

Supplementary

Carbon Dioxide Adsorption over Activated Carbons Produced from Molasses Using H₂SO₄, H₃PO₄, HCl, NaOH, and KOH as Activating Agents

Karolina Kielbasa ¹, Şahin Bayar ², Esin Apaydin Varol ², Joanna Sreńscek-Nazzal ¹, Monika Bosacka ³, Piotr Miądlicki ¹, Jarosław Serafin ^{4,*}, Rafał J. Wróbel ^{1,*} and Beata Michalkiewicz ¹

¹ Faculty of Chemical Technology and Engineering, Department of Catalytic and Sorbent Materials Engineering, West Pomeranian University of Technology in Szczecin, Piastów Ave. 42, 71-065 Szczecin, Poland

² Faculty of Engineering, Department of Chemical Engineering, Eskisehir Technical University, Eskisehir 26555, Turkey

³ Faculty of Chemical Technology and Engineering, Department of Inorganic and Analytical Chemistry, West Pomeranian University of Technology in Szczecin, Piastów Ave. 42, 71-065 Szczecin, Poland

⁴ Department of Inorganic and Organic Chemistry, University of Barcelona, Martí i Franquès, 1-11, 08028 Barcelona, Spain

* Correspondence: jaroslaw.serafin@qi.ub.es (J.S.); rafal.wrobel@zut.edu.pl (R.J.W.)

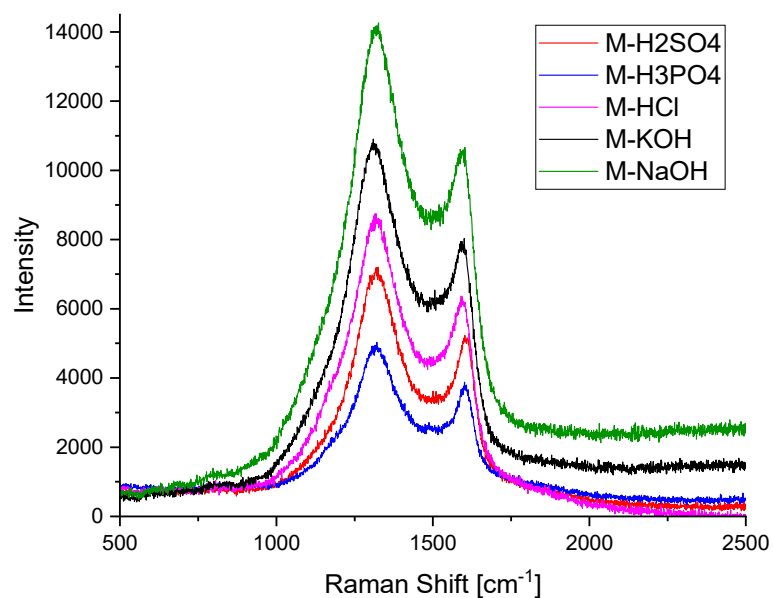


Figure S1. Raman spectra of the activated carbons produced from molasses

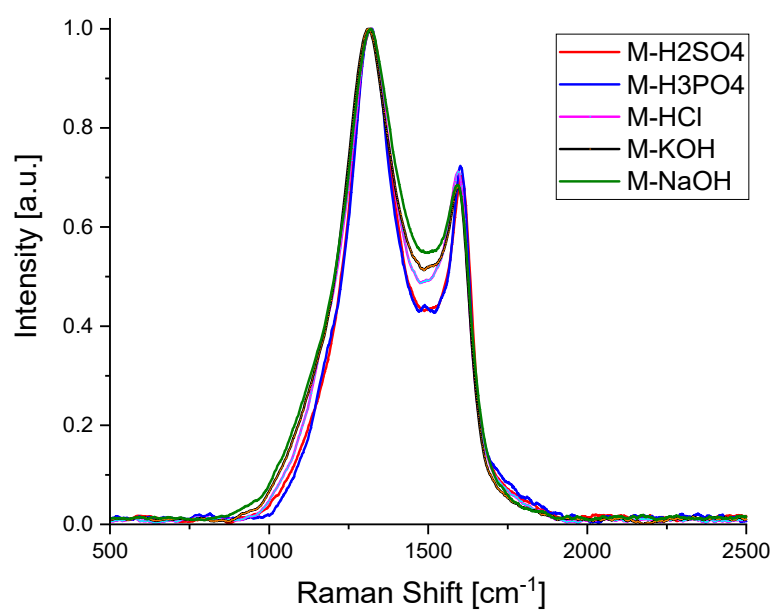
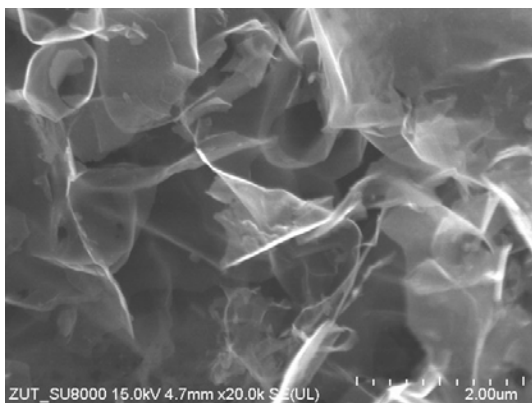
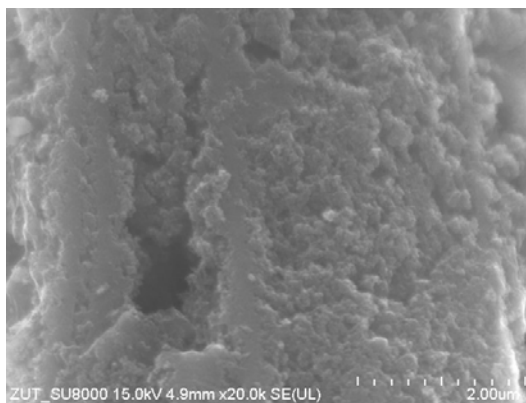


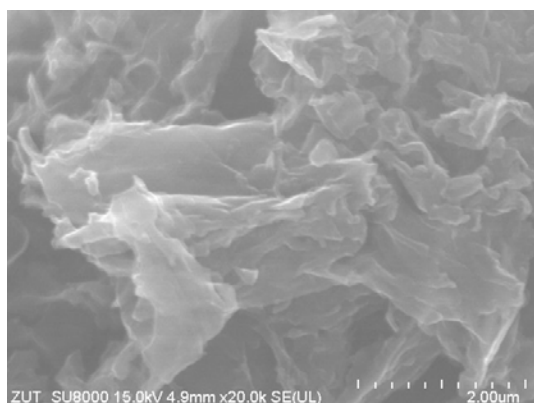
Figure S2. Raman spectra of the activated carbons produced from molasses after the smoothing, baseline subtracting and normalizing to the D band intensity



