

Article

Energy-Recovery Pressure-Reducer in District Heating System

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Abstract: Already existing man-made infrastructures that create water flow and unused pressure are interesting energy sources to which micro-hydropower plants can be applied. Apart from water supply systems (WSSs), which are widely described in the literature, significant hydropower potential can also be found in district heating systems (DHSs). In this paper, a prototype, a so-called energy-recovery pressure-reducer (ERPR), utilized for a DHS, is presented. It consisted of a pump as a turbine coupled to a permanent magnet synchronous generator (PMSG). The latter was connected to the power grid through the power electronic unit (PEU). The variable-speed operation allowed one to modify the turbine characteristics to match the substation's hydraulic conditions. The proposed ERPR device could be installed in series to the existing classic pressure reducing valve (PRV) as an independent device that reduces costs and simplifies system installation. The test results of the prototype system located in a substation of Cracow's DHS are presented. The steady-state curves and regulation characteristics show the prototype's operating range and efficiency. In this study, the pressure-reducer impact on the electrical and hydraulic systems, and on the environment, were analyzed. The operation tests during the annual heating season revealed an average system's efficiency of 49%.

Keywords: hydroelectric power generation; pump as a turbine (PAT); power generation control; hydraulic systems; variable speed drives; water resources

1. Introduction

Micro-hydropower plants (MHPs), whose power output is typically below 100 kW, have gained increasing attention due to their energy recovery capability in existing infrastructures [1]. A potential energy source can be found in any system that comprises water flow and unused pressure, i.e., water networks dealing with drinking water, wastewater (raw or treated), irrigation water, runoff water (rain or storm water), as well as cooling and heating systems [2,3]. Besides respecting basic water parameters (flow rate and pressure), the MHP can be designed according to water quality (wastewater) and temperature (cooling and heating systems). The generation of electrical energy is a supplementary function of water infrastructures. Therefore, a bypass valve and a secure shutdown system for the turbine are required. MHPs as renewable energy sources provide benefits for both the supplier (reduction of transmission losses) and the customer (reliability and reduced price) [4].

In recent literature, water supply systems (WSSs) are emphasized as the main man-made infrastructure that offers micro-hydropower potential. WSSs that are located in lower topographic areas suffer from excess pressure. This energy surplus, which is commonly dissipated via pressure-reducing valves (PRVs) [5,6], can be recovered by applying MHPs. The excess pressure is mainly present in transmission pipes and between sub-grids, but also inside the network and at the building entrance. Pressure reduction also leads to a decreasing leakage problem because water loss increases with

increasing pressure [7]. However, the MHP location that maximizes the energy production may not be optimal regarding leakage reduction [8]. The optimal location of the MHP within urban WSSs is difficult because of the complex network topology (multiple loops) and asymmetric water demand. Therefore, earlier studies have mainly been conducted in particular locations [9,10].

The MHP's efficiency is affected mainly by the water turbine's characteristics. To obtain high efficiency under a wide range of parameter variations, a traditional turbine can be used. In literature, some dedicated turbine solutions for power generation from water pipelines can be found. For instance, a novel vertical-axis water turbine [11] and an inline five blade tubular propeller turbine [12] were analyzed (through computational fluid dynamic calculations) and successfully tested. However, the available power at a given WSS location is limited. To shorten the payback period of the turbine, costs need to be minimized. Therefore, pumps-as-turbines (PATs) seem to enable a good compromise between efficiency, operating range, and costs [13–16]. Unfortunately, the prediction of the PAT's performance is still a troublesome issue, and procedures that select the best solution for given conditions are under development [17]. A specific design procedure, the so-called Variable Operating Strategy, of an MHP is developed in References [18–20]. The procedure uses PAT as a production device that maximizes the energy production under variable operating conditions (flow discharge and pressure drop). Two power plant regulation systems are considered. In the hydraulic regulation mode, the system is composed of the dissipation (PRV) and production (PAT) branch bypassed by another dissipation (PRV) branch. The electrical regulation mode employs an inverter ensuring variable rotational speed.

Another system with hydropower potential is presented by a district heating system (DHS). This infrastructure is not well investigated yet regarding energy recovery. The energy production analysis presented in Reference [21] (on the example of the Cracow DHS) has confirmed the system's high potential. Similar to a WSS, the water parameters (pressure and flow rate) fluctuate in time. This is caused by the daily and seasonal changes in outdoor temperatures. The excessive energy can also result from landform features, but the main cause of the excess pressure is the system's growth. This situation requires higher pressure at the heat source, which consequently creates points where the pressure needs to be reduced. The values of the reduced pressure and flow rate can be identified in the piezometric graphs that present the pressure distribution in the network at specific locations, considering a geodesic profile. In Reference [21], a calculation of the recoverable surplus energy is presented with two variants that differ in energy recovery location (variant I: substations, variant II: network mains). The advantage of variant I is that the produced energy can be utilized directly for the installation, e.g., by circulating pumps. If the annual heat season lasts 6 months and the MHP's average efficiency equals 50%, the calculated recovery energy measures 1.7 GWh/year and 2.7 GWh/year for variants I and II, respectively. An economic analysis enabled a calculation of the investment's return time, which lasted 5 and 7 years for variants I and II, respectively.

The mentioned analysis indicated the DHS's significant potential for energy recovery. Therefore, a prototype device, a so-called energy recovery pressure reducer (ERPR) applying a centrifugal PAT, was designed [22]. The prototype (2 kW) contains a permanent magnet synchronous generator (PMSG) and a power electronic unit (PEU). The PEU allows for an improvement in the ERPR's conversion efficiency and enhances the operating range by applying variable speed operation [23,24]. The preliminary tests were performed in a real heating network. The identified steady-state characteristics present the dependence of reduced pressure on the turbine speed, and the maximal system efficiency equals 60%. Further, the tests indicate some issues that need to be improved, such as high water temperature (bearing, generator cooling) and the ERPR's operating range (turbine type).

This paper presents an improved ERPR prototype that was tested in the Cracow DHS. The ERPR is located in the network's substation with a heat exchanger where the circulating pumps utilized all recovered energy. The prototype ERPR of 5 kW consisted of a multi-stage vertical PAT combined with a PMSG connected to the grid through a PEU. Besides the steady-state characteristics, the influence of the ERPR on the electrical and hydraulic systems, and on the environment, were analyzed. Therefore,

noise, as well as electrical and vibration signals, were investigated in detail. Furthermore, the ERPR operation during the annual heating season is presented and analyzed.

