

Article

Support effect on the performance of Ni₂P catalysts in the hydrodeoxygenation of methyl palmitate

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Supplementary Materials

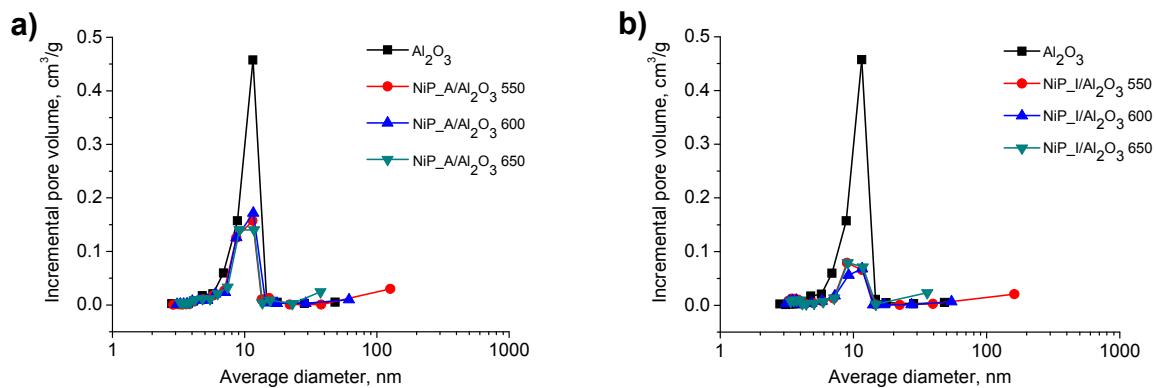


Figure S1. Pore size distributions determined from the desorption branch of N_2 isotherm for (a) $\text{NiP}_\text{A}/\text{Al}_2\text{O}_3$ and (b) $\text{NiP}_\text{I}/\text{Al}_2\text{O}_3$ catalysts reduced at 550, 600 and 650 $^\circ\text{C}$ as well as for Al_2O_3 support.

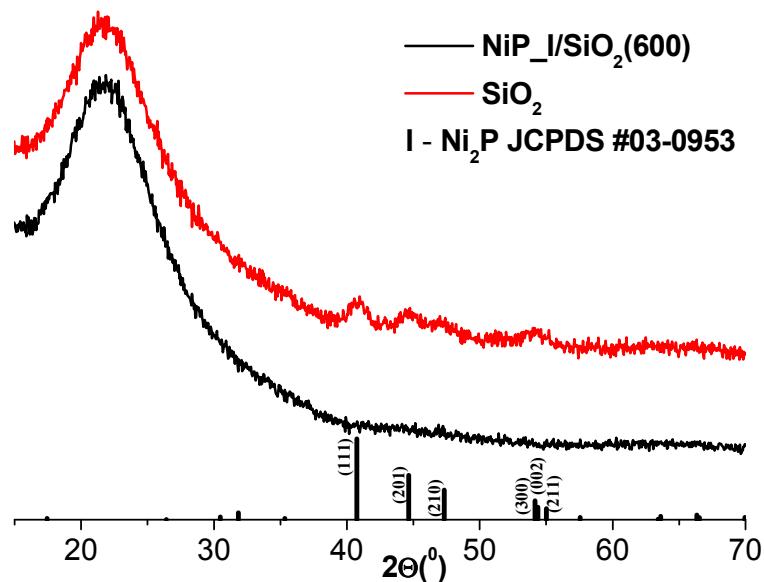


Figure S2. XRD patterns of NiP_I/SiO₂(600) catalyst prepared from phosphite precursor and reduced at temperature of 600 °C and SiO₂ support.

