

Review

From Lab to Fab: Development and Deployment of Direct Air Capture of CO₂

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Abstract: Direct Air Capture (DAC) is a promising technology to fight climate change by capturing carbon dioxide (CO₂) from the air. For DAC to be a negative emissions technology, the captured CO₂ must be removed permanently, but can also be used as a net-zero technology to produce sustainable chemicals, fuels or other materials. This review presents a comprehensive survey of recent advancements, challenges, and potential applications of DAC technology, with an emphasis on the recent rapid increase in the number of DAC developers, the majority of them being founded in the past 4 years. Through pilot projects and recent commercial deployments, several DAC companies have made significant advances and demonstrated their scalability. Cost and energy efficiency remain significant impediments to the wide deployment of DAC. Integration with emission-free energy sources and utilization of waste heat are being researched to boost the total energy efficiency of DAC systems. Further research of electrochemical technologies for regeneration or direct capture are needed, as well as the development of new, modified, or hybrid adsorbents for improved capture efficiencies. Moreover, favorable regulations and financial incentives are crucial for enhancing the viability of DAC projects and will need to substantially increase if Paris Agreement goals are to be achieved.

Keywords: direct air capture; negative emissions technology; CO₂ capture, utilization, and storage; DAC technology developer; CO₂ capture cost; DAC literature review



Citation: Barahimi, V.; Ho, M.; Croiset, E. From Lab to Fab: Development and Deployment of Direct Air Capture of CO₂. *Energies* **2023**, *16*, 6385. <https://doi.org/10.3390/en16176385>

Academic Editors: Abdul-Ghani Olabi, Michele Dassisti and Zhen Zhang

Received: 31 July 2023

Revised: 26 August 2023

Accepted: 28 August 2023

Published: 3 September 2023



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1. Introduction

In the 2015 Paris Agreement, 196 nations vowed to establish a long-term goal of keeping the global average temperature rise well below 2 °C above pre-industrial levels [1]. The atmospheric carbon dioxide (CO₂) concentration is currently at 423 ppm, or 3300 GtCO₂, which is more than it has ever been in the last 800,000 years [2]. If the climate and economic growth targets are to be met, negative emissions technologies are certain to play a significant role in mitigating climate change by removing 10 GtCO₂/year globally by mid-century and 20 GtCO₂/year globally by the end of the century [3]. In this scenario, direct air capture (DAC), a possible negative emissions technology, plays an increasing role [4–6]. DAC is a revolutionary approach to mitigating climate change by removing CO₂ directly from the atmosphere and storing or utilizing it in various applications [7]. There are currently 27 DAC plants worldwide in operation, mostly small demonstration projects, removing almost 0.01 MtCO₂ annually, and 130 DAC facilities are in various stages of development for a total removal capacity of around 5 MtCO₂/year [8]. To put this into perspective, the 2050 net-zero emission scenario indicates a CO₂ removal from DAC of about 75 MtCO₂/year in 2030 [8].

DAC technology relies on chemical or physical processes to capture CO₂ from ambient air [9]. The technology typically involves three main steps: adsorption/absorption, desorption, and purification. In the adsorption/absorption step, a sorbent/solvent is used to selectively bind CO₂ from the air while allowing the passage of other gases. The CO₂-loaded sorbent/solvent is then processed in the desorption step, where the CO₂ is separated

from the sorbent before final purification. The purified CO₂ can then be stored [10,11] or utilized in various applications, such as in the production of synthetic fuels or building materials [12]. Figure 1 represents the number of published articles over time with “direct air capture” in the title, using the ScienceDirect database. This figure highlights the exponential growth of research interest in DAC in the last 5–6 years.

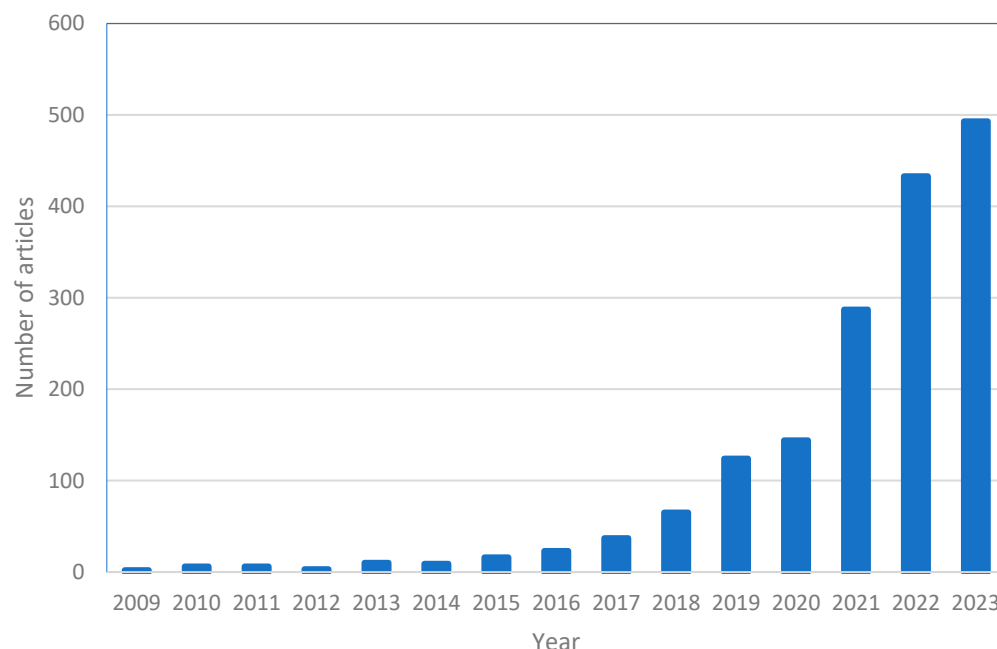


Figure 1. Number of published articles over time containing “direct air capture” in the title from ScienceDirect database (August 2023).

Unlike carbon capture technologies developed for large stationary sources, such as power plants or industrial facilities, the location of DAC systems is more flexible. For example, it can be located close to storage sites because it is not dependent on a source of CO₂ other than air, which makes it an option to offset hard-to-abate emissions [13]. One significant challenge associated with DAC is its high energy requirement, and hence its high cost [14]. Yet, DAC is a new and developing technology, and researchers and companies are actively working on developing more energy-efficient processes and reducing DAC costs [15,16].

This review paper describes the rapidly evolving DAC field. The liquid and solid sorbents explored, equipment required, and overview of DAC processes are described in the DAC Technologies section. After an overview of CO₂ storage and utilization, this paper presents a comprehensive panorama of DAC-focused companies and their latest developments. Finally, an analysis of DAC energy demand and costs is presented. All tonnes reported are in metric tonnes and costs in US dollars (USD).

2. DAC Technologies

The extremely low CO₂ concentration in the atmosphere and intense competition from other components in air, particularly water, impose stringent thermodynamic requirements on DAC technologies [17]. Liquid sorbent and solid sorbent technology are the two most prevalent DAC capture media [15,16]. In addition, various alternative technologies for DAC have been proposed, including electrochemical techniques [18], membrane capture [19], and ion-exchange resins [20].

Since CO₂ is an acidic gas, most sorbents (solid or liquid) used to remove CO₂ from gas streams must be of a basic character for sorption to take place. After each sorption step, the sorbent must release the CO₂ it has trapped, which returns it to its initial condition and enables it for subsequent rounds of capture. The sorbent is a crucial component of DAC

and the optimum sorbent for a DAC system must meet several requirements. Desirable characteristics of sorbents include high selectivity and affinity for CO₂, stability in the relevant pH and temperature windows, high capacity for CO₂, long cyclability, fast CO₂ uptake and release kinetics, nontoxicity, and low cost [21]. From a process standpoint, the capture is ideally carried out at ambient temperatures and pressure because it is unprofitable to pressurize, cool, or heat large volumes of air (which eliminates membrane or cryogenic-based separation technologies), and the energy for capture should come from non-emitting sources to prevent the release of additional CO₂ during the process (i.e., to attain net-zero or negative emissions) [22]. In this section, we present more details on different DAC technologies.

2.1. Liquid Sorbent Technology

2.1.1. Aqueous Alkaline Solvents

Aqueous sorbents with a high CO₂ selectivity, such as sodium hydroxide (NaOH), potassium hydroxide (KOH), and calcium hydroxide (Ca(OH)₂), are strong bases used as a sorption technique for DAC. In 1999, Lackner et al. [23] proposed absorption using Ca(OH)₂ in a three-reaction process (see Table 1). The number of OH groups that may react with CO₂ and, consequently, the rate of CO₂ absorption are both severely constrained by the solubility of Ca(OH)₂ in water, which is very low (0.025 M) at room temperature. In 2006, Baciocchi et al. [24] proposed the use of NaOH in a four-reaction process because it enables significant CO₂ binding while also increasing carbonate solubility in water. While Ca(OH)₂ and NaOH both offer strong binding to CO₂, NaOH has the benefit of producing a carbonate with higher water solubility, which also avoids scaling on the inner surfaces of the absorption column. However, the high solubility of sodium carbonate hinders direct precipitation. Similar procedures and regeneration techniques to those described here could also be used with KOH to capture CO₂. However, KOH is more expensive than NaOH and is commercially produced at a scale that is a hundred times lower. On the other hand, KOH requires lower regeneration energy than NaOH [25].

Table 1. Aqueous Alkaline Solvents Reactions. A in AOH can be Na or K.

Alkaline Type	Ca(OH) ₂	AOH
Air Contactor	$\text{Ca(OH)}_2(\text{aq}) + \text{CO}_2(\text{g}) \rightarrow \text{CaCO}_3(\text{s}) + \text{H}_2\text{O}(\text{l})$ (1)	$2\text{AOH}(\text{aq}) + \text{CO}_2(\text{g}) \rightarrow \text{A}_2\text{CO}_3(\text{aq}) + \text{H}_2\text{O}(\text{aq})$ (2)
Causticizer	–	$\text{A}_2\text{CO}_3(\text{aq}) + \text{Ca(OH)}_2(\text{aq}) \rightarrow 2\text{AOH}(\text{aq}) + \text{CaCO}_3(\text{s})$ (3)
Calcliner	$\text{CaCO}_3(\text{s}) + \text{Heat} \rightarrow \text{CaO}(\text{s}) + \text{CO}_2(\text{g})$ (4)	$\text{CaCO}_3(\text{s}) + \text{Heat} \rightarrow \text{CaO}(\text{s}) + \text{CO}_2(\text{g})$ (5)
Slaker	$\text{CaO}(\text{s}) + \text{H}_2\text{O}(\text{l}) \rightarrow \text{Ca(OH)}_2(\text{aq})$ (6)	$\text{CaO}(\text{s}) + \text{H}_2\text{O}(\text{l}) \rightarrow \text{Ca(OH)}_2(\text{aq})$ (7)

The main process flow of the liquid sorbent system is depicted in Figure 2, which has two chemical cycles that work concurrently. In the first cycle, air is passed through the air contactor where it meets the aqueous solution (KOH or NaOH) and CO₂ is absorbed at ambient temperature and pressure. Due to the diluted concentration of CO₂ in air, contactor designs for CO₂ capture from air are distinct from those of conventional packed towers used in point-source carbon capture; it has been observed that the most advantageous configuration is for very short columns with very large cross-sections [26]. In the second cycle, the pellet reactor or causticizer regenerates the sorbent solution by reacting with calcium hydroxide (Ca(OH)₂) to form CaCO₃. The produced CaCO₃ is heated to about 900 °C in the calciner to release CO₂, and the reaction outputs of CaO are sent into the slaker unit to react with water and form Ca(OH)₂ for use in subsequent cycles [27]. It should be emphasized that because moisture must be eliminated before calcination in a kiln, water loss throughout the process results in a significant energy cost. Zeman et al. [28] demonstrated the importance of water loss in their system, with an average mass loss of 90 gH₂O/gCO₂.

