



Article

Nitrate Attenuation in Degraded Peat Soil-Based Constructed Wetlands

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Abstract: Constructed wetlands (CWs) provide favorable conditions for removing nitrate from polluted agricultural runoff via heterotrophic denitrification. Although the general operability of CWs has been shown in previous studies, the suitability of peat soils as a bed medium for a vertical flow through a system for nitrate attenuation has not been proven to date. In this study, a mesocosm experiment was conducted under continuous flow with conditions aiming to quantify nitrate (NO_3^-) removal efficiency in degraded peat soils. Input solution of NO_3^- was supplied at three different concentrations (65, 100, and 150 mg/L). Pore water samples were collected at different depths and analyzed for NO_3^- , pH, and dissolved N_2O concentrations. The redox potential (Eh) was registered at different depths. The results showed that the median $\text{NO}_3\text{-N}$ removal rate was 1.20 g/(m²·day) and the median removal efficiency was calculated as 63.5%. The nitrate removal efficiency was affected by the NO_3^- supply load, flow rate, and environmental boundary conditions. A higher NO_3^- removal efficiency was observed at an input NO_3^- concentration of 100 mg/L, a lower flow rate, and higher temperature. The results of pore water pH and NO_3^- and N_2O levels from the bottom of the mesocosm suggest that N_2 is the dominant denitrification product. Thus, degraded peat soils showed the potential to serve as a substrate for the clean-up of nitrate-laden agricultural runoff.

Keywords: nitrate attenuation; degraded peat; bed medium; constructed wetlands; mesocosm experiment

1. Introduction

Nitrogen (N) is an important nutrient in terrestrial and aquatic ecosystems. Around 120 million tons of nitrogen gases (N_2) per year are converted worldwide from the atmosphere into reactive nitrogen forms such as ammonium and nitrate by mineral fertilizer production and N-fixation by leguminous crops [1]. Most of the nitrogen reaching the terrestrial environment (directly or indirectly) is dissolved in surface runoff and infiltrating water. Regardless of the environmental compartment into which reactive N is released, much of the transported load ends up as $\text{NO}_3\text{-N}$ in the aquatic environment [2]. Especially in lowland catchments with intensive agriculture, $\text{NO}_3\text{-N}$ loads from agricultural fields may easily exceed 2000 kg/(km²·year), impacting drinking water quality [3]. In the German lowlands, the average $\text{NO}_3\text{-N}$ losses from tile-drained field sites were found to vary between 340 and 2180 kg/(km²·year) [4].

Constructed wetlands (CWs) are often established as engineered systems to remove nitrate (i.e., denitrification) in wastewater or agricultural runoff by microbial denitrification and plant uptake [5].

Denitrification is an anaerobic respiration process in which nitrogenous oxides, principally NO_3^- and NO_2^- , are used as terminal electron acceptors and are hence reduced into the gaseous products nitric oxide (NO), nitrous oxide (N_2O), and dinitrogen (N_2) [6]. CWs generally consist of designed basins containing water, substrates, and plants. The type of substrates are important in CWs, because they provide storage capacity for contaminants via adsorption processes; in addition, many chemical and biological transformation processes occur at the surfaces of the various substrates. Wood products such as chips are commonly employed as denitrification beds in constructed wetlands due to the low cost and high C:N ratio (30:1 to 300:1, depending on the wood materials) [7–9]. Several other substrates, such as maize cobs and wheat straw, have also been proved suitable as denitrification beds [10]. Peat soils have a relatively low permeability and high organic carbon content, which will enhance the residence time of solutes or wastewater [11,12]. Thus, peat soils could potentially serve as denitrification beds for CWs. However, there are few studies about the performance of peat soils as denitrification bed materials [13–16].

Peatlands only cover 3% of the total global land area but store about one-third of the world's soil carbon. Drainage of peatland results in aeration and degradation of the peat, leading to the emission of greenhouse gases (e.g., CO_2) and losses of organic carbon [17]. For instance, greenhouse gas emissions of a peatland in Mecklenburg–Western Pomerania (northeast Germany) was estimated to be about 6.2 million tonnes of CO_2 equivalent per year [18]. Rewetting of peatlands is an effective practice to reduce greenhouse gas emissions, but may not affect nitrogen dynamics [19]. The uppermost highly degraded peat layers are recommended to be removed before any peatland restoration, because they will further release large amounts of organic compounds (e.g., dissolved organic carbon) into the downstream water bodies [20]. It has been reported that peat soils have a large amount of dead-end or closed pore volumes ranging from 40 to 80 vol % of total pore spaces [21–23]. Large numbers of immobile pores can be found in oxygen-depleted water regions, providing a favorable region for denitrification [15]. Highly degraded peat samples have been shown to have a high fraction of small (or immobile) pore regions [24], which can increase the denitrification activities. They can thus be used as a suitable substrate for nitrate attenuation in CWs. This could be especially interesting in landscapes with scattered spots of fen peat. These local small-scale drained peatlands and wetlands have often been unsuccessfully converted into crops or grasslands, and may serve in the future as CWs for the cleanup of agricultural runoff [15,25].

