

Supplementary Materials: Effect of Textural Properties and Presence of Co-Cation on NH₃-SCR Activity of Cu-Exchanged ZSM-5

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Table S1. Calculated parameters for adsorption and desorption kinetics.

	r_j^{ads}		$r_{\text{NO}}^{\text{des}}$		$r_{\text{NH3}}^{\text{des}}$	
	$k_j^{\text{ads}} \cdot C_j \cdot \theta_{\text{vs}}$	$k_{\text{NH3}}^{\text{ads}}/\text{s}^{-1}$	$k_{\text{NOx}}^{\text{des}}/\text{s}^{-1}$	$Ea_{\text{NOx}}^{\text{des}}/\text{kJ mol}^{-1}$	$k_{\text{NH3}}^{\text{des}}/\text{s}^{-1}$	$Ea_{\text{NH3}}^{\text{des}}/\text{kJ mol}^{-1}$
		$k_{\text{NOx}}^{\text{ads}}/\text{s}^{-1}$				
H-ZSM-5	$(2.0 \pm 0.3) \times 10^3$	$(5.8 \pm 0.5) \times 10^3$	$(1.9 \pm 0.2) \times 10^{-2}$	37 ± 2	$(1.7 \pm 0.3) \times 10^{-2}$	29 ± 3
Cu-ZSM-5	$(2.0 \pm 0.3) \times 10^3$	$(2.9 \pm 0.5) \times 10^3$	$(7.6 \pm 0.4) \times 10^{-3}$	84 ± 4	$(1.7 \pm 0.3) \times 10^{-3}$	16 ± 3
Na-Cu-ZSM-5	$(2.0 \pm 0.3) \times 10^3$	$(3.7 \pm 0.5) \times 10^3$	$(6.6 \pm 0.3) \times 10^{-3}$	109 ± 3	$(2.5 \pm 0.3) \times 10^{-3}$	16 ± 3
Cu-ZSM-5 (NaOH)	$(2.0 \pm 0.3) \times 10^3$	$(1.5 \pm 0.5) \times 10^3$	$(3.9 \pm 0.1) \times 10^{-3}$	45 ± 3	$(5.7 \pm 0.3) \times 10^{-3}$	24 ± 3
Cu-ZSM-5 (TPAOH)	$(2.0 \pm 0.3) \times 10^3$	$(2.2 \pm 0.5) \times 10^3$	$(5.36 \pm 0.01) \times 10^{-2}$	47.5 ± 0.2	$(2.6 \pm 0.3) \times 10^{-3}$	23 ± 3
Cu-ZSM-5 (NaOH/TPAOH)	$(2.0 \pm 0.3) \times 10^3$	$(1.3 \pm 0.5) \times 10^3$	$(1.6 \pm 0.1) \times 10^{-2}$	42 ± 1	$(1.4 \pm 0.3) \times 10^{-3}$	20 ± 1

* All rate constants are reported at the temperature of 150 °C. ** Temperature influence on the adsorption rate constants was considered negligible.

Table S2. Preparation procedures applied for modifications of parent ZSM-5.

Samples	Preparation procedure
H-ZSM-5	1) Calcination of NH ₄ ⁺ -ZSM-5 (550 °C, 4 h, 1 K min ⁻¹).
Cu-ZSM-5	1) Modification of H-ZSM-5 with an aqueous solution of copper precursor (0.05 M, 24 h, RT).
Cu-ZSM-5 (NaOH)	1) Modification of NH ₄ ⁺ -ZSM-5 with an aqueous solution of 0.2 M NaOH, TPAOH or mixture of NaOH and TPAOH (65 °C, 2 h under reflux);
Cu-ZSM-5 (TPAOH)	2) A triple ion-exchange with 0.5 M NH ₄ NO ₃ (60 °C, 1 h) in case of NH ₄ ⁺ -ZSM-5 treated with NaOH and NaOH/TPAOH; calcination of obtained materials (550 °C, 4 h, 1 K min ⁻¹);
Cu-ZSM-5 (NaOH/TPAO H)	3) Modification of H-ZSM-5 with an aqueous solution of copper precursor (0.05 M).
Na-Cu-ZSM-5	1) Modification of H-ZSM-5 with an aqueous solution of co-cation precursor (0.05 M, 80 °C, 2 h); 2) Modification of Na-ZSM-5 with an aqueous solution of copper precursor (0.05 M, 24 h, RT).