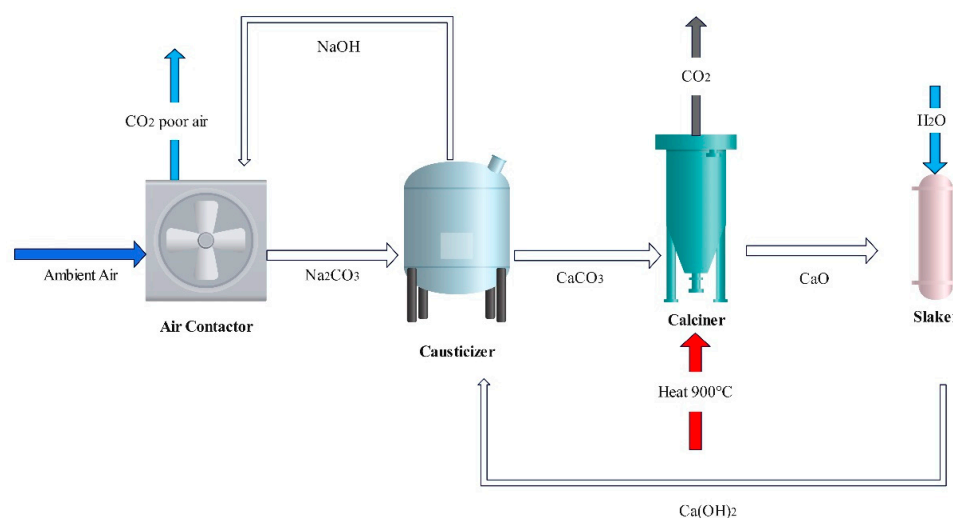


Figure 2. Schematic diagram of a typical NaOH liquid sorbent process.

2.1.2. Aqueous Amines

Since 1930, aqueous solutions of primary and secondary amines have been used to capture CO₂ from natural gas and hydrogen at high partial pressures [29]. Aqueous amines such as monoethanolamide (MEA), diethanolamine (DEA), and methyl diethanolamine (MDEA) are the most often used amines for CO₂ absorption [30]. High reaction rates, appropriate CO₂ absorption capacities, maturity of the technology and low cost compared to alternative processes are all benefits of amine solutions. However, the main disadvantages of amine solutions are oxidative degradation, high volatility of most amine solvents and high regeneration heat [17,31]. Recent studies have examined the use of aqueous amine solvents for DAC [32]. Miao et al. [32] have shown experimentally that primary and secondary amines function best, absorbing around 85% of the CO₂ from air, similar to NaOH under the same conditions. One of the most effective sorbents for DAC are aqueous unrestricted primary amines since they are just as effective as aqueous alkali hydroxides while also having the ability to save energy because sorbent regeneration occurs at lower temperatures [33,34].

2.1.3. Ionic Liquids (IL)

Salts that are liquid at ambient conditions are known as ionic liquids (ILs). ILs offer virtually limitless structural and chemical tunability since they are mostly composed of large organic ions [35,36]. In addition to strong CO₂ solubility and selectivity, ILs display excellent performance in CO₂ capture due to their stability, low volatility, and flexibility of design options [37–39]. However, a disadvantage of ILs for CO₂ capture is their higher viscosity compared to that of conventional solvents, resulting in difficult manufacturing and purification procedures [40]. On the other hand, there are several options to reduce the viscosity such as proper mix of cations and anions, length of the alkyl chain of cations, or addition of a co-solvent [39,41]. Polar solvents, such as water, have a greater effect on viscosity reduction than non-polar solvents, such as benzene and toluene [39,42]. Attaching CO₂-philic functional groups to ILs can dramatically enhance their CO₂ collection ability [41]. Moitra et al. [43] used CaO- and superbase-ionic liquids (SIL)-bifunctionalized sorbents to capture CO₂; these sorbents demonstrated rapid interaction kinetics, high CO₂ uptake capacity, facile CO₂ release, and stable sorption/desorption cycles. New research proposes that immobilizing ILs in porous materials with large surface areas and specific active sites, such as MOFs, might remedy the difficulties caused by ILs [44–46], which is discussed further in the MOF part under Section 2.2.

2.2. Solid Sorbent Technology

Figure 3 shows a typical adsorption process. This type of technology includes adsorption chambers containing solid sorbents where cyclic adsorption and desorption procedures are carried out. During the adsorption process, ambient air, usually propelled by fans, passes through the contactor and CO₂ is adsorbed onto the solid sorbent at ambient temperature, while CO₂-poor air exits the system. Air contactors for solid sorbents may take different forms including monolithic, fluidized bed, fixed bed, and moving bed designs [47]. Contactor design plays an important role in reducing the overall pressure drop of the air passing through (thereby reducing costs). After the sorbent is saturated with CO₂, the system switches from adsorption to desorption. During this process, the adsorption chamber is isolated from the surrounding environment and the residual air is evacuated. The sorbent is then exposed to different conditions such as increased temperature, releasing a CO₂ stream of high purity. In addition to temperature, cycles involving changing pressure, humidity, or their combinations can also be used in the capture–regeneration cycle [48]. Once CO₂ desorption is complete, the sorbent is then returned to initial conditions to begin a new cycle.

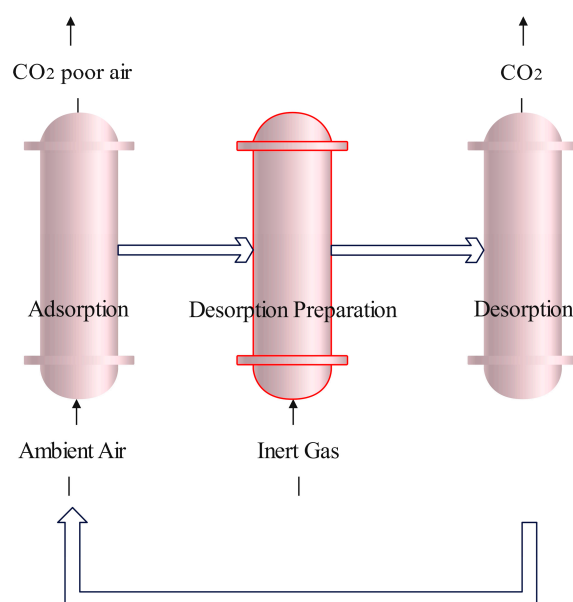


Figure 3. Schematic diagram of a typical solid sorbent-based process. CO₂ is captured during the adsorption step until the capacity of the sorbent is reached. In the desorption preparation step, the chamber is closed and, depending on the process, the pressure/temperature/humidity are changed to favor CO₂ desorption. During the desorption step, the CO₂ released from the sorbent is removed from the chamber.

2.2.1. Adsorbents

This section focuses on the most studied physical adsorbents for DAC application, specifically zeolites, activated carbon (AC), and metal organic frameworks (MOFs).

- **Zeolites**

Zeolites are three-dimensional porous crystalline aluminosilicates composed of a periodic array of TO₄ tetrahedral (T = Si or Al) that are extensively utilized for gas separation. Aluminum substitution for silicon in the zeolite lattice produces isomorphism, resulting in a structure with a net negative charge and a strong affinity for quadrupolar molecules, such as CO₂ [49]. Zeolites have high availability, low cost, large surface area and tailorable pore cavities which lends them to be a good molecular sieve for CO₂ separation [50]. The main CO₂ capture mechanism is physical adsorption where the CO₂ molecules are bound to carbonate molecules by π -coordination or ion–dipole interactions; in addition, chemical modification strategies have also been explored to improve CO₂ capacity such as amine

modification, silica modification, and ion exchange [50]. One drawback is that the sorption capacity and CO₂/N₂ selectivity of zeolites for DAC applications remain problematic. Zeolite sorption capacity depends on zeolite type, therefore adding amine to create functionalized zeolites aids to increase it [51]. Zeolites are known to also adsorb moisture [50] and therefore a desiccant bed is usually required to collect the moisture from the air to offset the reduction in adsorption capacity in humid environments. This approach often requires greater energy input and expensive equipment [50,52].

- Activated Carbon (AC) and Porous Carbon

Carbon-based adsorbents may be created in several forms, including carbon allotropes (carbon nanotubes (CNTs) and graphene), activated carbons (AC), porous carbons, amorphous carbon, biomass-derived carbons, pyrogenic carbons, template-based carbons, carbon molecular sieves, carbon aerogels (CAs), and carbon nanofibers (CNFs) [53]. Carbonaceous adsorbents typically feature a range of pore sizes, consisting of micropores (<2 nm), mesopores (2–50 nm) and macropores (>50 nm). The meso- and macropores facilitate the movement of molecules to the micropores, where 90% of the adsorption takes place through van der Waals interactions [49]. Economically speaking, activated porous carbons could be more favorable for CO₂ capture over other carbon-based adsorbents which require expensive precursors and chemicals for functionalization in addition to high energy consumption [53]. In general, the preparation techniques of raw materials have an impact on the properties of AC. Important variables in the preparation stages include pyrolysis, activation temperature, and holding duration [54]. Due to its low cost, large surface area, resistance to moisture, readily customizable features such as porosity, excellent stability, and low regeneration energy, AC has also attracted interest for CO₂ capture [55]. Low chemical activity makes it easy to regenerate and guarantees that it does not react with the sorbate; however, this also results in low CO₂ uptake capacity at low partial pressures [56] which has led to different strategies to improve capacity such as physical or chemical activations, doping (with nitrogen, oxygen or sulfur), amine addition, and carboxylation [49,53]. Kamran et al. [57] investigated the influence of different chemical activation agents on polyacrylonitrile (PAN)-based porous carbon sorbents for CO₂ collection and they demonstrated stability of their sorbents over a small number (four) of adsorption–desorption cycles.

- Metal Organic Frameworks (MOFs)

MOFs are highly porous crystalline materials composed of metal-containing nodes connected by organic ligand bridges and created by powerful coordination bonds. One advantage of MOFs is the ability to customize their structure based on desired surface area, pore volume and functionalization [58]. MOFs are considered a promising separation technology for environmental applications such as water treatment and CO₂ removal [59]. MOF synthesis and post-synthetic modification methods can result in different capture mechanisms such as interaction with open metal sites, Lewis basic sites (like amines), polar functional groups [60], molecular sieving through pore size control, flexible or stimuli-responsive frameworks [58,60], or improving CO₂ selectivity by creating hydrophobic frameworks [60]. For example, Liu et al. [61] functionalized MIL-100(Fe), UiO-66(Zr) and MIL-100(Cr) MOFs by grafting N-(2-Aminoethyl)ethanolamine (AEEA) after the initial MOF synthesis. While the secondary amines of AEEA reacted with the metallic vacancy sites on the MOFs to produce grafts, the exposed primary amine acted as the main CO₂ adsorption site, resulting in excellent thermal stability, structural stability, and improved CO₂ capacity. In another study by Qiu et al. [46], a Ni-MOF was functionalized with [MeTBDH]₂[HFPDO], a superbase-derived ionic liquid (SIL). The hybridized SIL-MOF demonstrated an improved CO₂ uptake at 0.4 mbar (close to 400 ppm) due to a stronger interaction strength between the SIL and CO₂. Uptake also improved as humidity increased; however, capture kinetics suffered due to hydrogen bonding formation and partial blocking of pores. Despite the benefits, the cost of MOFs, particularly the organic ligand, may be prohibitive to its widescale adoption [58].