In this study, we use a mesocosm experiment setup under controlled flux conditions to investigate the NO_3^- turnover processes in a lowland fen with highly degraded peat soils (soil organic matter content of 55% by weight) and examine the suitability of degraded peat for denitrification beds. The objectives of the study were: (1) to quantify the nitrate removal rate and efficiency under continuous flow conditions over a long-term period; (2) to explore the factors affecting the nitrate removal efficiency in peat soils; and (3) to evaluate the possibility of using degraded peat as filter medium in a constructed wetland to reduce nitrates from agricultural runoff.

2. Materials and Methods

2.1. Field Site and Sampling

The peat for the mesocosm experiment was collected from a small fen at Dummerstorf, 15 km southeast of the city of Rostock, Germany. It is a typical drained peatland in northern Germany with a highly degraded peat top soil. The soil carbon content of the top soil is 33.0% by weight [15,26]. The uppermost highly degraded peat was removed (0–20 cm depths) and transported to a greenhouse at the University of Rostock for the mesocosm experiment. The peat sample was homogenized manually (not sieved to maintain stable aggregates) using a clean rod, and any field-grown plant roots were removed. The peat material originated from a field, which is subjected to regular plowing; we thus assume that the mesocosm setup with homogenized peat material still reflects field conditions [15].

Homogenization was considered necessary to prevent the establishment of preferential flow paths and ensure the validity of the study.

2.2. Mesocosm Experimental Setup

To simulate a vertical flow through constructed wetland with open surface water, a container (polyethylene box) with dimensions of 100 cm length \times 50 cm height \times 30 cm width was used as experimental vessel (Figure 1). Drainage was facilitated through a 4-cm-thick layer of gravel at the bottom of the container, covered with a geo-textile membrane. Peat soil with field moisture content was filled into the container and the redox probes were installed vertically at different depths during the filling procedure. The depth of the peat in the mesocosm was 40 cm, with a total volume of 0.12 m³. Bulk density was adjusted according to field conditions. The space above the peat was used to maintain a surface water table of 3 to 4 cm above the soil. The mesocosm container with peat soil was saturated from the bottom to minimize and remove the entrapped air from the peat, and during the experiments, the flow direction followed the gravimetric potential from top to bottom. The design of the flow through vessel corresponded to a constructed vertical flow wetland with an open water surface, as can be established in tile-drained landscapes where small scale fens often develop in local depressions.

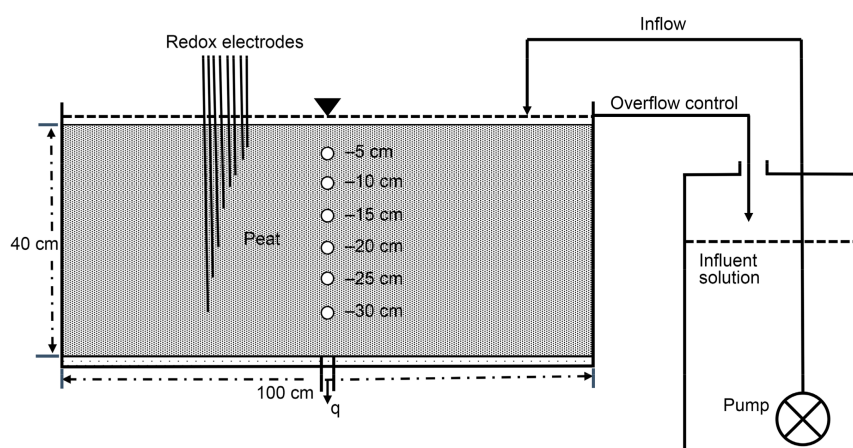


Figure 1. Schematic diagram of the mesocosm experimental set-up and illustration of water and gas sampling locations (−5, −10, −15, −20, −25, −30 cm, and effluent).

The input solution (pH = 7) contained 244 mg/L potassium nitrate (KNO₃) with three different NO₃[−] concentrations adjusted to 65, 100, and 150 mg/L. An NO₃[−] concentration of 65 mg/L (N₆₅) was chosen to represent the average annual NO₃[−] concentration in the ditch near the peat excavation site [27]. NO₃[−] concentrations of 100 mg/L (N₁₀₀) and 150 mg/L (N₁₅₀) represented two and three times the threshold given in the standard drinking water guidelines (50 mg/L [28]), respectively. The turnover experiment was conducted from April to August 2011. N₆₅ was firstly applied, application continued for 50 days, and then the N₁₀₀ was continuously applied for 28 days. After that, the concentration was shifted to N₁₅₀ and maintained for 42 days. Water sampling along the flow path was performed after the turnover experiment.

