



# **Review Recent Progress in Electrolyte Additives for Highly Reversible Zinc Anodes in Aqueous Zinc Batteries**

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**Abstract:** Aqueous zinc batteries (AZBs) are one of the most promising large-scale energy storage devices by virtue of their high specific capacity, high degree of safety, non-toxicity, and significant economic benefits. However, Zn anodes in aqueous electrolyte suffer from zinc dendrites and side reactions, which lead to a low coulombic efficiency and short life cycle of the cell. Since electrolytes play a key role in the Zn plating/stripping process, versatile strategies have been developed for designing an electrolyte to handle these issues. Among these strategies, electrolyte additives are considered to be promising for practical application because of the advantages of low cost and simplicity. Moreover, the resulting electrolyte can maximally preserve the merits of the aqueous electrolyte. The availability and effectiveness of additives have been demonstrated by tens of research works. Up to now, it has been essential and timely to systematically overview the progress of electrolyte additives in mild acidic/neutral electrolytes. These additives are classified as metal ion additives, surfactant additives, SEI film-forming additives, and complexing additives, according to their functions and mechanisms. For each category of additives, their functional mechanisms, as well as the latest developments, are comprehensively elaborated. Finally, some perspectives into the future development of additives for advanced AZBs are presented.

Keywords: zinc batteries; electrolyte additives; zinc metal anode; zinc dendrites; side reactions

## 1. Introduction

The growing concerns about the environment and sustainability in world energy markets have promoted the development and utilization of renewable energy sources [1]. In order to cope with the intermittent features of renewable energy, efficient energy storage systems (ESSs) are greatly desired. Lithium-ion batteries (LIBs) are deemed as one of most important ESSs by virtue of their high energy and power densities. Nevertheless, safety issues and high costs limit their more widespread applications [2–5].

Recently, aqueous rechargeable multivalent metal-ion batteries have been considered as promising alternatives to conventional LIBs due to their high degree of safety, desirable performance, and low cost [6–8]. In particular, Zn anodes deliver the merits of a high theoretical capacity (820 mAh g<sup>-1</sup>), low redox potential (-0.763 V vs. SHE), non-toxicity, and abundant reserves (0.02 wt% of the enclosure content). Therefore, aqueous zinc batteries (AZBs) demonstrate promising potential in large-scale energy storage systems and have received significant attention [9,10]. However, their practical applications have been hindered by some problems residing in Zn anodes, such as side reactions and zinc dendrites. These deteriorate the AZB's performance and, thus, are desired to be resolved [11–13].

Intensive research has focused on developing and optimizing Zn metal anodes in terms of their compositions, architectures, etc. [14,15]. Indeed, these strategies can alleviate the aforementioned issues to some extent. On the other hand, further investigation in



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**Copyright:** © 2023 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). aqueous electrolyte is urgently needed, since electrolytes plays a central role in the Zn plating/stripping process and provide channels for ion transportation [16,17]. To this end, versatile manipulating strategies have been reported for designing electrolytes for highly reversible and dendrite-free Zn anodes, including a zinc salt design, the water-in-salt strategy, co-solvent strategies, hydrogel electrolytes, and additives [18]. Among these strategies, adjusting electrolyte composition by adding a small quantity of additives is regarded as promising because of the advantages of low cost and simplicity. Moreover, the resulting electrolyte can maximally preserve the merits of the aqueous electrolyte. The availability and effectiveness of additives in solving the Zn anode problems have been demonstrated by a number of reported studies.

To date, several excellent reviews have given a good overview of the development of electrolytes from the perspectives of co-solvent strategies, hydrogel electrolytes, etc. [19–21], but systematic reviews focusing on electrolyte additives are scarce. Since mild acidic/neutral electrolytes are considered to be promising due to their relatively high stability with zinc metal and their use by most of the recently reported works, we are, thus, motivated to summarize the state-of-the-art development in electrolyte additives for highly reversible and dendrite-free Zn anodes in mildly acidic/neutral electrolytes. Herein, challenges with Zn anodes are briefly introduced at first, including zinc dendrites and side reactions. After that, recent developments in electrolyte additives are summarized and thoroughly elaborated. According to their functions and mechanisms, additives are classified into four categories: metal ion additives, surfactant additives, solid electrolyte interphase (SEI) film-forming additives for advanced AZBs are presented.

#### 2. Challenges with Zn Anode

With the advantages of high security, low price, abundant reserves, and environmental friendliness, zinc metal, thereby, extensively serves as the anode in AZBs. However, as known to us, Zn anodes in aqueous electrolyte suffer from issues including zinc dendrites and side reactions, which are detrimental to the performance of AZBs [22]. The formation of zinc dendrites is usually induced by the uneven distribution of the electric field and the uncontrolled 2D diffusion of  $Zn^{2+}$  on the anode surface [23]. Specifically, the initiation of dendrites is usually formed at the preferential nucleation sites of the Zn anode surface. Next, zinc ions are inclined to deposit on the sites exhibiting minimal surface energy, which are usually the bulges of initial dendrites, causing the so-called "tip effect" [24,25]. As a result, the electric field on the zinc anode surface is distributed unevenly, accelerating the dendritic growth [24]. The brittle zinc dendrites produced during charging tend to fracture and form dead zinc when discharging, seriously affecting the performance of AZBs. Terrifically, dendrites will penetrate the separators, which eventually induces short circuits in the AZBs.

