Review

Synopsis of Factors Affecting Hydrogen Storage in Biomass-Derived Activated Carbons

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Abstract: Hydrogen (H_2) is largely regarded as a potential cost-efficient clean fuel primarily due to its beneficial properties, such as its high energy content and sustainability. With the rising demand for H_2 in the past decades and its favorable characteristics as an energy carrier, the escalating USA consumption of pure H_2 can be projected to reach 63 million tons by 2050. Despite the tremendous potential of H_2 generation and its widespread application, transportation and storage of H_2 have remained the major challenges of a sustainable H_2 economy. Various efforts have been undertaken by storing H_2 in activated carbons, metal organic frameworks (MOFs), covalent organic frameworks (COFs), etc. Recently, the literature has been stressing the need to develop biomass-based activated carbons as an effective H_2 storage material, as these are inexpensive adsorbents with tunable chemical, mechanical, and morphological properties. This article reviews the current research trends and perspectives on the role of various properties of biomass-based activated carbons on its H_2 uptake capacity. The critical aspects of the governing factors of H_2 storage, namely, the surface morphology (specific surface area, pore volume, and pore size distribution), surface functionality (heteroatom and functional groups), physical condition of H_2 storage (temperature and pressure), and thermodynamic properties (heat of adsorption and desorption), are discussed. A comprehensive survey of the literature showed that an "ideal" biomass-based activated carbon sorbent with a micropore size typically below 10 Å, micropore volume greater than 1.5 cm^3/g, and high surface area of 4000 m^2/g or more may help in substantial gravimetric H_2 uptake of >10 wt% at cryogenic conditions (-196 °C), as smaller pores benefit by stronger physisorption due to the high heat of adsorption.

Keywords: hydrogen storage; activated carbon; surface morphology; thermodynamics; heat of adsorption

1. Introduction

Hydrogen (H_2) is the most abundant element in the universe. It is also the lightest element with a high energy content (142 MJ/kg of higher heating value), which makes it a sustainable and non-toxic energy carrier [1–5]. With its favorable fuel characteristics, the escalating demand of H_2 in the U.S. can be projected to be 63 million tons by 2050, which will be equivalent to 14% of the total energy demand [6]. Various methods have already been developed for H_2 generation, such as natural gas reforming, electrolysis, gasification, etc., and a few methods are in development, such as high-temperature water splitting, photobiological water splitting, etc. [7–15]. Although the current primary source of H_2 production is natural gas, it can be produced from coal and biomass.

Despite the tremendous potential of hydrogen generation and its widespread application, H_2 transport and storage remain two major challenges. Various efforts have been undertaken to store H_2 both chemically (metal hydrides, methanol, ammonia, etc.) [16–21] and physically (activated carbon (ACs) [4,22–29], metal organic frameworks (MOFs) [30–34], covalent organic frameworks (COFs) [35,36], etc.). Chemical storage is mainly used for long term H_2 storage where a high density of hydrogen can be stored in chemical

form (e.g., NH_3). However, the regeneration of H_2 after chemical storage is often energy intensive. On the other hand, a short-term H_2 storage option with a lower heat of hydrogen regeneration and higher H_2 recovery is crucial for vehicles and fuel cells. For fast kinetics and high reversibility of H_2 over multiple cycles, physical storage in porous material has proven more economically viable than chemical storage for short-term storage [37,38]. Among the porous materials, the most widely studied H_2 storage materials are MOFs and porous AC materials [39–41]. For example, AC material derived from cellulose acetate can store as high as 8.1 wt% at 20 bar and at −196 °C [42]. When comparing materials for physisorption of H_2, AC adsorbents have several distinct advantages over crystalline materials, which are related to their ease of availability, low cost, and superior chemical, mechanical, and thermal stabilities. In addition, ACs are easy to regenerate, have low densities (lightweight), fast kinetics, and tunable pore structures [3,43]. Most importantly, an abundance of biomass in nature and the configurable properties of ACs during the process of activation for enhanced H_2 adsorption have been emphasized in the literature [44–46].

This article presents a profound literature review to distinctly identify the most favorable characteristics of biomass-derived adsorption materials for H_2 uptake. As biomass-derived AC offers the opportunity to tune its properties, this article thoroughly investigated the following parameters: the surface morphology and functionality of AC, its thermodynamic properties, and the physical conditions while seeking a high H_2 uptake by the AC. This article also broadly highlights the recent developments in metal-doped activated carbon composites (spillover mechanism) to shed light on possible material modification in the practical application of hydrogen storage at ambient conditions.