The flow rate (Q) for the entire experiment was maintained at about 24 liters per day (with a flux of about 8 cm/day; $q = Q/A$, A is the cross-sectional area of the bed container) and was adjusted by varying the hydraulic head. A self-constructed tipping counter, converting an effluent volume of 0.07 liter into an electric pulse, registered the flow rate. The redox potential Eh (mV) was measured at −5, −10, −15, −20, −25, and −30 cm depths below the peat surface by using custom-made 6-mm-diameter redox platinum electrodes (Sentec Ltd. Braintree, Essex, UK) connected to a Delta T DL2e data logger (Delta T Devices Ltd., Cambridge, UK). The measured values were corrected to the standard hydrogen potential E0 (mV) by adding the temperature-corrected voltage of the reference

electrode according to the manufacturer's specifications. The temperature was additionally registered in the container with a Pt100 resistor-type temperature sensor (Ziehl industrie-elektronik GmbH, Schwaebisch Hall, Germany). More details about a similar mesocosm experimental setup can be found in Kleimeier et al. [15].

2.3. Pore Water Sampling

Six micro-piezometers (8-mm PVC pipes) were installed along the flow-path of the mesocosm for the pore water sampling at different depths. Piezometers were mounted horizontally into the peat-body in 5-cm intervals along the central flow path with Teflon gasket tape. The effluent sampling was performed automatically in 12-h intervals, using an ISCO 6712 automated portable sampler (Teledyne Isco Inc., Lincoln, NE, USA). The sampling ports were water- and gas-tight, not interfering with the adjusted flow rate.

The water and gas samples along the flow path were sampled with a 50-mL Braun Perfusor syringe (Carl Roth GmbH, Karlsruhe, Germany), 0.45- μ m syringe-filters (Carl Roth GmbH, Karlsruhe, Germany), and a drip-infusion bag containing nitrogen gas. A syringe was connected to the piezometer (via a flexible extension tube, Carl Roth GmbH, Karlsruhe, Germany) to extract 50 mL of gas containing pore water. The sample (25 mL) was transferred into a second syringe, passing through the 0.45- μ m filter. Immediately thereafter, 25 mL of N₂-gas were added to the syringe to create an anaerobic headspace via a 3-way luer-lock valve. The water samples were degassed by a 90-s ultrasonic treatment immediately after the sampling. The water sample was then transferred into 30-mL PE flasks, gassed with N₂ (to maintain the anaerobic state), and stored at 4 °C until analysis. The gas-phase was transferred into two 10-mL Exetainers (Labco, Ltd., Lampeter, Wales, UK), and analyzed for N₂O using a gas chromatograph (Shimadzu Europa GmbH, Kyoto, Japan). The content of dissolved gas was calculated using Henry's law. In addition, for the water samples, nitrate (NO₃[−]) concentrations were analyzed with an iron chromatograph (METROHM IC 700, Metrohm GmbH & Co. KG Filderstadt, Filderstadt, Germany).

2.4. Parameters and Statistical Analyses

The input NO₃-N_{load} and nitrate removal rate (NO₃-N_R) are given in consumed mass per unit of time and area, g/(m²·day).

$$\text{NO}_3 - \text{N}_{\text{load}} = C_{\text{in}} \times Q / (1000 \times A \times 4.43) \quad (1)$$

$$\text{NO}_3 - \text{N}_R = \Delta C \times Q / (1000 \times A \times 4.43) \quad (2)$$

where C_{in} is the inflow solution concentration (mg/L); Q is the flow rate (L/day); A is the cross-sectional area of the mesocosm system (m²); and ΔC is the difference between the inflow and effluent (C_{out}) concentrations. The nitrate removal efficiency (N_{effi}) was calculated as follows:

$$N_{\text{effi}} = (\text{NO}_3 - \text{N}_R / \text{NO}_3 - \text{N}_{\text{load}}) \times 100\% \quad (3)$$

In order to derive a statistical model that represents the observed nitrate removal rate and efficiency as a function of environmental parameters (temperature, flow rate, and redox potential), the redox potential was grouped into three redox zones: zone 1, aerobic (>500 mV); zone 2, anoxic (150 mV < Eh < 500 mV); and zone 3, anaerobic (Eh < 150 mV) [15,29]. It was intended to calculate the thickness of the soil layer having anoxic or anaerobic conditions over the investigated time (cm/day, namely as the thickness and time duration of redox zone (TD_{zone}). Thus, TD_{zone1}, TD_{zone2}, and TD_{zone3} represent the thickness and time duration of redox zone 1, zone 2, and zone 3, respectively. Non-parametric Kruskal–Wallis [30] tests were performed to analyze whether nitrate removal rate, efficiency, and environmental parameters differed significantly among the three different nitrate input stages. To reveal the influence of nitrate load and environmental parameters on nitrate removal rate

and efficiency, a stepwise linear regression analysis was conducted and all statistical analyses and modeling were performed using the default “stats” package of R [31].