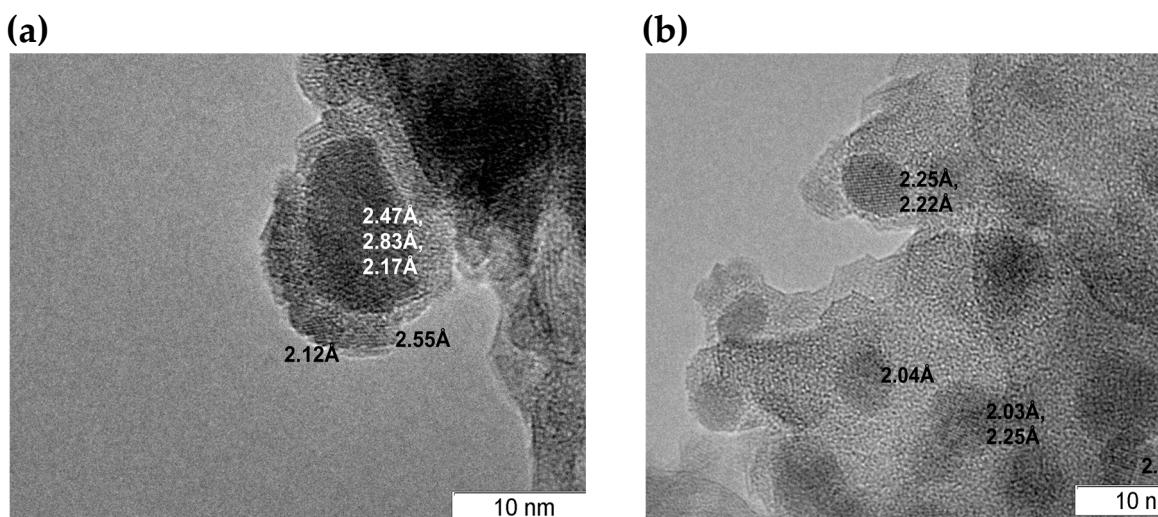


Figure S3. TEM images of Ni_xP_y/γ-Al₂O₃ catalysts prepared from different precursors: (a) NiP_A/Al₂O₃ 650 and (b) NiP_I/Al₂O₃ 600.

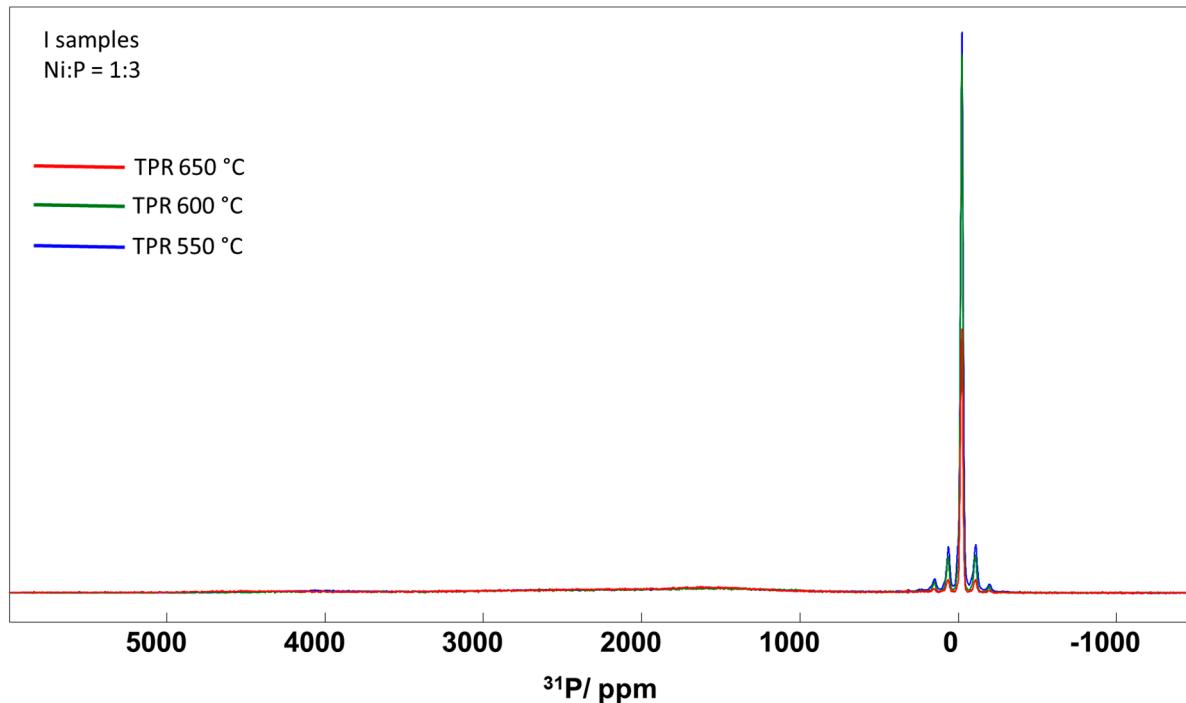


Figure S4. Full-scale mass-normalized 14 kHz MAS ^{31}P spectra of NiP_I/Al₂O₃ reduced at 550, 600 and 650 °C. A significant decrease in intensity of the line corresponding to PO_x groups can be observed for the sample reduced at 650 °C.