Table S3. Relevant parameters for kinetic modelling.

Property	Symbol	Value
Bed length	Z	8.6 mm *
Bed porosity	α	0.29
Catalyst mass	m_{cat}	200 mg **
Volumetric velocity	\dot{V}	120 ml min ⁻¹ ***
Temperature of the mass flow controllers	T_{MFC}	293 K

*4.3 mm for TPD-NO_x tests; **100 mg for TPD-NO_x tests; ***50 ml min⁻¹ for TPD-NO_x tests

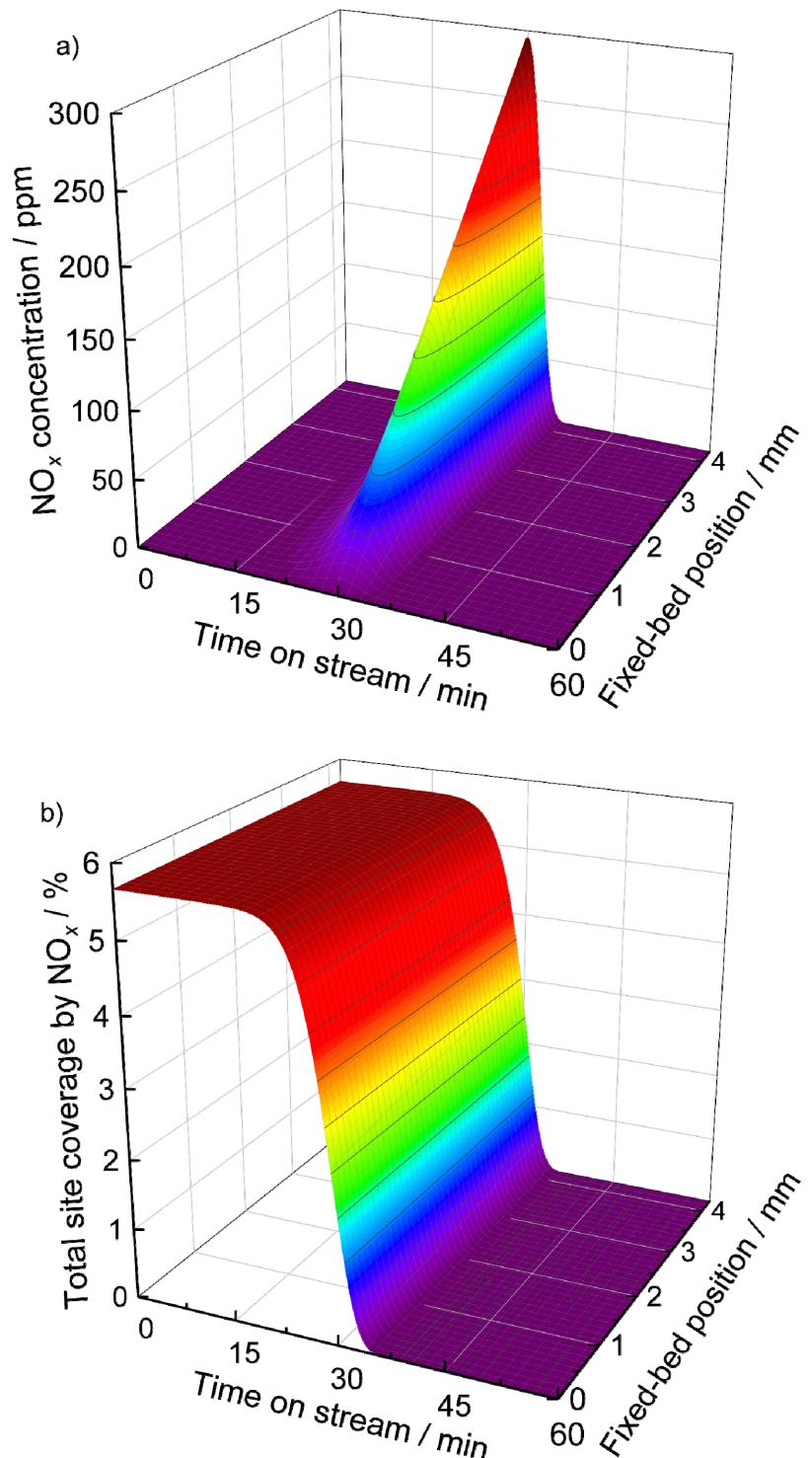