2. Pressure-Reduction System with Energy Recovery

2.1. Energy Potential

The main function of a DHS is to supply the customer with heating energy. Considering the initial investment, maintenance, and operation costs, the most prevalent solution is a two-pipe system, as presented in Figure 1a. Here, hot water is transported from the heat source to a substation through one pipe and returned by another [25]. In indirect systems, the parameters of the district heating medium (water), which is delivered from the heat source, are converted into suitable parameters (demanded by the customer) by a heat exchanger in the substation (Figure 1c). The heat exchangers transfer heat from the primary loop (district heating) to the secondary loop (customer) without mixing the fluids. This process requires a specific flow rate and water temperature of the primary loop. The supply temperature is changed (from 75 °C up to 120 °C), depending on the outdoor temperature, by the heat source according to a specific profile. The flow rate is adjusted by the substation's differential pressure (between input and output). The heat source should provide a differential pressure in the last substation (usually the worst-situated) equal to or higher than the minimal disposal pressure $\Delta p_{\min, \text{dis}}$ (usually 0.15–0.2 MPa). The latter is needed to cover the conduction losses of the heat exchanger and the control valve requirement (Figure 1b). The differential disposal pressure of the remaining substations is higher.

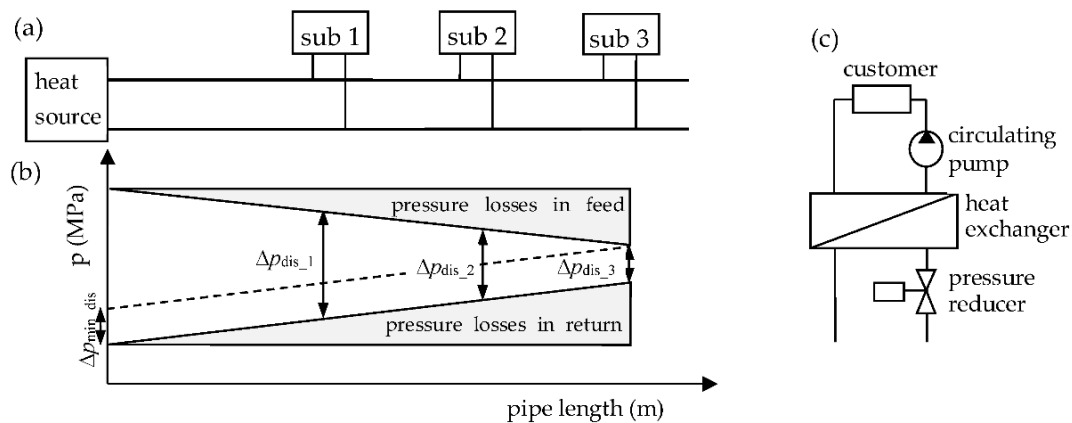


Figure 1. Pressure distribution in DHS: (a) two-pipe heating network; (b) pressure distribution along the heating pipe; (c) substation with heat exchanger.

The differential excess pressure of the substation n ($\Delta p_n = \Delta p_{\text{dis}, n} - \Delta p_{\min, \text{dis}}$) can be used by the ERPR to produce the electrical active power P (W) according to the formula:

$$P = \gamma \cdot H \cdot Q \cdot \eta = 10^6 \cdot \Delta p_n \cdot Q \cdot \eta \quad (1)$$

where γ (N/m³) is the specific weight of water, Q (m³/s) is the volumetric flow rate, H (m) is the head drop, η is the total ERPR efficiency, and $\Delta p_n = \gamma H$ (MPa) is the differential hydrostatic excess pressure of substation n , where $H = 106.4 \cdot \Delta p_n$ under water temperature equals 100 °C.

The total ERPR efficiency is the product of the turbine efficiency ($\eta_t = 0.5$ – 0.85), which depends on the flow range and rotational speed, generator efficiency ($\eta_g = 0.8$ – 0.97), and efficiency of the PEU ($\eta_p = 0.9$ – 0.98):

$$\eta = \eta_t \cdot \eta_g \cdot \eta_p \quad (2)$$

The actual ERPR efficiency depends on the operating parameters (flow rate and differential pressure) and applied technical devices (mainly the turbine type). The efficiency variation may be significant ($\eta = 0.35\text{--}0.8$) [26–29]. Thus, the ERPR design process has key importance for the system's profitability.

2.2. Topology of Substation with ERPR

The heat demand of the customer is highly dependent on the outdoor temperature. Usually, the flow rate of the secondary loop remains constant, whereas the temperature is adjusted. The secondary loop's temperature as a function of the outdoor temperature, the so-called heating curve, is implemented in a substation-control system, which adjusts the PRV (Figure 2). A proper control of the PRV requires minimal disposal pressure. Each excess pressure is recovered by the ERPR in the form of electrical active power (Equation (1)).

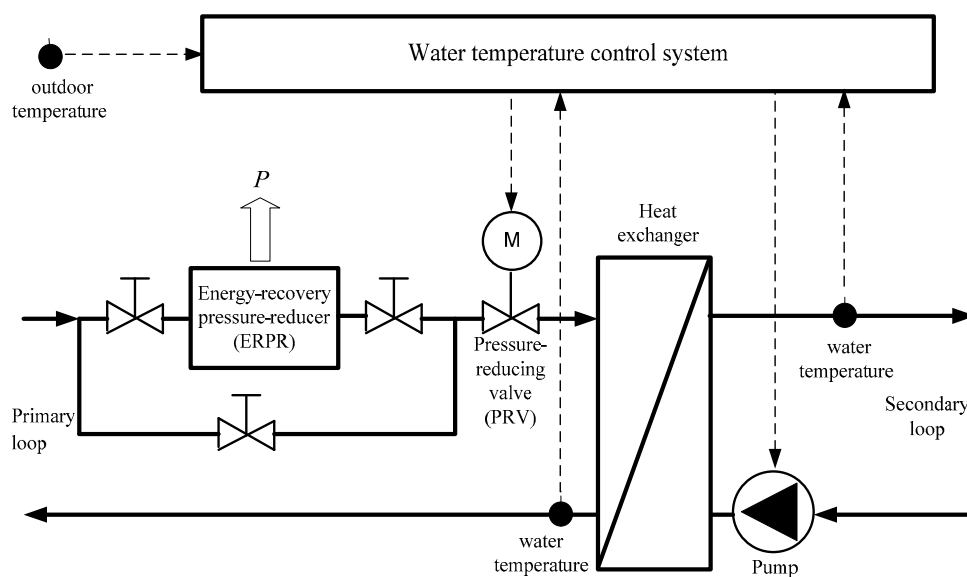


Figure 2. Block diagram of the district heating substation with ERPR.

To maximize the energy production, two system-regulation modes can be used. As presented in Reference [19], better features (wider range of operating conditions) are obtained using the hydraulic regulation mode, which is realized by a series–parallel combination of PAT and PRV. However, this regulation mode requires two regulated PRVs and a modification to the substation's control system.

