

# Supplementary Material

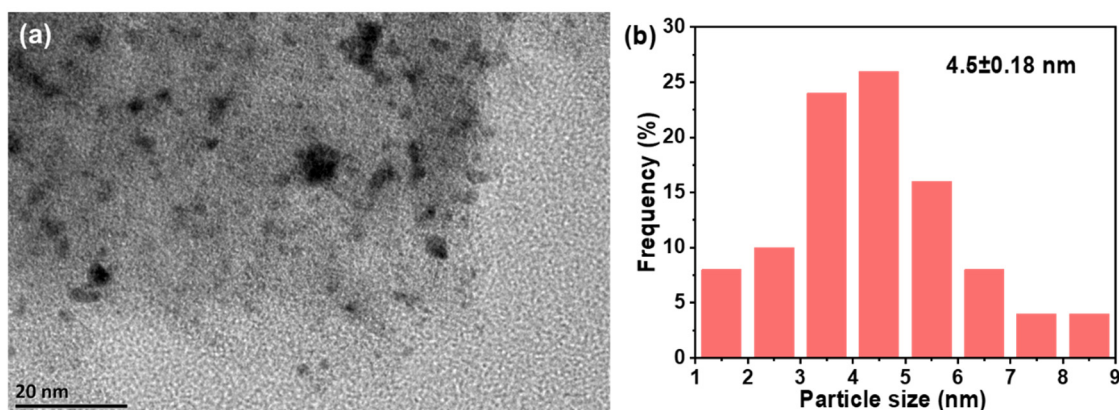
## Efficient hydrogen production from aqueous-phase reforming of biomass-derived oxygenated hydrocarbons over an ultrafine Pt nanocatalyst