Figure S1. (a) NO concentration in the gas phase and (b) NO surface coverage as a function of time on stream and position in the reactor during the TPD- NO_x at 150 °C over Na-Cu-ZSM-5 conversion (conditions: 0.1 g of catalyst, 50 mL min⁻¹, 0 ppm NO, heat-up rate 10 K min⁻¹, initial temperature 50 °C).

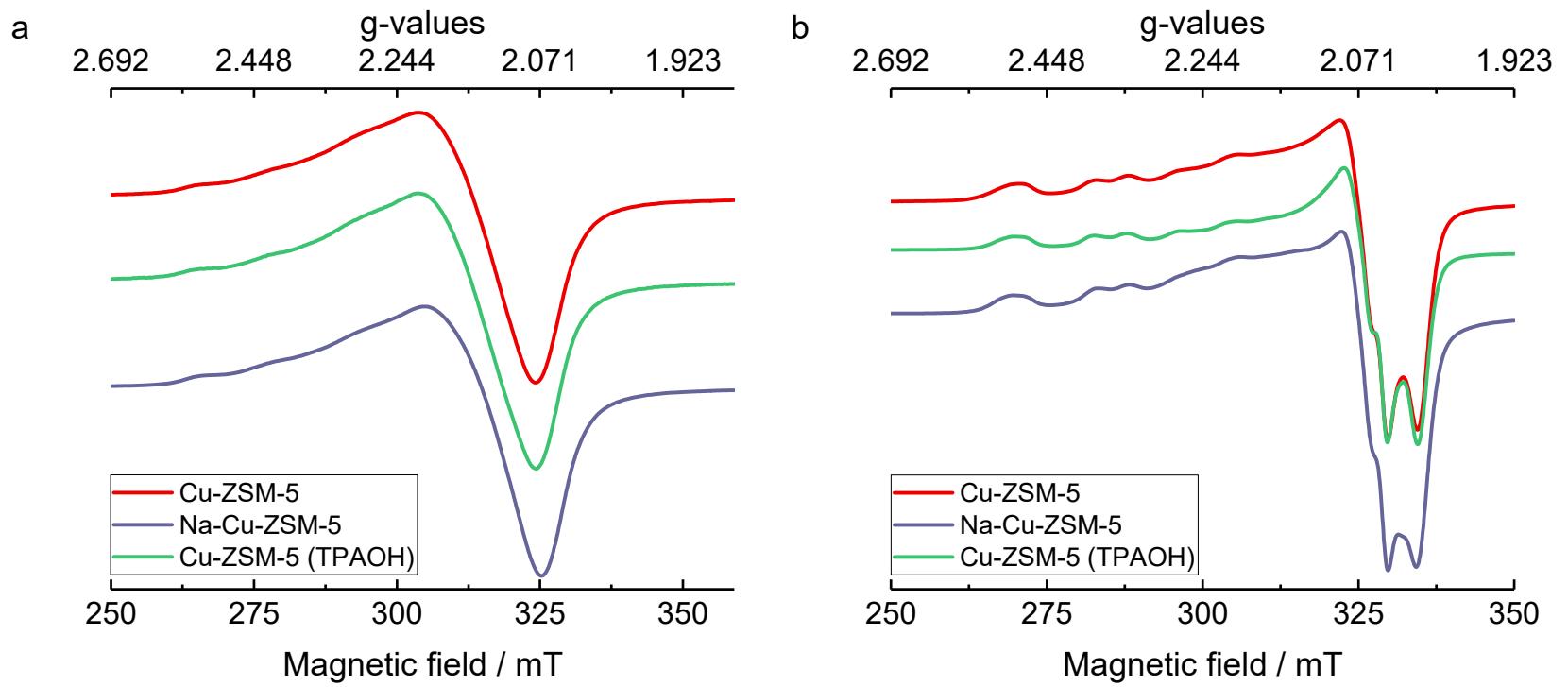


Figure S2. Experimental cw-EPR spectra of (a) hydrated and (b) dehydrated Cu-ZSM-5 acquired at room temperature.

