

# Assessment of photocatalytic production of hydrogen from biomass or wastewaters depending on the metal co-catalyst and its deposition method on TiO<sub>2</sub>

Mikel Imizcoz, Alberto V. Puga\*<sup>‡</sup>

Instituto de Tecnología Química, Universitat Politècnica de València-Consejo Superior de Investigaciones Científicas, Avenida de los Naranjos, s/n, 46022 Valencia, Spain.

<sup>‡</sup> Current address: Departament d'Enginyeria Química, Universitat Rovira i Virgili, Av. dels Països Catalans, 26, 43007 Tarragona, Spain

alberto.puga@urv.cat

## Supporting Information

**Table S1.** Product yields for the photocatalytic reforming of glucose under simulated solar light on *M*/TiO<sub>2</sub>.<sup>[a,b]</sup>

Photocatalyst	Production rate/ $\mu\text{mol g}_{\text{cat}}^{-1} \text{h}^{-1}$		TOF <sup>[c]</sup> / $\text{s}^{-1}$
	H <sub>2</sub>	CO <sub>2</sub>	H <sub>2</sub>
H <sub>2</sub> <sup>DP</sup> Au/TiO <sub>2</sub>	993.8	73.8	1171
H <sub>2</sub> <sup>DP</sup> Ag/TiO <sub>2</sub>	320.2	17.0	298
H <sub>2</sub> <sup>DP</sup> Cu/TiO <sub>2</sub>	560.4	59.0	44
H <sub>2</sub> <sup>DP</sup> Pt/TiO <sub>2</sub>	1706.9	250.3	306
<sup>PD</sup> Au/TiO <sub>2</sub>	905.6	83.8	2169
<sup>PD</sup> Ag/TiO <sub>2</sub>	402.4	30.7	796
<sup>PD</sup> Cu/TiO <sub>2</sub>	904.3	56.3	134
<sup>PD</sup> Pt/TiO <sub>2</sub>	1912.7	158.2	1353
<sup>IM</sup> Au/TiO <sub>2</sub>	298.3	10.3	5993
<sup>IM</sup> Ag/TiO <sub>2</sub>	203.8	13.2	1099
<sup>IM</sup> Cu/TiO <sub>2</sub>	259.3	23.0	27
<sup>IM</sup> Pt/TiO <sub>2</sub>	157.1	29.6	52

<sup>[a]</sup> Stirred suspensions of the photocatalyst (25 mg) in aqueous glucose (5% w/v, 25 mL) were irradiated under simulated solar light (AM1.5G, 1.0 kW m<sup>-2</sup>) under Ar atmosphere (1.4 bar) at 25 °C for 2 h.

<sup>[b]</sup> Estimated standard deviations for H<sub>2</sub> production rates lie within a  $\pm 5\%$  error bar, as determined by independent results. <sup>[c]</sup> The activities per active site (TOF) were calculated according to the average co-catalyst particle size as listed in Table 1, assuming semi-spherical morphology and {111} facet surface atom densities.

**Table S2.** Hydrolysis of  $\alpha$ -cellulose in acidic aqueous media in short thermal cycles at different temperatures.<sup>[a]</sup>

T/°C	cycle	yield/% <sup>[b]</sup>				global saccharide yield/% <sup>[c]</sup>	conversion/% <sup>[d]</sup>	molar balance/% <sup>[d]</sup>
		glucose	xylose	HMF	furfural			
160	#1	7.6	67.4	-	-	18.3	21.5	96.8
	#2	4.8	18.4	-	-	7.2	30.6	94.9
	#3	3.7	7.8	-	-	4.5	35.0	95.0
	<i>overall</i>	16.2	93.6	-	-	29.9	35.0	95.0
180	#1	9.1	22.2	4.3	23.9	11.5	41.3	77.9
	#2	4.9	10.0	2.6	2.1	6.5	59.2	69.0
	#3	3.0	7.0	2.0	0.5	4.2	70.3	63.8
	<i>overall</i>	17.1	39.2	8.9	26.6	22.1	70.3	63.8