By applying the electrical regulation (ER) mode [20], the ERPR can be added in series to the existing PRV as an independent device without any modifications to the control system (Figure 2). The system modification concerns only the ERPR bypass, which is required for a safe operation. In case of a situation where the differential excess pressure of the substation exceeds the operation range of the ERPR, or the ERPR breaks, the PRV takes over the pressure control. The ER enables the variable speed operation method. Therefore, the characteristic PAT curves are modified by changing the turbine speed to match the load conditions (instant flow rate and differential pressure). The low costs of the electromechanical components and engineering can shorten the payback period of this system. Furthermore, the installation process is simple, and does not require modifications to the existing control system. Therefore, this solution is proposed in this paper.

The ERPR should be carefully designed regarding the variability of the hydraulic conditions of the specific substation to maximize the average efficiency, which corresponds to the system capability [19]. This implies that the ranges of the most frequently occurring flow rates and differential excess pressures have to be covered by the PAT curves of the highest efficiency.

2.3. ERPR Unit

To reduce costs, the ERPR unit was based on the PAT. The turbine was connected to the PMSG, which has a higher and more stable efficiency under load variation than an induction machine. The regulation process (control of turbine speed) was performed by a full-scale PEU. The PEU matches the parameters of the electrical energy generated by the PMSG to the power system requirements. This enabled an on-grid operation [30]. The structure of the proposed ERPR is presented in Figure 3.

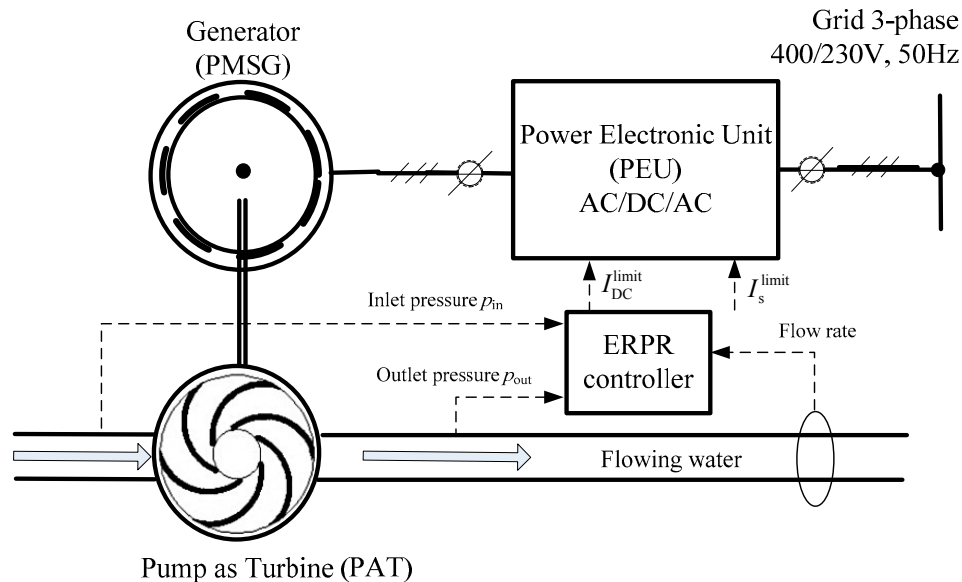


Figure 3. Main elements of an ERPR.

The ERPR controller measures the actual inlet and outlet pressure, as well as the flow rate. Different ERPR control targets are possible. It can regulate one of the hydraulic parameters (pressure drop, outlet pressure, or flow rate), maximal electrical power, or maximal efficiency. Furthermore, by integrating the ERPR into the substation control system, the water temperature of the secondary loop can be adjusted. However, it should be noted that the main function of the ERPR is the maximization of the energy recovery. Considering the limited operation range of the PAT, the substation control should be performed by the PRV. Thus, the control mode that provides maximal electrical active power and keeps the differential pressure higher or equal to the minimal disposal value seems to be the most appropriate.

Nowadays, there are many PEU solutions on the market that can be used for the proposed ERPR. The most popular are the two types presented in Figure 4.

The first system presented in Figure 4a consists of a diode bridge rectifier (AC/DC), a circuit that raises the DC voltage (DC/DC booster), and a PWM (pulse width modulation) inverter controlled by the DPC-SVM (direct power control with space vector modulation) algorithm [31,32]. The second type, shown in Figure 4b, employs a PWM rectifier (also called the sinusoidal rectifier) instead of a diode rectifier and a DC/DC booster.

The generator load can be controlled with the current limits I_s^{limit} and $I_{\text{DC}}^{\text{limit}}$ of the PEU. The current limit changes allow for the modification of the regulation curves as a function of rotational speed [33,34]. This is presented in Figure 5.

The current limit of the inverter (I_s^{limit}) corresponds to the electrical active power of the PEU assuming a constant grid voltage and no reactive power. Furthermore, after neglecting the power losses of the PEU, it can be stated that I_s^{limit} controls the generator's active power (Figure 5a). The second control parameter $I_{\text{DC}}^{\text{limit}}$ is proportional to the generator current, and in the case of a PMSG, it corresponds to the generator torque (Figure 5b).

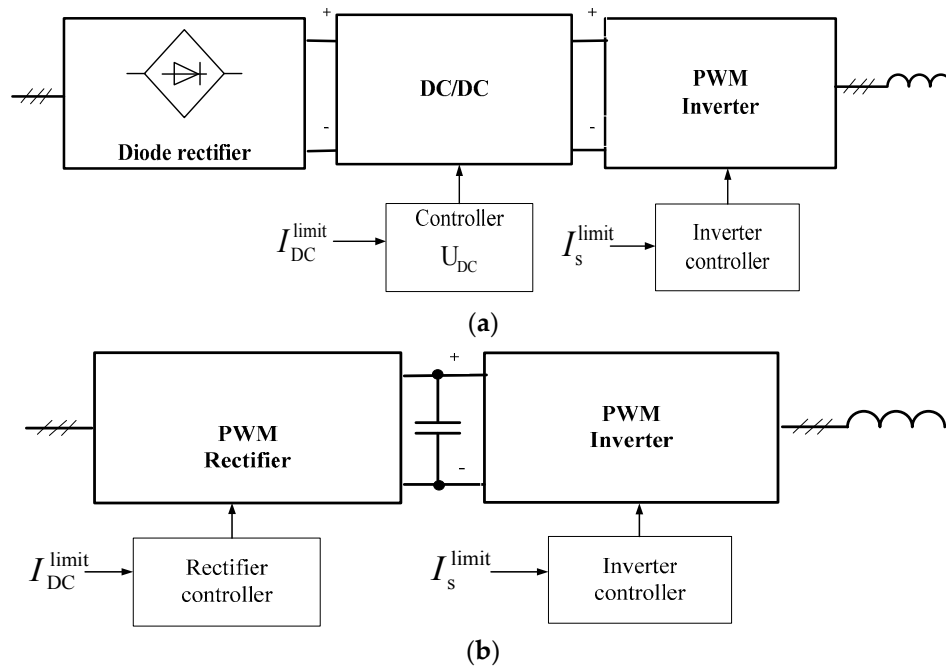


Figure 4. Block diagram of a Power Electronic Unit (PEU) with: (a) a diode rectifier and DC/DC booster; and (b) a PWM rectifier.