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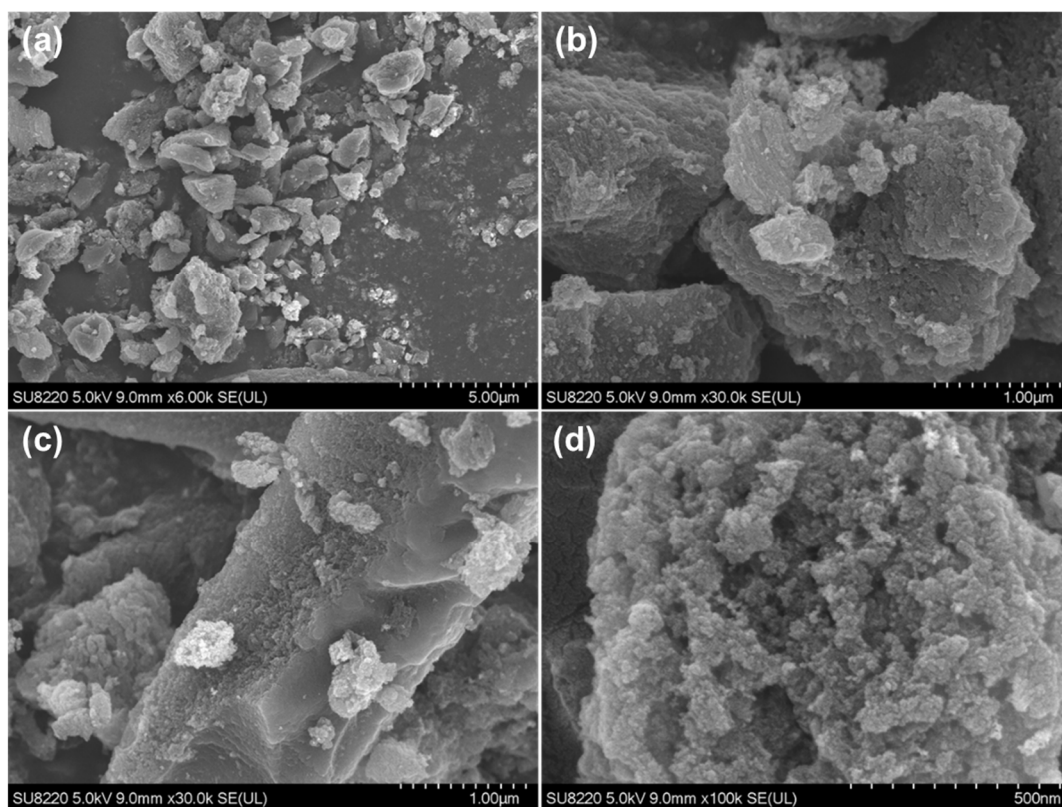
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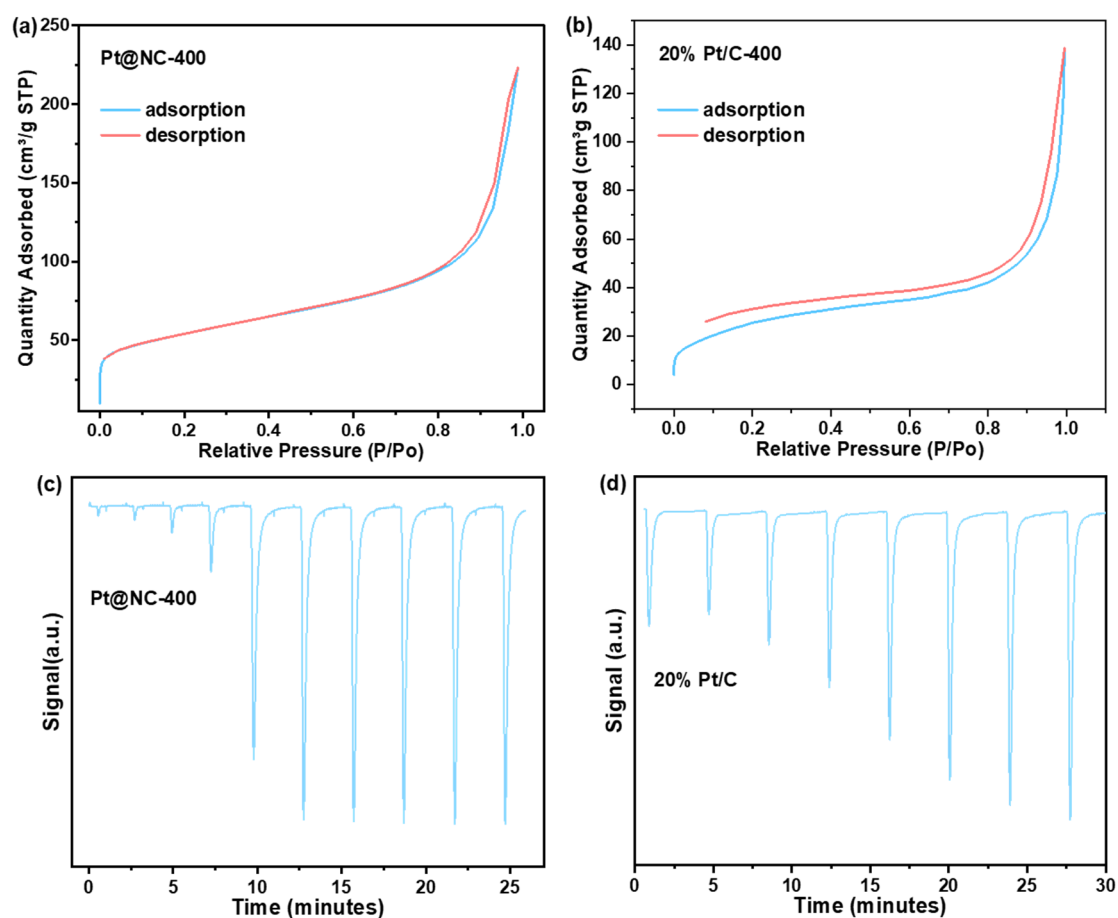
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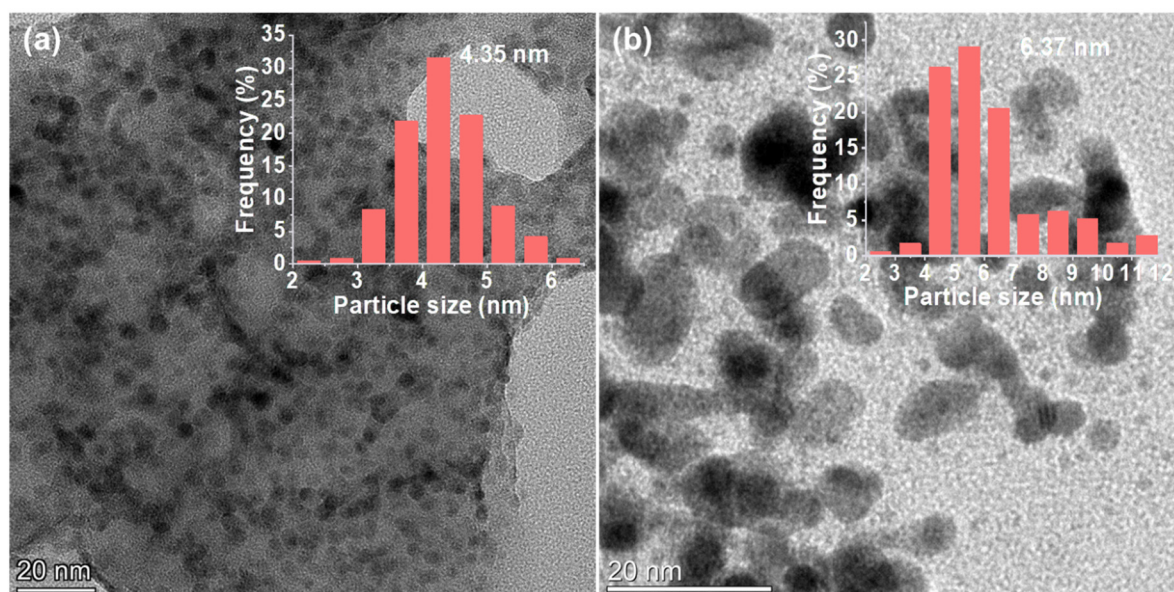
**Figure S1.** (a) TEM image of 20% Pt/C; (b) statistical distribution of Pt particle size of 20% Pt/C.