*concentrations of biomass-derived oxygenated substances in the hydrolysate used for photocatalytic H<sub>2</sub> production experiments*

		c/%(w/v)			
160	#1	0.53	0.85	-	-
		c/%(mM)			
160	#1	29.5	56.5	-	-

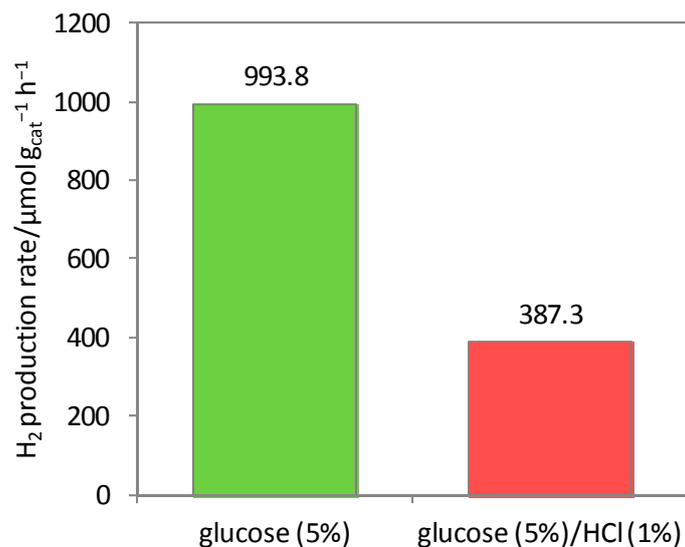
<sup>[a]</sup> Reaction conditions:  $\alpha$ -cellulose (6.00 g) in aqueous HCl (1% w/v, 60 mL), N<sub>2</sub> atmosphere, heated to the specified temperature (ramp  $\approx 10$  °C min<sup>-1</sup>) and then, allowed to cool down naturally to room temperature.

<sup>[b]</sup> Yields relative to the expected amounts of either glucose or xylose ( $\approx 85:15$  w/w) units in the starting  $\alpha$ -cellulose, as determined by HPLC using an Aminex<sup>®</sup> HPX-87H column. <sup>[c]</sup> Global yields relative to the total amount of saccharide units in the starting  $\alpha$ -cellulose. <sup>[d]</sup> Conversions and molar balances are cumulative.

**Table S3.** Product yields for the photocatalytic reforming of the  $\alpha$ -cellulose hydrolysate obtained after a first hydrolysis cycle at 160 °C<sup>[a]</sup> under simulated solar light<sup>[b]</sup> either directly or after UV pre-treatment<sup>[c]</sup> on M/TiO<sub>2</sub>

Photocatalyst	Production rate/ $\mu\text{mol g}_{\text{cat}}^{-1} \text{h}^{-1}$	
	H <sub>2</sub>	CO <sub>2</sub>
<i>simulated sunlight irradiation on raw hydrolysate</i>		
<sup>H,DP</sup> Au/TiO <sub>2</sub>	< 0.1	64.1
<sup>PD</sup> Pt/TiO <sub>2</sub>	0.2	75.8
<sup>H,DP</sup> Cu/TiO <sub>2</sub>	0.1	129.3
<i>UV pre-treatment on raw hydrolysate</i>		
<sup>H,DP</sup> Cu/TiO <sub>2</sub>	17.3	125.8
<i>simulated sunlight irradiation on after UV pre-treatment</i>		
<sup>H,DP</sup> Cu/TiO <sub>2</sub>	2.9	93.4

<sup>[a]</sup> Hydrolysis conditions at 160 °C (cycle #1) as described in Table S2. <sup>[b]</sup> Stirred suspensions of the photocatalyst (25 mg) in  $\alpha$ -cellulose hydrolysate (25 mL) were irradiated under simulated solar light (AM1.5G, 1.0 kW m<sup>-2</sup>) under Ar atmosphere (1.4 bar) at 25 °C for 2 h. <sup>[c]</sup> Irradiated by a similar procedure as described in [b] for simulated sunlight, but using an Hg lamp (125 W,  $\approx$  1.5 kW m<sup>-2</sup>). <sup>[e]</sup> Determined by HPLC using an Aminex<sup>®</sup> HPX-87H column.