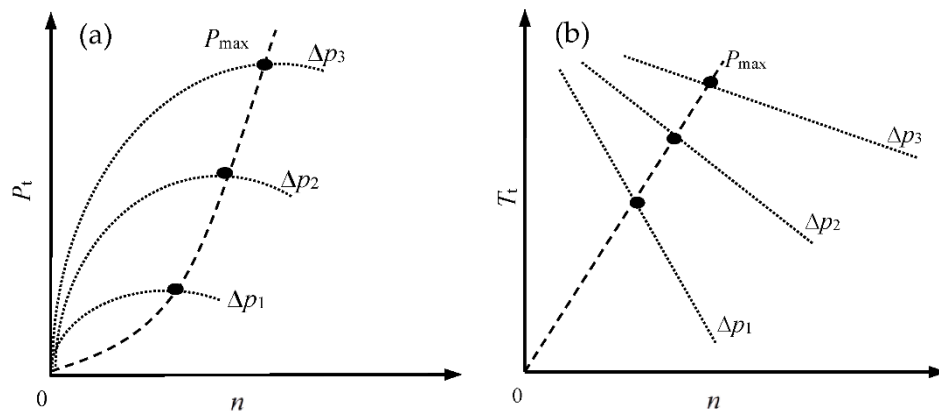


Figure 5. PEU control curves showing characteristics of: (a) power $P(n)$ and (b) PMSG torque $T(n)$ for different values of I_s^{limit} and $I_{\text{DC}}^{\text{limit}}$.

The selection of the control parameter must be done by considering the shape of the turbine curves. Examples of curves for different values of reduced pressure in the speed domain are presented in Figure 6. It can be noticed that under some conditions the PEU and PAT torque curves can be parallel to each other. This situation may result in speed oscillations and even in an unstable control. Therefore, the ERPR control should be performed at the $I_{\text{DC}}^{\text{limit}}$ limit. The presented figures also contain the optimal operation curve that provides the maximal turbine power and, therefore, the control target.

The speed value, located at the cross point of the PEU and PAT torque characteristics, is set by $I_{\text{DC}}^{\text{limit}}$ for a specific reduced pressure, as presented in Figure 7. The main function of the ERPR controller is to adjust the turbine speed according to the set reduced pressure to provide the maximal electrical active power of the PEU. According to the chosen control mode, the reduced pressure is equal to the actual differential excess pressure of the substation.

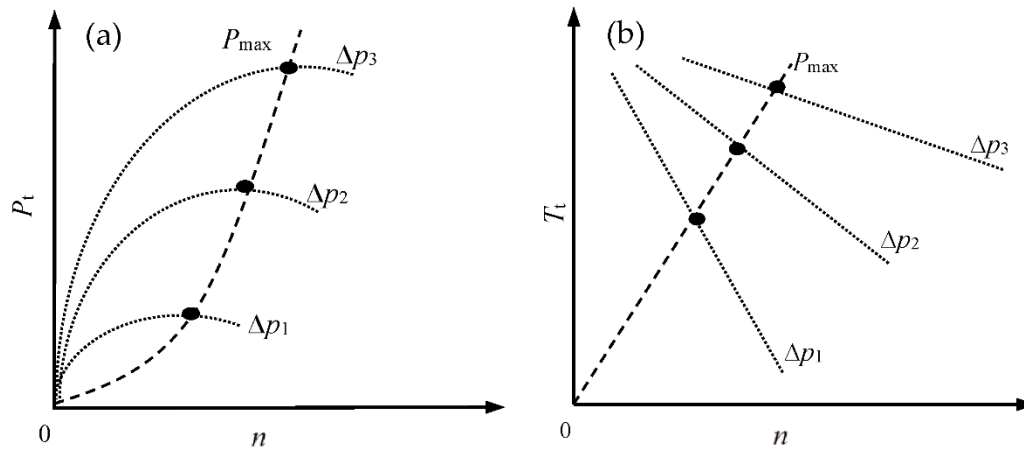


Figure 6. PAT curves showing characteristics of: (a) power $P_t(n)$; and (b) torque $T_t(n)$ for different values of reduced pressure Δp .

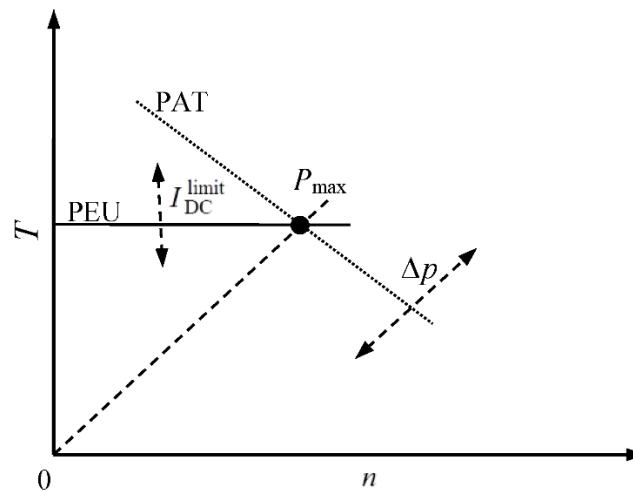


Figure 7. Location of optimal operation point according to torque characteristic (PEU and PAT).

3. ERPR Prototype and Steady-State Characteristics

The ERPR prototype was installed in a DHS substation that contained a heat exchanger of 1.8 MW thermal power, and had a nominal flow rate of $0.0064 \text{ m}^3/\text{s}$ and an available differential disposal pressure of 0.7 MPa. The chosen turbine was a three-stage vertical PAT with a nominal flow rate of $0.0058 \text{ m}^3/\text{s}$ and a reduced pressure of 0.5 MPa ($H = 53.2 \text{ m}$). The PAT was connected through box-coupling to the PMSG with a synchronous speed of 3000 rpm. The PEU of 5.5 kW contained the two optional rectifier types (diode bridge rectifier with DC/DC booster and sinusoidal PWM rectifier), as presented in Figure 4. The rated values and nominal parameters are listed in the Appendix A (Table A1). The ERPR prototype installed in the substation of the Cracow DHS is shown in Figure 8. All measurements were performed according to the ISO 9906 standard (grade 2B) [35]. The test installation was equipped with additional valves allowing for the control of the substation input pressure.

The ERPR performance was identified by the steady-state characteristics of the PEU active power (Figure 9a), estimated turbine torque (neglecting PMSG and PEU efficiency) (Figure 9b), and flow rate (Figure 9c) under four different values of reduced pressure (0.45, 0.55, 0.6, and 0.68 MPa). Additionally, the total ERPR efficiency was calculated (Equation (1)) and shown in Figure 9d. Figure 10 presents the electrical energy production and total efficiency in the flow-rate domain. The measurement points are marked by crosses.