In terms of the side-reaction issues of Zn anodes, hydrogen evolution (HER) is the most concerning one among corrosion, HERs, and passivation [26]. Hydrogen evolution side reactions will continuously reduce the coulombic efficiency of the cell [27]. Moreover, a portion of the produced  $H_2$  will adsorb on the Zn surface. Zn deposition is prevented on the site adsorbed by  $H_2$ , which further accelerates the uneven Zn deposition and dendritic growth [28]. In a word, dendrite formation and HER side reactions are the root causes of unsatisfactory electrochemical performance of a Zn anode [29].

#### 3. Electrolyte Additives

Although aqueous electrolytes possess superiority in safety, cost, and ionic conductivity, issues with zinc anodes in aqueous electrolytes, including dendritic growth and side reactions, as mentioned in Section 2, need to be resolved. In this regard, researchers have made continuous efforts and adopted various strategies, such as solvent regulation [30], water-confined separators [31], and hydrogel electrolytes [32]. Among these strategies, additives can not only address the above-mentioned problems well, but also save materials and avoid the complex fabrication procedures. Trace amounts of additives in aqueous electrolyte can greatly improve the electrochemical performance of the zinc anode [33].

Various additives have been adopted to improve the properties of aqueous zinc batteries. According to their functions and mechanisms, we classify the additives into four categories, as follows:

- Metal ion additives: metal ions can be reduced before zinc to provide additional deposition sites, or they cannot be reduced during zinc deposition and form an electrostatic shielding layer to suppress the tip effect.
- (2) Surfactant additives: the molecules/ions that adsorb on the electrode surface, thereby, modulate the anode/electrolyte interfacial environment and homogenize the Zn<sup>2+</sup> flux.
- (3) SEI film-forming additives: the additives will be consumed by reactions to form a protective interfacial layer on the anode surface, which can prevent the hydrogen evolution reaction and dendrite formation by suppressing the 2D diffusion of Zn<sup>2+</sup> on the substrate surface.
- (4) Complexing additives: the interaction between these additives and zinc ions is stronger than that between zinc ions and water, and they can enter the solvation sheath of Zn<sup>2+</sup>, weaken the activity of water molecules, and change the zinc deposition kinetics.

In this section, we will review the recent developments and detailed mechanisms for each category of these additives.

#### 3.1. Metal Ion Additives

Metal ion additives with different reduction potentials inhibit the formation of zinc dendrites through different mechanisms. To be specific, metal ions with high reduction potentials ( $Bi^{3+}$ ,  $Pd^{2+}$ ,  $Co^{2+}$ ,  $Ni^{2+}$ ) will be reduced before  $Zn^{2+}$  and form uniformly distributed metal sites in situ that can be used as heterogeneous nucleation sites. Therefore, metal ion additives effectively inhibit the undesirable 2D diffusion of  $Zn^{2+}$  and dendritic growth [34-37]. Chang et al. adopted 1.67 mmol  $L^{-1}$  of  $Pd^{2+}$  and  $Ni^{2+}$  as additives to investigate their inhibitory effects on Zn dendrites. From the scanning electron microscopy (SEM) images (Figure 1a,c), it can be seen that the morphology of the zinc deposition after adding  $Pd^{2+}$  displayed smaller spherical depositions compared to that without any additives. However, tiny Zn dendrites were still observed when adding  $Ni^{2+}$  and  $Cu^{2+}$  to the electrolyte (Figure 1b,d). Although the preferential deposition of Zn dendrites,  $Zn^{2+}$  tended to form zinc alloys with  $Pd^{2+}$  rather than with  $Ni^{2+}$ ; thus,  $Pd^{2+}$  led to a more homogeneous zinc deposition [37].

Similarly, Ma et al. found that the addition of 0.2 mol  $L^{-1}$  CoSO<sub>4</sub> to aqueous electrolyte can also exhibit an inhibitory effect on Zn dendrites. Furthermore and interestingly, the electrochemical window of the electrolyte was widened to 2.2 V. As a result, the Zn/Co<sub>3</sub>O<sub>4</sub> battery delivered great durability, which maintained 92% capacity retention even after 5000 cycles [36].

On the other hand, metal ions with lower reduction potentials (Na<sup>+</sup>, Mg<sup>2+</sup>, Mn<sup>2+</sup>, Ce<sup>3+</sup>) can homogenize the flux of Zn<sup>2+</sup> through a cationic electrostatic shielding mechanism, thereby inhibiting the tip effect [37–40]. Xu et al. demonstrated the successful use of a Zn/NaMnO<sub>2</sub> battery by adding 0.25 mol L<sup>-1</sup> Na<sub>2</sub>SO<sub>4</sub> to the ZnSO<sub>4</sub> electrolyte. They observed that the added Na<sup>+</sup> ions would form an electrostatic shield around the tips of Zn. This would drive Zn<sup>2+</sup> ions to deposit in non-tip regions, preventing the formation of Zn dendrites. As expected, a homogeneous Zn deposition morphology was observed in the modified electrolyte, and the Zn/Zn symmetric cells exhibited a low overpotential (48.8 mV) and excellent cycling stability (300 h) [41].



**Figure 1.** SEM images of Zn deposits obtained at -1.5 V vs. Zn/Zn<sup>2+</sup> for 400 s with different additives of (**a**) none, (**b**) Ni<sup>2+</sup>, (**c**) Pb<sup>2+</sup>, and (**d**) Cu<sup>2+</sup> [37]; SEM images of Zn deposition in (**e**) 2 M ZnSO<sub>4</sub> and (**h**) ZnMg-0.1 electrolytes after 20 cycles at the fully charged state. Optical images of Zn deposition in (**f**) 2 M ZnSO<sub>4</sub> and (**g**) ZnMg-0.1 electrolytes, and (**i**) zoom in view of (**f**) [38].

