BESS. Among LIBs, Bauer (NCA), M-B (NCM), Ell (NCM) have similar environmental performances; the same considerations can be done for Bauer (SSNCA), M-B (SSNCM), Ell (NCM) and Zack (LFP). The worse batteries are the Notter (LMO), Zack (LFP), Bauer (LTO) and the respective SSLIBs, whose low energy density compromise their environmental performances. The obtained results are coherent with those of our previous work [40] where Bauer (NCA) was assessed as the best solution. Indeed, in both cases Bauer (NCA) and Ell (NCM) environmental performances are very close to each other. This means that, although the simulation model and some input data have been slightly changed and a BESS recycling model has been improved, the best solutions can be obtained mixing cobalt with other more common metals.

In the perspective of replacing LIBs with alternative BESS, Deng (LiSB) is currently very far from the performances of the other batteries because, despite its high energy density, its lifespan is too low to be competitive with the others. Contrarily the Peters (SIBs), Eco. (ZEBRA) and Weber (VRFB) proposals all have good environmental performances; their impact is similar to that of Ell (SSNCM) ones. Considering the operative parameters in Table 1, these devices can improve in terms of energy density. Particularly, Peters batteries (SIB) are still at a research level and the number of cycles which can be performed will probably increase as well as the energy density and, considering that they are already competitive with LIBs stationary batteries, the potential is very large. It's important to stress that LiSBs, despite currently presenting a high environmental impact, should not be under-evaluated because they have some very good characteristics like their energy density, but it's very important to improve strongly their lifespan and the recycling processes in order to be competitive with the other devices.

## 5. Conclusions

In this paper the environmental sustainability assessment of SHSs equipped with different types of batteries is performed through a three-steps methodology including design, modelling and LCA. Some of these batteries, namely LIBs, currently represent a benchmark in the market whereas others have a lower maturity. A sensitivity analysis of the installation site is proposed considering different European countries, at different latitude, represented by their capital city.

From the results it is possible to draw conclusions concerning three major points:

- Geographical dependencies on the variation of battery types: the choice of the most sustainable BESSs does not change significantly with the installation site. Regardless of the solar radiation profile and energy demand curves, Ell (SSNCM) batteries are assessed as the best in almost every country (16.76–24.87 Pts/MWh). M-B (SSNCM) (17.62–23.41 Pts/MWh), M-B (SSLFP) (18.46–26.13 Pts/MWh), Peters (SIB) (21.22–27.51 Pts/MWh) and Weber (VRFB) (18.38–26.31 Pts/MWh) environmental performances are all close to Ell (SSNCM).
- Structural properties and operative characteristics of batteries: the main strength of the mentioned SSLIBs is in having a high energy density. Peters (SIB) devices instead take great advantage of the low impact on natural resources consumption as sodium is more abundant on the Earth's surface whereas Weber (VRFB) batteries have a very long lifespan. Even though SSLIBs guarantee an important improvement compared to simple LIBs and currently they have the most sustainable eco-profile, Peters systems (SIBs) probably have the lowest maturity level among the cited BESSs, therefore the highest potential for the future. Deng batteries (LiSBs), penalized by their short

lifespan, are by far the most impactful battery whereas all the others have an intermediate environmental impact.

- SHSs' environmental advantages and batteries contributions to their eco-profiles in the various European countries: extending the overview to the overall SHS, it is possible to conclude that the choice of the batteries affects the results in southern Europe countries where the percentage contribution is the most relevant, whereas in northern Europe they have a minor contribution. Considering the best batteries, their impact is usually of the order of 10% of the total thanks to the materials recovery in the EoL, while without this percentage it could be more than double. Grid-connected SHSs are always more profitable compared to the off-grid ones, especially in northern countries, thanks to the possibility to inject more electricity to the grid avoiding the use of a diesel generator. Both types of SHSs are generally more sustainable than the national electricity mix, except for FR where the grid electricity is estimated to have a very low impact, and DK where off-grid configuration is more impactful.

**Supplementary Materials:** The following are available online at <http://www.mdpi.com/1996-1073/13/13/3454/s1>, Supplementary Materials provide all the results of the SHS modelling, complete life cycle data inventories and midpoint LCA results for all the installation sites.

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## Abbreviations

aBESS	Alternative Battery Energy Storage System
AIB	Aluminium-ion Battery
BESS	Battery Energy Storage System
CC	Charge Controller
CO	Construction
DK	Denmark
DME	Dimethyl Glycol
DoD	Depth of Discharge
DOL	Dioxolane
EoL	End of Life
ES	Spain
FU	Functional Unit
FR	France
GR	Greece
HU	Hungary
In	Inverter
IT	Italy
ISO	International Organization for Standardization
LCA	Life Cycle Assessment
LCI	Life Cycle Inventory
LCIA	Life Cycle Impact Assessment
LCO	Lithium Cobalt Oxide
LCP	Lithium Cobalt Phosphate
LFP	Lithium Iron Phosphate
LIB	Lithium-ion battery

LiPON	Lithium Phosphorous Oxy-Nitride
LiSB	Lithium-sulphur Battery
LiTFSI	Lithium Bistrifluoromethanesulfonimide
LMNO	Lithium Manganese Nickel Oxide
LMO	Lithium Manganese Oxide
LTO	Lithium Iron Titanate
NCA	Nickel Cobalt Aluminium
NCM	Nickel Cobalt Manganese
NMMT	Nickel Manganese Magnesium Titanium Oxide
OP	Operation
PON	Polyacrylonitrile
PT	Portugal
PV	Photovoltaic
PV-GIS	Photovoltaic Geographical Information System
RF	Reference Flow
RO	Romania
SHS	Solar Home System
SIB	Sodium-ion Battery
SOC	State of Charge
SOH	State of Health
SSLFP	Solid State Lithium Iron Phosphate
SSLIB	Solid State Lithium-ion Battery
SSLMO	Solid State Lithium Manganese Oxide
SSLTO	Solid State Lithium Iron Titanate
SSNCA	Solid State Nickel Cobalt Aluminium
SSNCM	Solid State Nickel Cobalt Manganese
VRFB	Vanadium Redox Flow Battery
ZEBRA	Zero Emissions Batteries Research Activity

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