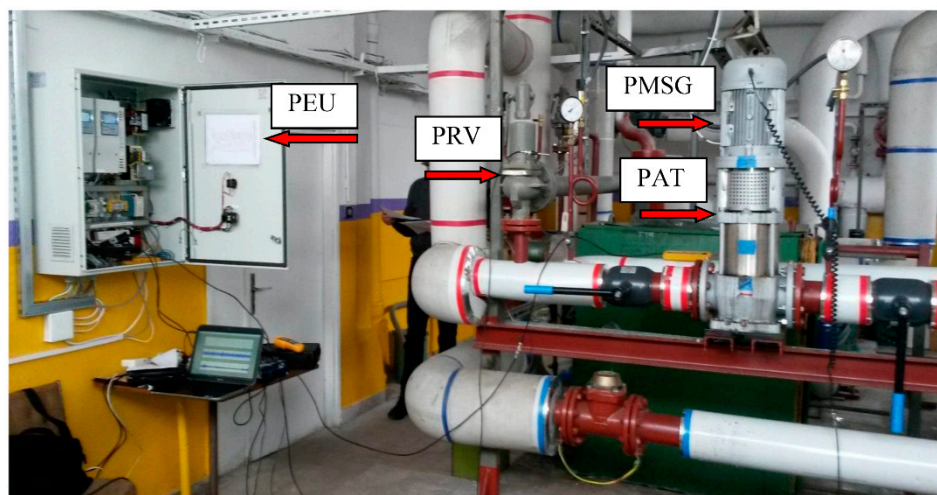


Figure 8. ERPR prototype installed in the substation of the Cracow DHS.

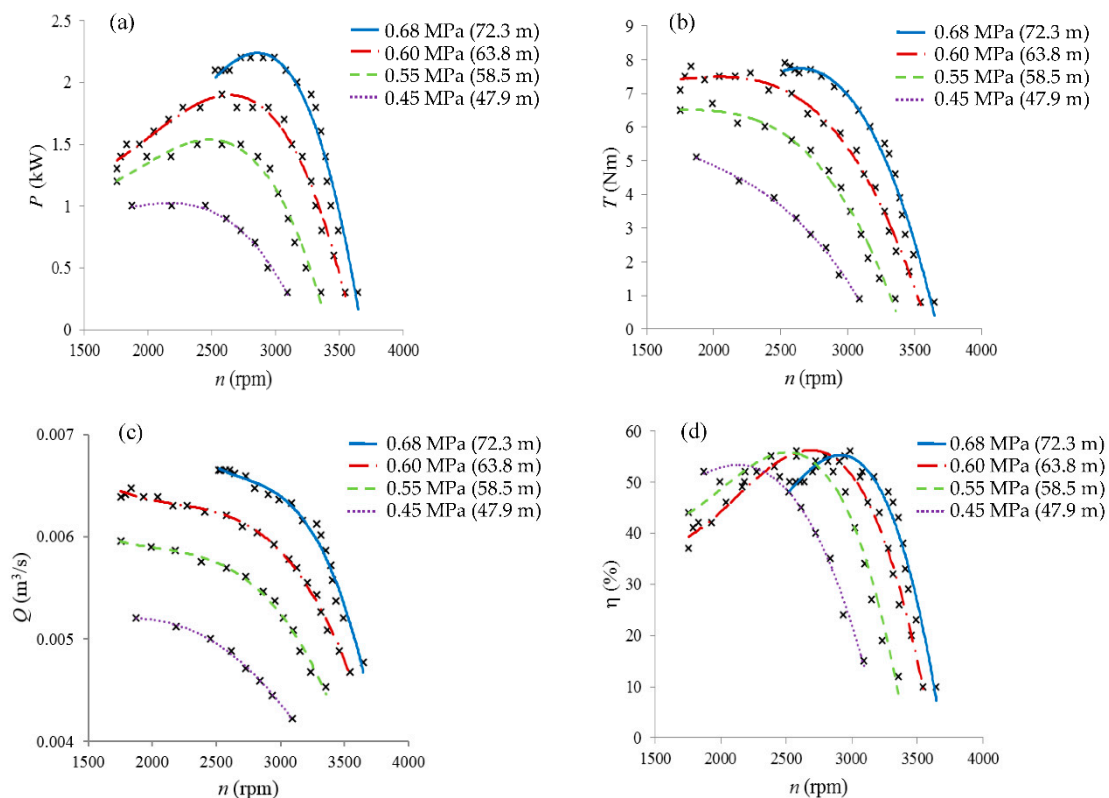


Figure 9. Characteristic ERPR curves of: (a) PEU active power; (b) calculated turbine torque; (c) flow rate; and (d) total efficiency in turbine speed domain under four reduced pressure values.

To estimate the ERPR's operation range under different working conditions of the substation, Figure 11 is presented. It shows the speed-regulation characteristics of the ERPR in the reduced pressure–flow-rate domain with isolines of constant efficiency. The presented measurement results enabled an estimation of the operation range and capability of the ERPR prototype. The useful operation area lies between 80% and 140% of the nominal reduced pressure and between 85% and 120% of the nominal flow rate. Considering the maximal power-control mode, the turbine speed should be adjusted according to the differential excess disposal pressure (equals the reduced pressure)

variation (optimal curve marked with black bold line). This operation leads to a total ERPR efficiency of more than 50%.

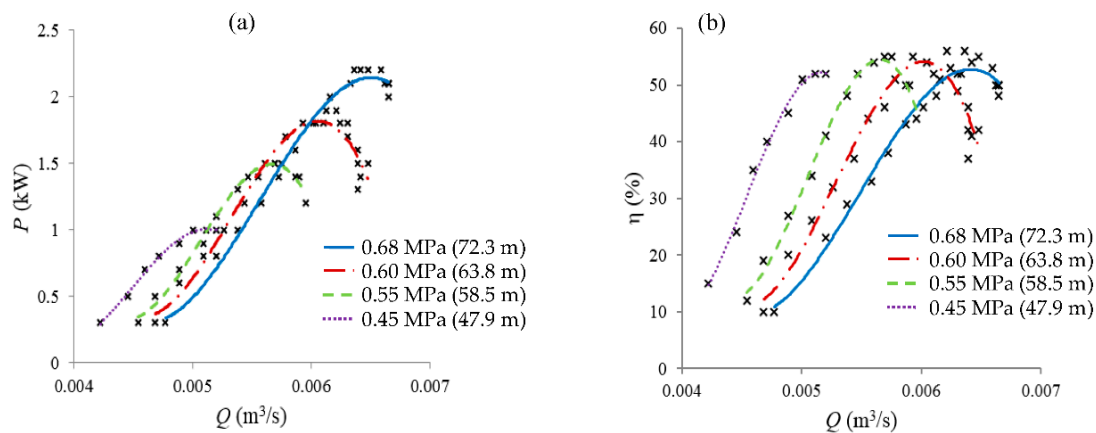


Figure 10. Characteristic ERPR curves of: (a) PEU active power; and (b) total efficiency in flow-rate domain under four reduced pressure values.