2. Factors Affecting H_2 Storage in Biomass-Derived Activated Carbons

2.1. Role of Surface Morphology of Activated Carbons on H_2 Storage

H_2 adsorption capacity is governed by the factors that affect the adsorbate–adsorbent interactions. The most important factors in determining adsorptive H_2 uptake in porous materials are surface area, micropore volume, and pore size [47–60]. The mechanism for H_2 storage by means of physisorption is the van der Waals attraction between the surface of the ACs and the H_2 molecules [61]. On the other hand, the van der Waals interaction between the H_2 molecules is weak; therefore, to expect a few layers of hydrogen packing onto an adsorbent surface is impractical [62]. As the H_2 adsorption on AC will be a monolayer, a large specific surface area (SSA) is found to be beneficial for higher uptake. The ACs derived from different biomasses, along with their physiochemical properties, surface morphology, and hydrogen adsorption capacity at 77 K, are listed in Table 1. The significance of SSA for a substantial H_2 uptake is reflected in the increasing tendency from 2.1 to 8.9 wt% with the increase of SSA from 687 to 3771 m^2/g, as seen in Figure 1, which is also in line with several other literature that reached an analogous conclusion for biomass-derived AC [47–51,53,55,63–65]. From Table 1, to name a few examples, hemp stem, cellulose acetate, and melaleuca bark-derived activated carbons exhibit a trend of an increasing quantity of H_2 adsorbed in the range of 1.57–3.28 wt% (at 1 bar), 3.1–3.9 wt% (at 1 bar), and 1.21–3.91 wt% (at 10 bar) for a corresponding SSA of 922–3241 m^2/g, 2001–3771 m^2/g, and 1092–2986 m^2/g, respectively.
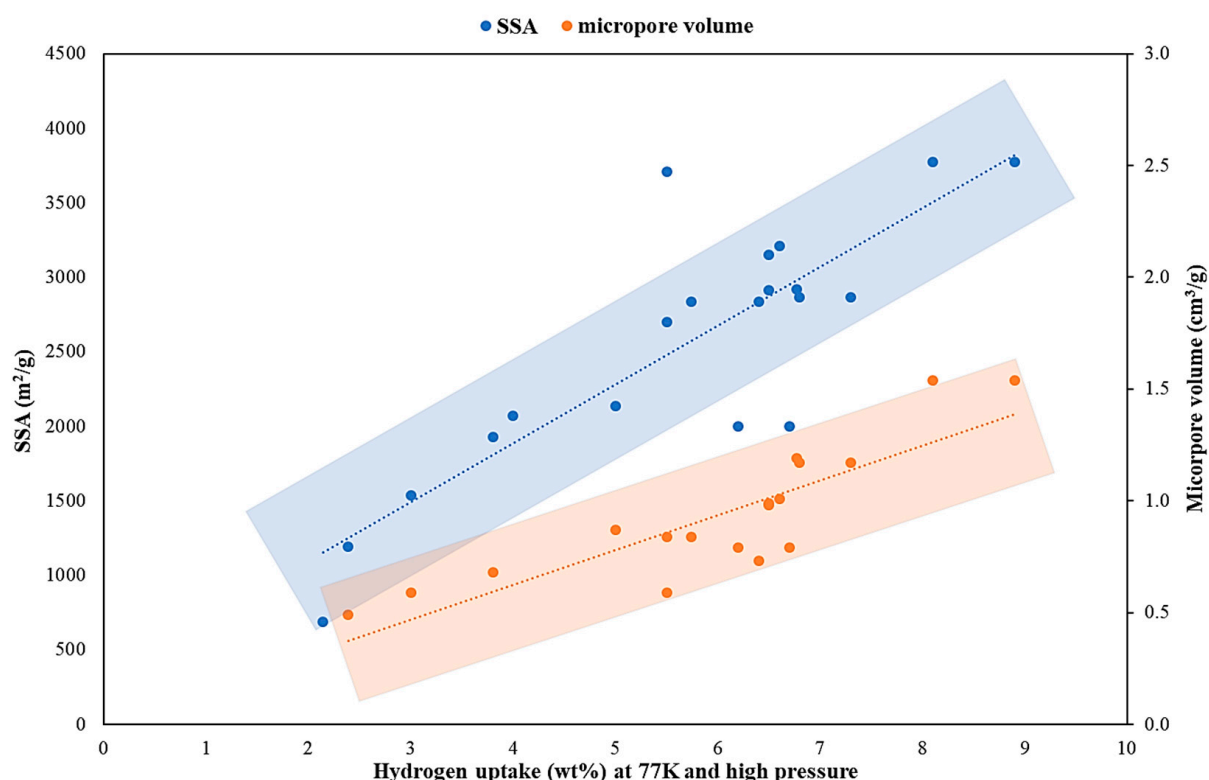
Figure 1. Correlation between the hydrogen uptake capacity at 77 K with high pressure and the micropore volume and specific surface area (data from Table 1).

However, correlating the H_2 uptake solely with SSA might not be adequate to justify the quantity of H_2 adsorbed. This is mainly because the different carbon materials exhibit different morphological properties, such as micropore volume, pore size distribution, and surface functionality. For example, it can be observed from Table 1 that the H_2 uptake capacity of beer lees-derived AC decreases with the increase in SSA, while doubling the SSA of hemp stem-derived AC barely enhances H_2 uptake by 10 wt%. In addition, beer lees and sword-bean shell-derived ACs have H_2 uptake capacities of 2.92 and 2.25 wt%, respectively, despite having a very similar SSA (SSA 1927 and 1930 m^2/g, respectively). A similar observation was reported by Yakobson et al. [62] and Ujjal Kumar Sur [66], where they reported 5.0 and 7.7 wt% of H_2 uptake, respectively, on graphene with a similar SSA (~2600 m^2/g). These examples clearly substantiate the necessity to rather consider the synergistic effect of the significant surface morphological properties of porous ACs.