M-NaOH

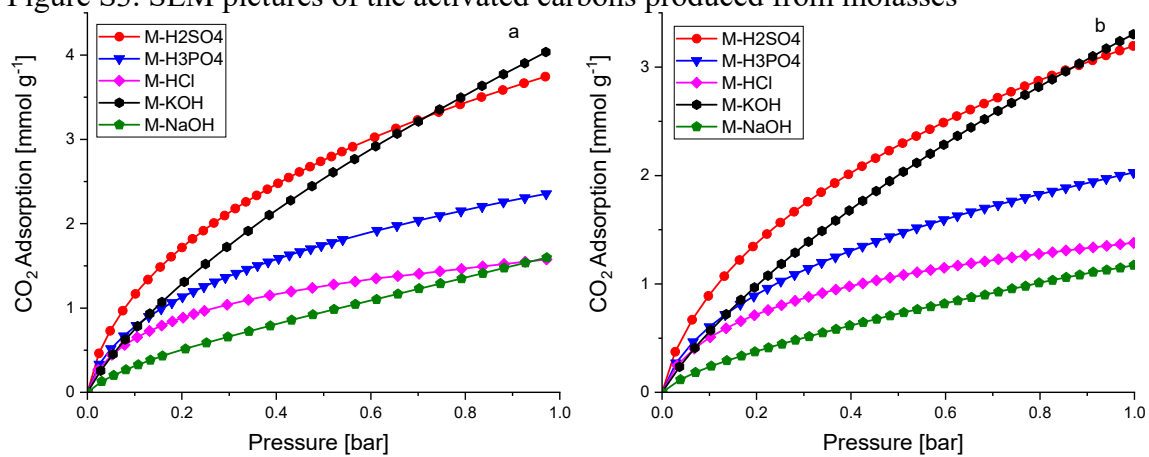


M-H3PO4



M-HCl

Figure S3. SEM pictures of the activated carbons produced from molasses



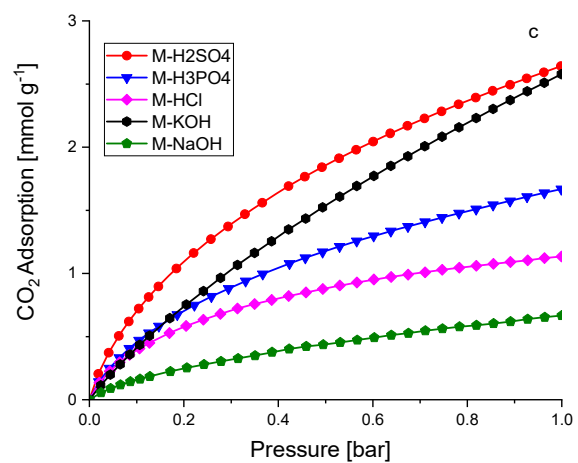
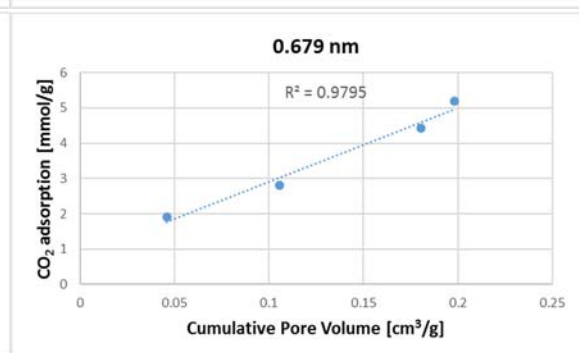
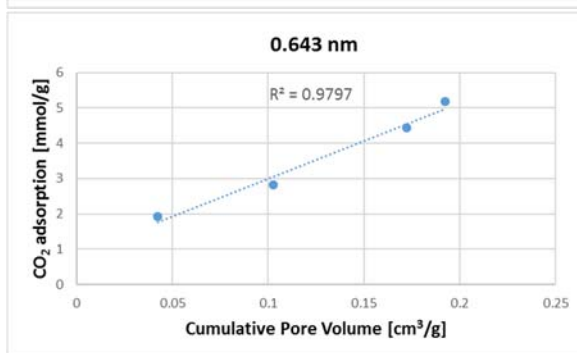
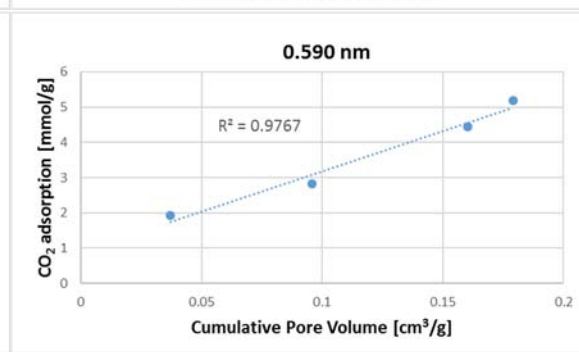
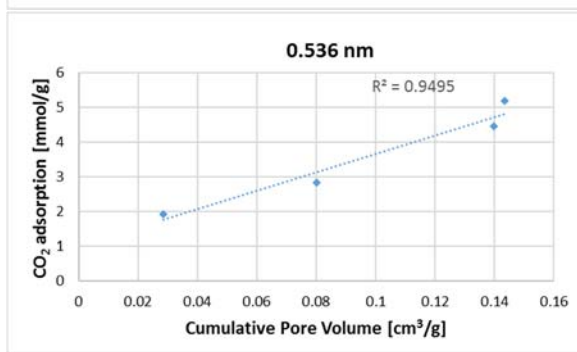
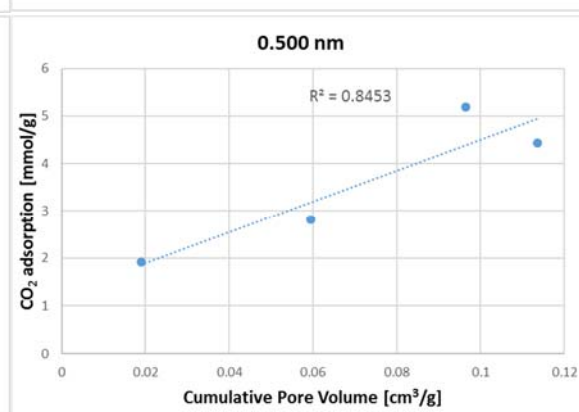
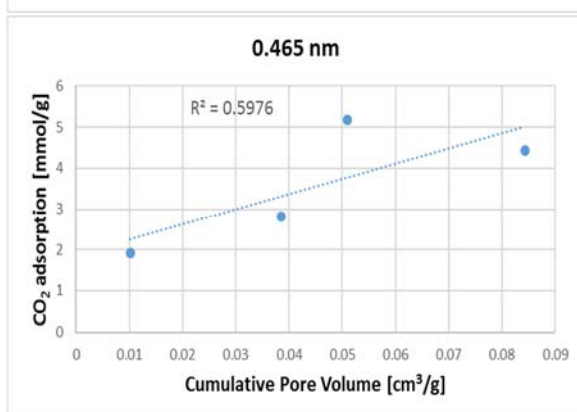
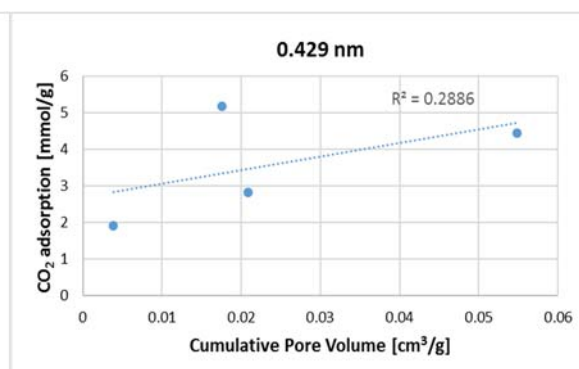