2.2.2. Ion-Exchange Resin

Ion-exchange resins are cross-linked polymers to which ions can electrostatically bind and are named for their ability to exchange ions of the same charge type when in contact with an ion-containing solution. Both anion- and cation-exchange resins exist; the name indicates which type of ion can be exchanged. In the 100+ years of ion-exchange resin history, they have been used for various applications including water treatment, hydrometallurgy, catalysis and more [62]. Lackner [63] proposed the use of a strong-base ion-exchange resin with OH^- charge to capture CO_2 . Rather than exchanging ions, the OH^- reacts with CO_2 to form carbonate (CO_3^{2-}) and bicarbonate (HCO_3^-), and CO_3^{2-} further reacts with CO_2 to form HCO_3^- until full capacity of the resin is reached when it is saturated in the bicarbonate state. Moisture swing using water vapor releases the CO_2 back into a gaseous state, although other studies have demonstrated regeneration of other resin types using temperature swing and even seawater [64]. Amine-functionalized ion-exchange resins (usually quaternary ammonium based) have also been studied. Wang et al. [65] found that poor adsorption kinetics occurred when temperature decreased from 20°C to 0°C , and humidity increased, but the effect of temperature could be mitigated by decreasing resin particle size from 30 to 5 μm . Higher porosity, such as through large inner pore sizes, can also improve uptake kinetics [66]. Although a functionalization process is required to improve the commercially available ion-exchange resins for use in DAC, the maturity of the industry is still beneficial from an economic standpoint. However, further research on these resins specifically for DAC is needed, as current studies show they may be limited to deployment in warmer and drier climates unless engineering design is used to overcome these challenges.

2.2.3. Desorption/Regeneration

Several desorption/regeneration processes have been considered for DAC, such as temperature swing adsorption (TSA), pressure swing adsorption (PSA), vacuum swing adsorption (VSA) and moisture swing adsorption (MSA). The regeneration process can be repeated multiple times, with the adsorption and desorption cycles occurring sequentially in different parts of the sorbent bed. The adsorption and desorption cycles can also be controlled by adjusting the pressure and temperature of the system, which allows for further optimization of the process.

- Temperature swing adsorption (TSA)

TSA uses increased temperature to desorb CO_2 from solid sorbents [67] and is a commonly used to regeneration technique. In the case of amine-based CO_2 adsorbents, lab experiments have shown that TSA regeneration is preferable [15]. Utilizing an inert gas instead of air may reduce oxidative deterioration of sorbents. In addition, TSA has the option of using pure CO_2 as a stripping gas to produce high-purity CO_2 ; however, in the case of amine-functionalized sorbents, there is a risk of urea production owing to deactivation of the adsorbent [68].

- Pressure swing adsorption (PSA) or vacuum swing adsorption (VSA)

PSA and VSA work by utilizing the different adsorption characteristics of CO_2 and other gases at different pressures to selectively capture CO_2 from the air. In PSA, the filtered air is compressed and then fed into a vessel filled with a solid sorbent material, such as zeolites or activated carbon, which selectively adsorbs CO_2 while allowing the passage of other gases [69]. To regenerate the sorbent material and release the captured CO_2 , the pressure in the vessel is reduced, which causes the sorbent to desorb the CO_2 . The desorbed CO_2 can then be collected and stored, or used for various applications, such as in the production of synthetic fuels [70]. In VSA, CO_2 adsorption occurs at ambient pressure and depressurization occurs during regeneration. One of the advantages of PSA technology is its ability to capture large quantities of CO_2 over time. However, PSA/VSA technology requires a significant amount of energy, particularly for the compression and desorption steps, which increases the cost of DAC systems. Researchers and companies are actively

working to develop more energy-efficient PSA and VSA processes and improve the overall efficiency of DAC systems [71,72]. The combination of temperature and vacuum swing has been used several times for DAC [9,16,73].

- Moisture swing adsorption (MSA)

Lackner [63] developed MSA to absorb CO₂ from the air, alleviating the high regeneration costs of amine-functionalized sorbents by substituting the temperature and pressure swing processes. MSA uses the conventional method of ion hydration to trap CO₂ from the air and release it in a controlled way [31]. The method involves coating a solid support with heterogeneous ion-exchange resin (usually polymeric materials). By using an amine-coated anion exchange resin, for example, it is possible to capture CO₂ from dry air in the atmosphere and then release it when it is exposed to water [74]. MSA is interesting because it uses the latent heat of evaporation instead of the energy needed for PSA or TSA. All that is needed is a source of water, and the latent heat of evaporation provides all the energy needed to drive the process. The main problem with the process though, is that the capture must be performed in a dry atmosphere, which indicates this method may be less appropriate for humid areas. The energy consumption of moisture-swing sorbent has been estimated to be about 50 kJ/mol CO₂ [75].

Comparing MSA technology to more traditional temperature or pressure swing adsorption reveals various advantages: (1) Instead of using expensive energy, low-cost water may be used to swing sorbents between sorption and desorption; (2) water sorption and CO₂ sorption on the resin proceed in opposing directions, eliminating the energy penalty for sorption and desorption of water; (3) the moisture swing may simplify the system design by eliminating the need for heating and cooling devices. MSA also has its own disadvantages: (1) To keep anion impurities from contaminating the resin, the water must be relatively pure; (2) the system's performance is affected by the weather, and hot, dry climates work best for MSA; (3) the partial pressure of the emitted CO₂ is relatively low because of the moisture fluctuation, therefore requiring extra concentration processes prior to storage [76]. In the case of cold and humid environments, combining a moisture swing and a slight thermal swing might enhance the desorption performance.

The intended use of CO₂ determines its purity requirement and may influence the DAC system regeneration method. If the use is for an agricultural greenhouse and a low concentration of CO₂ is desired, the moisture swing adsorption technique can represent a good option. For example, CO₂ can improve agricultural greenhouse plant performance by capturing the gas directly from the air outside and releasing it inside the greenhouse using adsorbents made of K₂CO₃ or Na₂CO₃.

2.3. Electrochemical Technology

Various electrochemical methods have been investigated for the capture and separation of CO₂. Such techniques include direct CO₂ capture using an electrochemical cell, CO₂ capture via redox-active materials, and regeneration of CO₂ binding sorbents for reuse. Advantages of electrochemical techniques include operating temperatures and pressures lower than temperature or temperature-vacuum swing adsorption [77] and easy integration with renewable energy sources [78].

2.3.1. Electrochemical Capture

One method for direct capture involves feeding air to one side of a polymer electrolyte membrane electrochemical cell and isolating the CO₂ on the permeate side (see Figure 4). The advantage of this method is that it does not rely on a large pressure gradient like conventional membrane separation. This type of system was first reported by the National Aeronautics and Space Administration for CO₂ removal from spacecrafts [79]. More recently, Muroyama et al. [80] tested commercial alkaline anion exchange membranes (AEM) for the capture of 0.1–100% CO₂ in a N₂ gas feed. At the cathode, CO₂ reacts with OH[−] to form CO₃^{2−} or HCO₃[−], which travel to the anode side. H₂ was used to depolarize the anode, resulting in the formation of CO₂, H₂O at the outlet. Condensing the water out

would leave a mixture of CO_2 and residual H_2 , which could be useful for synthetic fuel and chemical production, as discussed in a later section. It was noted that at sub-percent levels of CO_2 , low faradaic efficiency and high energy consumption made decoupling the capture and CO_2 isolation/sorbent regeneration step more sensible [80].

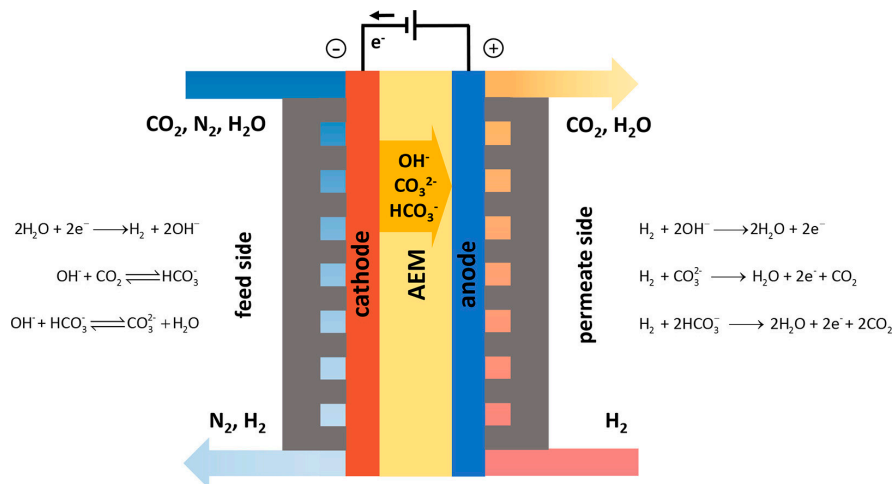


Figure 4. Schematic of AEM CO_2 separation device [80].

Another method for direct capture of CO_2 uses redox-active materials. Redox-based capture has two subcategories: direct and indirect. The direct method uses a redox-active sorbent where its affinity for CO_2 is electrochemically activated or deactivated. This has been called electrochemically mediated complexation separations [81]. Common sorbents studied include quinones, bipyridines, disulfides, and transition metals [81,82]. The indirect method electrochemically activates/deactivates the affinity of a redox-active competitor for the CO_2 -binding sorbent. When activated, the sorbent has higher attraction to the competitor than to CO_2 , causing the sorbent to release CO_2 and bind to the competitor instead. This has been referred to as electrochemically mediated competitive complexation separation [81]. For both methods, the main steps of the cycle are activation, capture of CO_2 , deactivation, and desorption of CO_2 . Seo et al. [83] used the 1-AP nitrate to capture CO_2 and then regenerate it through an electrochemical H-cell containing an anion exchange membrane separating the two (see Figure 5). The measured work required to capture from ambient air was 162 $\text{kJ}_\text{e}/\text{mol CO}_2$. In a recent report by the same authors [84], the commercial organic dye, neutral red (NR), was used as a redox-active compound due to its oxygen insensitivity and was combined with a hydrotropic agent, nicotinamide (NA), to improve CO_2 solubility in the aqueous solution. The estimated work required for capture from ambient air was 65 $\text{kJ}_\text{e}/\text{mol of CO}_2$, which is an improvement over 162 $\text{kJ}_\text{e}/\text{mol CO}_2$.

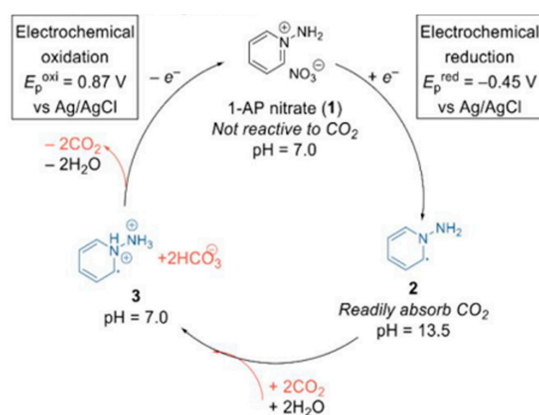


Figure 5. Aqueous Amine and Electrochemical to capture and release CO_2 [83].

2.3.2. Electrochemical Regeneration

The most common electrochemical system is to first capture CO_2 using a sorbent followed by separation of CO_2 and subsequent regeneration of the sorbents [77]. Electrochemical separation can involve bipolar membranes (BPM), monopolar membranes, or a combination thereof. As the most energy-demanding part of the liquid sorbent-based processes is the sorbent regeneration, which can involve heating to upwards of 900°C , it is therefore natural for researchers to investigate alternative methods for regeneration [77]. In addition, several DAC companies are either planning to use electrochemical regeneration or exploring its use [85]. Below, we discuss monopolar and bipolar membrane electro dialysis technologies.