In addition to SSA, presence of an adequate volume of small pores is another key factor that attributes to H_2 uptake. According to the International Union of Pure and Applied Chemistry (IUPAC), the pore sizes of the adsorbent are classified as macropores (pore radius, r > 50 nm), which exist at the entrance of the carbon materials and serve as carriers. At the same time, mesopores (2 < r < 50 nm) contribute to adsorption, whereas adsorption itself takes place on the micropores (r < 2 nm). The interaction energy between the H_2 molecules and carbon adsorbents can be enhanced by narrowing the pore size due to overlap of the potential fields from both sides of the pore wall to a degree determined by the pore width [67]. For smaller pores, the overlap of van der Waals potentials due to the atoms of the adjacent walls favors stronger physisorption [59]. The total interaction between the adsorbate molecule and a solid is greater if the molecule can interact with a larger number of surface atoms, as what happens in small pores [56,68]. Therefore, smaller pores are more efficient in H_2 sorption due to stronger interaction with H_2 molecules [68].

The pore size range that is favorable to maximize hydrogen uptake is broadly found to be 0.7–1.5 nm. ACs with a homogenous pore size distribution (PSD) centered across

a narrow range (<0.7 nm) are not as efficient H_2 adsorbents as it saturates at very low pressures [59]. On the other hand, the contribution of pores larger than 1.5 nm in H_2 uptake is not significant as the H–H interaction inside such large pores are not strong enough. Several experimental results validated that the H_2 uptake is rather higher for small pores with the optimum slit pore width of 1.0 nm or smaller [4,50,52,56–60,69–74]. For instance, Gogotsi et al. reported H_2 storage normalized to SSA (also called hydrogen density) for a range of micropore sizes and concluded that the predominant H_2 uptake are preferable by a pore size range of below 1 nm [69]. In addition, several other researchers reached a similar conclusion that the best correlation between H_2 uptake and pore range was for pores smaller than 1 nm [55,75]. On the other hand, Cabria et al. presented a thermodynamic model that also showed the optimum pore width to be well below 1 nm [70]. However, along with the increase in pressure, H_2 adsorbed in the micropores tends to be saturated and, to a minor extent, small mesopores between 2 and 5 nm are then responsible for the remaining H_2 uptake capacity [53,70].

Complimentary to the pore size, H_2 uptake is associated with the cumulative volume of pores of <2 nm in size, which is quantified as a micropore volume and is a measure of the activated carbon's microporosity. Therefore, consistent with the discussion on the "ideal" pore size, micropore volume is another key parameter for H_2 storage ability, and a high micropore volume is nevertheless advantageous for higher H_2 uptake capacity. There is a linear tendency of increasing the gravimetric H_2 uptake of 2.14–8.90 wt% with an increase in micropore volume from 0.297–1.540 cm^3/g, as shown in Figure 1.

2.2. Role of Surface Functionality of AC on H_2 Storage

In addition to surface morphology, surface functionality is another crucial aspect of AC that could enhance the H_2 uptake capacity. Since the interaction between adsorbed hydrogen and carbon is weak due to van der Waals interactions, one of the ways to improve the heat of adsorption is via functionalization of the pore surfaces with heteroatoms (e.g., nitrogen, oxygen, etc.) [4,42]. Prior to the discussion of various heteroatoms' effect on the quantity of H_2 adsorbed, it is imperative to briefly overview the fate of biomass-derived activated carbons' elemental composition, as listed in Table 1.

As seen in Table 1, although biomass undergoing chemical activation develops a great improvement in the surface morphological factors, the heteroatoms' (nitrogen and oxygen) elemental weight percent shows a significant reduction from the corresponding precursor material. This could be explained by means of findings from Fourier-Transform Infrared Spectroscopy (FTIR) of various such ACs in the literature, where a decreased peak intensity or an even complete disappearance of certain bands, for example, C–N, C–NH–C, hydroxylic O–H, aromatic carbonyl/carboxyl C=O, and aliphatic ether and alcohol O–H, were noted [79–82]. Such a loss of functional groups results from the formation of a fused ring structure that aids in pore formation, by-producing volatile products like CO, H_2O, and CO_2 [83–85]. Removal of hydrogen (H) and oxygen (O) from the precursor during the chemical activation process leads to aromaticity development [86–88]. On the other hand, the formation of cyanide during alkaline activation is responsible for the loss of nitrogen (N) content in the ACs [77].

Table 1. The elemental and morphological parameters, with the hydrogen uptake at 77 K, of various biomasses and their corresponding hydrochar and activated carbon.