**Figure S2.** SEM images of 20% Pt/C catalyst.



**Figure S3.** N<sub>2</sub> adsorption and desorption curves and the CO pulse chemisorption curves of Pt@NC-400 and 20% Pt/C catalysts.



**Figure S4.** TEM images and particle size distributions of the spent Pt@NC-400 (a) and 20% Pt/C (b) catalysts after 8 times of in-situ cycling reaction.

**Table S1.** The particle size of Pt@NC-X catalysts.

Catalysts	Particle size <sup>a</sup> (nm)	Carbonization temperature (°C)
Pt@NC-300	3.4	300
Pt@NC-400	3.6	400
Pt@NC-500	4.3	500
Pt@NC-600	11.2	600
Pt@NC-700	24.8	700

<sup>a</sup> Pt particle sizes were calculated by Scherrer formula using XRD data.

**Table S2.** Main physiochemical properties of Pt@NC-400 and 20% Pt/C catalysts.

Samples	Pt loading <sup>a</sup> (wt. %)	S <sub>BET</sub> <sup>b</sup> (m <sup>2</sup> g <sup>-1</sup> )	V <sub>P</sub> <sup>b</sup> (cm <sup>3</sup> g <sup>-1</sup> )	d <sub>p</sub> <sup>b</sup> (nm)	Pt metallic surface area <sup>c</sup> (m <sup>2</sup> g <sup>-1</sup> )	Pt disper- sion <sup>c</sup> %
Pt@NC-400	32.2	135.3	0.31	14.4	11.6	14.6
20% Pt/C	22.9	105.6	0.24	10.5	6.8	12.0

<sup>a</sup> Pt loading in the calcined catalysts were examined by inductively coupled plasma optic emission spectrometry (ICP-OES). <sup>b</sup> The BET surface area, pore volume and pore size were obtained from N<sub>2</sub> physisorption. <sup>c</sup> Pt metallic surface area and Pt dispersion of the reduced catalysts were determined by CO chemisorption.

**Table S3.** Relative atomic ratios of the elements C, N, and Pt in the Pt@NC-400 catalyst measured by EDS.

Z	Element	Family	Atomic Fraction (%)
6	C	K	61.0
7	N	K	9.2
78	Pt	L	29.8

**Table S4.** Data statistics for the Pt 4f spectrum of Pt@NC-400 catalysts. <sup>a</sup>

Species	Peak position (eV)	Percentage (%)
Pt <sup>4+</sup>	72.8	1.2
Pt <sup>0</sup>	71.3	98.8

<sup>a</sup> Data in this table was obtained from the XPS experiment.