3. Results

3.1. Nitrate Turnover

The amount of nitrate ($\text{NO}_3\text{-N}$) applied in the various stages of the experiment ranged from 0.30 to $3.91 \text{ g}/(\text{m}^2\cdot\text{day})$ as determined on a daily basis analysis. The highest average input loading of $2.66 \text{ g}/(\text{m}^2\cdot\text{day})$ $\text{NO}_3\text{-N}$ was observed for the N_{150} experimental stage. The median $\text{NO}_3\text{-N}$ removal rate over the whole experiment was measured as $1.20 \text{ g}/(\text{m}^2\cdot\text{day})$ (Table 1). Removal efficiency of the entire mesocosm was 63.5%. The median value of difference between nitrate input and effluent concentrations (ΔC , $C_{\text{input}} - C_{\text{output}}$) was 64.0 mg/L . Although three nitrate concentrations (N_{65} , N_{100} , and N_{150}) were supplied into the mesocosm, there was no significant difference in nitrate removal rate between N_{65} , N_{100} , and N_{150} , whereas significances in nitrate load, $\text{NO}_3\text{-N}$ removal efficiency, and ΔC were observed (Table 1). A higher ΔC was observed at N_{100} . The lowest nitrate removal efficiency occurred at N_{150} with an average value of 49.0%. With decreases in the applied nitrate concentration to N_{100} and N_{65} , the nitrate removal efficiency increased to 83.0% and 72.7%, respectively.

Table 1. Nitrate as nitrogen ($\text{NO}_3\text{-N}$) removal rate, removal efficiency and ΔC (difference between nitrate input and effluent concentrations), mean \pm standard deviation, for different nitrate input concentrations: N_{65} (65 mg/L); N_{100} (100 mg/L); N_{150} (150 mg/L). Two groups that are identified by the same letter (a, b, or c) are not significantly different from each other.

Nitrate Input Concentrations	Input Loading	Removal Rate	Removal Efficiency	ΔC
	$\text{g}/(\text{m}^2\cdot\text{day})$	$\text{g}/(\text{m}^2\cdot\text{day})$	%	mg/L
N_{65}	$1.72 \text{ b} \pm 0.90$	$1.19 \text{ a} \pm 0.57$	$72.7 \text{ a} \pm 16.1$	$47.2 \text{ b} \pm 10.5$
N_{100}	$1.46 \text{ b} \pm 0.50$	$1.15 \text{ a} \pm 0.30$	$83.0 \text{ a} \pm 18.2$	$83.0 \text{ a} \pm 18.2$
N_{150}	$2.66 \text{ a} \pm 0.69$	$1.22 \text{ a} \pm 0.34$	$49.0 \text{ b} \pm 10.9$	$73.3 \text{ a} \pm 16.2$
Median	1.92	1.20	63.5	64.0

3.2. Environmental Factors

Temporal variation of the temperature and fluxes over the entire experimental period are illustrated in Figure 2. The mean volumetric flow was 25.8 L/day with a standard deviation of 12.9 L/day . The mean temperature was 26.2°C and varied between daily average values of 15.5°C and 38.8°C over the 120 days of the experiment. A redox potential of less than 500 mV was observed at 5 cm soil depth and remained almost constant over the entire experiment period (Figure 2). Redox potentials at 5 to 15 cm depth ranged from 150 mV to 500 mV. Below a 30-cm depth, the redox potential remained under 150 mV over the observation period.

The temperature and flux varied between the three experimental stages of N_{65} , N_{100} , and N_{150} inputs (Figure 3). The flow rates at N_{65} were significantly higher than those at N_{100} and N_{150} , although we intended to maintain a constant flow rate. The average temperature for the N_{100} stage was 30.5°C , which was higher than that at N_{65} (25.6°C) and N_{150} (23.8°C). No significant differences in the thickness and time duration of the redox zone $\text{Eh} < 500 \text{ mV}$ among N_{65} , N_{100} , and N_{150} were detected. For denitrification zones ($150 \text{ mV} < \text{Eh} < 500 \text{ mV}$ and $\text{Eh} < 150 \text{ mV}$), the lowest values of TD_{zone2} and TD_{zone3} were observed in N_{100} and N_{150} stages, respectively (Figure 3).

A stepwise linear regression analysis was conducted to delineate the individual specific effect of temperature and flux variations on nitrate turnover processes. The models with four parameters were developed to predict the nitrate removal rate and efficiency (Figure 4). A summary of these linear model results is given in Table 2. According to the r^2 statistic, the regression models revealed a 68% and 65% of the overall variance for estimation of nitrate removal rate and efficiency, respectively. In both models, most of the variability was attributable to the nitrate load (about 48%). The flux and

temperature variations together accounted for approximately 20% of the total variation. Among them, the temperature contributes to 10% of the total variance.