Precursor	Type	N (wt%)	C (wt%)	O (wt%)	H (wt%)	SSA (m²/g)	Micropore Volume, V_μ (cm³/g)	Total Pore Volume, V_T (cm³/g)	H_2 Uptake (wt%)	H_2 Uptake Pressure (bar)	Ref.
Bamboo	biomass	<0.3	46.12	33.22	6.29	N/A	N/A	N/A	N/A	N/A	[50]
	hydrochar	0.48	77.1	14	2.62	337	0.14	N/A	0.86 / 1.2	1 / 40	
		<0.3	90.11	5.99	0.52	3208	1.75	1.75	2.58 / 6.6	1 / 40	
	activated carbon	N/A	N/A	N/A	N/A	3148	0.98	1.6	2.67 / 6.5	1 / 40	
		N/A	N/A	N/A	N/A	2914	0.99	1.85	2.50 / 6.50	1 / 40	
Sword-Bean Shells	activated carbon	1.78	65.06	30.51	2.65	1537	0.59	N/A	2.1 / 3.0	1 / 40	[49]
		1.39	78.42	19.35	0.84	1930	0.68	0.97	2.25 / 3.8	1 / 40	
		1.56	92.9	4.8	0.74	2702	0.84	1.48	2.52 / 5.5	1 / 40	
		1.67	96.28	1.44	0.61	2838	0.84	1.54	2.63 / 5.74	1 / 40	
Posidonia Oceanica	hydrochar	1.8	58	37.5	2.8	41	N/A	0.1	N/A	N/A	[76]
	activated carbon	0.6	92.7	4.6	2.1	2810	N/A	0.48	6.3	80	
Wood Chips	hydrochar	0.2	69.2	28.8	1.8	425	N/A	0.11	N/A	N/A	
	activated carbon	0	95.6	3.2	1.2	2835	N/A	0.73	6.4	80	

Table 1. *Cont.*

Precursor	Type	N (wt%)	C (wt%)	O (wt%)	H (wt%)	SSA (m²/g)	Micropore Volume, V_μ (cm³/g)	Total Pore Volume, V_T (cm³/g)	H₂ Uptake (wt%)	H₂ Uptake Pressure (bar)	Ref.
Melaleuca bark	biomass	0.51	58.13	33.45	7.91	N/A	N/A	N/A	N/A	N/A	[77]
	hydrochar	0.43	82.26	15.41	1.9	N/A	N/A	N/A	N/A	N/A	
	activated carbon	0.35	87.66	10.98	1.01	1092	0.4	0.46	1.21	10	
		0.28	88.69	9.6	0.89	1806	0.64	0.82	2.16	10	
		0.21	91.56	7.59	0.64	3170	1.07	1.51	4.08	10	
		0.19	91.89	7.39	0.53	2986	0.86	1.63	3.91	10	
Cellulose Acetate	hydrochar	N/A	66.2	29.9	3.9	N/A	N/A	N/A	N/A	N/A	[4]
	activated carbon	N/A	76.1	22.8	1.1	2001	0.79	0.95	3.1	1	
									6.2	20	
									6.7	30	
			78.3	20.6	1.1	2864	1.17	1.17	3.4	1	
									6.8	20	
									7.3	30	
			81.4	17.9	0.7	3771	1.54	1.54	3.9	1	
									8.1	20	
									8.9	30	
Beer Lees	activated carbon	N/A	N/A	N/A	N/A	1927	0.754	0.797	2.92	1	[48]
						2092	0.889	1.152	2.74	1	
						2408	1.089	1.505	2.43	1	
Hemp stem	activated carbon	N/A	N/A	N/A	N/A	922	0.4	0.49	1.57	1	[78]
						1365	0.48	0.73	2.58	1	
						1917	0.78	1.02	2.81	1	
						2368	0.88	1.27	2.72	1	
						3018	0.68	1.73	2.94	1	
						3241	0.74	1.98	3.28	1	

However, the question that needs to be addressed is the correlation of H_2 uptake with the quantity of various heteroatom and surface functional groups. Such an influence is difficult to assess due to the synergistic effect of the surface properties and surface chemistry on H_2 uptake. Simultaneous variation in elemental composition and surface morphology properties limits the ability to independently determine the effect of either variable.

Regarding the effect of oxygen, Blankenship et al. eliminated such ambiguities by comparing ACs with a similar porosity but different oxygen content, which lead to different H_2 uptake. The material stored more H_2 possibly because of its oxygen-rich nature [42]. The enhanced uptake is due to the high binding energy between oxygen and hydrogen, resulting from a higher adsorption energy. Similar findings were confirmed by Shayeganafar and Shahsavari, where they have studied the effect of oxygen content on pillared graphene material on H_2 uptake [89]. Nonetheless, challenges are posed due to the contradictory results about the effect of oxygen from various other research works. For instance, Georgakis et al. observed that functional groups containing oxygen induce a decrease in the H_2 adsorption capacity, and this effect is more pronounced with the narrow pores. They accounted this behavior mainly to three factors, namely, an increase in weight due to oxygen, steric hindrance effects, and weaker oxygen–hydrogen interactions compared to carbon–hydrogen [90]. Conversely, few other research groups concluded that the oxygen groups do not affect H_2 uptake as no significant differences were detected by comparing its capacity with that of pristine carbons [89,91].