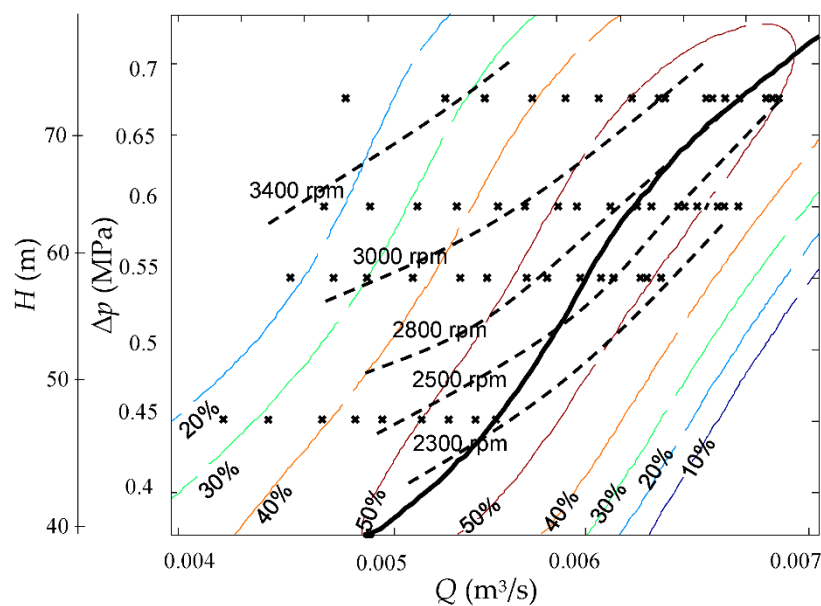


Figure 11. Speed regulation characteristics of ERPR in reduced pressure–flow-rate domain with isolines of constant efficiency.

4. Operation Features

4.1. ERPR Impact Analysis

The ERPR device was installed between a hydraulic system and an electrical power system. Thus, the negative influence of the ERPR on these systems needed to be analyzed. Additionally, the influence on the environment (sound measurements) needed to be estimated.

The prototype PEU contained two optional rectifiers, as described in Section 2.3. These two most popular structures differed in price, control complexity, and signal quality of the generator. The bad quality of electrical signals may have induced additional noise and vibrations of the ERPR during operation. This issue was investigated in this section by analyzing the quality of the generator's electrical signals, sound, and ERPR vibrations.

The curves of the generator's and PEU's electrical signals (voltage and current) over time are presented below. Figure 12 presents the results of the PEU with a diode bridge rectifier (Figure 4a), whereas Figure 13 presents those of the system with a sinusoidal rectifier (Figure 4b). The presented measurements were performed under similar electrical generator conditions (1 kW power and 2100 rpm). In order to evaluate the higher harmonics, an FFT (Fast Fourier Transform) analysis was performed. As expected, the generator current for the case of the sinusoidal rectifier contained fewer higher harmonics in the range below 1 kHz. Furthermore, the harmonics' amplitudes were about 10 dB lower (with a reference level of 10^{-3} A) compared to those of the diode bridge rectifier's system. The additional drawbacks of the diode rectifier were the voltage spikes during the commutation process and the angle shift between the generator voltage and current that results in reactive power. The latter increased the generator current. Therefore, the active power needed to be limited. To estimate the impact of the PEU on the electrical power system, the total harmonic distortion parameter (THD) of the PEU output voltage needed to be analyzed. For both system types, the voltage quality ($\text{THD}_U \approx 1.5\%$) fulfils the standard requirements [36].

To estimate the influence of the generator current distortion on the vibrations of the ERPR and hydraulic pipes, the measurements of the vibration velocity in three directions were analyzed. Three measurement points located at the ERPR unit, feed, and return pipes, which are presented in Figure 14a, were selected. Three operating points (2200, 2500, and 2800 rpm) with the best efficiency were analyzed. The dominant vibrations occurred in the x- and z-directions for the generator and return pipe. To evaluate the vibration severity, the classification introduced by the ISO 10816-1 standard was used [37]. The ERPR belonged to Class I (up to 15 kW), for which the satisfactory condition is defined in the vibration-velocity range below 2.8 mm/s RMS (root mean square). Values that exceed 7.1 mm/s RMS are defined as unacceptable, and are a danger for the machine. All measurements satisfied the conditions, and the difference in vibration results of the diode bridge rectifier and sinusoidal rectifier was small. However, the substantial increase of the vibration values of the return pipe were visible. This shows that the ERPR vibrations were transmitted with a high magnitude through the feed pipe and heat exchanger to the return pipe.

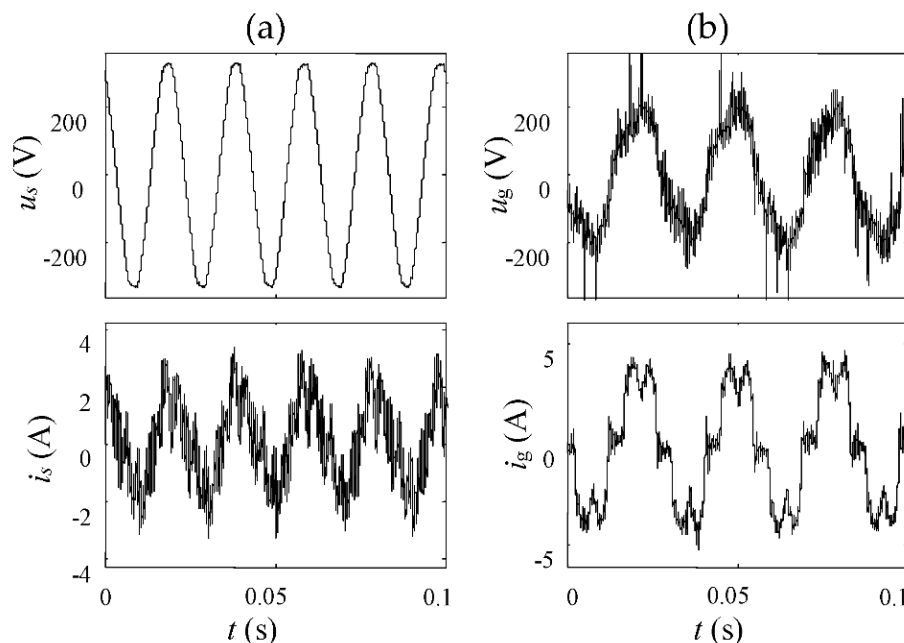


Figure 12. Electrical signal (voltage and current) analysis of the PEU with diode bridge rectifier: (a) PEU output signal; and (b) PMSG signal.