**Table S5.** APRM performance of Pt-based catalysts at different pyrolysis temperatures.

Catalyst	Pyrolysis temperatures (°C)	H <sub>2</sub> production rate ( $\mu\text{mol}_{\text{H}_2}/\text{g}_{\text{cat.}}/\text{s}$ )	ATOF ( $\text{h}^{-1}$ )
Pt@NC-300	300	391.6	1639.1
Pt@NC-400	400	1013.4	4242.1
Pt@NC-500	500	363.5	1521.4
Pt@NC-600	600	323.6	1354.7
Pt@NC-700	700	186.0	778.7

Reaction conditions: 5 mL of methanol solution ( $n(\text{CH}_3\text{OH})/n(\text{H}_2\text{O}) = 1:3$ ), 2 mg of catalyst, 2 MPa of  $\text{N}_2$ , reaction at 210 °C for 1.25 h. The catalysts were reduced in  $\text{H}_2$  at 200 °C for 2 h before reaction.

**Table S6.** Reproducibility test of APRM reaction catalyzed by Pt@NC-400.

Reaction times	H <sub>2</sub> production rate ( $\mu\text{mol}_{\text{H}_2}/\text{g}_{\text{cat.}}/\text{s}$ )	Relative deviation (%)
1	1013.4	4.0
2	957.1	-1.8
3	936.0	-3.9
4	999.5	2.6
5	964.8	-1.0
Average H <sub>2</sub> production rate ( $\mu\text{mol}_{\text{H}_2}/\text{g}_{\text{cat.}}/\text{s}$ )	974.2	-
Relative average deviation (%)	-	2.7

Relative deviation =  $100\% \cdot (x_i - \bar{x}) / \bar{x}$ , Relative average deviation =  $100\% \cdot |x_i - \bar{x}| / 5$ , where  $x_i$  is the hydrogen production rate for each reaction and  $\bar{x}$  is the average hydrogen production rate. Reaction conditions: 5 mL of methanol solution ( $n(\text{CH}_3\text{OH})/n(\text{H}_2\text{O}) = 1:3$ ), 2 mg of catalyst, 2 MPa of  $\text{N}_2$ , reaction at 210 °C for 1.25 h. The catalyst was reduced in  $\text{H}_2$  at 200 °C for 2 h before reaction.

**Table S7.** APRM performance of Pt@NC-400 and 20% Pt/C catalysts at different reaction temperatures.

Catalyst	T (°C)	H <sub>2</sub> production rate ( $\mu\text{mol}_{\text{H}_2}/\text{g}_{\text{cat.}}/\text{s}$ )	ATOF ( $\text{mol}_{\text{H}_2}/\text{mol}_{\text{Pt}}/\text{h}$ )	CO selectivity (%)
20% Pt/C	170	34.8	266.4	40.16
	190	208.4	1595.3	1.63
	210	357.3	2734.9	3.20
	230	634.7	4792.4	0.33
	250	676.5	5177.8	0.30
Pt@NC-400	170	240.1	1256.2	10.99
	190	594.2	2487.4	4.43
	210	1013.4	4242.1	2.92
	230	1187.5	4970.9	0.66
	250	1536.6	6462.4	0.62

Reaction conditions: 5 mL of methanol solution ( $n(\text{CH}_3\text{OH})/n(\text{H}_2\text{O}) = 1:3$ ), 2 mg of catalyst, 2 MPa of  $\text{N}_2$ , reaction at 170-250 °C for 1.25 h. The catalysts were reduced in  $\text{H}_2$  at 200 °C for 2 h before reaction.

**Table S8.** Differences in APR catalytic performance between Pt@NC-400 and 20% Pt/C catalysts under different feedstocks.