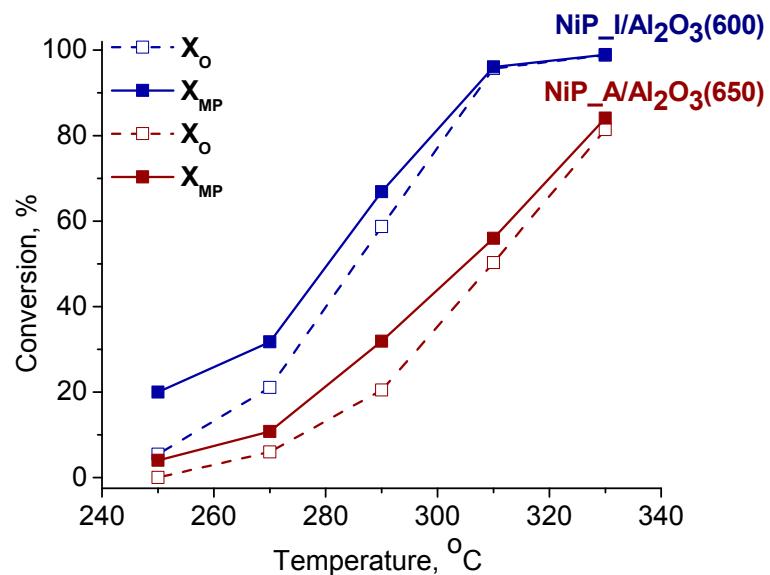


Figure S5. Temperature effect on the conversion of methyl palmitate (solid symbols, solid lines) and oxygen-containing compounds (empty symbol, dash lines) over NiP_A/Al₂O₃ 650 and NiP_I/Al₂O₃ 600 catalysts ($\text{P}_{\text{H}_2} = 3.0 \text{ MPa}$, $T = 250\text{--}330 \text{ }^{\circ}\text{C}$, $\text{H}_2/\text{feed} = 600 \text{ Nm}^3/\text{m}^3$, methyl palmitate LHSV = 9 h⁻¹).

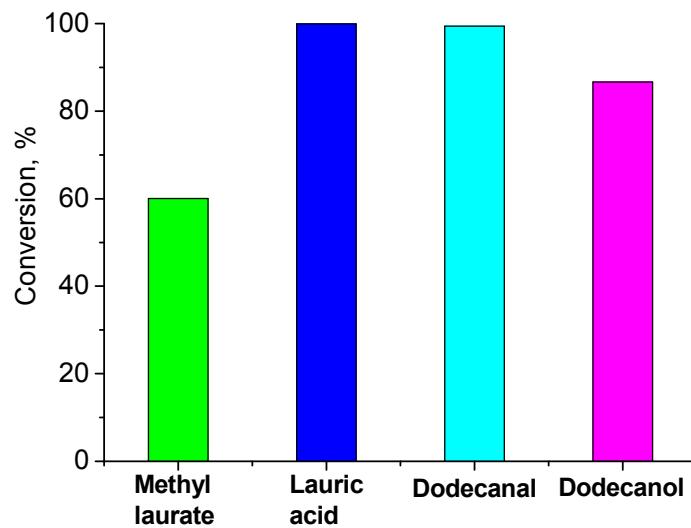


Figure S6. Conversions of methyl laurate, lauric acid, dodecanal and dodecanol over $\text{Ni}_2\text{P}/\text{SiO}_2$ catalyst at $T = 290\text{ }^\circ\text{C}$, $P_{\text{H}_2} = 3.0\text{ MPa}$, $\text{H}_2/\text{feed} = 600\text{ Nm}^3/\text{m}^3$ and reagent LHSV = 10.7 h^{-1} . Feed composition: 1 – 8.0 wt% of methyl laurate and 0.5 wt% of *n*-octane in *n*-decane; 2 – 7.6 wt% of lauric acid and 0.5 wt% of *n*-octane in *n*-decane; 3 – 7.0 wt% of dodecanal and 0.5 wt% of *n*-octane in *n*-decane; 4 – 7.1 wt% of dodecanol-1 and 0.5 wt% of *n*-octane in *n*-decane.