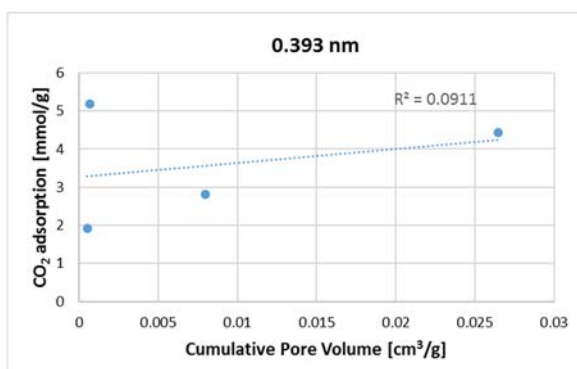
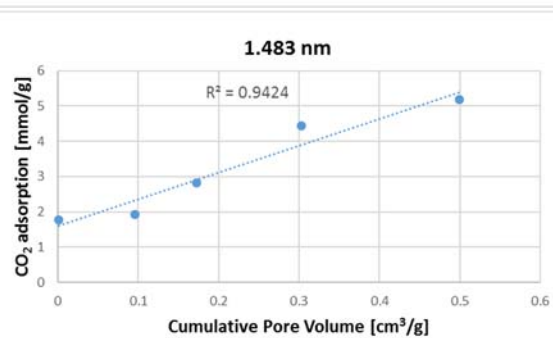
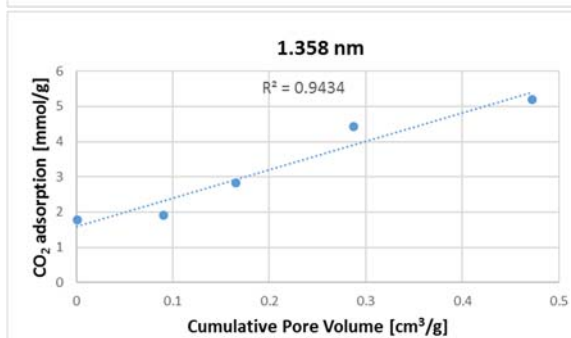
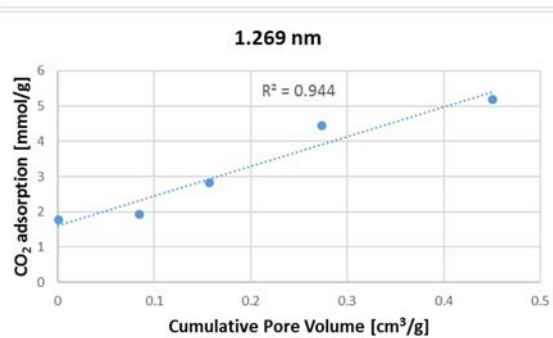
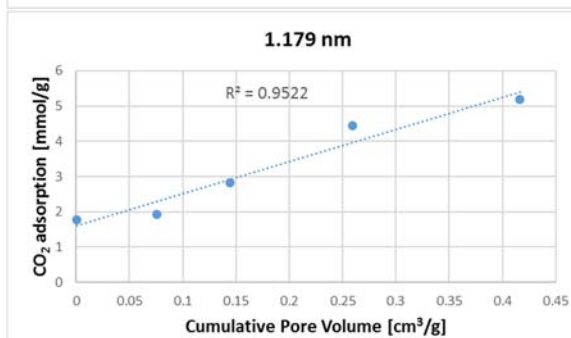
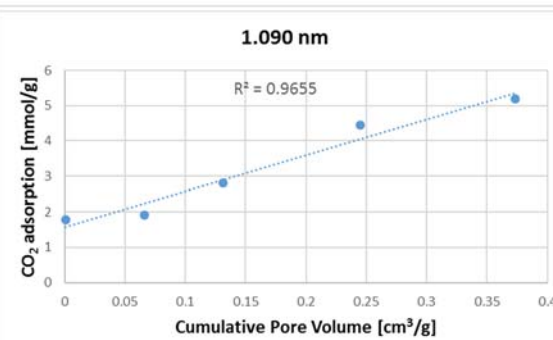
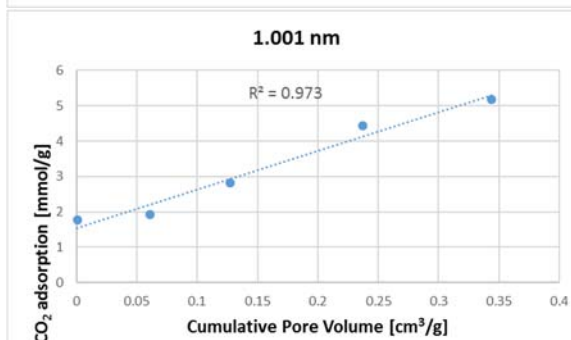
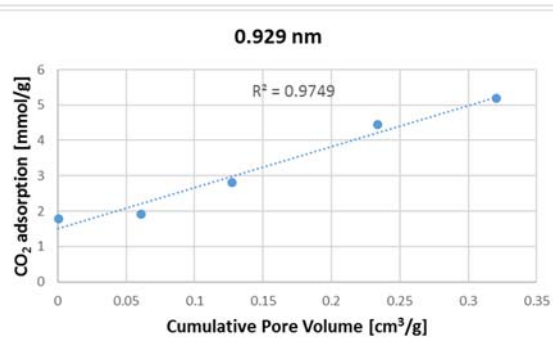
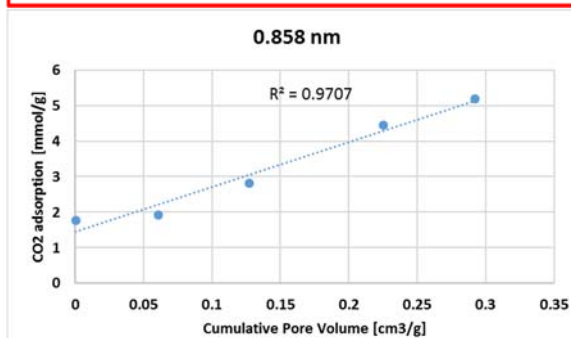
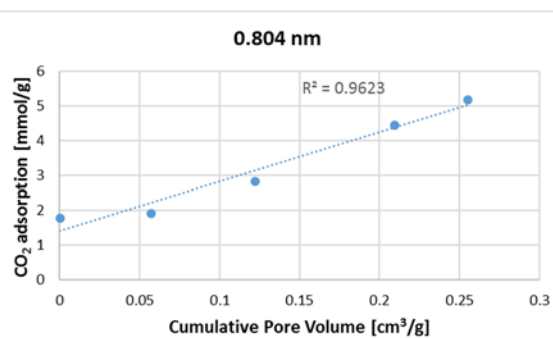
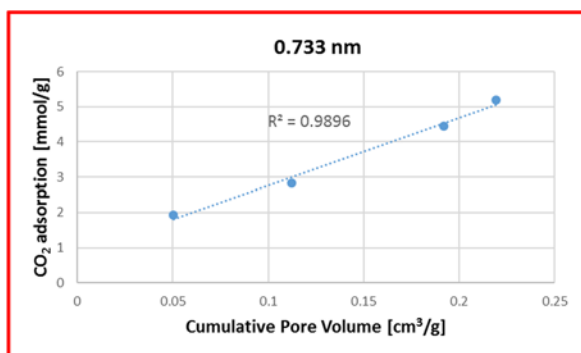


