

Techno-economic evaluation of iron and aluminum coagulants on Se(IV) removal

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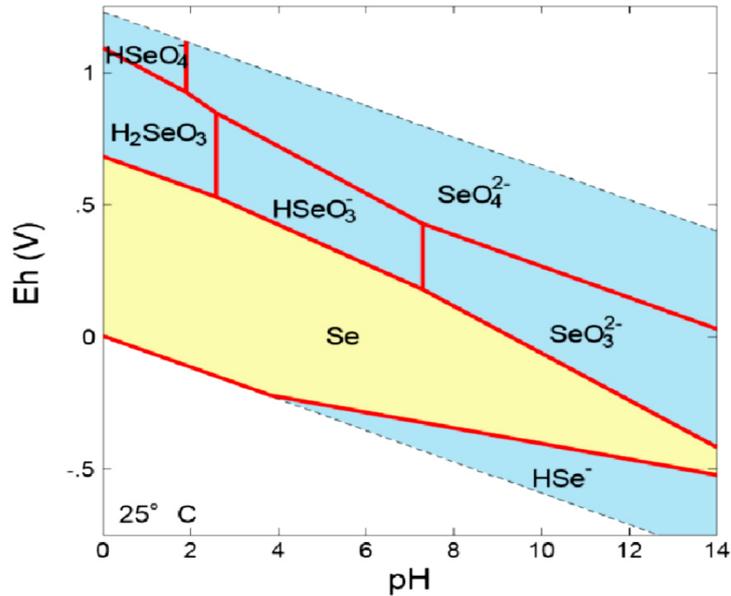


Figure S1. Selenium speciation as a function of Eh vs pH (Tabelin et al., 2018).

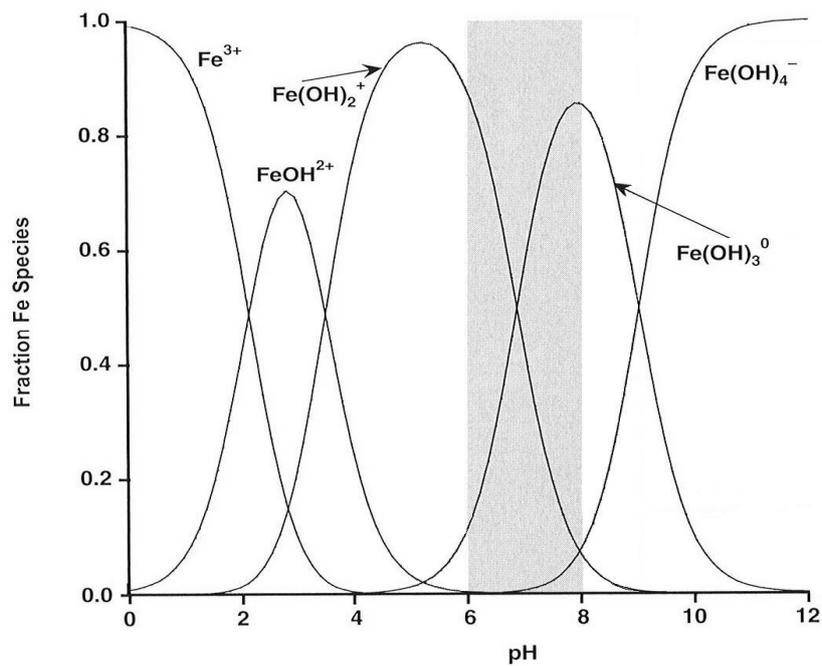


Figure S2. Fe(III) speciation as a function of pH.

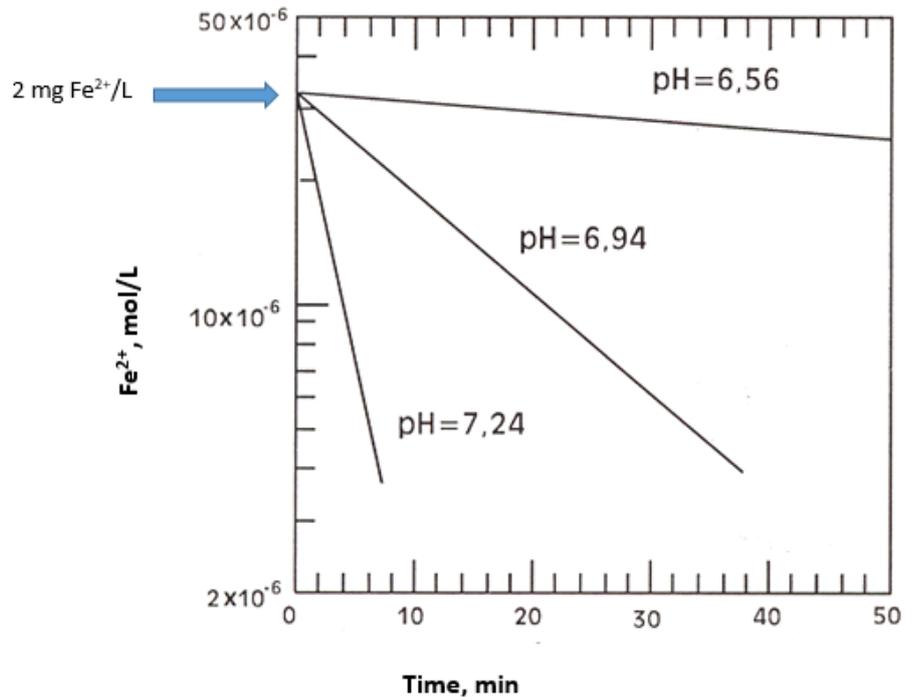


Figure S3. Oxidation rate of Fe(II) by oxygen as function of water pH (Stumm W. and Lee G.F., 1961)