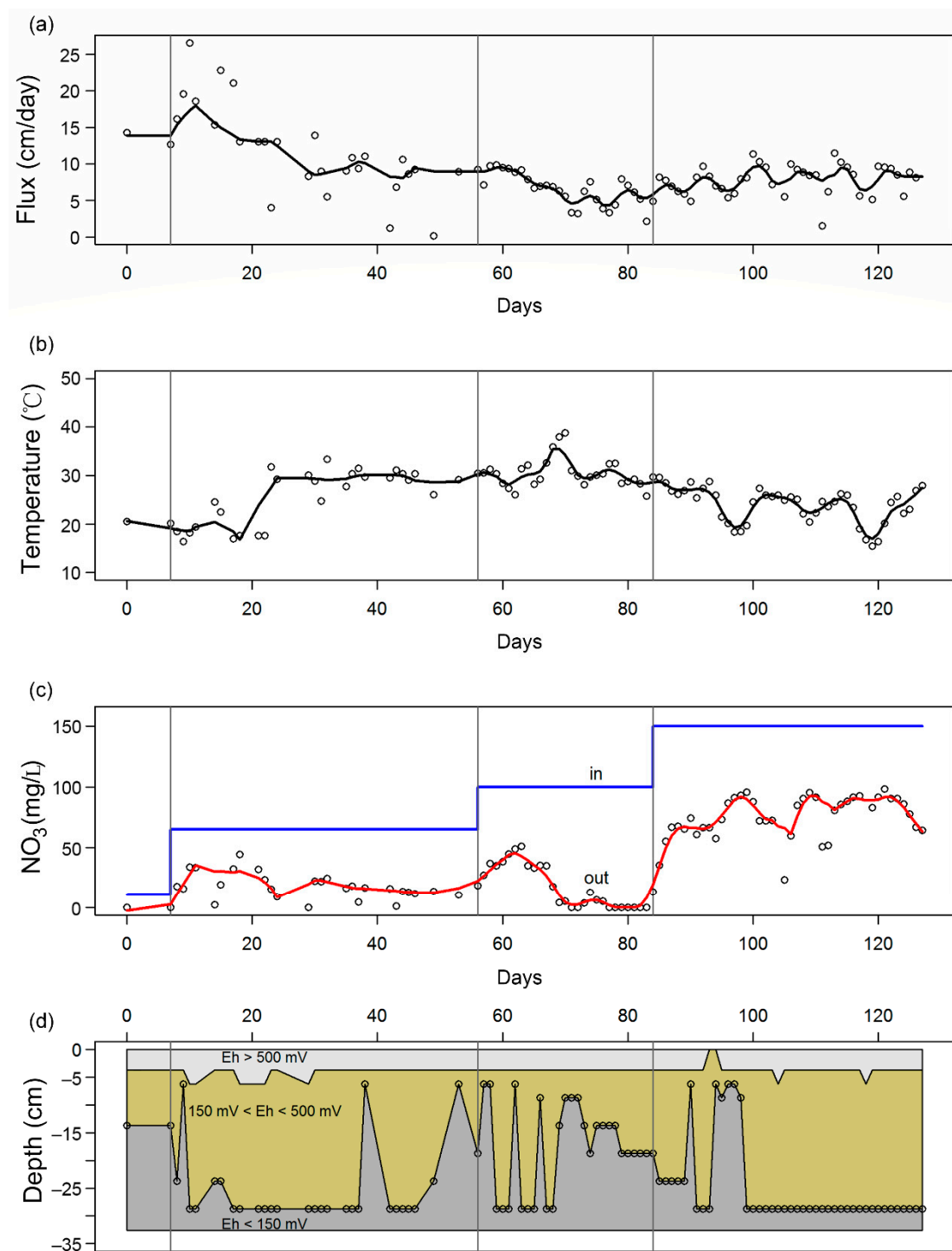


Figure 2. Overview of the flux (a), temperature (b), nitrate concentration (c), and redox potential zone (d) of the mesocosm experiment.

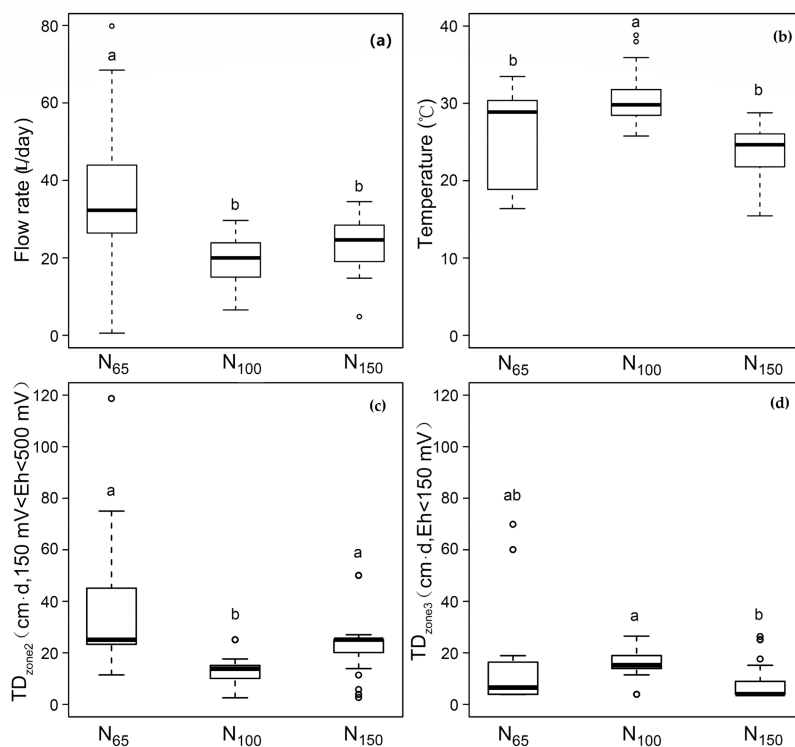


Figure 3. Boxplot of flow conditions, temperature, and thickness and time duration of redox zone (TD_{zone}) under different supplied nitrate concentrations of 65, 100, and 150 mg/L (N_{65} , N_{100} , N_{150} , respectively). Two groups that are identified by the same letter (a, b or c) are not significantly different from each other. (a) flow rate; (b) Temperature; (c) TD_{zone2} (150 mV < Eh < 500 mV); (d) TD_{zone3} (Eh < 150 mV).