Figure S4. CO₂ adsorption over activated carbons produced from molasses at the temperatures of 10 °C (a), 20 °C (b), 30 °C (c)





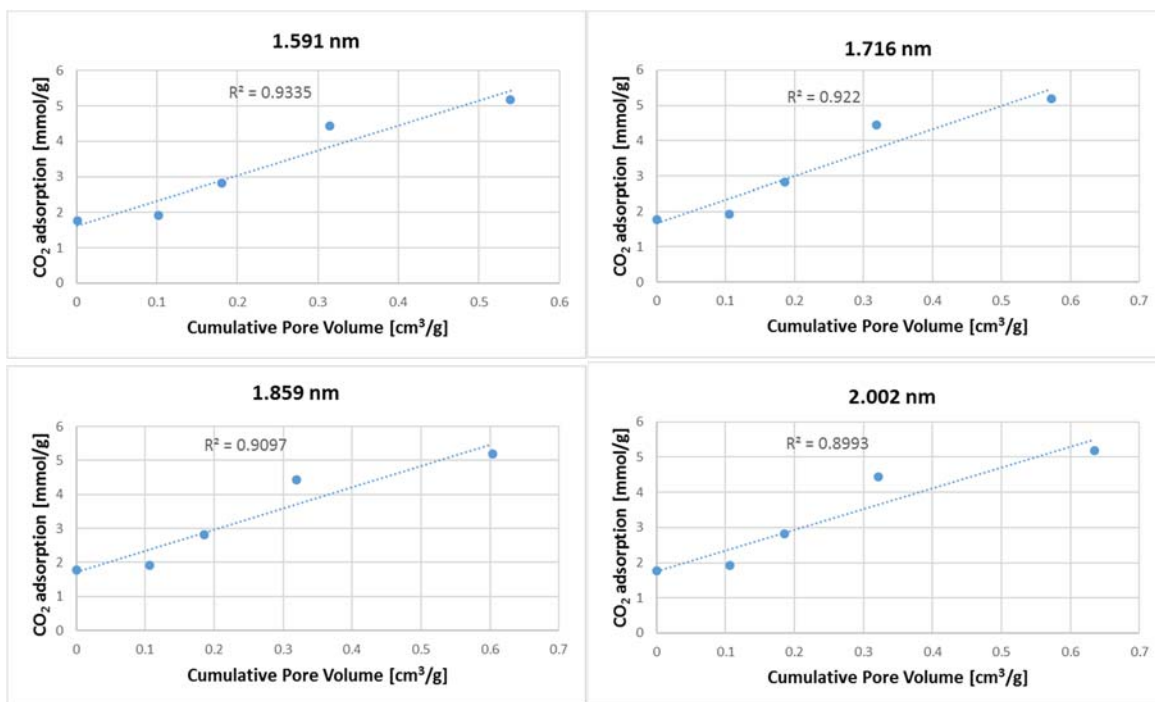
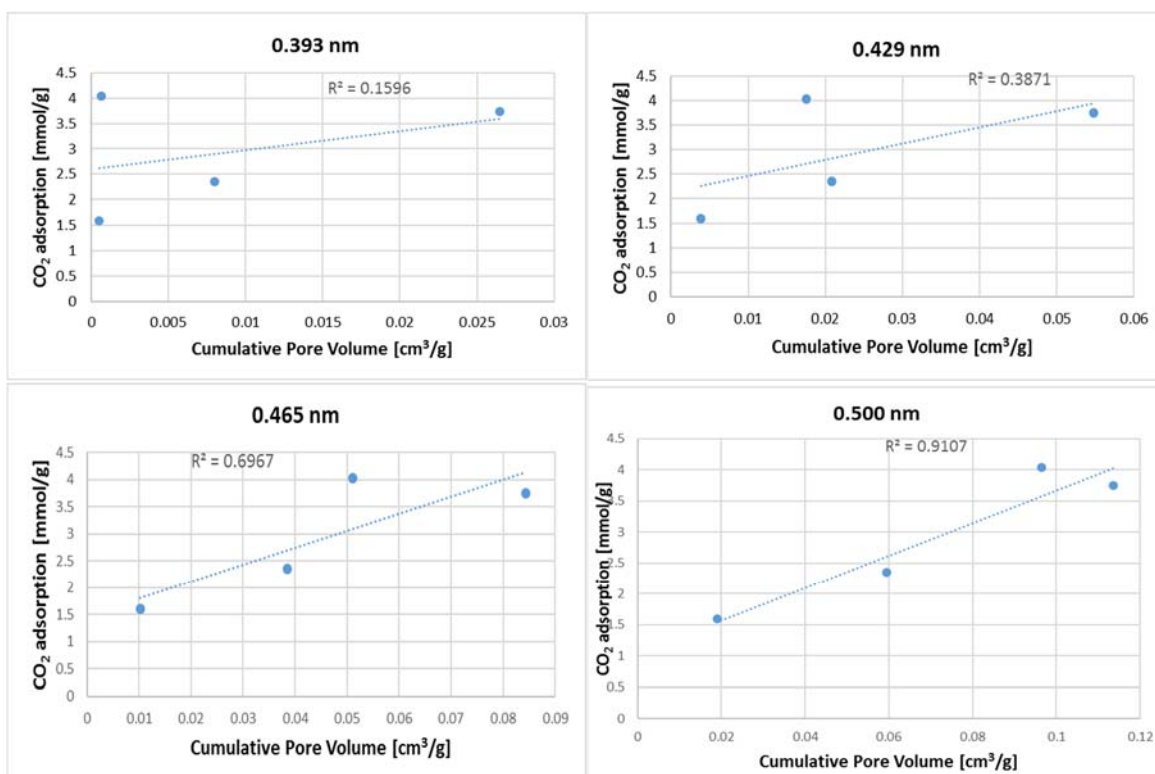
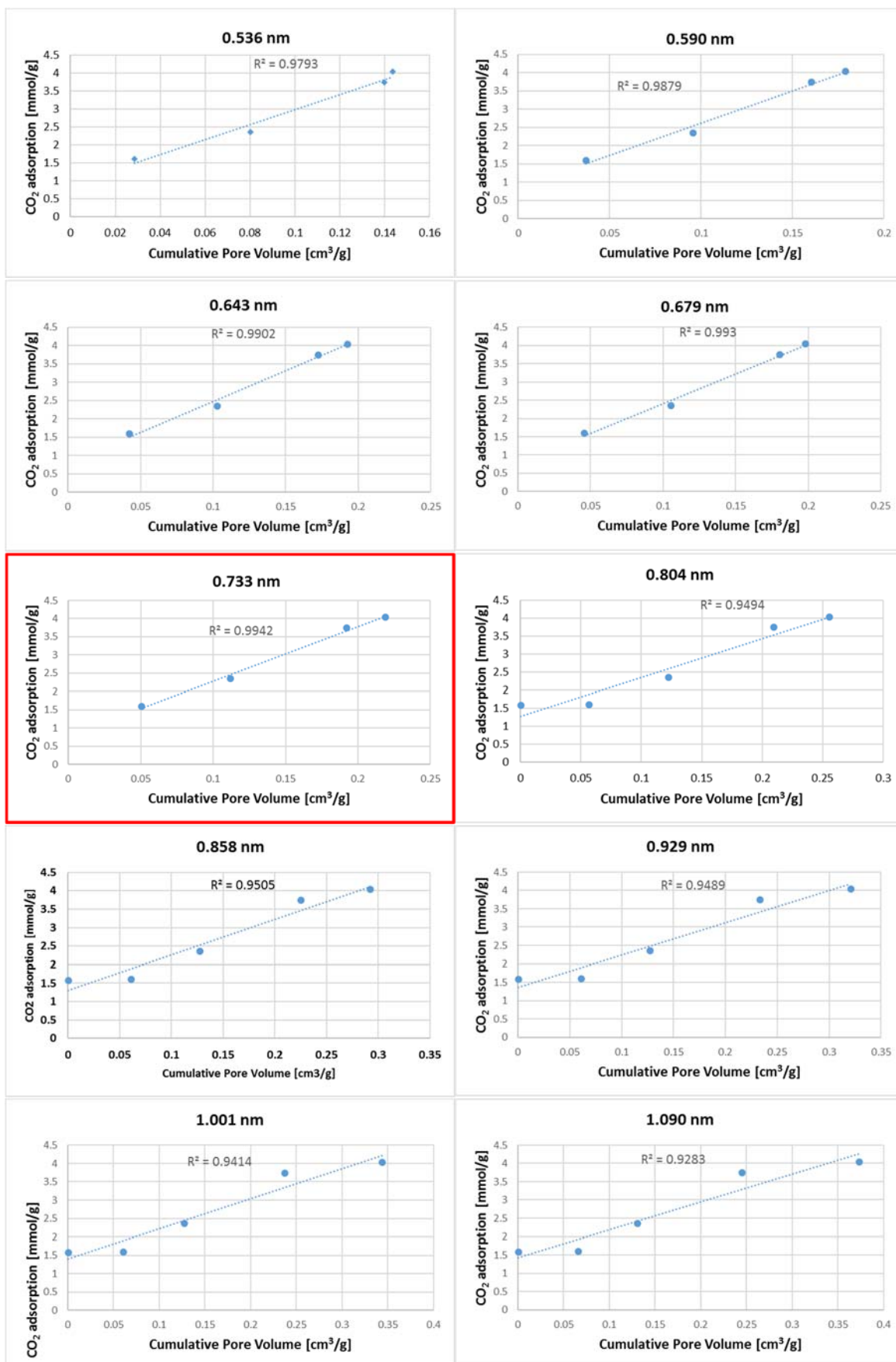