Regarding the effect of nitrogen, high N-doping is beneficial for H_2 adsorption at low pressure, but it is detrimental at high pressure [43]. At low pressure, H_2 is mainly adsorbed onto the carbon atoms neighboring the nitrogen. However, at high pressure, the presence of nitrogen may reduce the interaction between hydrogen and the carbon surface, thus influencing the overall H_2 adsorption capacity [43,92,93]. On the other hand, at room temperature, doped heterogeneous nitrogen atoms increase the heat of adsorption of the H_2 which improves the H_2 storage capacity [56]. A nitrogen atom can attract the electrons of the neighboring carbon atom, leading to an electron deficiency of carbon and high H_2 adsorption. On the other hand, a higher nitrogen content negatively affects the H_2 adsorption due to the decrease in adsorption energy caused by the adsorption of H_2 on both the nitrogen atom and the neighboring carbon atom [94].

From the above discussion, it is imperative to find out the optimum ratio of N/C at all conditions relevant to storage. Although it was found that the H_2 storage capacity is significantly suppressed, with an increase in the acidic group amounts [54,95], considering the controversial opinions about the influence of the oxygenated functional groups on H_2 uptake, quantifying and correlating the effect of various heteroatoms containing surface functional groups with H_2 uptake is yet to be explored. It can also be inferred that H_2 uptake might improve by increasing the heat of adsorption with the necessary doping or functionalization, but that must not pose any negative effect on the surface morphological properties of the adsorbate. More studies are required to assess the discrete effect of heteroatoms on the carbon–hydrogen heat of adsorption by ensuring all other relevant and influencing surface parameters remain the same at all conditions.

2.3. Role of Physical Conditions on H_2 Storage

The specific surface area and the microporous volume affect the H_2 adsorption capacity and, generally, H_2 uptake increases with the increase of these properties. Besides these, the adsorption temperature and pressure are also important parameters that influence the H_2 adsorption capacity. A summary of H_2 storage at different temperatures and pressure in biomass-based ACs is shown in Table 2.

Table 2. Hydrogen storage in biomass-derived activated carbon (activated using KOH) at various temperatures and pressures.

Precursor	Surface Area (m²/g)	Micropore Volume (cm³/g)	Temperature (K)	Pressure (bar)	H₂ Storage (wt%)	Ref.
Cellulose	3771	-	77	1	3.90	[4]
			77	20	8.10	
			298	20	0.50	[96]
Olive stone	1269	0.48	77	1	1.48	
			77	25	6.11	[59]
			298	200	1.22	
Chitosan	2919	1.19	77	1	2.71	
			77	20	6.77	[55]
			77	40	5.01	
Olive pomace	1192	0.49	77	1	1.23	
			77	40	2.39	[97]
			298	180	0.45	
Fungi	2137	0.87	77	1	2.40	[58]
			77	20	5.00	
Corncob	3708	0.59	77	1	3.20	
			77	40	5.50	[98]
			298	164	1.05	
Wood chips	2835	0.73	77	1	2.55	
			77	80	6.40	[76]
			298	80	0.55	
Tamarind seeds	1784	0.64	303	60	1.36	
			323	60	1.14	[99]
			348	60	0.88	
			373	60	0.81	
Empty fruit bunch	687	0.30	77	1	1.97	[100]
			77	20	2.14	
Coffee bean waste	2070	1.1	77	40	4.00	[51]
			298	12	1.10	

It can be observed from Table 2 that, in order to increase the H₂ storage capacity of the material, one should operate at a lower temperature and higher pressure, no matter what the precursor is. This is due to the physisorption nature of the AC materials, with van der Waals attraction as the driving force. The pores are nearly saturated at high pressures, which lead the greater H₂ uptake. On the other hand, favorability at lower temperatures can be explained by comparing the enthalpy of the adsorption, which is weak compared to the kinetic energy of the molecules at ambient conditions [101]. At low temperatures, the kinetic energy of H₂ is low, which makes adsorption easier onto the walls of the pores of the ACs, resulting in higher H₂ uptake [51]. Contrarily, with the increase in temperature, the kinetic energy of the H₂ increased and required more energy to adsorb [68]. For example, Chahine and Bose found that lowering the storage temperature from ambient temperature (293 K) to 175 K increased the H₂ adsorption by a factor of 5, and by a factor of 15 when the adsorption temperature is further lowered to 77 K [102].