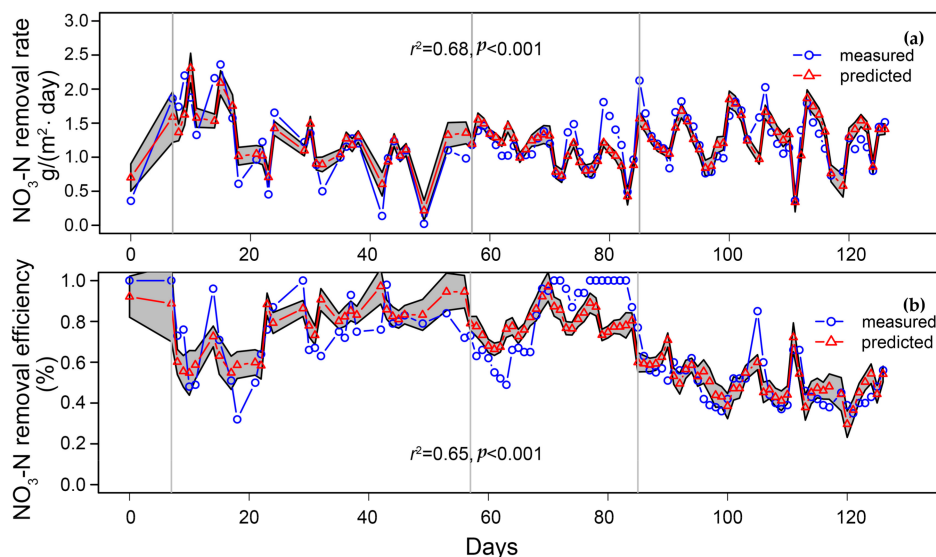


Figure 4. Measured (blue lines) and predicted (red line) values of nitrate removal rate and efficiency with multiple linear regression models. The grey zone is the 95% confidence of the interval of predicted values. (a) NO_3-N removal rate (b) NO_3-N removal efficiency.

Table 2. Multiple linear regression of nitrate as the nitrogen ($\text{NO}_3\text{-N}$) removal rate and efficiency with nitrate load, temperature, flow rate, and thickness and time duration of the redox zone (TD_{zone}). Level of significance ($p < 0.05$).

Index	Independent Variables	Coefficient	Explained Variance (%)
Removal rate, $\text{g}/(\text{m}^2 \cdot \text{day})$	Intercept	−0.800	−
	Input load	0.338	48.0
	Temperature	0.035	11.2
	Flow rate	0.014	6.8
	$\text{TD}_{\text{zone}3}^a$	0.004	2.2
	Adjusted r^2	0.668	−
Removal efficiency, %	Intercept	0.329	−
	Input Load	−0.152	46.8
	Temperature	0.018	8.1
	Flow rate	0.006	8.7
	$\text{TD}_{\text{zone}3}$	0.002	2.3
	Adjusted r^2	0.645	−

^a $\text{TD}_{\text{zone}3}$: Thickness and time duration ($\text{cm} \cdot \text{day}$) of redox zone 3 ($\text{Eh} < 150 \text{ mV}$).

4. Discussion

4.1. Nitrate Removal Rate and Efficiency

The nitrate removal rate of a biological denitrification process is strongly dependent on the multitude of possible C-sources for denitrification and the range of applied nitrogen loads. Nitrate removal is generally limited by the availability of C-sources [7]; adding an extra carbon source to denitrification bacteria in CWs could enhance the denitrification rate. In this study, a peat soil served as a C-source for the denitrification processes (C:N ratio of 10:1) [15]. The observed nitrate removal rates ($1.21 \text{ g}/(\text{m}^2 \cdot \text{day})$, $\text{NO}_3\text{-N}$) are significantly higher than those reported for CWs with mineral soils and natural wetlands ($\text{NO}_3\text{-N}$ from 0.06 to $0.92 \text{ g}/(\text{m}^2 \cdot \text{day})$) [32,33]. The values were within nitrate removal rates found for woodchips (ranging from 0.7 to $5.0 \text{ g}/(\text{m}^2 \cdot \text{day})$ $\text{NO}_3\text{-N}$) [7,34]. The obtained nitrate removal efficiency is higher than that reported for coco-peat (54%) and organic soils (20%) [16,35]. The reason probably was that lower oxygen concentrations (lower redox potential values) were observed in this study, especially at the bottom of the container. The nitrate removal rate at N_{100} was only a little lower than the rates estimated for wood-based filters (87% to 97%) [36]. However, at a later stage of the N_{100} variant, nitrate was almost completely removed (>95%), suggesting denitrification is limited by the nitrate concentration [36,37]. Thus, peat soils may have a comparable ability to wood products for removing nitrate in CWs.