Figure S5. CO₂ adsorption at 1 bar and 0°C as a function of the volume of pores which are equal to and below given diameter. The best fit was outlined in red.





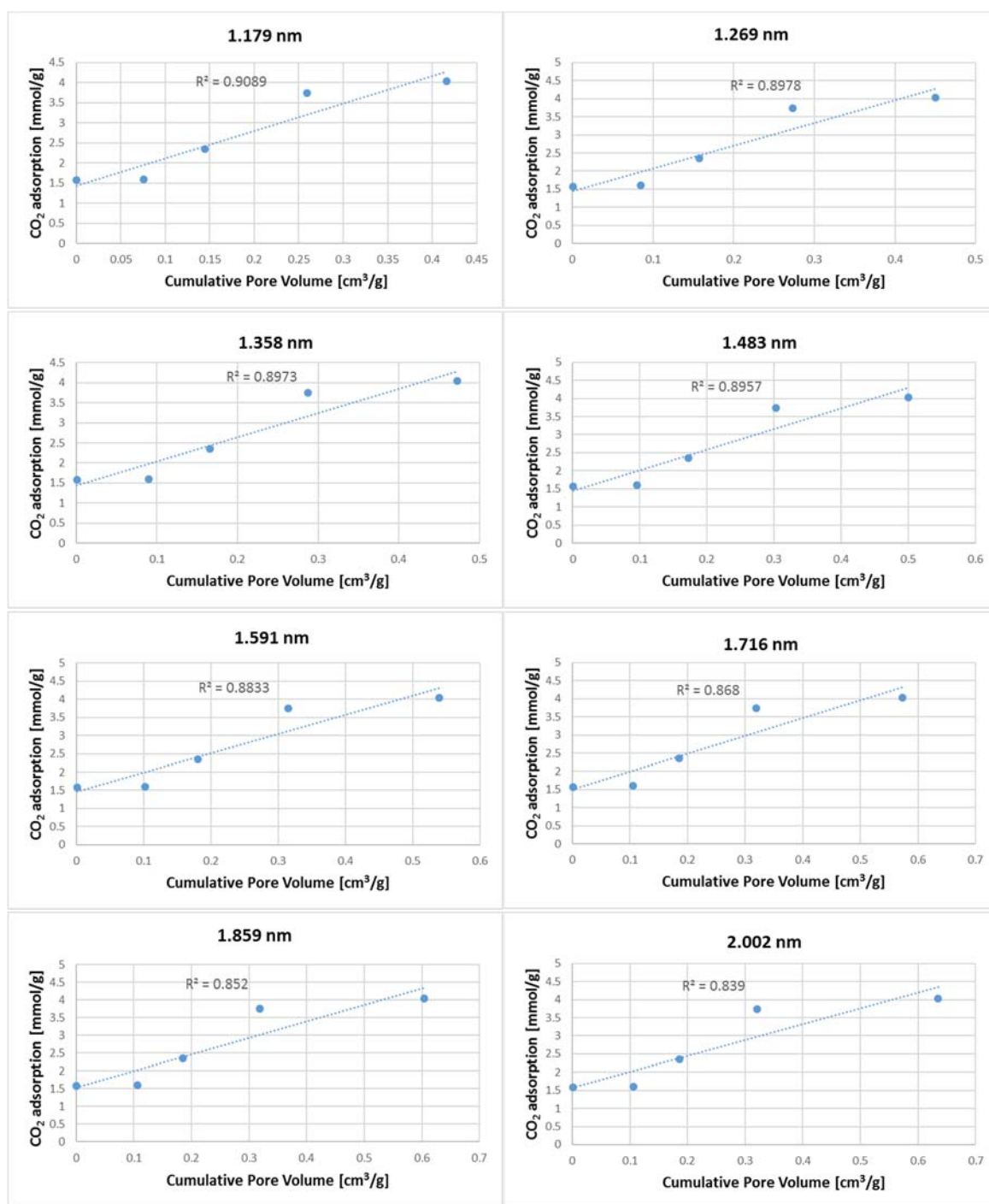
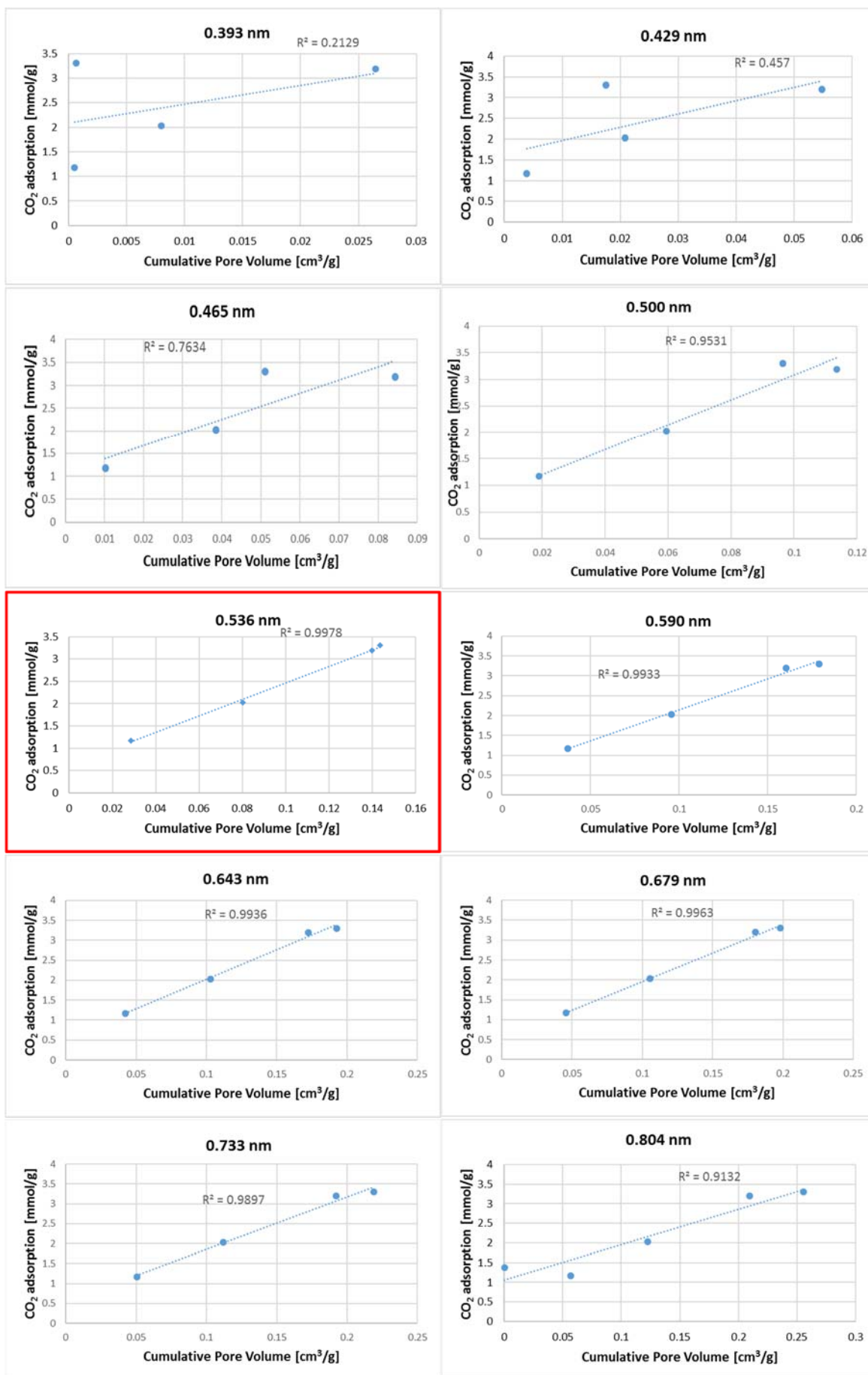
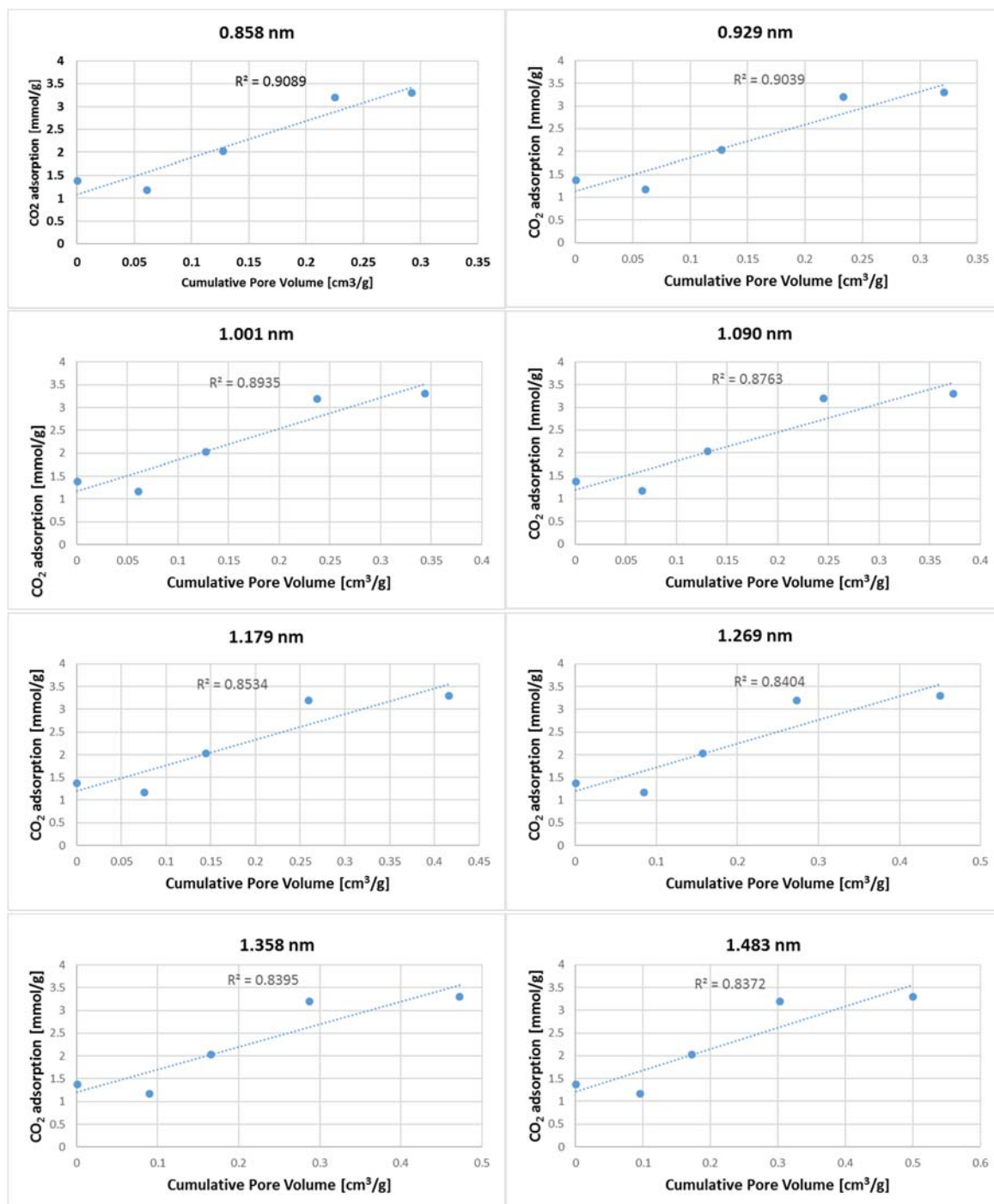


Figure S6. CO₂ adsorption at 1 bar and 10°C as a function of the volume of pores which are equal to and below given diameter. The best fit was outlined in red.