2.4. Role of Thermodynamic Properties on H₂ Storage

A higher heat of the adsorption, which translates to a stronger hydrogen attachment to the adsorbent, results in a higher H₂ coverage of the adsorbent surface, if sorption sites are available [67,78]. Yushin et al. confirmed it experimentally where H₂ uptake per SSA increases with the integrated average heat of adsorption [75]. The heat of adsorption of carbon-based material with H₂ adsorbed at ranges from 2–9 kJ/mol, which is considered to be weak [17,79,80]. However, H₂-framework interactions with the heat of adsorption enthalpies in the range of 15–25 kJ/mol are optimal targets for H₂ storage at near-ambient conditions, which correspond to an intermediate interaction ranging from

stronger physisorption to weaker chemisorption [81]. Although H_2 uptake depends on the choice of adsorbent, operating temperature, and pressure, it might be presumed that those parameters eventually affect the interaction energy. Hence, the H_2 uptake capacity is predominantly governed by the heat of adsorption.

For the adsorbent materials, the H_2 uptake capacity decreases with increasing temperature, where the strength of this decrease is determined by the heat of adsorption. Although the shapes of the isotherms are usually similar, the maximum H_2 uptake at high pressure and the slope of the isotherm at low pressures depend on the type of material, where the latter is also dependent on the heat of adsorption [103].

In addition, a high heat of adsorption is related to small pore size and the active sites being located at the edge orientation of the microdomains [43]. Surface energetic heterogeneity of the ACs can be understood from the adsorption energy distribution that has a close connection with the pore size distribution [48]. With a decreasing pore size, the absolute values of the heat of adsorption increase, indicating an increase in the interactions between H_2 and the framework structures. Several authors reached a similar conclusion, where they attributed the high heat of adsorption to a very small pore size [23,103–105]. For example, Jhung et al. illustrated the effect of pore size on the relative adsorption capacity per unit pore volume and the isosteric heat of the adsorption, where both decreased as the pore size diminished [104].

On the other hand, the heat of adsorption is also affected by surface functionality, which could be due to the effect on the adsorbate–adsorbent interaction. For example, Sevilla et al. found this for two different samples with similar surface morphological properties, but where the difference in oxygen content played a role in determining the strength of the interaction between the adsorbate and adsorbent. The sample with a higher oxygen content (7.1 wt%) has a lower heat of adsorption and hydrogen uptake than the sample with a lower oxygen content (5.2 wt%) [23]. In another study, Gogotsi et al. found that a slight increase in H_2 uptake corresponds to the increase in heat of adsorption due to the removal of functionality from the surface of the adsorbent via vacuum annealing [69].

Most studies focus on high pressure storage but, for applicability, deliverable capacity plays an important role in determining the true ability to store usable hydrogen, which is the amount of hydrogen adsorbed at high pressure minus the amount adsorbed at the discharge pressure. For practical applications, if the heat of the interaction is substantially high, the great affinity will eventually lead to a large amount of residual adsorptive at the delivery pressure, which will reduce its deliverable capacity. Bhatia and Myers derived an optimum adsorption enthalpy change ΔH°_{opt}, which represents the average or integral heat of adsorption for a delivery cycle, with the maximum delivery between two pressure points (P_1 and P_2) at a given temperature (T) and the entropy change (ΔS°) relative to the standard pressure (P_o) and ideal gas constant (R) [106]. For this equation, the absolute value is equal to the isosteric heat and it was derived assuming the adsorbent as homogenous with the adsorption isotherm type of Langmuir [68].

$$\Delta H^{\circ}_{opt} = T\Delta S^{\circ} + \frac{RT}{2} \ln\left(\frac{P_1 P_2}{P_o^2}\right) \tag{1}$$

Using this equation for a delivery cycle, exemplary reasonable values of adsorption and desorption pressures may be taken as P_1 = 30 bar and P_2 = 1.5 bar, respectively; $\Delta S^{\circ} = -8$ R (where, the unit of R is J.mol^{-1}.K^{-1}) for a variety of adsorbents, which upon substitution in equation 1 yields ΔH°_{opt} as -15.1 kJ/mol at T = 298 K and P_0 = 1 bar.

Combining the above discussions, it can be concluded that H_2 uptake capacity is ultimately driven by its microporous structure, with a small pore size enhancing the interaction energy. H_2 uptake capacity is also determined by the surface functionality, although a considerable amount of research has not been done yet for biomass-derived ACs, with some controversial findings of the negative effect of heteroatoms, such as oxygen and/or nitrogen. Additionally, H_2 uptake is undoubtedly related to the storage temperature, which shows a decrease with increasing temperature due to the weak heat

of adsorption. Thus, the heat of adsorption might be the fundamental determinant of H_2 uptake capacity, which is favorable at cryogenic conditions. However, for the purpose of practical application in the prospective hydrogen economy, the scientific community is also pursuing high hydrogen uptake at an ambient condition, where the optimum heat of energy is approximated to be in the range of 15–25 kJ/mol, which can be attained by enhancing the physisorption process by further improving the storage material.