4.2. Nitrate Load, Hydraulic Load, and Nitrate Removal Rate

Under nitrate-limiting conditions, an increasing nitrate input load would accelerate the nitrate removal process [38]. In this study, increasing the mean nitrate load from $1.46 \text{ g NO}_3\text{-N m}^{-2} \text{ day}^{-1}$ (N_{100}) to $2.66 \text{ g NO}_3\text{-N g}/(\text{m}^2 \cdot \text{day})$ (N_{150}) did not significantly improve the nitrate removal rate. We therefore assume that environmental factors (e.g., soil temperature) restrained the denitrification processes at N_{150} . When a nitrate load of less than $1.72 \text{ g}/(\text{m}^2 \cdot \text{day})$ $\text{NO}_3\text{-N}$ was supplied to the system, the nitrate effluent concentration ($<10 \text{ mg/L NO}_3\text{-N}$ or 50 mg/L NO_3) was always lower than the standard values for drinking water quality. However, at a larger nitrate load (e.g., $2.7 \text{ g}/(\text{m}^2 \cdot \text{day})$), the effluent concentration would often fall into the worst water quality class ($>20 \text{ mg/L NO}_3\text{-N}$). For the setting in this study, the nitrate load should be limited to below $1.7 \text{ g}/(\text{m}^2 \cdot \text{day})$ if degraded peat soil is used as the bed material to ensure water quality standards. In the regression models, the coefficient of the input load was positive for the nitrate removal rate but negative for nitrate removal efficiency because the nitrate removal rate increased less than the input load. Thus, removal efficiency decreased with increasing nitrate input load.

It has been reported that a higher hydraulic load commonly leads to high nitrate removal in CWs [39] because a higher flow rate often means a higher nitrate load and thus more nitrate available

for denitrifying bacteria [40]. In this study, a positive relation between the hydraulic load and nitrate removal rate could be confirmed from the daily data set (Pearson's correlation coefficient of 0.67, $p < 0.01$). Our results are in line with a previous study [39], which stated that the nitrate removal rate is higher under a high hydraulic load condition. However, nitrate input load ($C_{\text{input}} \times Q$) rather than flow rate (Q) has a high negative correlation with removal efficiency (Pearson's correlation coefficient of 0.69, $p < 0.01$). Therefore, the status of an environmental system such as a catchment shall be evaluated on the basis of the total nutrient mass that has been released into the system. Lower ΔC values were observed for N_{65} at which the hydraulic load was highest (Figure 5a). Comparable ΔC values were obtained for N_{100} and N_{150} . We assumed that under a comparable nitrate load, faster flow rates would shorten the nitrate retention time in the system, resulting in a less effective transformation process [41]. For N_{150} , the output nitrate concentration always exceeds the standards for nitrate in drinking water (NO_3^- , 50 mg/L). Therefore, nitrate removal is very efficient up to an input concentration of 100 mg/L. When summarizing all data, a medium negative correlation between flow rate and ΔC (Figure 5b) indicates that the retention time plays an important role in the nitrate attenuation in peat.

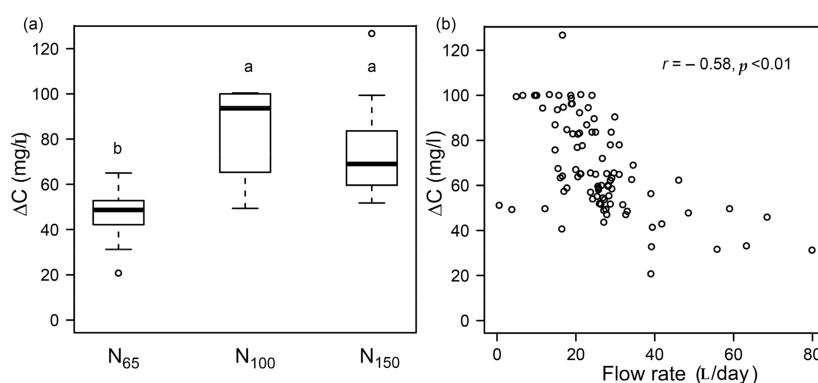


Figure 5. Boxplot of (a) ΔC (difference between nitrate input and effluent concentrations) under different supplied nitrate concentrations (N_{65} , N_{100} , N_{150}) and (b) scatter plot of flow rate (L/day) against ΔC .