Catalysts	H <sub>2</sub> production rate ( $\mu\text{mol}_{\text{H}_2}/\text{g}_{\text{cat}}/\text{s}$ )	ATOF ( $\text{mol}_{\text{H}_2}/\text{mol}_{\text{Pt}}/\text{h}$ )	CO selectivity (%)	Reaction mixture
20%Pt/C	357.3	2734.9	3.20	Methanol
Pt@NC-400	1013.4	4242.1	2.92	(1:3)
20%Pt/C	266.0	2035.8	1.52	Ethanol
Pt@NC-400	779.0	3260.9	1.55	(1:3)
20%Pt/C	239.1	1829.9	2.35	Propanol
Pt@NC-400	546.9	2289.4	0.89	(1:5)
20%Pt/C	850.9	6513.2	0.61	EG
Pt@NC-400	1072.2	4488.1	0.94	(1:2)
20%Pt/C	824.0	6306.8	0.34	1,2-PG
Pt@NC-400	1766.5	7394.5	0.31	(1:4)
20%Pt/C	201.6	1543.1	2.83	Sorbitol
Pt@NC-400	555.6	2325.7	0.60	(1:6)

Reaction conditions: 5 mL of alcohol solution, 2 mg of catalyst, 2 MPa of N<sub>2</sub>, reaction at 210 °C for 1.25 h. The catalysts were reduced in H<sub>2</sub> at 200 °C for 2 h before reaction.

**Table S9.** Hydrogen production performance of ARP catalyzed by Pt-based catalysts in recent literature.

Catalysts	H <sub>2</sub> production rate ( $\mu\text{mol}_{\text{H}_2}/\text{g}_{\text{cat}}/\text{s}$ )	ATOF ( $\text{mol}_{\text{H}_2}/\text{mol}_{\text{Pt}}/\text{h}$ )	CO selectivity (%)	Reaction condition	Reference
2%Pt/ $\alpha$ -MoC	129.6	4134	0.06	190 °C, nCH <sub>3</sub> OH/nH <sub>2</sub> O = (1:3), batch	2017[7]
1% Pt/NiAl <sub>2</sub> O <sub>4</sub>	7.3	-	0.05	210 °C, 10 wt% methanol, continuous flow	2019[18]
2% Pt/Al <sub>2</sub> O <sub>3</sub>	30.7	1077	0.4	240 °C, 10 wt% methanol continuous flow	2021[39]
1% Pt/ $\gamma$ -Al <sub>2</sub> O <sub>3</sub>	1.8	-	0.02	210 °C, 10 wt% methanol, continuous flow	2019[18]
6% Pt/SiO <sub>2</sub>	-	450000	undetected	210 °C, 10 wt% ethylene glycol, continuous flow	2022[40]
5% Pt/Al <sub>2</sub> O <sub>3</sub>	11840.3	-	undetected	250 °C, 10 wt% glycerol, continuous flow	2019[41]
Pt/LaNiO <sub>x</sub> -2	5.3	-	0.2	210 °C, 10 wt% methanol continuous flow	2022[42]
ZnO/Pt/Al <sub>2</sub> O <sub>3</sub>	-	26.4	undetected	250 °C 5 wt% 1-propanol continuous flow	2016[43]
Pt-Mn/C	-	1020	undetected	225 °C 10 wt% glycerol, continuous flow	2017[44]

**Table S10.** Catalytic stability performance of Pt@NC-400 and 20% Pt/C catalysts at 210 °C.

Catalysts	Cycle times	H <sub>2</sub> production rate ( $\mu\text{mol}_{\text{H}_2}/\text{g}_{\text{cat}}/\text{s}$ )	ATOF ( $\text{mol}_{\text{H}_2}/\text{mol}_{\text{Pt}}/\text{h}$ )	CO selectivity (%)
20% Pt/C	1	356.9	2734.9	0.0491
	2	279.9	2144.8	0.0903
	3	185.7	1423.0	0.0676
	4	169.8	1301.1	0.1020
	5	117.9	903.5	0.1313
	6	118.1	905.0	0.0850
	7	101.1	774.7	0.1168
	8	97.3	745.6	0.1186
Pt@NC-400	1	1013.4	4242.1	0.0470
	2	986.2	4128.3	0.0571
	3	815.3	3412.9	0.1026
	4	566.9	2373.0	0.1184
	5	545.6	2284.1	0.1297
	6	447.9	1874.8	0.1404
	7	412.6	1727.1	0.1668
	8	423.9	1774.6	0.1703

Reaction conditions: 5 mL of methanol solution ( $n(\text{CH}_3\text{OH})/n(\text{H}_2\text{O}) = 1:3$ ), 2 mg of catalyst, 2 MPa of N<sub>2</sub>, reaction at 210 °C for 1.25 h. The catalysts were reduced in H<sub>2</sub> at 200 °C for 2 h before reaction.