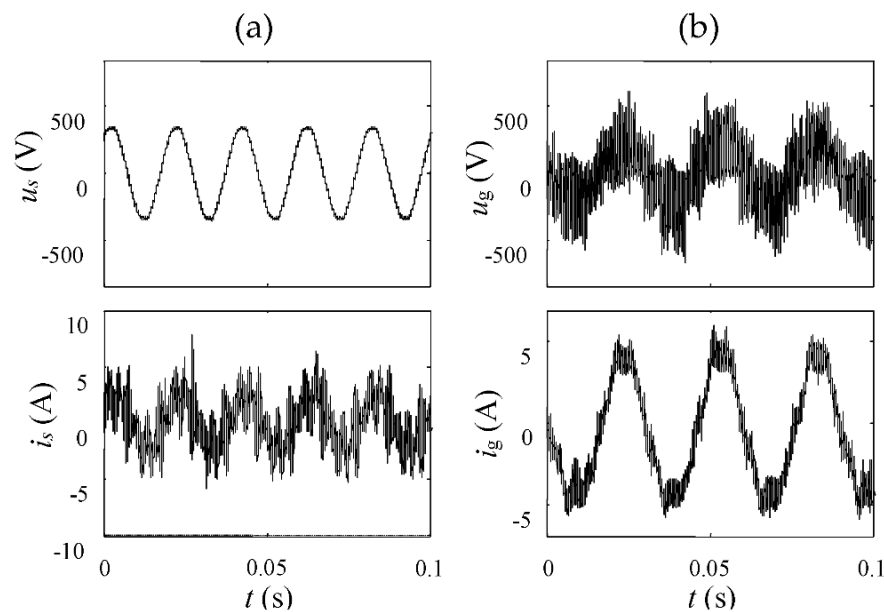


Figure 13. Electrical signal (voltage and current) analysis of the PEU with sinusoidal rectifier: (a) PEU output signal; and (b) PMSG signal.

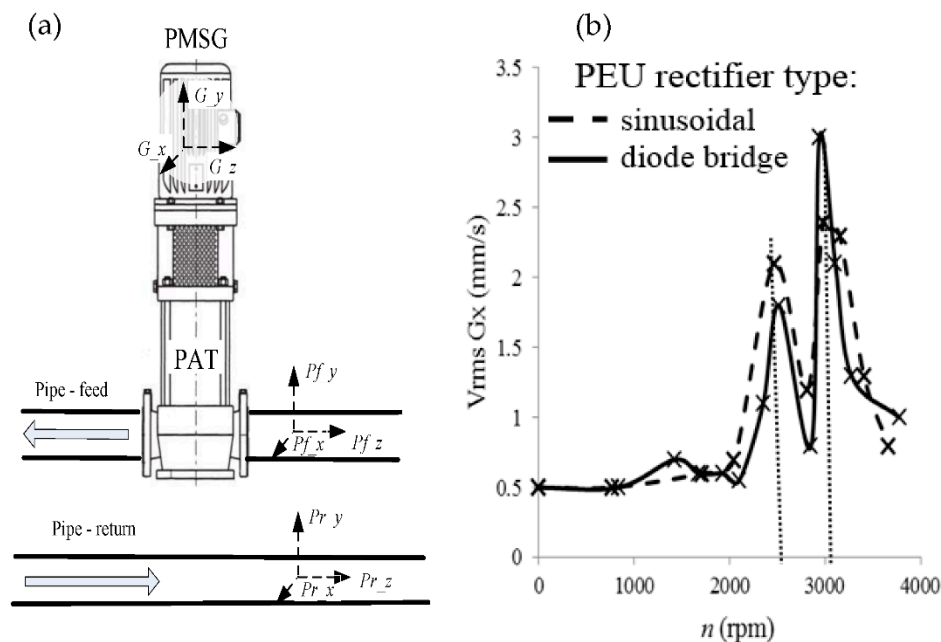


Figure 14. Vibration analysis: (a) location of measurement points; and (b) RMS-vibration velocity in speed domain for two types of PEU rectifier.

The ERPR worked at variable speed depending on the substation operating conditions. Therefore, the vibration values in the speed domain needed to be analyzed. Figure 14b presents the vibration velocity of the generator in the x-direction as a function of speed. The two resonant speeds (2500 rpm and 3000 rpm) were visible, and both were within the ERPR regulation area (Figure 11). Thus, they are especially dangerous. The vibration values for the sinusoidal rectifier were about 15% lower than those of the diode bridge rectifier in the second resonance area. Moreover, the resonance vibration for the diode bridge rectifier exceeded the satisfactory level. These phenomena must be considered while designing the mounting technique of the ERPR.

In the presented ERPR prototype, two main noise sources existed. Apart from the ERPR and pipes vibrations, the PEU generated sound resulting from the semiconductor-switching elements that caused higher harmonics in the electrical signals. The measurements performed at a 1 m distance from the device, in accordance with the measurement standard in [38], showed similar noise values for both PEU structures. The noise level increased with load from 65 dB (background noise) to 68 dB under 1.1 kW, and further to 72 dB for the nominal ERPR power. These values fulfil European standards regarding device noise limits [39] and international safety standards for workers exposed to noise [40].

The main common noise source in the DHS is the cavitation phenomenon in the PRV. It occurs when pressure decreases immediately below the vapor pressure directly behind the PRV. One of the methods that minimizes the cavitation risk is reducing the differential pressure over the PRV [41]. The proposed ERPR decreased this pressure to the minimal disposal value in the region before the PRV. Thus, it prevented cavitation. An implementation of the ERPR enabled an exact sizing of the PRV, improving control conditions, and prolonging the service life of the control equipment.

4.2. Operation Analysis during Annual Heating Season

The presented ERPR prototype, which was located in the substation in the Cracow DHS, was tested during five months of the annual heating season (from December to April). Figure 15 shows the curves of the main system parameters (grey line) with a one-day average filter curve (thick line) over time.