- Monopolar Membrane Electrodialysis

Monopolar ion exchange membranes (cationic or anionic) allow the permeation of one charge type from an electrolyte. Anion exchange membranes are positively charged and, therefore, attract and allow anions to pass through. Different arrangements using monopolar ion exchange membranes have been proposed for the electrochemical regeneration of CO_2 absorption solvents for DAC, including aqueous amines or aqueous alkaline solutions [86]. Shu et al. [78] coupled CO_2 capture using NaOH and absorbent regeneration using a three-chamber electrochemical stack configuration (see Figure 6). The H_2 -recycling electrochemical system (HRES) is connected to a membrane contactor that was first created for nitrogen recovery from wastewater. In the HRES, H^+ produced from oxidized H_2 reacts with the carbonate to form carbonic acid (H_2CO_3), which leads to CO_2 desorption once the pH is low enough. NaOH regeneration occurs in the cathode compartment [78].

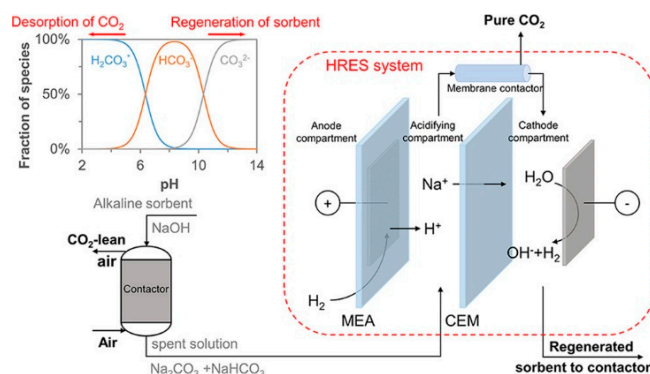
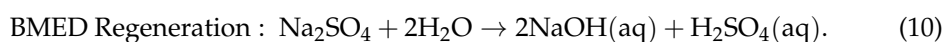
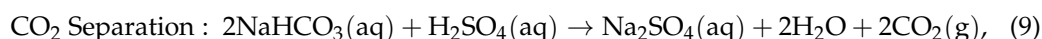
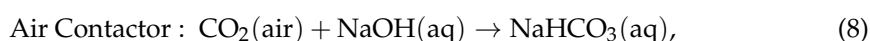


Figure 6. Aqueous alkaline solvent regeneration and CO_2 desorption in a continuous system using a H_2 –recycling electrochemical cell [78].

- Bipolar Membrane Electrodialysis

In the bipolar membrane electrodialysis (BPMED) process, aqueous carbonate (e.g., Na_2CO_3) is generated, as opposed to aqueous bicarbonate (e.g., NaHCO_3) in a conventional process. The process for BPMED is shown in Figure 7. A pH of less than 10 results in NaHCO_3 , while a pH greater than 10 produces Na_2CO_3 (see Reactions (2) and (8)). NaHCO_3 is then reacted with sulfuric acid to produce CO_2 , water, and sodium sulfate (Na_2SO_4) (Reaction (9)). Finally, Na_2SO_4 undergoes BPMED regeneration (Reaction (10)) to restart the absorption cycle.



Bipolar membranes (BPM) consist of two contacting monopolar membrane layers, one positively charged anion exchange membrane (AEM) and one negatively charged cation exchange membrane (CEM). The interfacial contact at the CEM and AEM is called the bipolar junction. BPMs can be stacked with an AEM or CEM to form a two-cell stack, or with both an AEM and CEM to form a three-cell stack. For acid-base regeneration, the aqueous products from the separation step are routed to the BPMED stack where the cells are separated into an acidic and a basic compartment [87,88]. Water molecules electro-dissociate into protons and hydroxide ions at the bipolar junction while the Na_2SO_4 also dissociates, and its applicable ions pass through the monopolar membrane to react with the H^+ and OH^- , resulting in the formation of H_2SO_4 and NaOH .

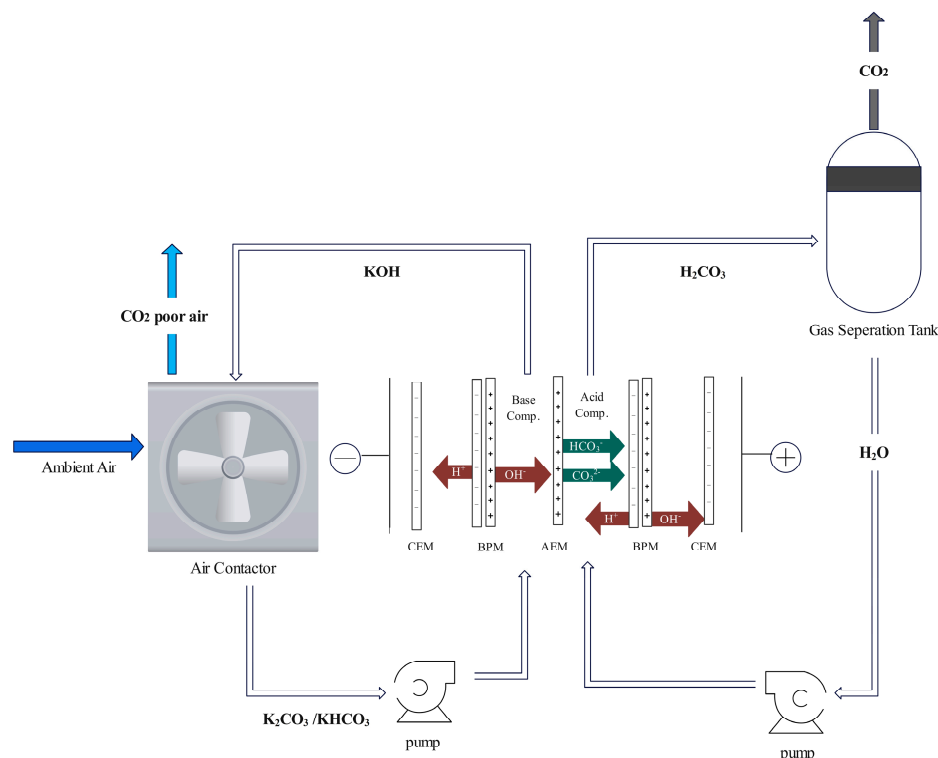


Figure 7. Schematic of an aqueous alkali hydroxide solution regeneration with BPM cells (adapted from [88]).

BPMED technology has already been commercialized by several manufacturers mostly in the production, regeneration, or recovery of acid and base salt solutions [87]. Advantages include the ability to utilize renewable electricity sources, and the closed loop design allowing sorbent reuse, although water must be inputted into the system. Challenges with BPMED include the cost being 3–10 times that of monopolar membranes which is associated with the smaller production scale, more complicated preparation of bipolar membranes, and potential chemical instability of the AEM which can be exposed to highly alkaline conditions ($\text{pH} > 11$) [87,89].

While much progress has been made in electrochemical research, challenges for scale-up persist including the need to reduce membrane cost, improve faradaic efficiency, improve CO_2 capacity [77,81], improve electron and charge transfer kinetics, as well as the presence of high operable current densities and membrane permselectivity [81].

3. Storage and Utilization of CO_2

In order for DAC to become a true negative emissions technology, the CO_2 captured must be permanently stored. Although utilizing CO_2 to produce chemicals or fuels could at best be net zero, such options not only displace fossil fuels, but also may provide sufficient economic benefits to accelerate the development and deployment of DAC technologies.

3.1. Geological Storage

In order to limit the release of CO₂ into the atmosphere and its greenhouse gas contribution to global warming, carbon sequestration can be used as a strategy for storing CO₂ in deep geologic formations. In 2021, the CO₂ Storage Resource Catalog estimated that the total potential storage capacity of CO₂ resources worldwide was roughly 13,000 GtCO₂ [90]. Geological carbon sequestration is the process of storing CO₂ in naturally occurring pore spaces in rock formations that operate as long-term CO₂ storage reservoirs [91]. Ideal conditions for geological storage are sedimentary basins with a caprock above with minimum thickness of 20 m, a CO₂ injection of at least 800 m deep (for CO₂ to be in supercritical state) and less than 2500 m [92]. The National Academy of Sciences conducted a thorough investigation of the price of carbon storage and determined that the levelized price range would be between USD 8.6 and USD 20.4/tCO₂, realizing that the cost of carbon storage is largely affected by pipeline needs and economies of scale [3].

3.2. Enhanced Oil Recovery (EOR)

Oil fields often undergo many phases of production. Natural pressure drives oil up the wells during the primary production phase. The pressure in the reservoir is raised in the secondary phase by using pumping fluids, such as water or natural gas, forcing more oil to the production wells. CO₂-EOR can be used in the tertiary phase, aiming to change the characteristics of the oil or the flow pattern to boost the recovery of the remaining oil. CO₂ interacts with oil, making it easier (e.g., changing the viscosity) for it to flow to the production wells. The resulting oil contains some CO₂, which is recovered and re-injected back in the reservoir [93].

EOR can recover up to 15–20% of the original field, and it accounts for about 3.5% of US domestic oil production annually [94]. EOR now utilizes around 80 MtCO₂/year, which is second only to the production of urea, which requires about 130 MtCO₂/year. The International Energy Agency (IEA) estimates that a net 0.19 tCO₂ is stored for each oil barrel produced using CO₂ that has been captured [93]. According to a recent study conducted by the United States National Energy Technology Laboratory (NETL), EOR may extract over 67 billion barrels of oil from commercially recoverable deposits. This estimate was predicated on the possibility of capturing 20 Gt of CO₂ from factories and other industrial sources. EOR may recover up to 40% of residual fossil fuel, while CO₂ is permanently captured and stored in the reservoir [95]. However, it appears paradoxical to use captured CO₂ to extract more oil that produces CO₂ through combustion, especially if the CO₂ is taken from the air using DAC. In this vein, the IEA has emphasized that, in order to meet the targets of the Paris Agreement, no new investments in fossil fuels should be undertaken, necessitating the discovery of alternative, economic, and environmentally sound uses for CO₂ [96].

3.3. Fuels and Chemicals

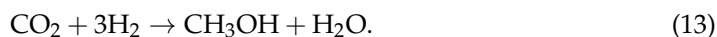
The production of fuels (e.g., gasoline, diesel or jet fuel) and chemicals (e.g., methanol, methane, formic acid or formaldehyde) from captured CO₂ is gaining momentum [97]. These synthetic fuels and chemicals are capable of directly or indirectly displacing traditional fossil fuels. In the case of fuels, the present transport infrastructure may still be utilized for the foreseeable future, and they might assist in decarbonizing difficult-to-abate sectors such as marine and air transport. Due to its high stability, thermodynamically unfavorable processes are needed to convert CO₂ into these chemicals, implying additional energy and hence costs [1].

Synthetic fuels and chemicals, e.g., through the Fischer–Tropsch synthesis, can be produced using syngas, a combination of H₂ and CO [98]. CO₂ reforming (also known as dry reforming) is an alternate way to produce syngas by combining two of the most significant greenhouse gases, CO₂ and methane (CH₄) (see Reaction (11)) [99]. Dry reforming requires high temperatures (900–1200 K) and may suffer from soot deposition which deactivates the catalyst; thus, it is not yet widely utilized [100]. Reverse water gas shift (RWGS) is another

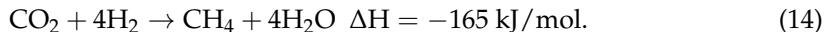
known CO₂ conversion method to syngas (see Reaction (12)), and various heterogeneous transition metal-based catalysts supported on metal oxides have been investigated between 200 and 600 °C [101–103].