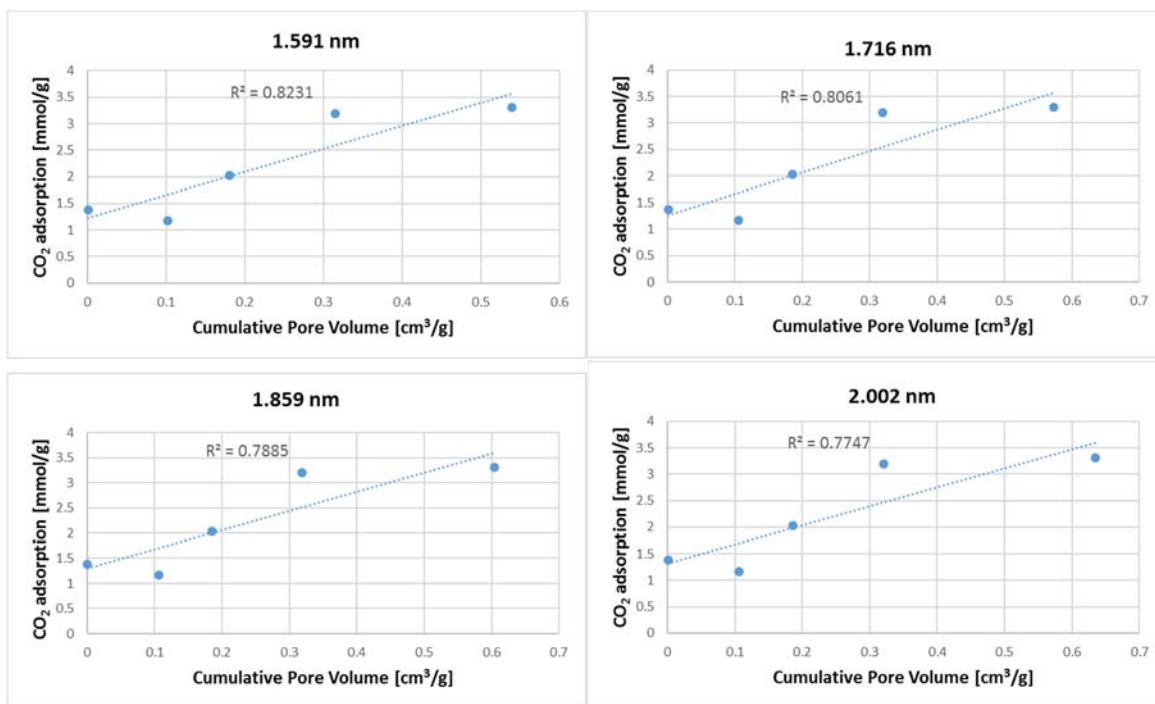
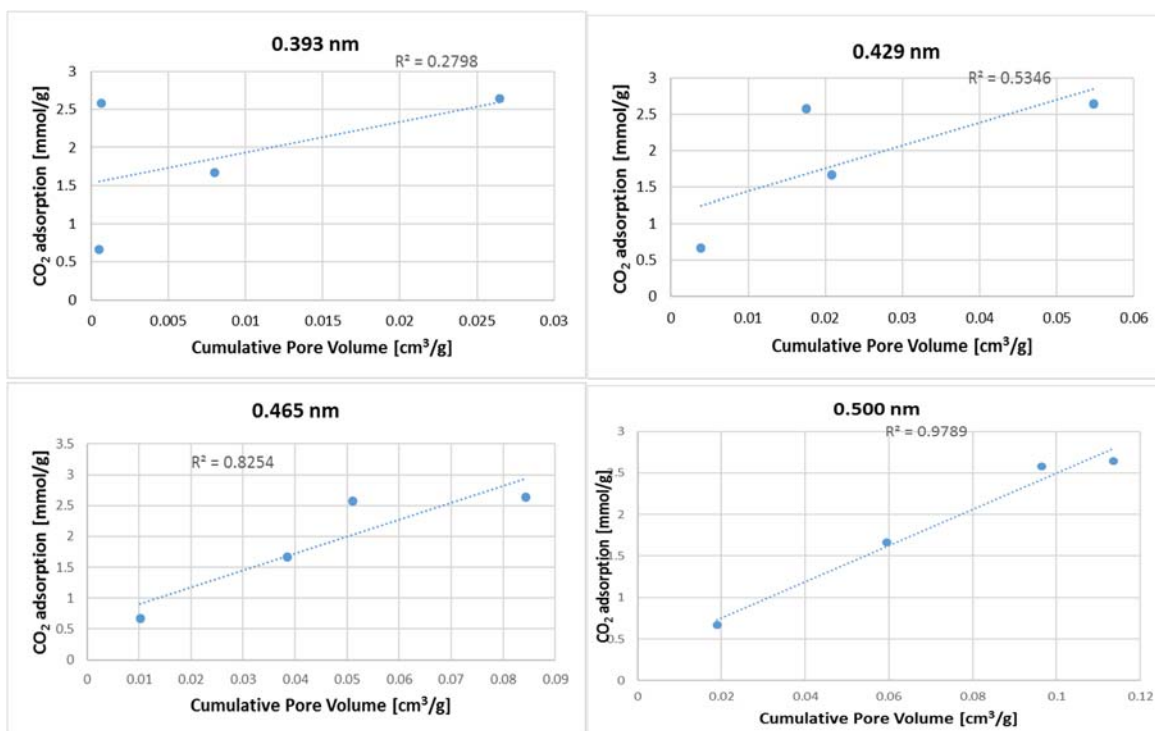
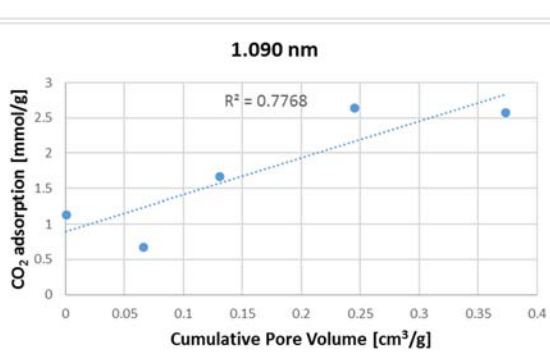
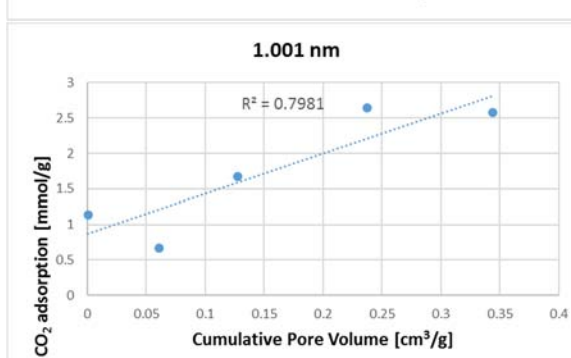
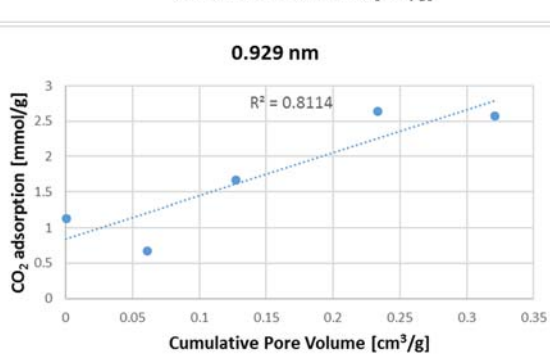
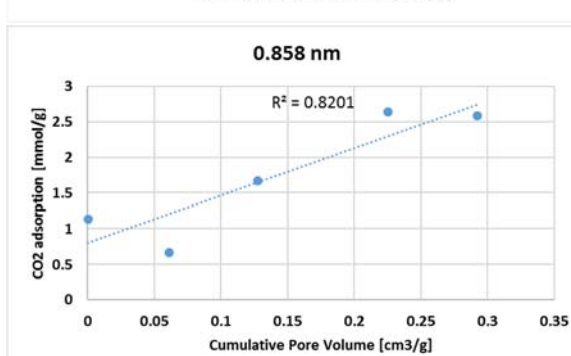
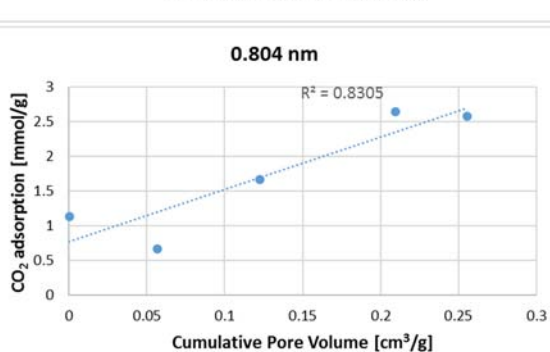
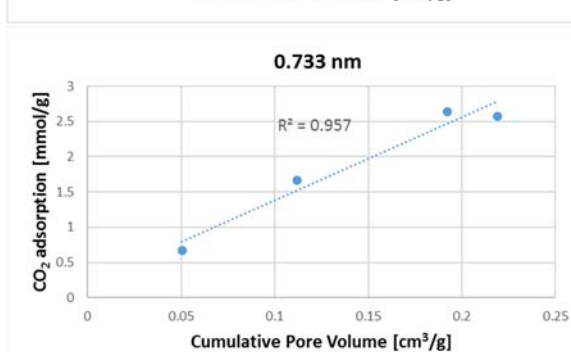
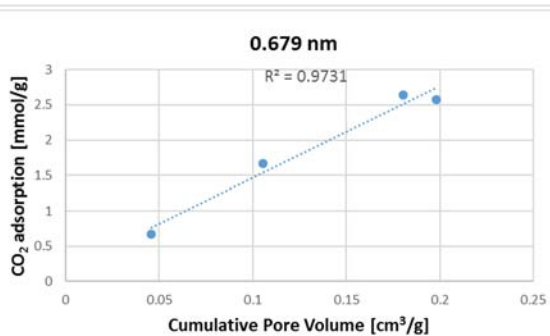
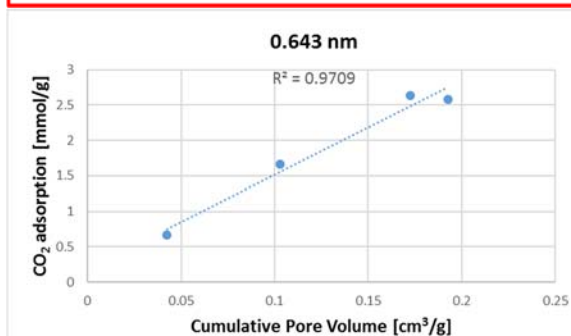
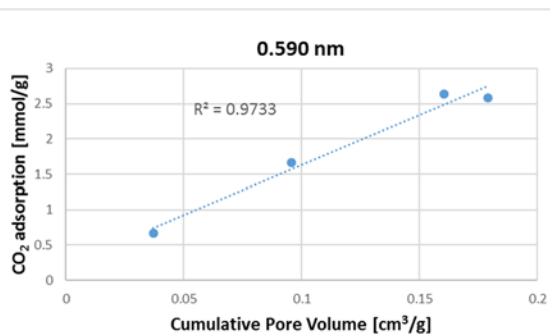
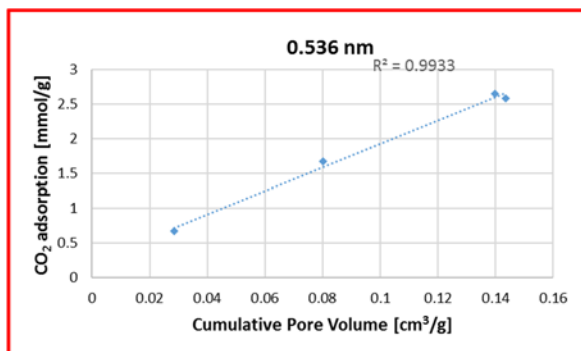


Figure S7. CO₂ adsorption at 1 bar and 20°C as a function of the volume of pores which are equal to and below given diameter. The best fit was outlined in red.