Moreover, the addition of metal ions can also mitigate the occurrence of side reactions. Taking the  $Mg^{2+}$  additive as an example, 0.1 M MgSO<sub>4</sub> was introduced into the ZnSO<sub>4</sub> electrolyte. It was found that  $Mg^{2+}$  showed strong interactions with water molecules. Such strong interactions were demonstrated to decrease the water activity and, thus, mitigate the hydrogen evolution. At the same time, flatter zinc deposition morphology was also obtained (Figure 1e–i). Additionally,  $Mg^{2+}$  and  $Zn^{2+}$  share the solvated H<sub>2</sub>O form  $(Zn^{2+}Mg^{2+}(H_2O)_6)$ , which reduces water molecule activity. Furthermore, the  $Mg^{2+}$  ions can form an electrostatic shield layer around the Zn surface due to electrostatic attraction. This layer isolates water from the zinc metal to prevent HERs, thereby reducing side reactions. Meanwhile, this layer can also drive  $Zn^{2+}$  ions to deposit in non-tip regions because of electrostatic repulsion, leading to a flatter deposition layer (Figure 2). As a result, the assembled Zn/Zn symmetric batteries with a MgSO<sub>4</sub> addition showed smaller overpotential (85.9 mV) and achieved a great durability that maintained 98.7% capacity retention after 10,000 cycles [38].



**Figure 2.** The scheme illustration of the Zn deposition process in the electrolyte without (**top row**) and with 0.1 M MgSO<sub>4</sub> additive (**bottom row**) [38].

## 3.2. Surfactant Additives

Unlike metal ion additives, surfactant additives can spontaneously distribute at the interface between the electrode and electrolyte due to reduced surface tension, preventing direct contact between active water and the zinc anode, thereby inhibiting the hydrogen evolution side reactions. Furthermore, the re-establishment of the interfacial environment changes the  $Zn^{2+}$  deposition kinetics and inhibits the growth of zinc dendrites. Considering these merits, the surfactant additives will be elaborated on in this section. There are four types, according to the dissociation properties of their polar groups: cationic surfactants, anionic surfactants, amphoteric surfactants, and non-ionic surfactants.

Cationic surfactants, especially ammonium surfactants such as tetrabutylammonium sulphate (TBA<sub>2</sub>SO<sub>4</sub>) and triethylmethylammonium chloride (TMA), have been used as additives in electrolytes to flatten the surface energy distribution [42-48]. For example, Zhu et al. added 29 mg  $L^{-1}$  cationic surfactant TBA<sub>2</sub>SO<sub>4</sub> to the electrolyte and found that TBA<sup>+</sup> with hydrophobic chains was adsorbed on the zinc surface to avoid hydrogen evolution. At the same time, the formed protective layer prevented the transport of solvated  $Zn^{2+}$ , which slowed down the Zn plating and ensured uniform deposition (Figure 3a,b) [42]. However, this inhibition effect of Zn deposition needs to be carefully controlled, so as to prevent HERs and achieve an acceptable rate capability. For this purpose, Guan et al. investigated three quaternary ammonium surfactants, benzyl dimethyl dodecyl ammonium chloride (DDBAC), dodecyl trimethyl ammonium chloride (DTAC), and benzyl trimethyl ammonium chloride (TMBAC), and analyzed the effects of their different hydrophobic groups on the modulation of Zn deposition behavior [43]. Experimental and theoretically calculated results revealed that the hydrophobic groups on surfactants were the decisive factor in affecting the kinetic process of zinc-ion deposition (Figure 4a). Among them, TMBAC obtained the brighter zinc deposition than did DTAC or DDBAC (Figure 3c–f) because the more hydrophobic groups on and higher surface activity of DTAC and DDBAC increased the polarization overpotential and destabilized the adsorption layer. Therefore, the Zn/Zn symmetric cells with addition of  $0.5 \text{ g L}^{-1}$  TMBA<sup>+</sup> exhibited the best performance, which achieved the compact deposition morphology without producing byproducts, and were able to cycle stably for more than 500 h at 10 mA cm<sup>-2</sup> and 5 mAh cm<sup>-2</sup>.

Additionally, anionic surfactants such as sodium dodecyl benzene sulfonate (SDBS) and sodium 3,3'-dithiodipropane sulfonate (SPS) have been reported and proved to be effective in solving Zn dendritic growth and anode corrosion issues [49–51]. Wang et al. used 10 mmol L<sup>-1</sup> SPS as an electrolyte additive in 1M Zn(OTf)<sub>2</sub>, and first-principles calculations revealed that SPS<sup>-</sup> tended to adsorb on other crystalline planes ((100) and (101)) rather than on the (002). As expected, deposition of Zn in the direction of (002) was effectively controlled (Figure 4b). Thus, dendritic growth and HERs were significantly inhibited at the same time. Benefitting from SPS<sup>-</sup>, the Zn/Zn symmetric cell cycled stably for more than 4000 h at 1 mA cm<sup>-2</sup> and 1 mAh cm<sup>-2</sup> [49].