Methanol is an important building block in the synthesis of olefins, dimethyl ether, and fuels, and is thus capable of displacing fossil fuels. In addition, methanol can be used as an energy carrier. As a liquid, it can be handled and transported more easily than gases or solids. Methanol is currently produced from syngas that, in turn, is created from fossil fuels. However, it can also be produced from CO₂ in one of the simplest processes available to convert CO₂ into liquid products [104,105]. Concentrated CO₂ can be hydrogenated over a metal or metal oxide catalyst (such copper (Cu), zinc oxide (ZnO), or aluminum oxide (Al₂O₃)) at relatively low temperature and pressure, about 225 °C and 50 bar, respectively, to produce methanol (CH₃OH) (see Reaction (13)). Renewable power to produce H₂ is required to make the methanol manufacturing process economically and ecologically sustainable [106,107].



CO₂ methanation is another viable method of using carbon dioxide [108]. Synthetic methane is an easily exportable fuel that may be used in the existing infrastructure for storage, transportation, and usage. CO₂ hydrogenation to methane over nickel catalysts was proposed more than 100 years ago via the Sabatier reaction, Reaction (14). The reactant H₂ can be generated from water electrolysis using grid electricity or renewable electricity [109].



Urea, formic acid, cyclic carbonates, and salicylic acid are the other most typical compounds produced from CO₂ [110]. However, few studies have explored the conversion of CO₂ captured from ambient air to these compounds [111].

3.4. Mineralization

Mineral carbonation involves the interaction of CO₂ with metal-containing materials, such as naturally occurring minerals or alkaline industrial waste [112]. In this utilization, CO₂ reacts with minerals rich in Ca and Mg to form carbonates, such as calcite (CaCO₃), magnesite (MgCO₃), dolomite (CaMg(CO₃)₂), and a host of metastable, hydrated carbonate minerals, such as hydro magnesite (Mg₅(CO₃)₄(OH)₂·4H₂O), nesquehonite (Mg(HCO₃)(OH)·2(H₂O)), dypingite (Mg₅(CO₃)₄(OH)₂·5H₂O) or hydrotalcite (Mg₆Al₂CO₃(OH)₁₆·4H₂O). At upper crustal pressures and temperatures below 300 °C, silicate minerals react with aqueous fluids to form talc (Mg₃Si₄O₁₂(OH)₂), brucite (Mg(OH)₂), serpentine (Mg₃Si₂O₅(OH)₄), and other hydrous phases. Excess magnesium creates brucite (Mg(OH)₂) in rocks with a magnesium to silicon ratio greater than 1.5. Hydrous silicates and brucite may also combine with CO₂ to generate carbonates [113]. Carbonate has a substantially lower standard Gibbs free energy than CO₂, implying that CO₂ storage by mineral carbonation is stable and permanent [114].

3.5. Biological Utilization

Biological utilization depends on living organisms using solar energy to convert CO₂ into organic carbon during photosynthesis, which is an indirect way of carbon sequestration. This environmentally friendly process turns CO₂ into value-added goods, such as bioethanol, through further processing [115].

Microalgae are seen as a potential alternative to terrestrial plants made of starchy and lignocellulosic materials for the production of biofuels, which could replace fossil fuels

and reduce GHG emissions [116]. The benefits of CO₂ conversion using microalgae are as follows: high photosynthetic efficiency, low concentration CO₂ sequestration applicability, quicker sequestration rate, reduced land usage, co-production of food, fuel, fine chemicals, etc. The majority of microalgae culture currently relies on flue gas as a source of carbon, but NO_x and SO_x in the gas hinder microalgae growth [117,118]. When CO₂ from DAC is used to produce microalgae, the impacts of gas toxicity are eliminated and site flexibility is increased. Additionally, the purity of CO₂ used as a feedstock for microalgae growth should be in the range of 5–35 vol.%, which is lower than most alternatives for CO₂ use, such as EOR and fuel synthesis, resulting in less energy-intensive processes [119].

Human food, protein-rich feed for animals, and slow-release fertilizer may all be made from autotrophic microbial biomass produced from CO₂ that has been captured. These are mostly accomplished by the absorption of H₂-oxidation bacteria which utilize CO₂ and hydrogen to generate carbonaceous chemicals and energy carriers [120,121].

4. DAC Companies

DAC-focused companies emerged as early as 2009, but many of the current players were only founded in the last 4 years. While companies that emerged from research institutions are working to develop their innovations, others are focused on adapting existing technologies from more mature industries for DAC. In this section, we provide an overview of the technology used and level of commercialization reached of several DAC companies. Table 2 summarizes important information about the DAC companies considered here.

4.1. Liquid Sorbent Technology

4.1.1. Carbon Engineering

Carbon Engineering (CE) was founded in Calgary, AB, Canada in 2009 and has since moved their headquarters to Vancouver, BC, Canada. The company developed a technique for carbon capture that combines KOH and Ca(OH)₂ solutions with a dual chemical loop similar to the one described above [26]. Since 2011, the company has been running a prototype, and since October 2015, it has been operating a demonstration plant in Squamish, BC, Canada with a capacity of 1 tCO₂/day [12]. In the Permian Basin of Texas, a commercial facility with a 1 MtCO₂/year collection capability is under construction and expected to be completed in late 2024. The CO₂ captured will be used for Enhanced Oil Recovery [122].

The KOH aqueous solution is used in the company's absorption process. The conventional closed counter-flow tower is replaced by an open-air contactor with a cross-flow and slab design, where air is forced horizontally and perpendicularly to the solution at a speed of 1.3 m/s. The aqueous solution flows downhill along a PVC structured packing. This new air contactor design allows for reduced fan power (hence a lower operating cost) and smaller absorber size (hence a lower capital cost). Instead of using a standard precipitator, a pellet reactor is used. The K₂CO₃ solution from the air contactor flows downwards and reacts with a slurry containing a 30% Ca(OH)₂ injected from the bottom. Natural gas is used to heat the calciner to the regeneration temperature of 900 °C, resulting in 0.48 tonnes of additional CO₂ generated by the process for every tonne of CO₂ captured from the air. All the CO₂ leaves the calciner at a purity of 97.1%, dry basis [12]. A fully electrical method is also being proposed by the business, in which high-temperature electrical heating would supply the thermal energy for calcination [27]. Rather than storage, CE has suggested a different method to handle the isolated CO₂, which is known as "thermo-catalysis". In this method, collected CO₂ interacts with renewable hydrogen produced by water electrolysis to create synthetic fuels like gasoline, diesel, and jet fuel. CE's pilot plant in British Columbia is also testing this process.

4.1.2. Carbon Blade

Established in 2021 in San Diego, CA, USA, Carbon Blade uses technology developed by RoCo® [123] which combines a sodium hydroxide (NaOH) solution and electrodialysis

bipolar membrane (EDBM) technology for regeneration [124]. All equipment, including integrated wind turbines, solar panels and rechargeable batteries to power this system, are designed to fit within or attached to the DAC container which can be placed at a carbon utilization or storage site. In 2022, the company created its first gas–liquid contactor prototype. For 2023, the company has plans for various levels of testing in Iceland and California, with a goal for their first 1000 units to be in operation in 2025. Estimated cost is near USD 100/tCO₂ [124], and the energy requirement is up to 1.5 MJ/kg CO₂ compared to 3.5–4 MJ/kg CO₂ for liquid amine solvent systems [125].

The contactor is placed on a vertical rotor, allowing for rotation in low wind speeds much like a vertical axis wind turbine. The leaf-like contactor surface consists of sandwiched hydrophobic polymer membranes, which allows the passage of air and contact with the basic solution flowing on the inner surface of the membrane. CO₂ is captured as an aqueous sodium bicarbonate and is returned to the gaseous state using a reaction with sulfuric acid (H₂SO₄), which simultaneously creates water and sodium sulfate with CO₂. The CO₂ is separated while the sodium sulfate and water move onto the regeneration step with the help of bipolar membrane electrodialysis. While the contactor design takes advantage of natural convection even in low wind speeds to reduce overall system energy requirements, this is a trade-off for the rate of capture. The company estimates that wind speeds of 7–8 km/h are required to remove 1 tCO₂/day for a contactor surface area of 200 m² [125]. In addition, this liquid sorbent technology is likely to suffer the same concern of freezing conditions. Also, because water is an input into the system, this design is less suitable for arid locations.

4.1.3. Greenlyte Carbon Technologies

Greenlyte Carbon Technologies (GCT) is a spinoff from the Universität Duisburg-Essen in Germany. Founded in 2022, the company plans to complete its first 100 tCO₂/year demonstration plant named Greenberry 2 by September 2023 [126], install their first commercial demonstration plant in 2024, and partner with a hydrocarbon synthesizer to commission a 1 ktCO₂/year plant in 2026 [127]. GCT plans to build modular containerized systems that can be used for direct air capture or flue gas capture with a capture rate of 10 kg/h. The absorbent formulation can be adjusted to a specific CO₂ concentration.

In the GCT process, CO₂ is first absorbed with a liquid sorbent mixture consisting of water, polyethylene glycol (PEG) or polyols, and potassium carbonate, sodium carbonate, amino acids or mixtures of these components, to form a hydrogen carbonate. The liquid mixture can be tailored to operate within −30 °C to 50 °C. The hydrogen carbonate then undergoes either two-chamber or three-chamber electrolysis to generate gaseous oxygen, carbon dioxide, and hydrogen, or releases the CO₂ by applying waste heat [127]. The advantage of the three-chamber bipolar membrane process is that all gaseous products are generated within separate chambers, avoiding the need for a post-separation process. Alternatively, two-chamber electrolysis with a Ni(OH)₂ anode results in the O₂ binding to the electrode and only CO₂ and H₂ being initially released, which can be used in synthetic hydrocarbon production.

4.1.4. Mission Zero Technologies

Mission Zero was founded June 2020 as a spinout from Deep Science Ventures in London, Great Britain, that is currently focused on utilizing off-the-shelf technologies for fast DAC deployment. By 2024, they expect to have an integrated 1000 tCO₂/year capture and storage plant utilizing carbon storage company 44.01's peridotite mineralization technology in the Al Hajar mountains in Oman. Project DRIVE in the UK is another planned 120 tCO₂/year pilot capture and storage plant, integrating capture and manufactured limestone (M-LS) production using the process of O.C.O Technology [128].

The company uses an aqueous mixture containing cationic polymeric amine, polyethyleneimine (PEI), to absorb CO₂. The CO₂ reacts with water to form carbonic acid and subsequently dissociates into H⁺ and HCO₃[−]. Carbonic anhydrase or a zinc-cyclen catalyst

in the solution accelerates the ion formation process. The contactor is a gas sparger or a falling film reactor [129]. After leaving the contactor, the absorbent solution enters the electrochemical regeneration step where it passes over anion and cation exchange electrolyte beads to dissociate the H^+ and HCO_3^- from the capture solution. The ions then pass through their respective ion-exchange membranes into a second solution using either capacitive deionization ion-separation or electrodialysis. Both of these technologies are well established in the water purification industry. As the concentration of ions increase in the non-aqueous second solution, chemical equilibrium causes the ions to reform carbonic acid which dissociate into CO_2 gas and water. The CO_2 can be isolated at this point with a purity of 98% [130]. At least some of the anions in the second solution react with a mineral or salt to form a precipitated material that is released from the second solution. The core process energy consumption is less than 800 kWh/tCO₂ [131].