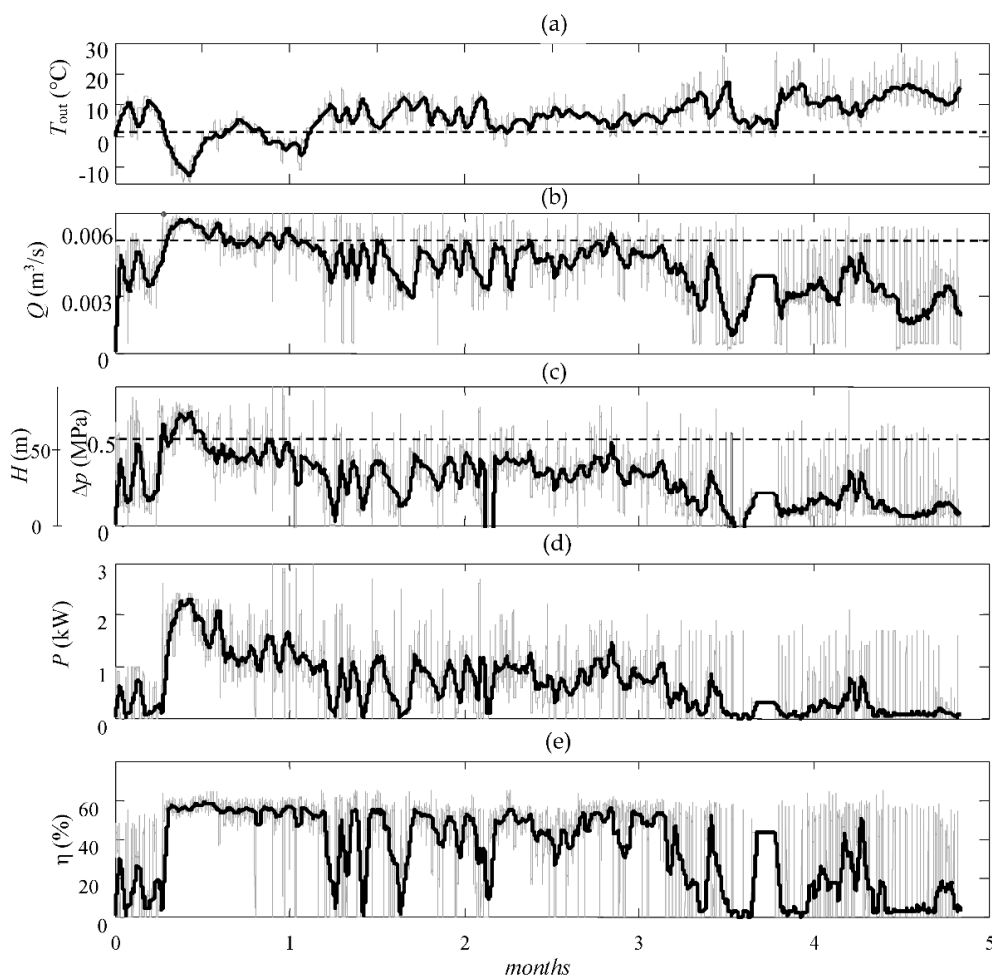


Figure 15. Curves of: (a) outside temperature; (b) flow rate; (c) reduced pressure; (d) electrical active power; and (e) total ERPR efficiency during the 5 months of heating season (from December to April) in the Cracow DHS substation.

The operation of the DHS substation was mainly dependent on outdoor temperatures. The nominal values of the ERPR ($\Delta p = 0.5$ MPa, $Q = 0.0058$ m³/s) were achieved when the outdoor temperature measured approximately 2 °C (dashed line). This is the usual average temperature for this location in the chosen period. The analyzed heating season was characterized by a quite high average temperature of 6.6 °C, which lead to only 2.42 MW of recovered energy. The average flow ($Q_{\text{avg}} = 0.0045$ m³/s) and average reduced pressure ($\Delta p_{\text{avg}} = 0.25$ MPa) were much below the nominal values. Most of the time the operating conditions were outside the ERPR regulation area (Figure 11). Nevertheless, the average ERPR efficiency (49%) was satisfactory.

5. Conclusions

In this paper, we proposed an ERPR device for a DHS. The chosen system structure, which consisted of an ERPR in series with a PRV, lowered installation costs and simplified system installation. To separate the ERPR control from the substation regulation system, an ERPR operation mode was proposed that provided the highest electrical active power, and kept the differential pressure equal to the minimal disposal value of the substation.

The presented analysis of the ERPR operation showed the low impact on electrical and hydraulic systems, as well as on the environment. The resulting vibration and noise values were similar for both PEU structures. Therefore, the cheaper solution with a diode bridge rectifier can be used. The vibration analysis in the speed domain revealed the resonance phenomenon, which must be considered while designing the mounting technique for the ERPR.

The presented example for energy recovery in a DHS in the city of Cracow indicated significant potential. Energy-recovery profitability depends on the equipment price and system efficiency. The economic analysis presented in Reference [21], resulting in a payback period of 5 to 7 years, assumes costs of approximately 1200 Euro for a standardized ERPR device (1 kW), and 1700 Euro if an extra design process is necessary. The total costs of the presented prototype were 1900 Euro/kW. Considering large ERPR numbers and equipment optimization, these cost levels are achievable. Furthermore, the presented analysis of the ERPR prototype in the substation of the Cracow DHS showed that the average total efficiency in the heating season is 49% despite the unusual operation conditions resulting from unusually high outdoor temperatures. The efficiency value confirmed the assumption made in Reference [21] (average efficiency value of 50%).

In conclusion, the installation of the ERPR in the Cracow DHS was economically feasible. To apply these results to other DHSs, factors such as the specific network structure, local market, and legal nature conditions should be considered.

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Conflicts of Interest: The authors declare no conflict of interest.

Abbreviations

DHS	district heating system
DPC-SVM	direct power control with space vector modulation
ER	electrical regulation
ERPR	energy-recovery pressure-reducer
FFT	fast Fourier transform
MHP	micro-hydropower plant
PAT	pump as turbine
PEU	power electronic unit
PMSG	permanent magnet synchronous generator
PRV	pressure reducing valve

PWM	pulse width modulation
RMS	root mean square
THD	total harmonic distortion
WSS	water supply system

Appendix A

Table A1. Rated Values and Nominal Parameters.

Three-Stage Vertical PAT in Turbine Mode:
Max power: $P_{t_max} = 3$ kW
Max torque: $T_{t_max} = 12$ Nm
Reduced pressure range: $\Delta p = 0.20$ – 0.75 MPa
Water head: $H = 21$ – 80 m
Water flow range: $Q = 0.004$ – 0.007 m ³ /s
Specific turbine speed: $n_s = 11$ rpm kW ^{1/2} m ^{−4/3}
Rotor material: brass
PMSG:
Apparent power: $S_g = 5.5$ kVA
Voltage: $U_g = 360$ V
Speed: $n_g = 3000$ rpm
Current: $I_g = 8.8$ A
Efficiency: $\eta_g = 93\%$
Frequency: $f_g = 50$ Hz
PEU:
Active power: $P_p = 5.5$ kW
Input voltage range: $U_{p_in} = 40$ – 460 VAC
Max input current: $I_{p_in} = 12$ A
Input frequency range: $I_{p_in} = 5$ – 100 Hz
Max DC voltage: $U_{p_dc} = 710$ V
Switching frequency: $f_s = 5$ kHz

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