In addition, natural amphoteric surfactants such as arginine (Arg) and cysteine (Cys) have also been extensively studied [52–55]. For example, Lu et al. added 0.1 mol L<sup>-1</sup> of the hydrophilic amino acids, including Arg, serine (Ser), and glutamic acid (Glu), to aqueous electrolyte to investigate the factors that influence the stability of the adsorption layer. DFT calculations revealed that Arg<sup>+</sup> delivered the highest adsorption energy and a better stability of the adsorption layer. Because the adsorbed Arg layer can isolate water and guide Zn<sup>2+</sup> flux during the plating process, the electrolyte with Arg<sup>+</sup> showed a better ability to inhibit HERs and dendritic growth. Consequently, the assembled cell exhibited ultra-long stable cycling, even up to 2200 h at 5 mA cm<sup>-2</sup> and 4 mAh cm<sup>-2</sup> [52].



**Figure 3.** In situ optical microscopy observations of the Zn deposition process at 10 mA cm<sup>-2</sup> in (a) blank and (b) 0.05 mM TBA<sub>2</sub>SO<sub>4</sub> additive electrolytes [42]. In situ optical microscopy observations of Zn deposition at 5 mA cm<sup>-2</sup> in electrolytes with different additives: (c) Blank, (d) 0.5 g L<sup>-1</sup> DDBAC, (e) 0.5 g L<sup>-1</sup> DTAC, and (f) 0.5 g L<sup>-1</sup> TMBAC [43].



**Figure 4.** The scheme illustration of the Zn deposition process in 2M ZnSO<sub>4</sub> electrolyte (**a**) with or without TMBAC [43] and (**b**) with or without SPS additive [49].

Furthermore, non-ionic surfactants can also be adsorbed on the Zn surface to regulate the Zn deposition process, such as polyethylene oxide (PEO), poly(4-styrenesulfonic acid sodium) (PSS), and poly(acrylamide-co-methylacrylate) copolymer (APA) [56–60]. It is worth noting that the hydrophilicity and hydrophobicity of the surfactants are of great significance in rebuilding the interfacial environment. Different from other kinds of surfactants, the hydrophilicity of polymer surfactants can be facially adjusted in many ways so as to optimize the AZB performance. For instance, a hydrophilicity-tunable nonionic copolymer additive, 1 wt.% APA, was introduced to traditional Zn(OTf)<sub>2</sub> electrolyte. The Zn/Zn symmetric cells achieved a superior cycle life (Figure 5a–c) and a high CE with an average of 99.3% (Figure 5e). Surprisingly, the operating temperature of the Zn/Zn cell was significantly widened, ranging from 50 °C down to -30 °C (Figure 5d), because the hydrophilicity-tunable APA tuned the coordination environment of Zn<sup>2+</sup> and, thus, lowered the freezing point of the electrolyte (Figure 5f,g) [56]. Finally, Table 1 summarizes the surfactant additives and corresponding Zn anode cycling performance.



**Figure 5.** Cycling performance of Zn/Zn cells cycled at (**a**) 5 mA cm<sup>-2</sup>, (**b**) 10 mA cm<sup>-2</sup>, and (**c**) at varied current densities; (**d**) cycling performance of Zn/Zn cells cycled under varied temperatures at 1 mA cm<sup>-2</sup>; (**e**) coulombic efficiency of Zn/Cu cells at 1 mA cm<sup>-2</sup> and 1 mAh cm<sup>-2</sup>; (**f**) <sup>1</sup>H NMR spectra in D<sub>2</sub>O and (**g**) infrared spectra in H<sub>2</sub>O for pristine- and APA-containing electrolytes [56].