4.2. Solid Sorbent Technology

4.2.1. Climeworks

Climeworks, a Swiss company that is a spinoff of ETH Zurich established in 2009, is a significant DAC development company [16]. The company progressed from creating its initial prototype in 2013 to operating the first commercial facility in the world in 2017, with a 900 tCO₂/year capture capability, in Hinwil, Switzerland. The Climeworks design is scalable and modular, and one collector can capture 135 kgCO₂/day [132]. A Class II amine-functionalized sorbent, such as 3-aminopropylmethyldiethoxysilane (APDES), loaded upon nano fibrillated cellulose (NFC), is used by Climeworks (APDES-NFC-FD). By using temperature vacuum swing adsorption (TVSA) and waste heat from a nearby incinerator, regeneration is accomplished at a temperature of 100 °C. A complete cycle lasts 4–6 h. Another commercial facility which began operation in September 2021, dubbed Orca, is located in Hellisheidi, Iceland, and is able to capture and store CO₂ at 700 m underground with a capacity of 4000 tCO₂/year. The captured CO₂ is combined with water and pumped underground, where it interacts with basalt rocks via mineral carbonation. Climeworks collaborates on mineralization with the Icelandic company, Carbfix, which specializes in underground CO₂ mineralization. For the regeneration step of the adsorbent bed, waste heat from a geothermal power plant is used. Including its 14 pilot plants [73] across Europe, the company's total operating plant capacity is 6900 tCO₂/year [14], with another 36,000 tCO₂/year plant (Mammoth) expected to complete construction in 2024. The plants use renewable energy or waste heat to capture CO₂ for storage, fuel, food, and beverage manufacturing. For example, the 150 tCO₂/year pilot plant in Troia, Italy utilizes the CO₂ to make methane, while the plant in Dresden, Germany aims to capture CO₂ to create carbon-neutral fuels (mostly diesel) while also utilizing renewable energy for hydrogen generation [122]. In 2017 or prior, the company planned to have removed 225 MtCO₂ (approximately 1% of total global emissions) by 2025 [48], which is highly unlikely now. As of 2019, the company was capturing at USD 600–800/tCO₂ but has a roadmap to achieving USD 100–150/tCO₂ by 2030 [133]. In 2022, they were selling carbon credits at USD 1000/tCO₂, but this could drop to USD 300–400/tCO₂ by 2030 [134]. Climeworks plans to expand operations in the US and announced in 2023 that it applied to participate in three hubs as part of the US Department of Energy's (DOE) Regional Direct Air Capture Hubs program [135].

4.2.2. Global Thermostat

In 2010, a Columbia University professor founded Global Thermostat in New York (NY, USA), and in 2020, the company relocated to a new research and development headquarters in Colorado. The company uses a Class I amine-functionalized polymer (most recent patents use poly(allylamine) or poly(vinyl amine)) [136] on a porous ceramic honeycomb monolith structure for capture. The regeneration ideally uses waste heat from nearby industry and is based on TVSA with a desorption temperature of 60 °C to 120 °C, but preferably below 100 °C [136,137], and a pressure of 0.2 bar or below [138]. The process produces CO₂ with a

purity greater than 95% [139]. To date, the company has had four pilot plants from 2011 to 2021 [140], with the first located at the Stanford Research Institute (SRI) International in Menlo Park (California), having a capacity of 1000 tCO₂/year [48]. In April 2023, they unveiled a 1000 tCO₂/year commercial-scale demonstration plant in Colorado; however, the site does not yet have the capability to store the CO₂ and is therefore venting any captured material [141]. Future plans include a 100,000 tCO₂/year capacity plant (front-end engineering and design (FEED) is already underway) [140] and potentially a small DAC unit in Chile [141]. While the cost for their former pilot plant in Huntsville, Alabama was previously quoted as USD 150/tCO₂ [142], costs have since increased as the company now believes they can reach USD 300/tCO₂ in 2025 [143]. Cost and energy consumption for the Colorado plant have not been disclosed.

4.2.3. Hydrocell and Soletair Power

Hydrocell, located in Järvenpää, Finland, was created in 1993 and initially focused on fuel cell technology but eventually led to developments in DAC and heat exchangers. The company's technology consists of a HCell brush-type heat exchanger and regenerative CO₂ scrubber using amine-functionalized polystyrene spherical beads. The system fits into a conventional shipping container and can capture 1.387 tCO₂/year. A TVSA cycle is used, where the adsorption lasts approximately 20 h, followed by 15 min of air evacuation, and heating using a glycol–water heat exchanger system for 30 min [144]. Their TVSA regeneration temperature ranges from 70 °C to 80 °C (the lowest value among the other systems considered) [145] and a vacuum of 5 mbar is used [146]. From 2017 to 2018, the company supplied their DAC system for the Soletair demonstration plant led by the Lappeenranta-Lahti University of Technology (LUT) and the VTT Technical Research Centre of Finland. The plant incorporated a solar power system, DAC system, electrolysis hydrogen production, and synthetic fuel production using a Fischer–Tropsch process. The goal after the piloting phase was to use the synthesis units in future EU projects [147]. Hydrocell is partners with Soletair Power. Established in 2016, Soletair Power uses technologies developed by LUT and the VTT Technical Research Centre of Finland. The company is focused on integrating DAC into commercial building HVAC systems, both indoors and outdoors. The CO₂ is stored in containers and supplied to concrete manufacturers for permanent storage. The company is also involved in utilization technology development. In 2021, they demonstrated a compact methane production module at Expo 2020 Dubai and installed an outdoor DAC unit at the ZBT hydrogen and fuel cell center in Duisburg, Germany in 2022. In 2023, they installed their HVAC-integrated DAC system at seed funding company Wärtsilä's Sustainable Technology Hub building in Vaasa, Finland. The HVAC-integrated system can capture up to 20 tCO₂/year [148].

4.2.4. Skytree

Skytree was created in 2014 in Amsterdam, The Netherlands, as a spinoff from the European Space Agency incubator program. The capture process, using benzylamine-based ion-exchange resin beads supported on crosslinked polystyrene, is based on electrostatic absorption and moisturizing desorption at 60 to 80 °C, utilizing low-grade heat [149]. The company currently plans to offer two modular models with capacities of 10 kg/day and 200 kg/day. Target utilization include enhancing growth in controlled horticultural environments, algae cultivation, and building material mineralization [150]. In July 2023, the company announced its first commercial DAC units for Growy vertical farms in the Netherlands after successfully completing field tests [151].

4.2.5. Carbon Collect

Carbon Collect Limited, formerly Silicon Kingdom Holdings, was founded in 2018 in Dublin, Ireland. The company's Mechanical TreeTM technology was developed by Professor Klaus Lackner, director of the Center for Negative Carbon Emissions at Arizona State University (ASU). The Mechanical TreeTM is a tower over 10 m tall consisting of

150 stacked sorbent layers designed to allow the passage of wind through them, foregoing the need for powered air flow. Each stack is about 1.5 m (5 ft) in diameter and holds six “leaves” [152]. For regeneration, the tower retracts into the 2.7 m (9 ft) tall base. The system is designed to use TVSA, MVSA, or MTVSA depending on the climate conditions. The sorbent is an anionic exchange resin such as quaternary ammonium functionalized poly(arylene ether sulfone) with iodide counterion [153] or quaternary ammonium functionalized polystyrene [154]. For MVTSA, the chamber is first partially evacuated to remove air contamination and then the water in the inner conduit is heated to 40–100 °C to create sub-atmospheric steam to release the CO₂ [155]. The CO₂-rich gas (5 kPa [155], or about 1% concentration [156]) and water vapor are collected. The CO₂ is then isolated by reacting CO₂ with sodium carbonate to form sodium bicarbonate [156]. NaHCO₃ may then undergo heating [156] or an electrochemical process to regenerate and release the CO₂ [154] at a purity between 95% and 99.9% [157]. The remaining water vapor is condensed, and energy is recovered. Depending on the ambient wind, sorption may take 30 to 60 min.

The first commercial-scale machine was installed at ASU’s Tempe campus in Q1 2022 with a capacity of 90 kg/day if ran continuously, and the company plans to initially deploy farms with a 1000 tCO₂ capacity [152]. A total of 250 large-scale Mechanical TreeTM farms can capture 1 GtCO₂ [158]. While the company is currently aiming for below USD 100/tCO₂ at full commercial scale, Lackner believes his technology could eventually bring the cost of carbon down to USD 30/tCO₂ [159]. Using MVTSA, the system consumes less than 70 kJ_e/mol or 440 kWh/tCO₂ [155].

4.2.6. Carbon Capture

Founded in 2019 in Los Angeles, CA, USA, Carbon Capture Inc. is focused on deploying deeply modular DAC systems designed for high-volume manufacturing and quicker development cycles. In October 2021, the company announced a feasibility study for a planned pilot project at the proposed Tamarack nickel mine near Duluth, Minnesota [160]. In September 2022 they announced Project Bison, a partnership with Frontier Carbon Solutions, to capture 5 MtCO₂/year by 2030 and inject it into Class VI wells for permanent storage in deep saline aquifers in Wyoming [161]. While the company has patents for using zeolites as their adsorbent, they have intentionally designed their system to accept a variety of sorbents including but not limited to amines and MOFs [162]. The company uses at least 25% by volume of CO₂ as the heat transfer medium for the temperature vacuum swing regeneration of the zeolites. Dry CO₂ is produced by condensing the moisture from the gas [163].

The DAC system runs at minimum in pairs to overcome the hydrophilic nature of zeolites. The incoming air first passes through a desiccant containing rotating wheel to remove 80–95% of the moisture from the air before the first DAC module captures the CO₂ and the remaining moisture. The desiccant is regenerated via a reverse dry air swing process where the dry air exiting a second DAC module passes through the first desiccant wheel; this method takes advantage of the water concentration difference between the desiccant and the exiting air stream rather than thermal energy. The desiccant wheel from the second stream is regenerated by the air exiting the first DAC module. The moisture from both desiccants is released back into the ambient air [164].

4.2.7. Verdox

As a spinoff from the Massachusetts Institute of Technology, Professor T. Alan Hatton, a specialist in electrochemical processes and separation, and Dr. Sahag Voskian first published their technology in 2019 in *Energy & Environmental Science* [82,165] and subsequently formed Verdox to commercialize their electro-swing adsorption technology. In early 2021, the company began testing its technology with aluminum manufacturer Norsk Hydro with a goal of reaching industrial scale by 2030. Norsk Hydro has a minority ownership of Verdox [166].

Verdorex uses a reduced polyanthraquinone adsorbent in a sandwich electrode structure. In each sandwich center is a ferrocene electrode layered between two electrolyte membrane separators, followed by a quinone electrode on either side. Each electrode is synthesized by impregnating a non-woven carbon fiber mat with either a quinone- or ferrocene-carbon nanotube-polymer solution. The porous electrodes are assembled and lastly moistened with a liquid salt electrolyte. CO₂ adsorption is triggered when voltage is applied, initiating a redox reaction where the ferrocene is oxidized and polyanthraquinone is reduced. In its reduced state, the quinone has a high affinity for CO₂, and this affinity is reversed by applying voltage in the opposite direction to release the CO₂ [167].

Lab tests showed a capture rate of 90% for CO₂ concentrations of 0.6 to 10%, a capture capacity drop of 30% over 7000 charge-discharge cycles, and the energy use of 1 GJ/tCO₂ captured or 40–90 kJ/mol CO₂ [82]. Projected capital and operating costs are USD 50–100/tCO₂ [167].

4.2.8. TerraFixing

TerraFixing is a Canadian company founded in 2020 in Ottawa, ON, Canada. The company utilizes proprietary zeolites for CO₂ adsorption with a capture capacity of approximately 1.0–2.5 mmol/g, where capacity increases as temperature decreases [168]. Their zeolites also tout a lower heat of sorption than Climeworks, Global Thermostat and Heirloom, reducing energy requirements to 1 MWh/tCO₂ [168]. If electricity cost is USD 0.03/kWh or less, the company can capture CO₂ for USD 40/tCO₂ or less [169]. To take advantage of thermodynamics, the company is focused on deployment in cold and dry climates including Canada, Norway, Alaska, Russia, Finland, Greenland, Tibetan plateau, and Antarctica. Access to and price of renewable energy varies widely between these locations.