4.3. Influence of the Temperature and Redox Potential on Nitrate Reduction

The nitrate removal efficiency is temperature- and oxygen-dependent [42–44] because higher temperature and oxygen availability increase the microbial activity in soils. In mineral soils, optimum temperatures for nitrification range from 15 to 35 °C [45] and for denitrification from 25 to 35 °C [46]. The highest nitrate removal efficiency was observed at the N_{100} period in which higher temperatures (about 30 °C) prevailed. Likewise, the regression model analysis clearly expressed the importance of temperature for the denitrification process in this study, where the temperature was more important than the extent and duration of oxygen-depleted zones (Table 2). A positive relationship was also found between nitrate removal efficiency and the TD_{zone} of denitrification zones, with redox potentials of less than 150 mV (Pearson's correlation coefficient of 0.31, $p < 0.01$). The thickness and time duration of the denitrification zone represent another factor affecting the nitrate removal efficiency, although they are less important than temperature, flow rate, and input loading (Table 2).

4.4. Nitrate Turnover Along the Flow Path

Redox-sensitive solution sampling with a 5-cm resolution along the central flow path was conducted additionally to the regular automated effluent sampling. Measurements for nitrate and pH as well as the dissolved gas N_2O are shown in Figure 6. As expected, the redox potential decreases with increasing depth. Below a depth of 15 cm, the conditions are anaerobic. In general, nitrate concentrations were relatively high in the upper 25 cm. Lower nitrate concentrations were found closer to the bottom of the mesocosm in areas with lower redox potential indicating the bottom part of the

container as the active denitrifying zone. The pH values ranged between 7.5 and 8, suggesting that N_2 is the dominant denitrification product [47]. The dissolved N_2O concentrations at all depths were low, confirming that the denitrifying bacteria convert nitrate to nitrogen gas (N_2) under anaerobic conditions [48].

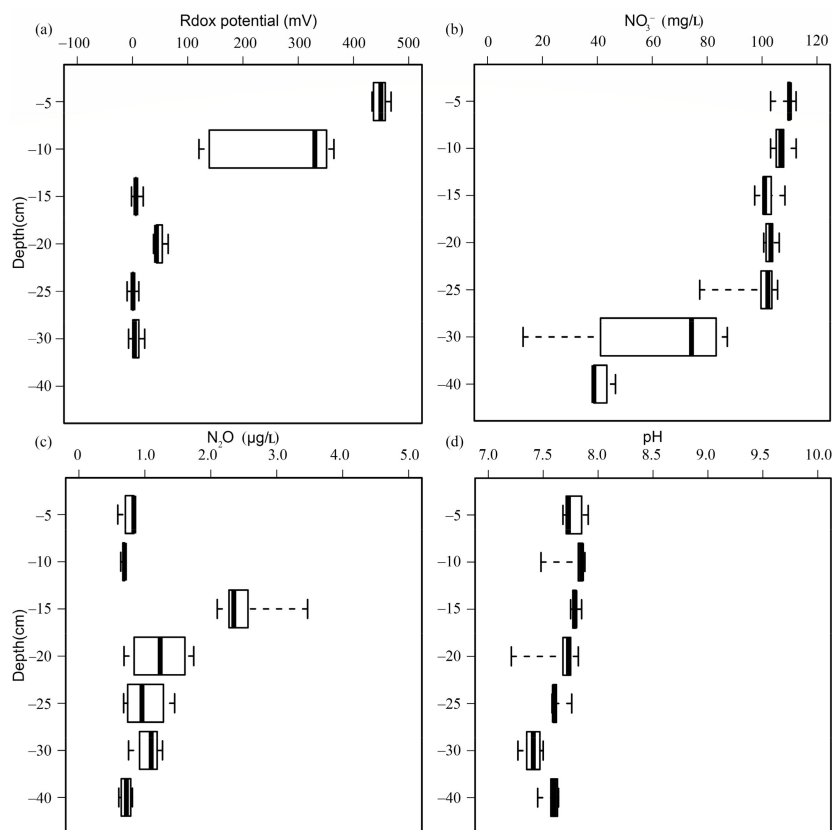


Figure 6. Redox potential (a), nitrate NO_3^- (b), and dissolved gasses N_2O (c) as well as the pH (d) at different depths in the mesocosm experiment.

5. Conclusions

In this study, we examined the suitability of degraded peat as a bed medium and C-source for nitrate removal in constructed wetlands. The nitrate removal rates and efficiency in degraded peat soils were comparable to those observed in woodchips reactors. The observed nitrate removal efficiency was strongly affected by the nitrate load and the environmental parameters, including flow rate, temperature, and redox potential. The highest removal efficiency (and ΔC) was obtained at N_{100} , with a lower flow rate and higher temperature. The lowest nitrate removal efficiency occurred at N_{150} , with an average value of 49.0%, where the nitrate removal efficiency increased to 83.0% and 72.7% with decreases in the applied nitrate concentration to N_{100} and N_{65} , respectively. Under a comparable nitrate input load, a continuous and low flow rate over a long-term period would extend the nitrate retention time, resulting in a more effective transformation process. The results showed that under a comparable nitrate load conditions, the nitrate retention time gets shorter under faster flow rates, resulting in a less effective nitrate transformation process. This paper clearly demonstrates the suitability of degraded peat as a bed medium for nitrate removal in constructed wetlands. For practical field-scale applications, the “flushing effect” of nitrate and dissolved organic carbon at early stages of the establishment of a CW should be taken into account to avoid unintended contamination of surface water bodies [15].

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