Туре	Additive	Cycling Stability	Refs.
	$29 \text{ mg L}^{-1} \text{ TBA}_2 \text{SO}_4$	$300 \text{ h} (2.0 \text{ mA cm}^{-2}, 2.0 \text{ mA h cm}^{-2})$	[42]
Cationia	$1 \text{ mol } L^{-1} \text{ TMA}$	$\begin{tabular}{ c c c c } \hline Cycling Stability \\ \hline 300 h (2.0 mA cm^{-2}, 2.0 mA h cm^{-2}) \\ 2000 h (1.0 mA cm^{-2}, 2.0 mA h cm^{-2}) \\ 3000 h (1.0 mA cm^{-2}, 2.0 mA h cm^{-2}) \\ 4500 h (0.25 mA cm^{-2}, 0.25 mA h cm^{-2}) \\ 500 h (10 mA cm^{-2}, 5.0 mA h cm^{-2}) \\ 500 h (10 mA cm^{-2}, 5.0 mA h cm^{-2}) \\ 1500 h (0.5 mA cm^{-2}, 0.5 mA h cm^{-2}) \\ 4000 h (1.0 mA cm^{-2}, 1.0 mA h cm^{-2}) \\ 2200 h (5.0 mA cm^{-2}, 4.0 mA h cm^{-2}) \\ 2300 h (5.0 mA cm^{-2}, 5.0 mA h cm^{-2}) \\ 580 h (1.0 mA cm^{-2}, 1.0 mA h cm^{-2}) \\ 3000 h (1.0 mA cm^{-2}, 1.0 mA h cm^{-2}) \\ 3000 h (1.0 mA cm^{-2}, 1.0 mA h cm^{-2}) \\ 1300 h (2.0 mA cm^{-2}, 2.0 mA h cm^{-2}) \\ 2500 h (5.0 mA cm^{-2}, 5.0 mA m^{-2}) \\ 2500 h (5.0 mA cm^{-$	[45]
Cationic	$10 \text{ mmol } \text{L}^{-1} \text{ TEAB}$	$3000 \text{ h} (1.0 \text{ mA cm}^{-2}, 2.0 \text{ mA h cm}^{-2})$	[46]
surfactants	$1 \text{ mol } \mathrm{L}^{-1} \mathrm{TS}$	Cycling Stability $_2SO_4$ 300 h (2.0 mA cm <sup>-2</sup> , 2.0 mA h cm <sup>-2</sup> )IA2000 h (1.0 mA cm <sup>-2</sup> , 2.0 mA h cm <sup>-2</sup> )EAB3000 h (1.0 mA cm <sup>-2</sup> , 2.0 mA h cm <sup>-2</sup> )S4500 h (0.25 mA cm <sup>-2</sup> , 0.25 mA h cm <sup>-2</sup> )EAC500 h (10 mA cm <sup>-2</sup> , 5.0 mA h cm <sup>-2</sup> )EAS1500 h (0.5 mA cm <sup>-2</sup> , 0.5 mA h cm <sup>-2</sup> )EAS2200 h (5.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS2200 h (5.0 mA cm <sup>-2</sup> , 5.0 mA h cm <sup>-2</sup> )EAS3000 h (1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS2300 h (5.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS500 h (1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )EAS	[47]
	$0.5 \mathrm{~g~L^{-1}}$ TMBAC		[43]
Anionic surfactants	$0.1 \text{ mol } \mathrm{L}^{-1} \mathrm{SDBS}$	$1500 \text{ h} (0.5 \text{ mA cm}^{-2}, 0.5 \text{ mA h cm}^{-2})$	[50]
	$10 \text{ mmol } \text{L}^{-1} \text{ SPS}$	$4000 \text{ h} (1.0 \text{ mA cm}^{-2}, 1.0 \text{ mA h cm}^{-2})$	[49]
A much a tarri a	$0.1 \text{ mol } \mathrm{L}^{-1} \mathrm{Arg}$	$ \begin{array}{cccc} L^{-1} \mbox{ TS} & 4500 \mbox{ h} (0.25 \mbox{ mA cm}^{-2}, 0.25 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ TMBAC} & 500 \mbox{ h} (10 \mbox{ mA cm}^{-2}, 5.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ TMBAC} & 1500 \mbox{ h} (0.5 \mbox{ mA cm}^{-2}, 0.5 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ L}^{-1} \mbox{ SPS} & 4000 \mbox{ h} (1.0 \mbox{ mA cm}^{-2}, 1.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ L}^{-1} \mbox{ Arg} & 2200 \mbox{ h} (5.0 \mbox{ mA cm}^{-2}, 4.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ L}^{-1} \mbox{ Cys} & 2300 \mbox{ h} (5.0 \mbox{ mA cm}^{-2}, 5.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ L}^{-1} \mbox{ Cys} & 2300 \mbox{ h} (5.0 \mbox{ mA cm}^{-2}, 1.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ L}^{-1} \mbox{ TH} & 580 \mbox{ h} (1.0 \mbox{ mA cm}^{-2}, 1.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ WPEO} & 3000 \mbox{ h} (1.0 \mbox{ mA cm}^{-2}, 1.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ WPEO} & 3000 \mbox{ h} (1.0 \mbox{ mA cm}^{-2}, 1.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ WPEO} & 3000 \mbox{ h} (1.0 \mbox{ mA cm}^{-2}, 1.0 \mbox{ mA h cm}^{-2}) \\ \hline 1 \mbox{ MA cm}^{-2} \mbox{ mA h cm}^{-2} \mbox{ mA h cm}^{-2} \\ \hline 1 \mbox{ mA h cm}^{-2} \mbox{ mA h cm}^{-2} \mbox{ mA h cm}^{-2} \mbox{ mA h cm}^{-2} \\ \hline 1 \mbox{ mA h cm}^{-2} $	[52]
Amphoteric	$10 \text{ mmol } \text{L}^{-1} \text{ Cys}$	2300 h (5.0 mA cm <sup><math>-2</math></sup> , 5.0 mA h cm <sup><math>-2</math></sup> )	[53]
surfactants	$10 \text{ mmol } \text{L}^{-1} \text{ TH}$	$\begin{array}{c} 4500 \text{ h} (0.25 \text{ mA cm}^{-2}, 0.25 \text{ mA h cm}^{-2}) \\ 4500 \text{ h} (0.25 \text{ mA cm}^{-2}, 0.25 \text{ mA h cm}^{-2}) \\ 500 \text{ h} (10 \text{ mA cm}^{-2}, 5.0 \text{ mA h cm}^{-2}) \\ 5 & 1500 \text{ h} (0.5 \text{ mA cm}^{-2}, 0.5 \text{ mA h cm}^{-2}) \\ 5 & 4000 \text{ h} (1.0 \text{ mA cm}^{-2}, 1.0 \text{ mA h cm}^{-2}) \\ 5 & 2200 \text{ h} (5.0 \text{ mA cm}^{-2}, 4.0 \text{ mA h cm}^{-2}) \\ 5 & 2300 \text{ h} (5.0 \text{ mA cm}^{-2}, 5.0 \text{ mA h cm}^{-2}) \\ 5 & 3000 \text{ h} (1.0 \text{ mA cm}^{-2}, 1.0 \text{ mA h cm}^{-2}) \\ \hline 3 & 3000 \text{ h} (1.0 \text{ mA cm}^{-2}, 1.0 \text{ mA h cm}^{-2}) \\ \hline 3000 \text{ h} (1.0 \text{ mA cm}^{-2}, 1.0 \text{ mA h cm}^{-2}) \\ \hline 1 & 3000 \text{ h} (2.0 \text{ mA cm}^{-2}, 2.0 \text{ mA h cm}^{-2}) \\ \hline \end{array}$	[55]
Non-ionic surfactants	0.5 wt% PEO	$3000 \text{ h} (1.0 \text{ mA cm}^{-2}, 1.0 \text{ mA h cm}^{-2})$	[57]
	0.2 wt% PEO	$800 \text{ h} (1.0 \text{ mA cm}^{-2}, 1.0 \text{ mA h cm}^{-2})$	[59]
	1 wt% PAM	1300 h (2.0 mA cm $^{-2}$ , 2.0 mA h cm $^{-2}$ )	[60]
	$ \begin{array}{cccc} \text{on-ionic} & 0.2 \text{ wt\% PEO} & 800 \text{ h} (1.0 \text{ mA cm}^{-2}, 1.0 \text{ mA h cm}^{-1} \\ \text{factants} & 1 \text{ wt\% PAM} & 1300 \text{ h} (2.0 \text{ mA cm}^{-2}, 2.0 \text{ mA h cm}^{-1} \\ 1 \text{ wt\% APA} & 2500 \text{ h} (5.0 \text{ mA cm}^{-2}, 5.0 \text{ mA h cm}^{-1} \\ \end{array} $	$2500 \text{ h} (5.0 \text{ mA cm}^{-2}, 5.0 \text{ mA h cm}^{-2})$	[56]