Incoming air passes through a particulate filter, water capture bed, and CO₂ adsorbent bed. Desiccant in the water capture bed dehumidifies the air to ensure water is not adsorbed by the zeolites. A five-step cycle is used: adsorption, blowdown, evacuation, pressurization, waterbed regeneration. The blowdown removes weakly adsorbed components of N₂, O₂, and Ar by applying a vacuum, the evacuation steps release the adsorbed CO₂ via a temperature-vacuum swing, and then dry air is pushed through the adsorbent bed in the reverse direction to return the bed back to ambient pressure. This dry air picks up the residual heat from the CO₂ desorption step and flows through the water capture bed to regenerate the desiccant [170].

4.2.9. Noya

Noya was founded in 2020 in San Francisco, CA, USA. The company's initial aim was to take advantage of various types of existing cooling tower infrastructures ranging from commercial buildings to industrial cooling towers. In August 2021, Noya's first pilot plant was installed in San Leandro, California at Alexandre Family Farm, where an estimated 0.55–1.1 tCO₂/year is captured as heat is removed from the dairy pasteurization process [171]. CO₂ captured using this method costs less than USD 100/tCO₂ [172]. In 2022, the US Inflation Reduction Act increased the incentive for geologic storage to USD 180/tCO₂ for companies that capture 1000+ tCO₂ per deployment, which resulted in Noya pivoting towards developing modular DAC systems in Q4 2022, which can be sited at geologic storage locations [173].

Despite the pivot, aspects of their technology have not changed. The DAC system utilizes activated carbon monolith supports [174] for their sorbent, and a temperature-vacuum swing is used for regeneration. The sorbent material may include MgO, Al₂O₃, K₂CO₃, activated carbon, monoethylamine, glycine or sarcosine.

4.2.10. Heirloom Carbon Technologies

Heirloom was founded in April 2021 in San Francisco, CA, USA. The company uses alkaline solid Ca(OH)₂ powder (limestone) on large trays, stacked vertically to minimize land area requirements and increase air-to-sorbent contact. By using natural convection,

they avoid using fans to force air through the contactor, which reduces energy use to less than 0.05 GJ/tCO₂ from 0.5–1 GJ/tCO₂ [175]. The capture and regeneration processes follows a similar method as that of aqueous Ca(OH)₂, where CaCO₃ is formed upon reaction with CO₂ and then undergoes calcination at 900 °C and hydration regeneration steps (see Reaction(4)). Where their process differs is in the use of an electric kiln to avoid additional generation of CO₂ from direct fossil fuel burning in their process [176].

The carbonation process requires less than 3 days for 85% carbonation, even at low wind speeds. Heirloom has a long-term target of USD 50/tCO₂ removed [177], and while they currently use 2500 kWh/tCO₂, they have targeted total energy requirement of less than 1500 kWh/tCO₂, or 54 GJ/tCO₂ [175,178]. Key areas of interest for deployment in the US based on existing low-carbon power plants, power plant capacities, and limestone sources include San Francisco, Columbia River Valley in Washington, and East Texas and Louisiana. The humidity of these regions is also advantageous due to the ability to accelerate the rate of CO₂ uptake [48]. In February 2023, captured CO₂ from Heirloom’s headquarters in Brisbane, California was permanently stored in concrete in partnership with CarbonCure and Central Concrete. In March 2023, non-profit science and technology development company Battelle in collaboration with Heirloom and Climeworks submitted a proposal to the US DOE for Project Cypress DAC Hub in Louisiana [179].

4.2.11. Sustaera

Sustaera spun off from the US research and development company Susteon in June 2021 and is based in Durham, NC. The company utilizes a low-cost sodium carbonate-based adsorbent on a monolith substrate. The monolith reduces pressure drop during capture, reducing the power required to move air through their contactor. While their current bench scale unit captures 1–2 kgCO₂/day, their commercial units capture about 8 tCO₂/day or less than 3000 tCO₂/year. Each unit contains 16 modules and each module contains approximately 400 monoliths. A regeneration temperature of ~80 °C is used and the systems use only solar and wind energy. The adsorbent has a desorption energy requirement of about –65 kJ/mol. The company has chosen to use widely available materials so that no new infrastructure needs to be developed. Its first 300 tCO₂/year pilot project is underway, with expected operation in 2023. In 2024, they plan to operate 3000 tCO₂/year commercial units and continuously scale up from there. While their first module cost is about USD 175/tCO₂, they expect to reduce that to USD 100 or less at commercial scale [180].

4.2.12. Octavia Carbon

Founded in 2022, Octavia Carbon is the Global South’s first DAC company, headquartered in Nairobi, Kenya. The company leverages Kenya’s basaltic geology and highly renewable powered grid, including geothermal and hydropower, which make it ideal for both CO₂ capture and carbon mineralization. Its Wangari 1 pilot plant is planned to be operational by 2024, with a capacity of 1000 tCO₂/year [181]. In July 2023, the company also announced another 1000 tCO₂/year pilot called Project Hummingbird, in partnership with carbon mineralization company, Cella, to be built in Kenya’s Rift Valley [182]. Once scaled to 40,000 tCO₂/year, the expected carbon credits sale price is between USD 300 and 500/tCO₂ [183]. Few technological details have been disclosed; however, it is speculated that it will be very similar operationally to Climeworks’ Orca plant in Iceland, utilizing waste heat from geothermal power production for the regeneration process.

Table 2. DAC Company Information Summary.

Sorbent State	Company	Sorbent	Desorption Method	Capacity (CO ₂ /year) ¹	Capture Cost (USD/tCO ₂)	Country of Origin	Representative Patent(s) ²
Liquid	Carbon Engineering	KOH	Calcination	365 t; 500 kt-1 Mt (2024)	USD 94–232	Canada	[184,185]
Liquid	Carbon Blade	NaOH	EDBM	1000 units (2025)	~USD 100	United States	[125]

Table 2. Cont.

Sorbent State	Company	Sorbent	Desorption Method	Capacity (CO ₂ /year) ¹	Capture Cost (USD/tCO ₂)	Country of Origin	Representative Patent(s) ²
Liquid	Greenlyte Carbon Technologies	PEG or polyols, and K ₂ CO ₃ , Na ₂ CO ₃ , amino acids or mixtures of these	Electrolysis	100 tCO ₂ (Q4 2023); 1 ktCO ₂ (2026/2027)	Unknown	Germany	[186]
Liquid	Mission Zero Technologies	PEI (polyethyleneimine)	Electrochemical	1000 tCO ₂ (2024)	Unknown	Great Britain	[129]
Solid	Climeworks	Amine-functionalized nanofibrillated cellulose	TVSA	6.9 kt; 42.9 kt (2024)	USD 600–800; USD 100 (2030)	Switzerland	[187–189]
Solid	Global Thermostat	Aminopolymer	TVSA	1 kt CO ₂ ³ ; 100 kt CO ₂ (under FEED)	USD 300 (2025)	United States	[136–139]
Solid	Hydrocell/Soletair Power	Amine-functionalized polystyrene spherical beads	TVSA	20 t	Unknown	Finland	[145,190]
Solid	Skytree	Benzylamine-based ion-exchange resin beads	TSA	10 Mt cumulative capture (2030)	Unknown	Netherlands	[191]
Solid	Carbon Collect	Ammonium functionalized polymer	MVTSA (TVSA and MVSA capable)	33 t	USD 100 target	Ireland	[153,154]
Solid	Carbon Capture	Zeolites	TVSA	5 Mt (2030)		United States	[163,164]
Solid	Verdax	Polyanthraquinone	Electroswing adsorption	Unknown	USD 50–100	United States	[191–193]
Solid	TerraFixing	Zeolites	TVSA	Unknown	USD 40 ⁴	Canada	[170]
Solid	Noya	May include MgO, Al ₂ O ₃ , K ₂ CO ₃ , activated carbon, monoethylamine, glycine or sarcosine.	TVSA	~1 t	<USD 100 ⁵	United States	[194]
Solid	Heirloom	Limestone Ca(OH) ₂	TSA	Unknown	USD 50 target	United States	[195]
Solid	Sustaera	Sodium carbonate supported on monolith	TSA	300 ton (2023); 3000 ton (2024)	USD 175; ≤USD 100 target	United States	[196,197]
Solid	Octavia Carbon	Unknown	Not disclosed, likely TSA	1000 tCO ₂ (2024)	USD 300–500	Kenya	Not available

¹ Capacity may include current and planned capacity. ² Active or pending patents applicable to DAC. Not an exhaustive list of patents. ³ Only includes most recent pilot plant. ⁴ Assuming electricity cost of USD 0.03/kWh. ⁵ Cost prior to company pivoting business plan. See section on company.

5. DAC Energy Demand and Cost

Reducing energy demand and cost is essential for a large-scale deployment of DAC. Both gross cost of capture and the net removal cost of capture may be reported in the literature [3,48]. Gross cost of capture is the cost per unit of CO₂ at which the CO₂ must be sold in order to cover the process of removal. The net removal cost of capture takes into account the net life-cycle emissions of the capture process, including upstream emissions and is, therefore, higher than gross cost [48].

The key variables that affect DAC cost are described below:

- Capital cost, which involves the cost of equipment and the cost of land. The plant's capacity affects these factors.
- Operating costs are the costs associated with running a business, or with running a machine, part, piece of equipment, or facility. Energy, equipment maintenance, and labor costs are critical elements in DAC plants.
- Every technology has certain unique costs attached to it. The cost of the solid sorbent and the lifetime of solid sorbent are crucial in solid sorbent technology. Since reaction efficiency is never 100%, liquid technology requires make-up inputs, such as water and sorbent [12]. In DAC plants, the air contactor's design is also crucial. Adding several fans to increase the air velocity in the air contactor improves the plant's performance but adds to the capital and operating cost.

The mean energy requirement for operation of either solid sorbent or liquid solvent DAC methods consists of approximately 80% thermal energy and 20% electrical energy; therefore, the source of energy is a major aspect influencing both net carbon removal and the cost of DAC systems [73,198]. For solid sorbent systems, estimated heating requirements are 2.9–5.5 GJ/tCO₂ and the electricity requirements are 0.6–1.1 GJ/tCO₂ [14]. The largest consumer of energy in solid sorbent systems is the regeneration process, including thermal energy to heat both the sorbent and contactor, and electrical energy for the vacuum pumps to remove residual air from the contactor, if VSA/TVSA is used. It has been estimated that sorbents with lower regeneration energies may decrease thermal energy needs by 3 GJ/tCO₂, with certain sorbents claiming regeneration energies as low as 1 GJ/tCO₂ [12,198–200]. The contactor fans, which are needed to counteract the pressure loss through the contactor, are also a major consumer of electricity [3], although it should be noted that some DAC companies have purposely designed contactors relying on natural ambient convection to eliminate this power demand [124,152,177].

Thermal energy needs for the liquid solvent systems have been reported to range from 5.25 to 8.1 GJ/tCO₂, with electricity requirements of 1.3 to 1.8 GJ/tCO₂ [14]. The range of energy requirements stems from differences in the packing material and contactor configuration utilized in the liquid solvent DAC process [12,201]. The highest energy usage in conventional liquid DAC processes occurs during the thermal regeneration of CaO in the calciner which produces high-purity CO₂. The energy to dry and warm the CaCO₃ pellets prior to feeding into the calciner comes in second [3]. Electrochemical systems may be able to reduce the cost of regeneration for liquid solvent systems. For example, the calciner in Carbon Engineering's pilot plant uses 5.25 GJ/tCO₂ released from calcination [12], whereas the minimum separation energy needed for BPM is ~2.73 kJ/tCO₂ for bicarbonate and ~5.45 kJ/tCO₂ for carbonate [81].