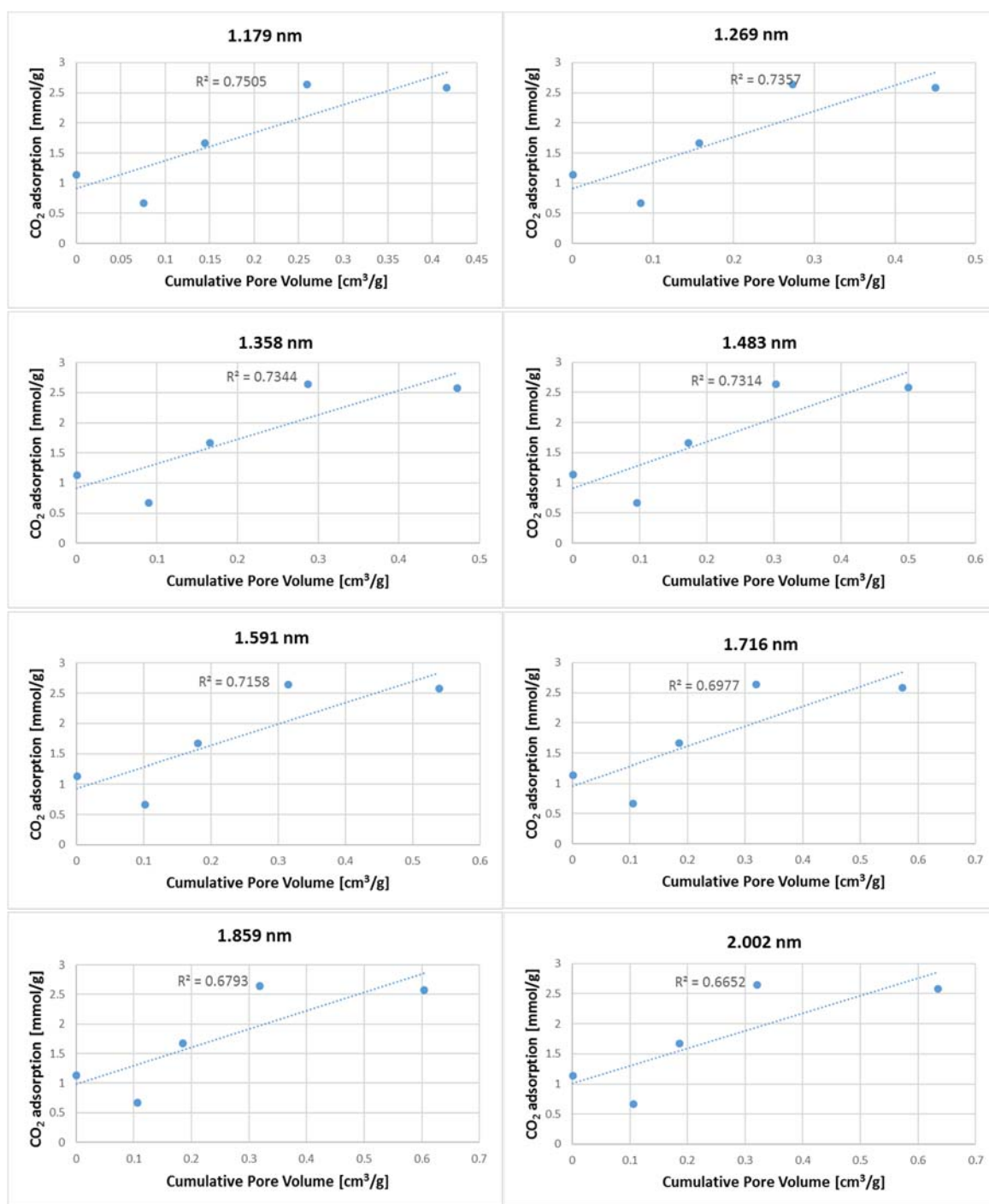


Figure S8. CO₂ adsorption at 1 bar and 30°C as a function of the volume of pores which are equal to and below given diameter. The best fit was outlined in red.

Table S1. CO₂ adsorption at different temperatures at the pressure of 1 bar

Sample	CO ₂ adsorption [mmol/g]			
	0 [°C]	10 [°C]	20 [°C]	30 [°C]
M-H ₂ SO ₄	4.44	3.74	3.2	2.64

M-H3PO4	2.82	2.35	2.03	1.67
M-HCl	1.77	1.58	1.38	1.13
M-KOH	5.18	4.04	3.3	2.58
M-NaOH	1.92	1.6	1.17	0.67

Table S2. Parameters of the Toth model for CO₂ adsorption at different temperatures

M-KOH			M-H2SO4			
Temperature	q _{mT}	b	n	q _{mT}	b	n
[°C]	[mmol/g]	[bar ⁻¹]		[mmol/g]	[bar ⁻¹]	
0	30.10	0.452	0.522	23.80	3.708	0.305
10	28.12	0.346	0.526	21.13	2.513	0.324
20	27.12	0.257	0.532	19.13	1.679	0.341
30	24.57	0.202	0.540	17.75	1.265	0.343

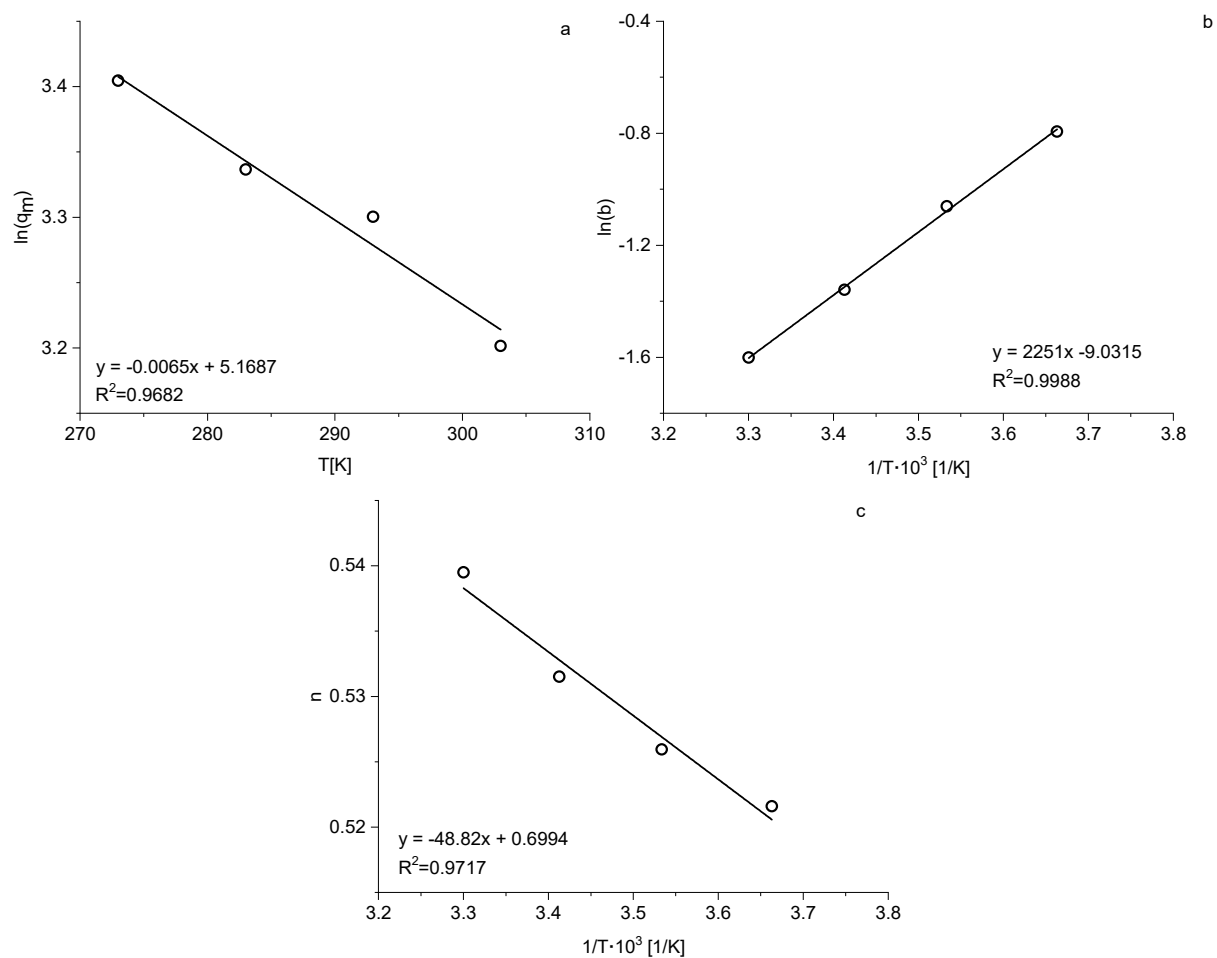


Figure S9. The plots: (a) $\ln(q_m)$ versus T , (b) $\ln(b)$ versus $1/T$, and (c) n versus $1/T$ applied to the calculation of the Toth parameters in equations (1–4) for M-KOH