Table 1. Summary of surfactant additives.

#### 3.3. SEI Film-Forming Additives

The adsorption layers at the electrode/electrolyte interface can be constructed by adding surfactants; in a like manner, a protective SEI film can be formed in situ on the anode surface by adding "SEI film-forming" additives. The SEI formed in situ can homogenize the Zn deposition and avoid HER occurrence by facilitating the 3D diffusion of  $Zn^{2+}$  and preventing the direct contact between the active water and the zinc, respectively. Zeng et al. revealed that  $Zn^{2+}$ -SEI composed of Zn phosphates could be generated by introducing 25 mmol  $L^{-1}$  Zn(H<sub>2</sub>PO<sub>4</sub>) <sub>2</sub> into the electrolyte. The Zn<sub>3</sub>(PO<sub>4</sub>) <sub>2</sub> 4H<sub>2</sub>O layer (~140 nm thick) formed in situ presented features of uniformity and denseness and was endowed with rapid transport kinetics, which inhibited electrolyte erosion and facilitated even Zn deposition. Therefore, the Zn/Zn cell presented stable cycling for over 1200 h at 1 mA cm<sup>-2</sup> and 1 mAh cm<sup>-2</sup> [61].

As known to us, fluorinated SEI has been extensively investigated in LIBs. Inspired by this, Wang et al. introduced 0.5 mol L<sup>-1</sup> of alkylammonium salt (Me<sub>3</sub>EtNOTF) to aqueous electrolyte. Through the depth profiles of XPS F1s spectra (Figure 6a–c), it can be seen that a fluorinated and hydrophobic interphase was formed in situ, as schematically illustrated in Figure 6d. The as-formed SEI was able to guard the Zn from water (but allow Zn<sup>2+</sup> to diffuse through) and promote lateral rather than vertical Zn<sup>2+</sup> migration and deposition, thereby preventing parasitic reactions and suppressing dendritic growth (Figure 7a–f). Therefore, the Zn/VOPO<sub>4</sub> coin cell presented stable cycling for over 6000 h at 2.0 A g<sup>-1</sup> in sharp contrast to that without additives (Figure 6e) [62]. Moreover, inspired by the bioadhesive of marine mussels, Zeng et al. formed a polydopamine SEI by an in situ reaction with 50 mmol L<sup>-1</sup> of dopamine (DA) additive. Consequently, the Zn/V<sub>2</sub>O<sub>5</sub> full battery gave ultra-long stable cycling up to 1000 cycles at a current density of 1 A g<sup>-1</sup>, with a limited electrolyte (9  $\mu$ L mAh<sup>-1</sup>) and a low anode/cathode capacity ratio (~2) [63].

Additionally, some 2D materials, such as graphene oxide (GO) and MXene, have been used as "SEI forming" additives in electrolytes in order to construct a self-assembled SEI [64–66]. Abdulla et al. added 0.16 wt% of GO to ZnSO<sub>4</sub> electrolyte. The GO added to the electrolyte formed an interface layer by closely adsorbing on the zinc surface. The GO layer could promote a homogeneous distribution of surface energy and provide more nucleation sites by virtue of its abundant polar functional groups (Figure 7g–l). As a result, the Zn/Zn symmetric cells were able to cycle stably for 200 h at 10 mA cm<sup>-2</sup>, 5 mAh cm<sup>-2</sup> [66].



**Figure 6.** XPS F1*s* spectra generated after Ar<sup>+</sup> sputtering for (**a**) 0 min, (**b**) 2 min, and (**c**) 10 min; (**d**) the scheme illustration of proposed SEI, consisting of small nodular particles embedded within a polymeric framework. (**e**) Cycling performance of the  $Zn/VOPO_4$  coin cell in both electrolytes at 2.0 A g<sup>-1</sup> [62].



Figure 7. Cont.



**Figure 7.** SEM images of the zinc anode at different scales: (**a**) 50 um, (**b**) 20 um, and (**c**) cross-section image without Me<sub>3</sub>EtNOTF additive after 50 cycles. SEM images of the zinc anode at different scales: (**d**) 50 um, (**e**) 20 um, and (**f**) cross-section image with 0.5 m Me<sub>3</sub>EtNOTF additive after 50 cycles [62]. SEM images after 200 plating/stripping cycles in the blank electrolyte at different scales: (**g**) 200 um, (**h**) 50 um, and (**i**) cross-section image; SEM images after 200 plating/stripping cycles in the electrolyte with GO electrolyte additive at different scales: (**j**) 200 um, (**k**) 50 um, and (**l**) cross-section image [66].