Current cost estimates from DAC companies vary widely, as shown in Table 2, and not all have released the information. Companies founded earlier generally have higher reported costs. Climeworks' first commercial plant reported an actual cost of USD 600/tCO₂ [202]. Carbon Engineering's estimated cost for a ~1 MtCO₂/year plant based on their pilot is USD 94–232/tCO₂ [12]. Global Thermostat has not released energy or cost information for its most recent demonstration plant in Colorado but estimates they can decrease their costs to USD 300/tCO₂ by 2025 [143]. Companies established more recently have the benefit of learning from these pioneer companies and generally have lower estimated costs. TerraFixing, under cold climate conditions, has estimated USD 40/tCO₂ assuming an electricity cost of USD 0.03/kWh [169]; however, securing such low electricity costs in their ideal climate zones may pose a challenge. For instance, the 2022 costs of electricity in Iceland and Finland for a >15,000 kWh consumption was USD 0.079 and USD 0.16, respectively, with all taxes and fees included [203]. Electricity costs in Canada vary widely, with Manitoba on the low end at ~USD 0.078/kWh and the Nunavut at the high end with ~USD 0.47/kWh in 2018, including fees and taxes, for residential consumption of 2000 kWh [204]. Assuming large consumer rates are half of residential rates, the rates are still above USD 0.03/kWh. Noya's original business plan of retrofitting cooling towers with DAC modules was estimated to be less than USD 100/tCO₂ [172], but changing their business plan towards the deployment of DAC at geologic storage sites will likely increase capital costs.

In addition to company-specific cost estimates, several research institutions have evaluated cost estimates for different DAC technologies, as listed in Table 3. Comparing the upper limit of estimated costs, modeling shows that liquid sorbent-based DAC has the potential to cost more than solid sorbent-based DAC. Given the high energy demand to run DAC, the cost of different energy sources has also been examined in the literature (see Table 4). For instance, the modeled net removal cost of capture for a liquid DAC system using electricity from wind and heat from natural gas is USD 156–293/tCO₂, and for a solid DAC system it is USD 113–326/tCO₂. Using natural gas for both electricity and heating provides USD 199–357/tCO₂ for liquid DAC systems and USD 124–407/tCO₂

for solid DAC systems [3]. If an electric calciner is used in a liquid DAC system, the estimated cost using geothermal power is USD 270–480/tCO₂ [205]. While emission-free power sources like geothermal, solar, wind, and nuclear energy are desirable, plant location may dictate the use of natural gas or coal for the provision of heat, particularly for high-temperature regeneration processes like calcination [27]. The rise of hydrogen as a fuel source could eventually replace fossil fuels, but it only makes sense to do so if it is generated from a carbon-free source. For solid sorbent systems, waste heat from other industrial processes could be used, but this may not align with storage locations. Also, if the industrial process emits CO₂, then flue gas capture makes more sense.

Table 3. Summary of DAC cost from research organizations.

Research Institution, Publication Year	Sorbent/Solvent	Net Removal Cost USD/tCO ₂	Capture Cost USD/tCO ₂	Comments	References
The American Physical Society, 2011	Alkaline NaOH	610–780	430–550	1 MtCO ₂ /year	[206]
Georgia Institute of Technology, 2012	Amino-modified silica adsorbent, TRI-PE-MCM-41	-	94.3–113.1	TSA regeneration	[207]
University of Twente, 2013	Davisil 646—TEPA Diaion HP2MG—TEPA PEI 60k—PMMA	-	150–200	Electricity cost: USD 0.1/kWh	[208]
ETH Zurich, 2013	Liquid sorbent—NaOH	518–610	376–430	1 MtCO ₂ /year Air contactor: Counter flow	[201]
Chemical Engineering Royal Military College of Canada, 2014	Liquid sorbent- NaOH	-	309–580	1 MtCO ₂ /year Contactor Type: Counter flow	[209]
University of Nottingham, 2014	PEI-silica adsorbent	152–425	91–227	40 tCO ₂ /day TSA regeneration	[210]
Potsdam Institute for Climate Impact Research, 2015	Alkaline NaOH	-	Near term total cost: 100–550 Long term total cost: 40–140	-	[211]
Georgia Institute of Technology, 2017	MIL101(Cr)-PEI-800	-	75.0–140.0	TVSA regeneration Lifetime of adsorbent: 3 years	[212]
	mmen-Mg ₂ (dobpdc)	-	60.0–190.0	TVSA regeneration Lifetime of adsorbent: 3 years	
National Academy of Sciences, 2018	Solid sorbent	89–877	88–228	Cost and energy demand depending on source of electricity and thermal energy	[3]
	Liquid sorbent	165–506	141–501	Cost and energy demand depending on source of electricity and thermal energy	
Harvard School of Engineering and Applied Sciences, 2018	Alkaline KOH	-	94–249	Air contactor: cross-flow packing (designed by CE)	[12]
CSIRO Energy, 2020	MEA	-	273–1227	Electricity cost: USD 20–USD 200/MWh Heat cost: USD 2–USD 20/GJ Plant life: 15–25 years Capital expenditure: ±30% Capture amount: 2300 tCO ₂ /year	[34]
Technische Universiteit Eindhoven, 2021	Alkaline KOH	-	419	Heat costs = USD 5 cents/kWhth Electricity costs = USD 10 cents/kWhel Plant costs = USD 25,000/m ³ Air contactor: cross-flow packing (designed by CE)	[213]
	MEA, aqueous Amine	--	537	Heat costs = USD 5 cents/kWhth Electricity costs = USD 10 cents/kWhel Plant costs = USD 25,000/m ³ Air contactor: cross-flow packing (designed by CE)	
National Energy Technology Laboratory, 2022	Solid (Monolith)	702	616	100,000 tCO ₂ /year Electricity price: USD 60/MWh	[47]
	Solid (Monolith)	430	-	1 MtCO ₂ /year Electricity price: USD 60/MWh	
	Solid (Packed Bed)	475	-	100,000 tCO ₂ /year Electricity price: USD 60/MWh	

Table 4. Cost comparison based on source of electricity and thermal energy.

Source of Energy		Liquid		Solid		References
		Net Removal cost (USD/tCO ₂)	Capture Cost (USD/tCO ₂)	Net Removal Cost (USD/tCO ₂)	Capture Cost (USD/tCO ₂)	
Electricity	Thermal					
Wind	Natural Gas	156–293	145–265	113–326	88–228	[3]
Solar	Natural Gas	165–293	145–265	113–326	88–228	
Natural Gas	Natural Gas	199–357	147–264	124–407	88–228	
Natural Gas/CCS	Natural Gas	230–400	220–390	-	-	[205]
Natural Gas/CCS	Electricity	300–490	330–560	-	-	
Solar	Electricity	480–840	430–690	-	-	
Wind	Electricity	380–610	360–570	-	-	
Geothermal	Electricity	270–480	250–440	-	-	
Power grid	Natural Gas	-	-	425	91	[210]
Natural Gas/CCS	Natural Gas	-	-	152	108	
Wind	Nuclear	-	-	227	227	

6. Conclusions and Outlook

A review of various DAC technologies was performed. Solid sorbent DAC is distinguished by its cyclic adsorption–desorption process and high sorbent flexibility, where considerations must be made for sorbent cost, CO₂ selectivity and degradation. Its low temperature regeneration requirement means thermal energy may be supplied by low-grade waste heat or renewable-based heat. In comparison, conventional liquid solvent DAC can run as a continuous process but has a more complex regeneration system requiring high temperatures. Water is a possible by-product isolated from solid DAC, whereas water is lost prior to the calcination stage of liquid DAC systems and, therefore, requires makeup water. While current solid sorbents rely mostly on micro- and mesopore structures to capture CO₂, the high customizability of MOFs could enable other mechanisms to improve capture capacity and CO₂ selectivity. Nonetheless, a balance of cost and performance needs to be considered and sorbent technology as a whole will benefit from further research to improve both these aspects. Electrochemical technologies are a promising alternative to the high-temperature regeneration process in liquid DAC systems, and many companies are investigating this approach to reduce overall energy needs. In addition, electrochemical direct capture systems and ion-exchange resins introduce new methods to capture CO₂ which use electro-swing and moisture swing desorption techniques, respectively. Air contactor design plays an important role in reducing overall pressure drop of the air passing through, thereby reducing energy and cost, while balancing surface area contact with the solvent or sorbent.

The high thermal and electrical energy requirements for DAC from non-GHG emitting sources is a major bottleneck to the success of DAC deployment. The use of an electric calciner or electrochemical regeneration could allow meeting all energy needs by electricity. More renewable plants will need to come online not only to replace fossil fuel powered generation, but to power DAC systems. Reliance on intermittent renewables alone could prove challenging without on-site storage systems. While many locations have promising capacity for renewables, location access and grid access can be a challenge that governments, grid managers, and companies will need to consider and plan ahead for.

In the last 4 years, there has been a significant increase in the number of companies developing DAC. Several DAC companies have already deployed pilot-scale DAC systems and at least one commercial scale plant. These systems have demonstrated the feasibility of DAC technology and have provided valuable data for future research and development. This research will be critical in reducing the current high cost of DAC systems. The entry of more DAC companies could benefit the industry through the introduction of novel technology, repurposing of established technologies, and opportunity for research partnerships.

Scaling up DAC systems to the level required to make a significant impact on global CO₂ emissions remains a significant challenge. To remove 10 GtCO₂/year, the current total

capacity of DAC projects in development will need to be 2000 times the current figure. Major funding for the industry and political support, such as the US Inflation Reduction Act of 2022, are vital to reaching the scale required as DAC companies are incentivized to build projects with an annual capacity of 1000 tonnes or greater in order to receive the tax credit of USD 180/tCO₂ for geologic storage or USD 130/tCO₂ for CO₂ utilization. However, funding for CO₂ removal technologies globally will need to increase 30 times by 2030 and by 1300 times by 2050 to achieve Paris targets [214]. Social acceptance of DAC is also a potential barrier, as it can be viewed as supporting continued fossil fuel use [1].

In conclusion, DAC technology is a promising solution to reduce atmospheric CO₂ concentrations and mitigate the impacts of climate change. While the technology is still in its early stages of development, researchers and companies are making significant progress in improving the efficiency and effectiveness of DAC systems. As more DAC companies enter the industry, increased collaborations or research partnerships are also expected to improve technology and accelerate the rate at which the industry expands. The authors predict accelerated rise in research and development of new, modified, or hybrid adsorbents, and of electrochemical technologies both in the areas of direct capture and regeneration of liquid sorbents due to the ease of integration with emission-free energy sources. With increasing concern over the environmental impact of greenhouse gas emissions, DAC technology has the potential to play a critical role in achieving net-zero emissions and addressing climate change.

Author Contributions: Investigation, M.H. and V.B. (equal contribution); writing—original draft preparation M.H. and V.B. (equal contribution); writing—review and editing, E.C.; supervision, E.C. All authors have read and agreed to the published version of the manuscript.

Funding: This research was funded by Environment and Climate Change Canada through the Climate Action and Awareness Fund, grant number EDF-CA-2021i010.

Data Availability Statement: This is a review paper and as such there are no new data being created.

Acknowledgments: For helpful discussions, the authors would like to thank Vanessa Schweizer, Juan Moreno-Cruz, Neil Craik, as well as Kasra Motlaghzade and Stephanie Cortinovis.

Conflicts of Interest: The authors declare no conflict of interest. This is a review paper; as such, the funder had no role in the design of the study; in the collection, analyses, or interpretation of data; in the writing of the manuscript; or in the decision to publish the results.

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