

Supplementary Materials

Table S1. Stoichiometry and kinetic equations of the anaerobic digestion for bioCH₄ production [1,2].

Conversion steps	Stoichiometry	Kinetic equations
Enzymatic hydrolysis		
Carbohydrate hydrolysis	(C ₆ H ₁₀ O ₅) _{is} → Y _c (C ₆ H ₁₀ O ₅) _s + (1 - Y _c) (C ₆ H ₁₀ O ₅) _{in}	R _S = k S
Protein hydrolysis	(Protein) _{is} → Y _p (Amino acids) + (1 - Y _p) (Protein) _{in}	R _S = k S
Bacterial steps		
Acidogenic glucose degrading	(C ₆ H ₁₀ O ₅) ₃ + 0.1115 NH ₃ → 0.1115 C ₅ H ₇ NO ₂ + 0.744 C ₂ H ₄ O ₂ + 0.5 C ₃ H ₆ O ₂ + 0.4409 C ₄ H ₈ O ₂ + 0.6909 CO ₂ + 0.0254 H ₂ O	$\mu = \mu_{max}(T) \left(\frac{1}{1 + \frac{K_s}{[(C_6H_{10}O_5)_s]}} \right)$
Lipolytic	C ₅₇ H ₁₀₄ O ₆ + 1.90695 H ₂ O + 0.04071 NH ₃ + 0.0291 CO ₂ → 0.04071 C ₅ H ₇ NO ₂ + 0.941843 C ₃ H ₆ O ₂ + 3 C ₁₈ H ₃₄ O ₂	$\mu = \mu_{max}(T) \left(\frac{1}{1 + \frac{K_s}{[GTO]}} \right)$
Long chain fatty acids (LCFA)-degrading	C ₁₈ H ₃₄ O ₂ + 7.7401 H ₂ O + 4.0834 CO ₂ + 0.2537 NH ₃ → 0.2537 C ₅ H ₇ NO ₂ + 8.6998 C ₂ H ₄ O ₂ + 3.4139 CH ₄ CH _{2.03} O _{0.6} N _{0.3} S _{0.001} + 0.3006 H ₂ O → 0.017013 C ₅ H ₇ NO ₂ + 0.29742 C ₂ H ₄ O ₂ + 0.02904 C ₃ H ₆ O ₂ + 0.022826 C ₄ H ₈ O ₂ + 0.013202 C ₅ H ₁₀ O ₂ + 0.07527 CO ₂ + 0.28298 NH ₃ + 0.001 H ₂ S	$\mu = \mu_{max}(T) \left(\frac{1}{1 + \frac{K_{s,LCFA}}{[LCFA]} + \frac{[LCFA]}{K_{i,LCFA}}} \right)$
Amino acid-degrading		$\mu = \mu_{max}(T)$
Propionate-degrading	C ₃ H ₆ O ₂ + 0.06198 NH ₃ + 0.314 H ₂ O → 0.06198 C ₅ H ₇ NO ₂ + 0.9345 C ₂ H ₄ O ₂ + 0.6604 CH ₄ + 0.1607 CO ₂	$\mu = \mu_{max}(T) \left(\frac{1}{1 + \frac{K_s}{[C_3H_6O_2]}} \right) \left(\frac{1}{1 + \frac{[C_2H_4O_2]}{K_{i,C2H4O2}}} \right)$

Butyrate-degrading	$C_4H_8O_2 + 0.0653 NH_3 + 0.5543 CO_2 + 0.8038 H_2O \rightarrow 0.0653 C_5H_7NO_2 + 1.8909 C_2H_4O_2 + 0.4452 CH_4$	$\mu = \mu_{max}(T) \left(\frac{1}{1 + \frac{K_s}{[C_4H_8O_2]}} \right) \left(\frac{1}{1 + \frac{[C_2H_4O_2]}{K_{i,C2H4O2}}} \right)$
Valerate-degrading	$C_5H_{10}O_2 + 0.0653 NH_3 + 0.5543 CO_2 + 0.8045 H_2O \rightarrow 0.0653 C_5H_7NO_2 + 0.8912 C_2H_4O_2 + 0.02904 C_3H_6O_2 + 0.4454 CH_4$	$\mu = \mu_{max}(T) \left(\frac{1}{1 + \frac{K_s}{[C_5H_{10}O_2]}} \right) \left(\frac{1}{1 + \frac{[C_2H_4O_2]}{K_{i,C2H4O2}}} \right)$
Acetoclastic methanogenic	$C_2H_4O_2 + 0.022 NH_3 \rightarrow 0.022 C_5H_7NO_2 + 0.945 CH_4 + 0.945 CO_2 + 0.066 H_2O$	$\mu = \mu_{max}(T) \left(\frac{1}{1 + \frac{K_s}{[C_2H_4O_2]}} \right) \left(\frac{1}{1 + \frac{[NH_3]}{K_{i,NH3}}} \right)$

Table S2. Details of life cycle inventory database for FW-based GM production in China [3].

Scenario	Base case	Wind	Photovoltaic	Hydro
FW	FW collection in lower-middle income country			
Heat	Heat, district or industrial, natural gas {GLO} market group for APOS, U			
		Electricity, high voltage {CN-BJ} electricity production, wind, >3MW turbine, onshore APOS, U	Electricity, low voltage {CN-BJ} electricity production, photovoltaic, 570kWp open ground installation, multi-Si APOS, U	Electricity, high voltage {CN-BJ} electricity production, hydro, run-of-river APOS, U
Electricity	Electricity, high voltage {CN} market group for APOS, U			

References

1. Angelidaki, I.; Ellegaard, L.; Ahring, B.K. A mathematical model for dynamic simulation of anaerobic digestion of complex substrates: focusing on ammonia inhibition. *Biotechnology and bioengineering* **1993**, *42*, 159-166.
2. Angelidaki, I.; Ellegaard, L.; Ahring, B.K. A comprehensive model of anaerobic bioconversion of complex substrates to biogas. *Biotechnology and bioengineering* **1999**, *63*, 363-372.
3. Wernet, G.; Bauer, C.; Steubing, B.; Reinhard, J.; Moreno-Ruiz, E.; Weidema, B. The ecoinvent database version 3 (part I): overview and methodology. *The International Journal of Life Cycle Assessment* **2016**, *21*, 1218-1230.