**Figure S1.** Photocatalytic H<sub>2</sub> yields from aqueous glucose at either natural pH or in an HCl-acidified medium on <sup>H,DP</sup>Au/TiO<sub>2</sub>. Stirred suspensions of the photocatalyst (25 mg) in aqueous glucose (5% w/v, 25 mL, without or with HCl, 1% w/v) irradiated under simulated solar light (AM1.5G, 1.0 kW m<sup>-2</sup>) under Ar atmosphere (1.4 bar) at 25 °C for 2 h.



**Figure S2.** Picture showing the amber colour of the α-cellulose hydrolysate (left) obtained at 160 °C (cycle #1, see Table S2 footnote), and the bleaching effect caused by the UV photocatalytic treatment leading to an almost colourless solution (right).

**Table S4.** Chemical characteristics of the rice husks hydrolysate,<sup>[a]</sup> and wastewaters used in photocatalytic experiments.

biomass hydrolysate or wastewaters	<i>c</i> /%(w/v) <sup>[b]</sup>					COD <sup>[c]</sup> / mg L <sup>-1</sup>	[N] <sup>[d]</sup> / mg L <sup>-1</sup>	$\sigma$ <sup>[e]</sup> / $\mu\text{S cm}^{-1}$
	sucrose	glucose	xylose	HMF	furfural			
rice husks hydrolysate	-	0.27	0.88	< 0.01	0.02	$\approx 10^3$ <sup>[f]</sup>	-	-
municipal wastewater	-	< 0.01	-	-	-	389	25	2130
juice production wastewater	0.02	0.04	0.03	-	-	$\approx 10^2$ <sup>[f]</sup>	-	2850

<sup>[a]</sup> Reaction conditions: milled rice husks (6.00 g) in an aqueous solution of concentrated HCl (1% w/v, 60 mL), N<sub>2</sub> atmosphere, heated to the specified temperature (ramp  $\approx 10$  °C min<sup>-1</sup>) and then, allowed to cool down naturally to room temperature. <sup>[b]</sup> Determined by HPLC using an Aminex<sup>®</sup> HPX-87H column. <sup>[c]</sup> COD: Chemical Oxygen Demand. <sup>[d]</sup> The major N species was [NH<sub>4</sub>]<sup>+</sup>. <sup>[e]</sup> Conductivity ( $\sigma$ ) measured using a Crison CM 35 device and a Crison + Pt 1000 Conductivity Cell. <sup>[f]</sup> Estimated from HPLC data.

**Table S5.** Product yields for the photocatalytic reforming of wastewaters under simulated solar light<sup>[a]</sup> on M/TiO<sub>2</sub>

Photocatalyst	Production rate/ $\mu\text{mol g}_{\text{cat}}^{-1} \text{h}^{-1}$	
	H <sub>2</sub>	CO <sub>2</sub>
<i>municipal wastewater</i>		
H, <sup>DP</sup> Au/TiO <sub>2</sub>	< 0.1	15.8
H, <sup>DP</sup> Cu/TiO <sub>2</sub>	0.1	18.2
<i>juice production wastewater</i>		
H, <sup>DP</sup> Au/TiO <sub>2</sub>	115.1	306.9
H, <sup>DP</sup> Cu/TiO <sub>2</sub>	10.7	291.2

<sup>[a]</sup> Stirred suspensions of the photocatalyst (25 mg) in the corresponding wastewater (25 mL) were irradiated under simulated solar light (AM1.5G, 1.0 kW m<sup>-2</sup>) under Ar atmosphere (1.4 bar) at 25 °C for 2 h.