3. Recent Advances in Material Development

The hydrogen storage capacity at room temperature on ACs is still challenging [107–109]. A promising way to increase the H_2 storage capacity is through surface modifications by promoting the spillover mechanism. The H_2 spillover process could be described in the three steps shown in Figure 2. In the first step, adsorption of molecular H_2 occurred on the catalyst surface. Dissociation of molecular H_2 on the catalyst surface takes place in the following step. Finally, the diffusion of dissociated atomic hydrogen occurred on the catalyst and support surface. In this case, a metal (dissociation source) nanoparticle (e.g., Pt, Pd, Ni, Ru, and Co) is loaded onto the surface of the carbon materials (receptor). The metal nanoparticles are additives that act as a catalytic active center for the dissociation of hydrogen during the process. In this case, the carbon receptor plays an important role as it provides the adsorption sites for the spillover hydrogen [110]. Spillover might be influenced by morphological factors, including porosity in the carbon skeleton, as migration needs metal–carbon contacts to occur. In addition, the number and quality of these bridges also depend on the structural and morphological properties of the metal–AC composites. In general, smaller particle composites have higher catalytic reactivity and is better for adsorption and dissociation of molecular H_2 on the composite adsorbent surface. For example, Zielinski et al. experimentally found that there is no correlation between H_2 uptake and the metal surface area [111]. However, they observed that the hydrogen adsorption declined with the decrease in SSA of the metal–AC composite despite having a higher metal surface area due to an increase in metal content. There are various techniques to prepare metal–carbon nanocomposites, such as wet impregnation, plasma reduction, sputtering, electrodeposition, thermal evaporation, etc. The pros and cons of these processes are discussed elsewhere [54,109,112–119].
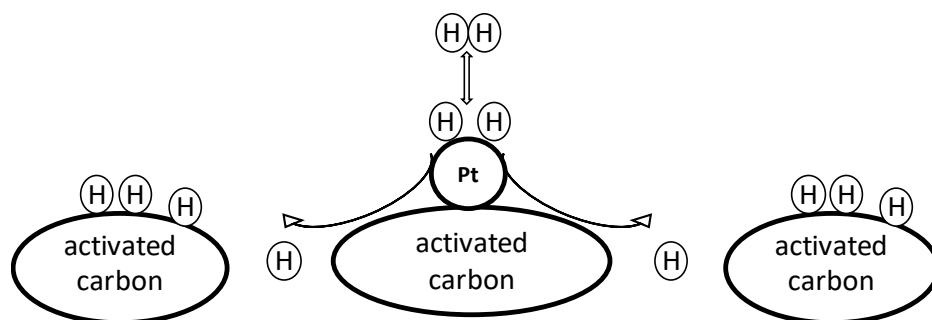

Figure 2. Spillover mechanism in the Pt–AC composite [120].

It can be interpreted from the literature that the surface diffusion of atomic hydrogen could be the rate-determining step for H_2 adsorption [121,122]. Thus, the kinetics of H_2 adsorption via hydrogen spillover may be characterized by a surface diffusivity (D) or diffusion time constant (D/R^2, where R is the characteristic radius of the sphere for diffusion) [121]. Due to the strong binding energy between the atomic hydrogen and carbon surface, it is difficult to make the atomic hydrogen diffuse over longer distances. The best method is to make more catalyst clusters dispersed on the interior surface of the nanopore of the porous storage support as it will assist atomic hydrogen diffusing into deep sites and enhance H_2 uptake [123].

However, it is difficult to achieve desirable dispersion at a high metal loading due to the aggregation of the metal. It lowers the SSA of the composite, which adversely impacts the H_2 storage capacity [124–126]. Some studies on metal-doped carbons reported that the existence of functional groups can facilitate the dispersion of fine metal catalysts that play an important role in the surface diffusion of the spillover H atoms to enhance the "chemical" adsorption of H_2 [127–130]. The oxygen functional groups in the spillover process act as a direct adsorption site (reversible or irreversible), enhancing the formation of an island of the spilled-over H atoms around the oxygen groups [127] and facilitating the surface diffusion and favorable adsorption of the atomic hydrogen (due to the continuous network or spatial dispersion of the oxygen groups) [128]. On the other hand, doping of N could create defects on the composite, helping to reduce the metal particle size and hence better dispersion. In addition, it enhances the spillover process by working as a hydrogen atom receptor. For example, Zhao et al. observed enhancement of H_2 storage capacity by around 10 wt% at room temperature after doping the nitrogen with a Pt–AC composite, provided that the Pt composition remained the same in the composite [126].

The enhancement in hydrogen uptake due to doping with various metals is shown in Table 3. It shows that, with the decrease in Pt content by half, H_2 uptake is enhanced by a factor of three. This could be explained by Pt being more reactive for molecular H_2 that inhibits dissociation of atomic hydrogen to move and diffuse into a porous carbon surface [131,132]. Unlike the use of precious metals like Pt for the purpose of doping, Ni has also been used. Ni is a less expensive metal but sufficiently active for H_2 uptake. H_2 adsorption is higher in case of Ni–AC because van der Waals interactions are higher between the Ni nanoparticles and the hydrogen molecules, which is the first step for the spillover mechanism [115,133,134]. As a result, Ni nanoparticles assist in the dissociation of hydrogen molecules into hydrogen atoms. However, H_2 storage capacity of the Ni/AC nanocomposites depends strongly on the Ni amount, as can be seen in Table 3, in that with just a 6% increase in Ni content, H_2 uptake declined by 33%. This could be explained by the adverse effect on the hydrogen spillover due to the agglomeration of Ni nanoparticles, possibly covering the AC surface and isolating it from hydrogen exposure, thereby blocking the access to porosity [109].