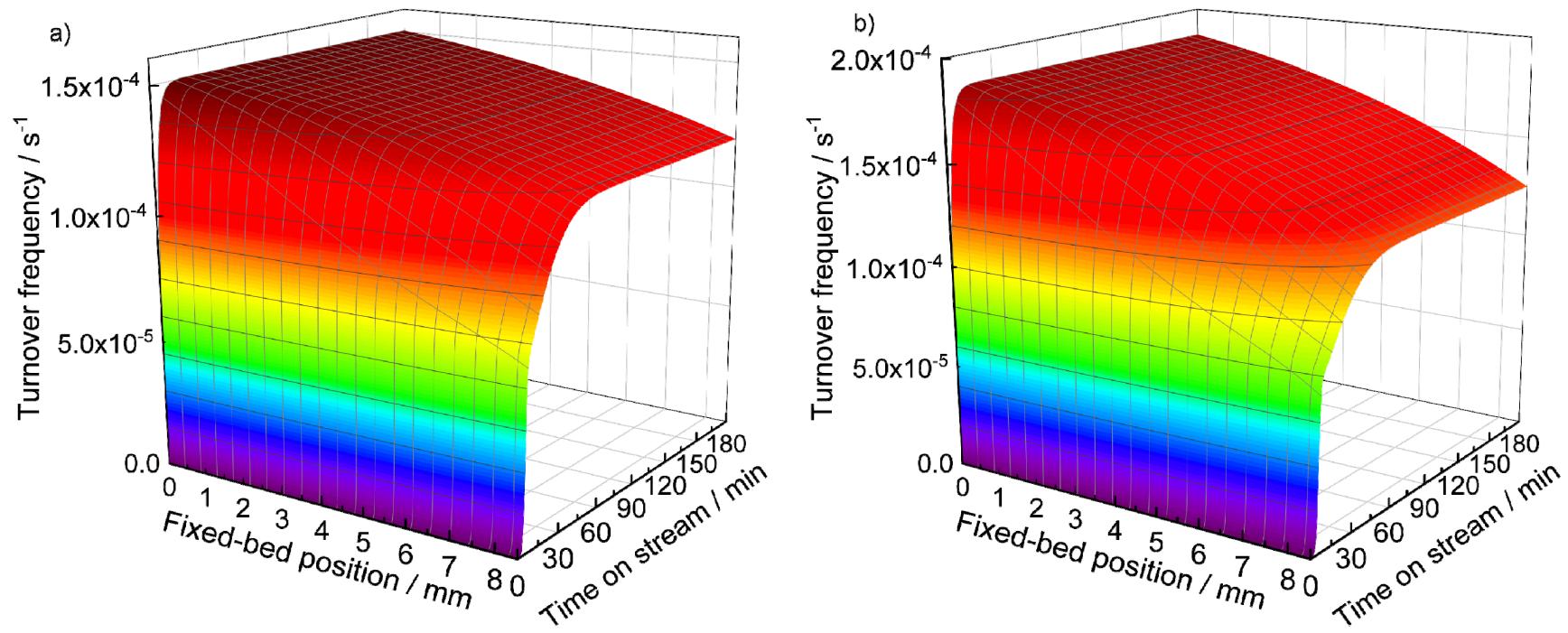


Figure S3. TOF₁ as a function of time on stream and position in the reactor for NH₃-SCR at 150 °C over Cu-ZSM-5 conversion in (a) absence and (b) presence of 5 vol.-% H₂O (conditions: 0.2 g of catalyst, 120 mL min⁻¹, 500 ppm NO, 575 ppm NH₃).