Text S1

The energy cost estimated as follows:

Water pumping from raw water buffer tank, coagulation (residence time: 5 min – mixing: 250±50 W/m³), flocculation (residence time: 30 min – mixing: 30±10 W/m³), backwash, sludge handling, reagents pumping, lights and collection of water in treated water tank.

It is obvious that the treatment energy and labor cost does not incorporate the cost of water pumping from initial source to raw water buffer tank, nor the cost of pumping the treated water to municipality distribution network, because this cost is not related to the treatment process.

➤ Estimation of energy cost e.g. for water flow 100 m³/h.

1. Raw water pumping energy
 $P_q = Q \rho g \Delta h / n = [(100 \text{ m}^3/\text{h})/3600 \text{ s} \times 1000 \text{ kg/m}^3 \times 9.81 \text{ m/s}^2 \times 10 \text{ mwc}] / 0.65 = 4,200 \text{ W} \approx 101 \text{ kWh/d}$
2. Coagulation – $V = 10^3 - 250 \text{ W/m}^3$
 $P_c = 10 \text{ m}^3 \times 250 \text{ W/m}^3 = 2,500 \text{ W} = 60 \text{ kWh/d}$
3. Flocculation – $50 \text{ m}^3 - 30 \text{ W/m}^3$
 $P_F = 50 \text{ m}^3 \times 30 \text{ W/m}^3 = 1,500 \text{ W} = 36 \text{ kWh/d}$
4. Dosing reagents pumps $\approx 4 \text{ kWh/d}$
5. Backwash: $Q_b = 300 \text{ m}^3/\text{h}$ for 12 min daily.
 $P_b = Q \rho g \Delta h / n = [(300 \text{ m}^3/\text{h})/3600 \text{ s} \times 1000 \text{ kg/m}^3 \times 9.81 \text{ m/s}^2 \times 10 \text{ mwc}] / 0.65 = 12,600 \text{ W} \approx 3 \text{ kWh/d}$
6. Sludge handling: Sludge pumping to thickener (0.5 kW for 12 h), scraper of thickener (0.5 kW for 24 h), filter press for sludge dewatering 3 kW for 4 h $\approx 30 \text{ kWh/d}$
7. Lights: $0.250 \text{ kW} \times 12 \text{ h} = 3 \text{ kWh/d}$

Conclusively, the spent electric energy for $(100 \text{ m}^3/\text{h}) \times 24 \text{ h/d} = 2,400 \text{ m}^3/\text{d}$ estimated to be:

$$101 + 60 + 36 + 4 + 3 + 30 + 3 = 237 \text{ kWh/d}$$

Which means $\sim 100 \text{ kWh}/10^3 \text{ m}^3$

Since the commercial electric energy cost in Greece is 0.1 €/kWh , it is concluded that the energy cost is around $10 \text{ €/}10^3 \text{ m}^3$, independently of water flow in the range of $25 - 250 \text{ m}^3/\text{h}$.

➤ *Estimation of labor cost e.g. for water flow in the range of $25 - 250 \text{ m}^3/\text{h}$.*

Commonly in Greece 1 worker is used for a water flow $\leq 50 \text{ m}^3/\text{h}$ and approximately 2 workers for a water flow $50 - 100 \text{ m}^3/\text{h}$ and 3 workers for a water flow $100 - 250 \text{ m}^3/\text{h}$ with a monthly cost around $1,500\text{€}$.

- ✓ Labor cost for $25 \text{ m}^3/\text{h} \approx (1,500\text{€/month}) / (25 \text{ m}^3/\text{h} \times 24 \text{ h/d} \times 30 \text{ d/month}) = 83 \times 10^{-3} \text{ €/m}^3 = 83 \text{ €/}10^3 \text{ m}^3$
- ✓ Similarly, the labor cost for $50 - 100 - 250 \text{ m}^3/\text{h}$ estimated $42 - 42 - 25 \text{ €/}10^3 \text{ m}^3$

According to the above-mentioned analysis of labor and energy cost is estimated as $60 \pm 30 \text{ €/}10^3 \text{ m}^3$ treated water. Furthermore, the total cost of treatment incorporates also the maintenance cost, which is estimated by the depreciation cost of the mechanical equipment at 5 years operation, which according to our experience is estimated around $20 \pm 5 \text{ €/}10^3 \text{ m}^3$ treated water.