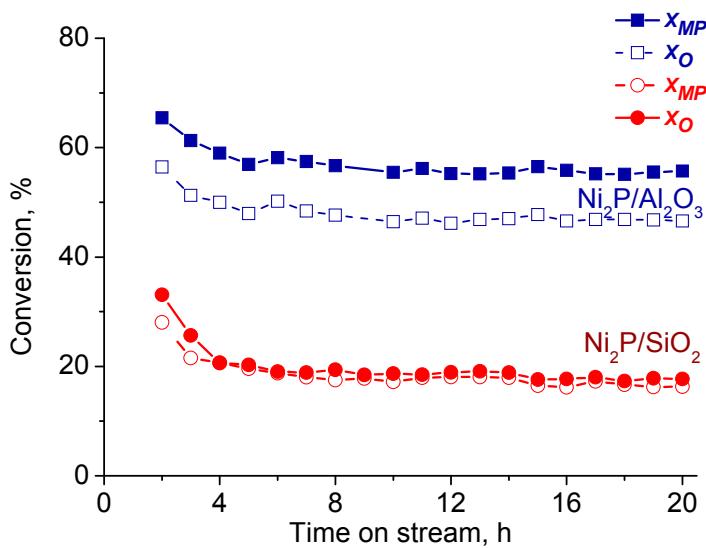


Figure S7. MP conversion (X_{MP}) and total oxygen-containing compounds conversion (X_o) as a function of time on stream for $\text{Ni}_2\text{P}/\text{Al}_2\text{O}_3$ and $\text{Ni}_2\text{P}/\text{SiO}_2$ catalysts at $T = 290\text{ }^\circ\text{C}$, $P_{\text{H}_2} = 3.0\text{ MPa}$, $\text{H}_2/\text{feed} = 600\text{ Nm}^3/\text{m}^3$ and methyl palmitate LHSV = $3.6\text{--}9\text{ h}^{-1}$.

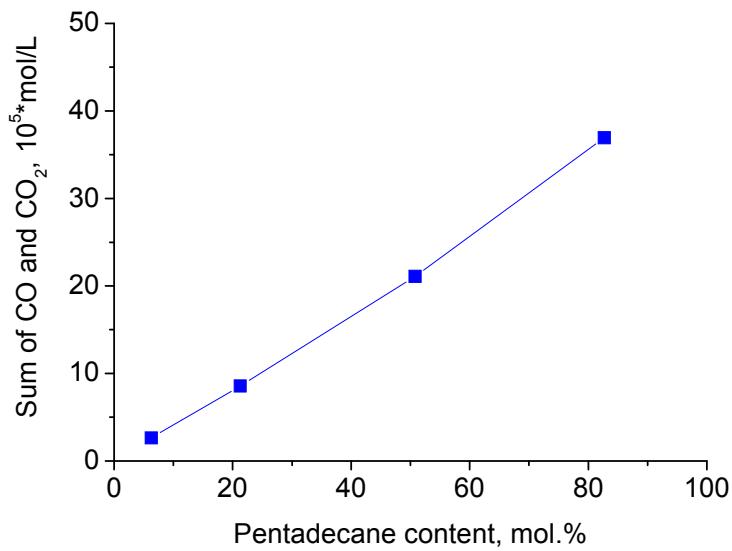


Figure S8. Dependence of the CO and CO₂ sum from pentadecane content in methyl palmitate hydrodeoxygenation over NiP_A/Al₂O₃ 650 catalyst ($P_{H_2} = 3.0$ MPa, $T = 290$ °C, H₂/feed = 600 Nm³/m³, methyl palmitate LHSV = 3.6–12 h⁻¹).



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