#### 3.4. Complexing Additives

The complexing additives added to aqueous electrolyte play a crucial role in reconstituting the solvated sheath layer of  $Zn^{2+}$ , which directly influences the zinc deposition kinetics and side reactions. Hitherto, according to the reports in the literature, halogen and amine molecules are the most commonly used complexing additives. Table 2 summarizes the complexing additives and corresponding Zn anode cycling performance.

Туре	Additive	Cycling Stability	Refs.
halogenated Zn salts	$1 \text{ mol } L^{-1} \text{ ZnI}_2$	$5000 \text{ h} (160 \text{ mA cm}^{-2}, 2.6 \text{ mA h cm}^{-2})$	[67]
ammonium	$\begin{array}{l} 1 \text{ mol } \mathrm{L}^{-1} \operatorname{NH_4OAc} \\ 4 \operatorname{mol} \mathrm{L}^{-1} \operatorname{NH_4} \mathrm{I} \end{array}$	3500 h (1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> ) 200 h (1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )	[68] [69]
Amine substituent	$\begin{array}{c} 0.1 \ \mathrm{mol} \ \mathrm{L}^{-1} \mathrm{BIS}\text{-}\mathrm{TRIS} \\ 75 \ \mathrm{mmol} \ \mathrm{L}^{-1} \ \mathrm{Na}_4 \mathrm{EDTA} \\ 0.5 \ \mathrm{mol} \ \mathrm{L}^{-1} \ \mathrm{TEHC} \\ 0.1 \ \mathrm{mol} \ \mathrm{L}^{-1} \ \mathrm{EDTA} \end{array}$	1000 h (1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> ) 2500 h (5.0 mA cm <sup>-2</sup> , 2.0 mA h cm <sup>-2</sup> ) 1100 h (1.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> ) 3000 h (5.0 mA cm <sup>-2</sup> , 1.0 mA h cm <sup>-2</sup> )	[70] [71] [72] [73]

Table 2. Summary of complexing additives.

By investigating a series of halogenated Zn salts, Jin et al. found that, unlike  $[Zn(H_2O)_6]^{2+}$ in the ZnSO<sub>4</sub> electrolyte, in the ZnCl<sub>2</sub> electrolyte,  $[ZnCl_2(H_2O)_6]$  was the dominant ionic state; in the ZnI<sub>2</sub> electrolyte,  $[ZnI]_4^{2-}$  was the dominant ionic state, and in the ZnBr<sub>2</sub> electrolyte, it was  $[ZnBr_2(H_2O)_6]$  and  $[ZnBr]_4^{2-}$  that coexisted in the ionic state. They further demonstrated that ionic complexes containing anions could reduce the water within the Zn<sup>2+</sup> solvation sheath to form solvation structures, such as  $[ZnBr]_4^{2-}$  and  $[ZnI]_4^{2-}$ , because the interaction force between ionic complexes containing anions and Zn<sup>2+</sup> was stronger than that between H<sub>2</sub>O and Zn<sup>2+</sup>. This prevents HERs, endowing halogenated Zn salt electrolytes with excellent electrochemical performance. Consequently, the Zn/carbon cloth asymmetric battery was capable of maintaining long-term cycling of over 5000 cycles at 160 mA cm<sup>-2</sup>, 2.6 mAh cm<sup>-2</sup> in 1 mol L<sup>-1</sup> ZnI<sub>2</sub> electrolyte [67].

As for amine molecules containing lone pairs of electrons, numerous studies have studied their potential as complexing additives [68]. For example, Han et al. added 1 mol  $L^{-1}$  of the ammonium acetate ( $NH_4OAc$ ) as a pH buffer to aqueous electrolyte to investigate the factors that influence the stability of the interface, as illustrated in Figure 8a. According to the density functional theory calculation, NH4<sup>+</sup> induced an electrostatic shielding effect at the interface (Figure 8b). At the same time,  $OAc^{-}$  as a pH buffer could effectively inhibit the occurrence of pH-sensitive side reactions. Therefore, it showed a better ability in inhibiting the dendritic growth and hydrogen evolution, leading to greatly improved cycling stability (Figure 8c). Consequently, the assembled Zn/Zn cell exhibited ultra-long stable cycling, even up to 3500 h at 1 mA cm<sup>-2</sup> and 1 mAh cm<sup>-2</sup> [68]. Furthermore, Chen et al. introduced 4 mol  $L^{-1}$  of NH<sub>4</sub>I into the Zn(OAc)<sub>2</sub> electrolyte and found that the NH<sub>4</sub><sup>+</sup> and I<sup>-</sup> could participate in the solvation structure and reduce the water activity, thus inhibiting the occurrence of side reactions. Additionally, NH4<sup>+</sup> was able to construct an electrostatic shield by adsorption to inhibit Zn dendrites. The assembled Zn/Cu half-battery achieved a cycle life of 200 h with a coulombic efficiency of 99.8% at 1 mA cm<sup>-2</sup> [69]. Furthermore, substituted amines or other complexing agents containing amines have also demonstrated their roles in modulating the solvation sheath, such as ethylene diamine tetra acetic acid tetrasodium salt (Na<sub>4</sub>EDTA) and triethylamine hydrochloride (TEHC) [70,71,74,75]. As demonstrated by Qian et al., the coordination effect of the amine ligand could be further enhanced by the induction effect of the substituent. As such, the ethyl substituent was chosen to modify the amine group, and the effects of  $0.5 \text{ mol } L^{-1}$  triethylamine hydrochloride, diethylamine hydrochloride, ethylamine hydrochloride, and ammonium chloride were investigated. As compared to NH<sub>4</sub>Cl, TEHC possessed a stable electron-donating ability, which enhanced its binding to  $Zn^{2+}$  and optimized the solvation shell of  $Zn^{2+}$ . Benefitting from TEHC, the Zn/Zn symmetric cell showed stable cycling for more than 1100 h at 1 mA cm<sup>-2</sup> and  $1 \text{ mAh cm}^{-2}$  [72].