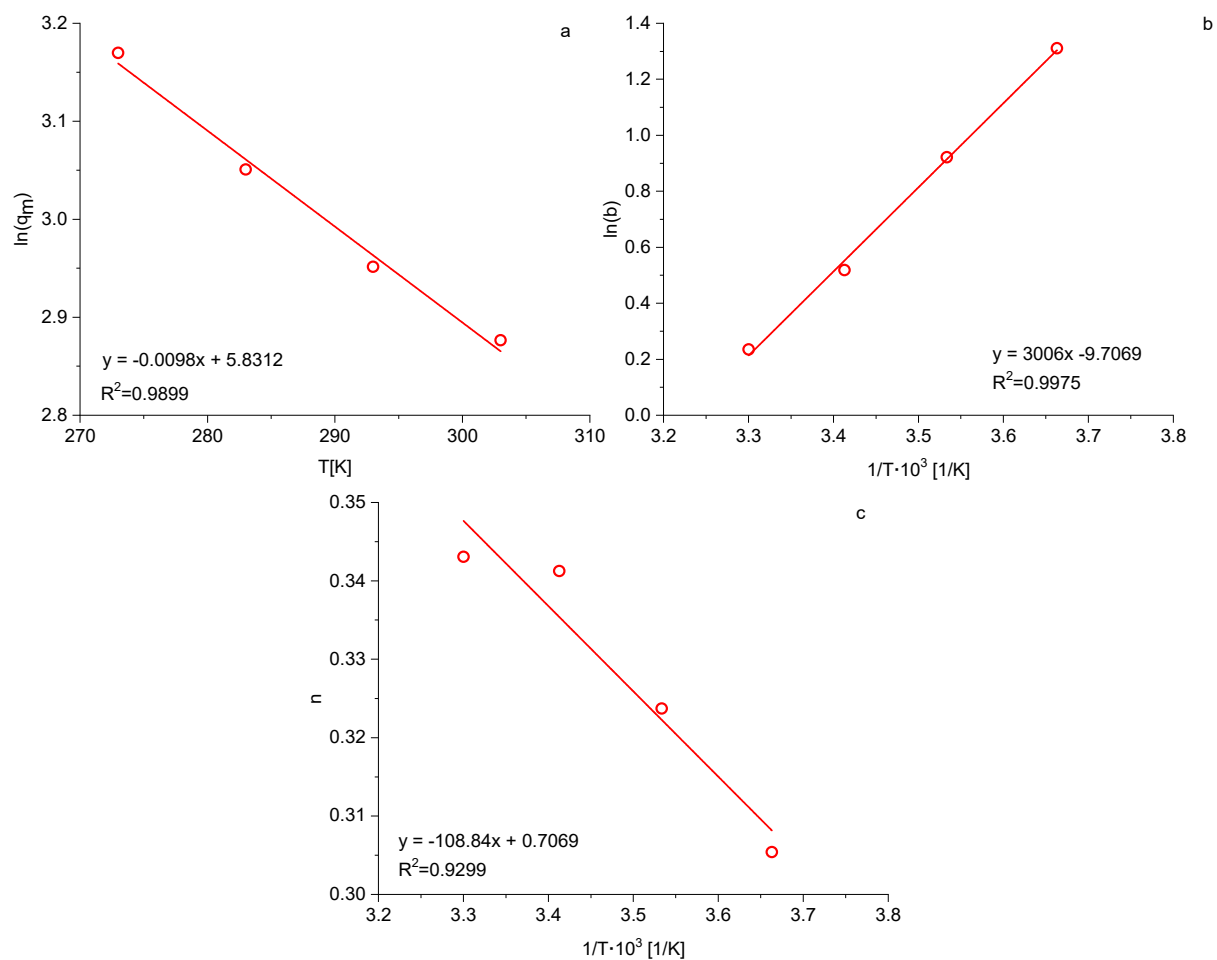


Figure S10. The plots: (a) $\ln(q_m)$ versus T , (b) $\ln(b)$ versus $1/T$, and (c) n versus $1/T$ applied to the calculation of the Toth parameters in equations (1–4) for M-H₂SO₄

Table S3. The parameters of the Toth temperature depended on equations for M-KOH and M-H2SO4 activated carbons

Parameter	M-KOH	M-H2SO4	Unit
Q	18715	24992	J/mol
b ₀	0.228	1.463	bar ⁻¹
n ₀	0.521	0.308	
α	0.179	0.399	
q _{m0}	30.19	23.55	mmol/g
χ	1.761	2.672	

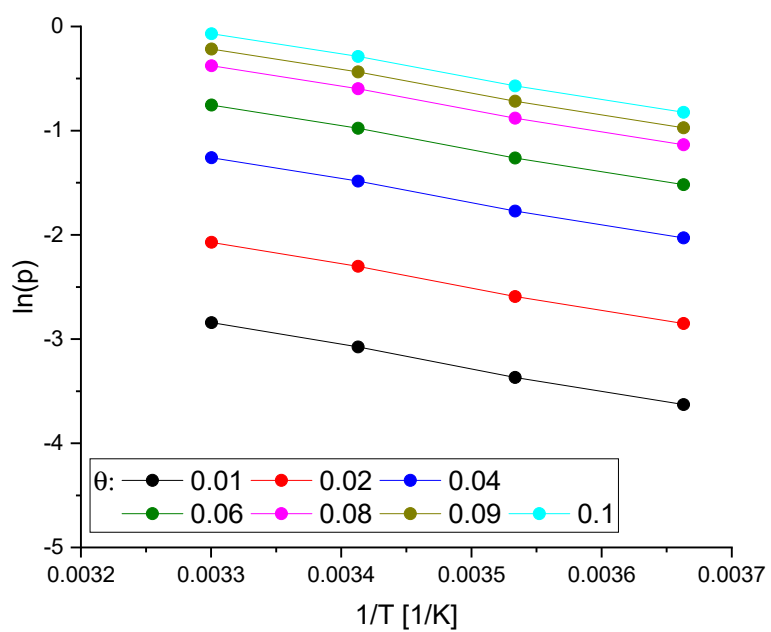


Figure S11. The plot of the function $\ln(p)$ vs $1/T$ for different surface coverage for M-KOH

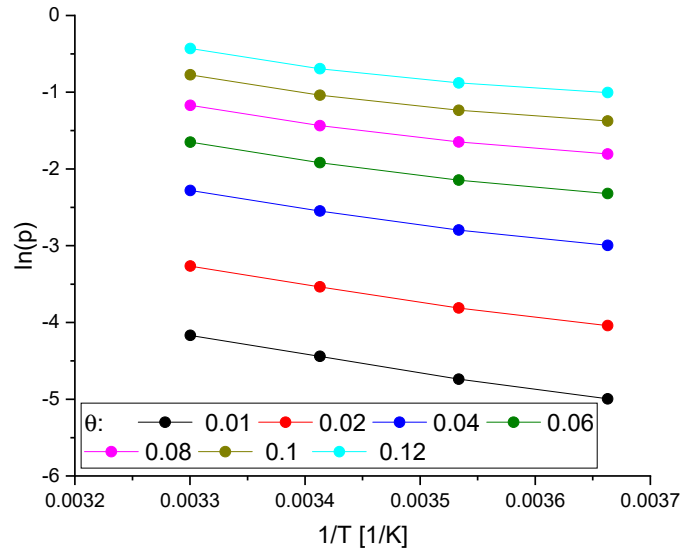


Figure S12. The plot of the function $\ln(p)$ vs $1/T$ different surface coverage for M-H₂SO₄

The isosteric heat of adsorption:

$$E_{iso} = -R \left(\frac{\partial \ln(p)}{\partial \left(\frac{1}{T}\right)} \right)_{\theta} \quad (S1)$$

Linear form of the equation (S1)

$$\ln(p)_{\theta} = -\frac{E_{iso}}{R} \frac{1}{T} + C \quad (S2)$$