Table 3. Hydrogen uptake comparison of various metal-doped activated carbons.

Storing Condition	Metal Content	H_2 Storage (wt%)		Change in Uptake (%) *	Ref.
		Without Dopant	With Dopant		
	10 wt% Pd	0.6	1.80	200	[135]
298 K 10 MPa	6 wt% Pt	0.84	1.34	60	[136]
	5.6 wt% Pt	0.60	1.20	100	[137]
	3 wt% Pt	0.30	0.90	200	[114]
298 K 3 MPa	1 wt% Ni	0.15	0.53	253	[111]
298 K 20 MPa	9.7 wt% Ni	very low	1.00	N/A	[138]
303 K 6 MPa	10 wt% Pd	0.41	0.53	29	[54]
303K 5 MPa	10 wt% Ni	0.82	1.60	95	[109]
298 K 18 MPa	2.5 wt% Pd/Pt	1.00	1.65	65	[131]
298 K 25 MPa	1.86 wt% Pd	0.60	1.40	133	[139]
77 K 40 bar	1.73 wt% Pd	2.39	2.46	3	[97]
298 K 180 bar	1.73 wt% Pd	0.45	0.52	16	[97]
298 K 180 bar	1.1 wt% Pt	0.45	0.53	18	[97]
298 K 25 bar	1.8 wt% Ni	0.126	0.13	2	[97]
	1.75 wt% Cu		0.13	6	
	3.71 wt% Ag		0.13	3	
	1.91 wt% Ni		0.09	−31	

* Changes with dopant were calculated with respect to without dopant.

Thus, it can be summarized that a great potential of enhanced H_2 uptake at room temperature can be envisioned using metal–AC composites. The surface porosity of the

metal–AC composite positively affects the H_2 uptake capacity unlike an increase in metal surface area. In terms of surface functionality, oxygen functional groups seem to improve the H_2 uptake ability of the composite. A similar effect of nitrogen doping was observed but the effect on H_2 uptake of the nitrogen functional groups in such composites is yet to be analyzed. A high metal level also shows a detrimental effect on hydrogen uptake due to metal aggregation. This calls for further analysis in determining the optimum concentration of the metal in a composite material.

4. Conclusions

This article discussed the key role of surface morphology as well as surface functionality on the substantial H_2 uptake capacity of biomass-derived AC at various storage conditions. It can be concluded that the H_2 adsorption capacity on biomass-derived AC depends on surface porosity, surface functionality, and the heteroatoms' content. The synergistic effect of these parameters affects the heat of adsorption, which is ultimately the determining factor of H_2 uptake.

Although a considerable amount of work has been done to exploit the standpoint of biomass-derived AC in H_2 storage ability, some significant voids still remain, which need to be addressed. These voids need to be explored in the future for its profound usage. For example, a plethora of lignocellulosic biomass is used as a suitable feedstock for AC preparation, where the analysis of the influence of its components (xylan, lignin, cellulose, etc.) on the adsorption capacity of H_2 is still unknown. On the other hand, precursor materials may also contain significant proportions of inorganics, but their effect on H_2 uptake has not been analyzed. The crystallinity of the various biomass-derived activated carbon is also an important structural parameter to be studied, as the literature shows that carbon's crystalline structure enhances the hydrogen adsorption capacity in case of hydrogen adsorption in graphene sheets [29].

In addition, the effect of surface functionality and the content of heteroatoms need more extensive analysis in terms of physical chemistry to understand the bonding and subsequent quantitative effect of those on the heat of adsorption. Studying the individual effect of various functional groups on the integrated heat of absorption might also provide insight into the principal influence of these groups on the interaction energy of hydrogen with carbon.

Lee and Park showed an enhancement of H_2 uptake by 5 times in an MOF–AC composites with metal doping compared to the corresponding pristine MOF [111]. This highlights the necessity to investigate various combinations of metal and biomass-derived ACs, which might have very high spillover as well as surface properties to improve hydrogen storage significantly at ambient conditions.

Finally, another significant gap in the literature that exists is assessing the mechanical strength of materials after a high number of gas storage cycles, such that it can be implemented for the practical application of hydrogen storage. Although Pedicini et al. [48] have shown stability for six cycles of H_2 storage, it is important to study longer cyclic storage with both adsorption and desorption capacity to assert an approximate structural strength of the material. Techniques to improve the strength of the ultra-micropores should be explored to prevent pore collapse and hence better cyclability of the material. It is also important to pay attention to lower the activation energy in the desorption of hydrogen for an improved usable capacity of the material. Furthermore, the adsorption kinetics in biomass-derived activated carbons need to be studied so that materials can be developed that have a minimum fill time with fully reversible characteristics.

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