**Figure 8.** (a) The scheme illustration of the Zn deposition and evolution process in blank electrolytes or with different additives; (b) binding energy for  $Zn^{2+}$  and  $NH^{4+}$  on Zn (101); (c) lifespan of Zn/Zn cells in the blank electrolytes and with the  $NH^{4+}$  additive [68].

Zhang et al. introduced 75 mmol  $L^{-1}$  of Na<sub>4</sub>EDTA as an additive into the ZnSO<sub>4</sub> electrolyte and found that the EDTA anion could be adsorbed on the Zn surface to suppress side reactions. Remarkably, the EDTA anion was allowed to enter the  $Zn^{2+}$  solvation shell thanks to the strong bonding between Zn<sup>2+</sup> and the EDTA anion. Thus, the desolvation process of hydrated  $Zn^{2+}$  could be accelerated to achieve uniform Zn deposition. Hence, the addition of Na4EDTA to the electrolyte enabled the assembled cell to deliver a high coulombic efficiency of 99.5% and ultra-long cycle life of 2500 h [71]. Furthermore, it is increasingly urgent to establish effective selection criteria by which complexing additives can be selected reasonably. Yang's group pioneered the use of the equilibrium constant of the complexation reaction (K) as a general criterion to accurately select a suitable complexing agent. By comparing the K values of Zn acetate, Zn oxalate, Zn glycinate, Zn nitrite triacetate, and Zn EDTA (Figure 9a), EDTA was found to exhibit the highest K value and chelated energies in the selected matrix (Figure 9b). Through a calculation of corrosion reaction pathways and energy intervals, it was proved that EDTA exhibited better inhibition of anode corrosion (Figure 9c-e). Meanwhile, it exhibited smoother galvanization, and ultimately, the Zn/Zn symmetric cells enabled long-term stable cycling for over 3000 h at  $5 \text{ mA cm}^{-2}$  and  $1 \text{ mAh cm}^{-2}$  [73].



**Figure 9.** (a) Molecular models of Ac, Ox, Gly, NTA, and EDTA; (b) the optimized molecular structures and corresponding chelation energies of Ac-Zn, Ox-Zn, Gly-Zn, NTA-Zn, and EDTA-Zn; (c) corrosion reaction pathways with different Zn–ligand complexes in various electrolytes; (d) relationship between log K value and the chelation energy and (e) energy intervals between the LUMO and HOMO of Ligand and Ligand-Zn [73].

### 4. Conclusions and Perspectives

Aqueous zinc batteries are deemed as one of the most promising large-scale energy storage systems due to their excellent sustainability and economics. Nevertheless, some issues, including zinc dendrites and side reactions, are the central obstacles restricting their large-scale applications. Among various strategies to cope with these issues, additives have received significant attention, owing to their facile and material-saving features. In this review, recent developments in electrolyte additives were comprehensively overviewed according to their functions and mechanisms, and the additives were classified into metal ion additives, surfactant additives, SEI film-forming additives, and complexing additives.

In summary, the four types of additives can largely suppress the formation of zinc dendrites due to distinct mechanisms. However, their abilities to inhibit HERs as well as corrosion are quite different. Metal ion additives are less satisfactory for the inhibition of the HER. Only the metal ions with reduction potentials lower than that of Zn<sup>2+</sup> can separate water molecules from Zn metal, to some extent, by forming an acceptably tight electrostatic shield layer. Surfactant additives can spontaneously form a tight protective layer via surface tension to block water molecules, but the low ionic conductivity of this protective layer significantly reduces the rate performance of the cell. Screen and optimization of the molecular structure of the surfactant is needed to achieve a high-rate capability. The SEI film-forming additives can form a dense and highly ionically conductive SEI, which effectively blocks water molecules to suppress HERs without sacrificing cell performance. However, the adhesion of the SEI film to zinc is troublesome, and it may easily peel off after repeated cycles. The complexing additive reduces the activity of water molecules through complexation with  $Zn^{2+}$  to inhibit the HER. However, compared to the former three additives with effective concentrations of mmol/L, complexing additives often work in the mol/L range, which increases the cost and diminishes the economic advantage of aqueous electrolytes.

In spite of these achievements, continuous efforts are needed to promote the development of additives from the following viewpoints:

- (1) Developing multifunctional additives that can solve both anode and cathode issues simultaneously is of great importance. For example, some metal ion additives can suppress the dissolution of metal ions from cathodes and, simultaneously, inhibit the dendritic growth of anodes. To this end, more advanced additives are urgently needed to modify both the anode and cathode at the same time, aiming at achieving a better overall performance of the battery.
- (2) Exploring the working principles of additives plays a key role in guiding the future development and design of electrolyte additives. It is essential to systematically investigate the influence of additive structure on the electrochemical performance, so as to establish the relationship of structure–mechanism performance on additives.
- (3) Studying the interactions between different additives in electrolyte is highly desired as well, which can help realize the synergistic effects that arise from various additives added to the electrolyte, achieving further improved cell performance.

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